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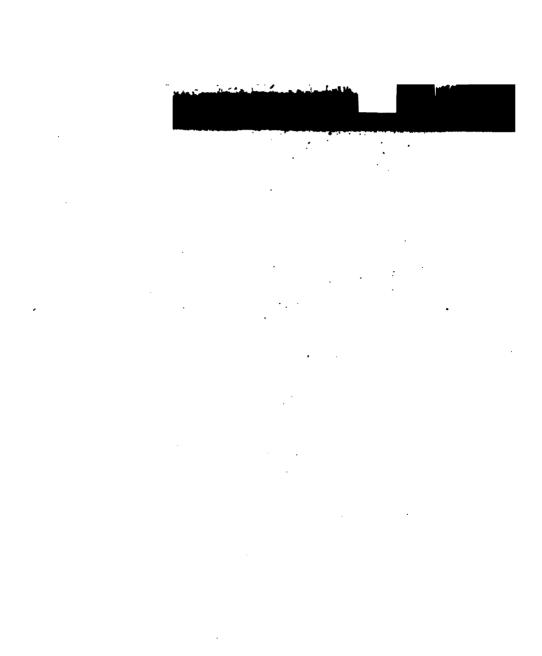
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GAS MANAGER'S HANDBOOK.

FIFTH EDITION.

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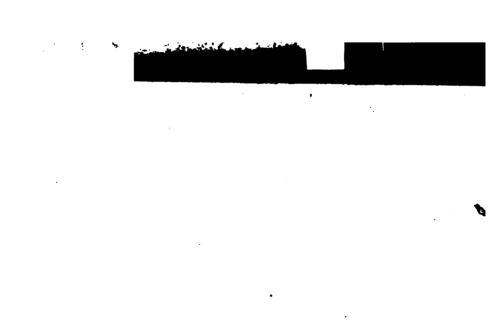


THE

GAS MANAGER'S HANDBOOK.

FIFTH EDITION.

Newbiesen 3-VC



HANDBOOK

FOR

GAS ENGINEERS

AND

MANAGERS.

В₹

THOMAS NEWBIGGING,

Member of the Institution of Civil Engineers.

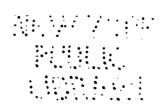
FIFTH EDITION, ENLARGED.

Nondon :

WALTER KING,

OFFICE OF THE "JOURNAL OF GAS LIGHTING," &c. 11, BOLT COURT, FLEET STREET, E.C.

1839.



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TO THE

FIFTH EDITION.

I am gratified with the reception which has been accorded to each successive Edition of the Handbook. It has been my earnest desire to make the work of the utmost possible use to those for whom it is specially intended. The Book is the fruit of long experience, and of much reading and thought. My ambition is that it may be referred to by the members of the profession, especially the younger members, and that it may afford them valuable assistance on occasions of difficulty and doubt.

I have reason to believe that the present Edition marks an important advance on those that have gone before. Considerable additions have been made to the text, and much of it has been re-written and otherwise improved.

T. N.

MANCHESTER, December, 1889.

914. Illumin eng. 600.



THE

GAS MANAGER'S HANDBOOK.

FIFTH EDITION.

New York : mig.

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NEWBIGGING'S HANDBOOK

POR

GAS ENGINEERS AND MANAGERS.

--

THE CHIEF KINDS OF COAL.

- Cannel or Parrot Coal.—The richest Gas-producing Coal, well-known by its hard smooth texture. The best varieties are found in different parts of Scotland, and at Wigan and Newcastle. The two latter yield Coke of fair quality; that from the former is less valuable, and much of it useless as fuel.
- Bituminous Coal.—For Gas-producing purposes the Coal most suitable is the bituminous class, which includes caking, splint, cherry, and other Coals containing bitumen. It is found widely distributed throughout the Kingdom; the better kinds being those found in Northumberland, Durham, Lancashire, Yorkshire, portions of Scotland, and to some extent in Wales. It yields Coke generally of excellent quality.
- Anthracite or (Hance Coal.—Chiefly Welsh, containing a large proportion of fixed carbon, but little volatile matter, and almost smokeless in burning. Excellent for steam purposes; but quite useless for the production of Illuminating Gas.
- Lignite or Brown Coult.—Found at Bovey Tracey, in Devonshire, in a small field near Lancaster, and near Lough Neagh, in Ireland. Of no great interest to the gas maker. Yields but little Gas and that of a low illuminating power, and a very unpleasant odour. Gives off a large quantity of water charged with acetic acid. Coke valueless as fuel.

TABULAR VIEW OF THE TRIAS, PERMIAN, AND CARBONIFEROUS SERIES IN ENGLAND AND WALES.

(PROFESSOR HULL.)

Lower Keuper sandstone. Upper mottled sandstone. New red sandstone or trias . Conglomerate beds. Lower mottled sandstone. Upper red sandstone of St. Bees, &c. Upper and lower magnesian limestones and marls of the Northern counties. Permian rocks Lower red sandstone of Lancashire, Cumberland. and Yorkshire, &c. (on the same horizon with) Red sandstones, marls, conglomerates, and breccia. of the central counties and Salop. Upper coal-measures with limestone, and thin coal seams. Upper carboniferous Middle coal-measures with thick coal seams. Lower coal-measures, or Gannister series, with thin coal seams and Carboniferous lower carboniferous fossils. rocks Millstone grit, with thin coal seams. Upper limestone shale, or Yoredale rocks. carboniferous Carboniferous limestone with shales, sandstones, and coal in the Northern counties and Scotland. Lower limestone shale.

Old red sandstone and Devonian rocks.

TABLES

Showing the Chief Substances of which Coal is Composed.

Percentage Composition.

NEWCASTLE COALS.

Name of Coal.	Spe- cific Gra- vity.	Car- bon.	Hy- dro- gen.	Nitro- gen.	Sul- phur.	Oxy- gen.	Ash.	Coke.
Willington		86.81	4.96	1.05	0.88	5.22	1.08	72 · 19
Tanfield	1.26	85 . 58	5.81	1.26	1.32	4.89	2.14	65 18
Bowden Close		84 . 92	4.53	0.96	0.65	6.66	2.28	69.69
Haswell Wallsend	1.28	83 · 47	6.68	1.42	0.06	8.17	0.50	62.70
Newcastle Hartley	1.29	81.81	5.50	1.28	1.69	2.58	7.14	64.6
Hedley's Hartley	1.81	80.26	5.28	1.16	1.78	2.40	9.12	72.8
Bates's West Hartley	1.25	80.61		1.52	1.85	6.21	4.25	
West Hartley Main	1.26	81.85	5.29	1.69		7.58	2.51	59:2
Original Hartley	1.25	81.18		0.72	1.44	8.03	3.07	58.2
Average of eighteen samples		01 10	0 00	· · · ·		0 00	00.	- CO 2
from different mines	1.25	82 · 12	5.31	1.85	1.24	5.69	8.77	60.67
LA	NCA	SHIR	E CO	ALS.				
Ince Hall Company's Arley .	1.27	82.61	5.86	1.76	0.80	7.44	1.58	64.0
Haydock, Rushey Park	1.32	77.65	5.23	0.50	1.73	10.91	3.68	59.4
Blackbrook, Little Delf	1.26	82.70	5.22	1.48	1.07	4.89	4.81	58.4
Wigan four feet	1.20	78.86	5.29	0.86	1.19	9.57	4.23	60.0
Cannel	1.23	79 23	6.08	.1.18	1.48	7.24	4.84	60.8
Caldwell and Thompson's								
Higher Delf	1 . 27	75.40	4.83	1.41	2.48	19.98	5.95	54.2
Average of twenty-eight sam- ples from different mines .	1.27	77.90		1.30	1.44	9.53	4.88	60.2
	RBY					00		1 00 2.
DE	1			1		1		
Earl Fitzwilliam's Elsecar .	1.296	81 · 98	4.85	1.27	0.91	8.58	2.46	61.6
Holyland and Co's Elsecar .	1.817	80.05	4.98	1.24	1.06	8.99	3.73	62.5
ButterleyCompany's Langley	1.264	77.97	5.58	0.80	1.14	9.86	4.65	54.9
Staveley	1.270	79 85	4.84	1.23	0.72	10.96	2.40	57.8
Average of seven samples	ļ	i I					i	i
from different mines	1.292	79.68	4.94	1.41	1.01	1 0·2 8	2.65	59.3
GLOU	CEST	ERS	HIRE	COA	LS.			
GLOU Coleford High Delf (Forest of		1		l I	<u> </u>	1	 I	!
	1.219	78.810	5.303	1.750	2.062			
Coleford High Delf (Forest of	1.219	78·810 76·502	5·303 5·380	1.750	2·062 1·669	8.659	6.700	
Coleford High Delf (Forest of Dean) .	1.219	78.810	5.303	1.750	2·062 1·669 2·370	8·659 8·840	6·700 9·210	62·6 59·7
Coleford High Delf (Forest of Dean) .	1·219 1·313 1·831	78·810 76·502	5·303 5·380 4·470	1·750 1·090 0·700	2·062 1·669 2·870	8·659 8·840	6.700	62·6 59·7
Coleford High Delf (Forest of Dean)	1·219 1·818 1·881 1·854	78·810 76·502 74·410	5·303 5·380 4·470 5·292	1·750 1·090 0·700 0·511	2·062 1·669 2·370 2·667	8 · 659 8 · 840 6 · 831	6·700 9·210 10·285	62·6 59·7 60·8
Coleford High Delf (Forest of Dean)	1·219 1·818 1·881 1·854 1·854	78·810 76·502 74·410 74·464	5·303 5·380 4·470 5·292 5·425	1·750 1·090 0·700 0·511 0·735	2·062 1·669 2·370 2·667 1·271	8 · 659 8 · 840 6 · 831 7 · 060	6.700 9.210 10.285 4.800	62·6 59·7 60·8 63·3
Coleford High Delf (Forest of Dean) """ """ Trenchard New Bowson, Cinderford	1·219 1·313 1·831 1·854 1·354 1·332	78·810 76·502 74·410 74·464 80·709	5·303 5·380 4·470 5·292 5·425 5·430	1·750 1·090 0·700 0·511 0·735 1·680	2·062 1·669 2·370 2·667 1·271 1·940	8·659 8·840 6·831 7·060 9·330	6.700 9.210 10.235 4.800 4.760	62·6 59·7 60·8 63·3 58·2
Coleford High Delf (Forest of Dean) """ """ Trenchard New Bowson, Cinderford	1·219 1·318 1·831 1·854 1·354 1·332 1·307	78·810 76·502 74·410 74·464 80·709 76·860	5·303 5·380 4·470 5·292 5·425 5·430 5·250	1·750 1·090 0·700 0·511 0·735 1·680 1·260	2·062 1·669 2·370 2·667 1·271 1·940 0·850	8.659 8.840 6.831 7.060 9.330 9.100	6·700 9·210 10·285 4·800 4·760 4·230	62·6 59·7 60·8 63·3 58·2 59·2
Coleford High Delf (Forest of Dean) " " " " " " " " " " " " " " " " " " "	1·219 1·318 1·381 1·354 1·354 1·332 1·307 1·374	78·810 76·502 74·410 74·464 80·709 76·860 79·310	5:303 5:380 4:470 5:292 5:425 5:430 5:250 5:613	1.750 1.090 0.700 0.511 0.735 1.680 1.260 0.940	2·062 1·669 2·370 2·667 1·271 1·940 0·850 1·457	8·659 8·840 6·831 7·060 9·330 9·100 6·391	6·700 9·210 10·285 4·800 4·760 4·230	62·6 59·7 60·8 63·3 58·2 59·2 60·9

NEWBIGGING'S HANDBOOK FOR

SOMERSETSHIRE AND OTHER COALS.

SOMERSETS	HIRI	E AN	D 0'	THE	CO	ALS.		
Name of Coal.	Spe- cific Gra- vity.	Car- bon.	Hy- dro- gen.	Nitro-	Sal- phur.	Oxy- gen.	Ash.	Coke.
Ashton	1.302	84 · 066	6.463	1.020	1.053	3.230	4.168	79.60
	1.808	84 - 912	4.976	0.840	1.586	4.166	3.520	
	1.290	82 · 470	5.008	1.190	1.039	6.842		
Nailsea	1.320	82 · 470 82 · 270 77 · 249 74 · 720	5.640	0.910	2.370	5.130		
Derbyshire Gas Coal	1.100	74.700	9.919	1.120	1.007	11.189	3·256 11·370	64.0
	1 302	78 905	5.486	0.840	1.471	10.928	2.420	55.4
		74 - 346		1 0 - 350	1.318	14 - 201	3.500	54 . 7
Bulwell Nottingham Gas Coal	1 • 291	77 184	5.517	0.770	1.251	12.518	2.760	60.0
" " Cannel.	1.269	¦78 • 680	5.872	0.700	0.690	9.378	4.680	56.6
	!	<u>L</u>	<u>!</u> .	!				_
	SCOI	CH	COAI	ls.				
Boghead	1 1 • 218	63 930	8-858	0.962	0.320	4.702	21 · 222	31.7
Boghead	1.200	76:090	5.220	0.962	1.530	5.050	10.700	58.4
Grangemouth	1.290	79.850	5.280	1.350	1.420	8.580	3.520	56 6
Eglinton	1.250		: 6·500	1.550	1.880	8.050	2.440	54.8
·				1·210		0.940	1.450	85 (
Aberaman, Merthyr Aberdare Co., Merthyr Anthracite (Jones and Co.)	1.810	88 280	4.240	1.660	0.910	1.650	3.260	85.6
Anthracite (Jones and Co.) .	1.375	91.440	8.460	0.210	0.790	2.580	1.520	92.
Coleshill	1.290	73 . 840	5.140	1.470	2.340	8.290	8.920	56 (
Liantwit	1.278	77.410	5.640	0.400	2.365	12.062	2.050	50.0
Coleshill Llantwit Nanigarw Llantwit Rhos Llantwit "" Holly Bush Tyr Filkens Llanhilleth Aber Rhondda Pontypridd Wallsend Energlyn	1.896	79 - 180	5.610	0.700	8 450	7.330	3.780	81.6
Rhos Llantwit	1.282	76 995	5 455	0.700	1.648	12 875	2 332	63.8
,, ,	1.302	75 452	5.497	0.840	2.812	13.023	2.876	63 (
	1.302	73.410	5.507	0.350	2.414	14.276	4.043	65.8
Holly Bush	1.269	80.117	5.045	0.019	0.597	8.022	3.002	64.6
Llanhilleth	1.274	87.640	6.085	1.120	1.636	2.209	1.810	70.5
Aber Rhondda	1.820	80 675	5.082	0.910	8.675	2.763	6.895	70.8
Pontypridd	1.811	79.820	5.470	0.700	3.950	3 750	6.810	65.6
Wallsend	1.817	78 270	5.380	0.770	1.860	8.900	4.820	66.0
Energlyn	1.812	83 120	4.900	0.980	1.870	5.890	2.800	60.
Rock Vawr	1.290	77.980	4.390	0.570	0.960	8.550	7.550	62
ANALYSIS OF TH					DD N	EWC	ASTI	Æ
	CUA	L (T	AYLOR	:).		D 0	4	
Silica						Per C		
Alumina			• • •	: :	· :	12.1		
Alumina						15.9		
Peroxide of Iron							•	
Peroxide of Iron Lime.				: :		9.8	9	
Peroxide of Iron Lime Magnesia				: :	: :	9·8	9 .3	
Peroxide of Iron Lime.				: :	: :	9.8	9 .3	

TABLE
SHOWING THE TOTAL AREA OF COAL MEASURES IN THE UNITED KINGDOM.

	Area of Co	al Measures.	Entire Area	of Country.	Proportion of
	Square Miles.	Acres.	Acres.	Square Miles.	Coal to the whole.
In England	6,039	3,864,960	81,770,615	49,643	1-8th
In Scotland & Islands, exclusive of Lakes.	1,720	1,100,000	18,944,000	29,600	1-18th
In North Wales In South Wales	210 950	184,400) 608,000 }	4,752,000	7,425	1-6th
In Ireland	2,940	1,881,600	20,399,608	31,874	1-11 th
In British Isles	•••	••	1,119,159	1,748	. –
Total	11,859	7,588,960	76,985,382	120,290	

Exclusive of wood-coal and lignite formations, and some small undefined areas.

ANALYSES OF COALS.

The following tabulated results of the analyses of the different kinds of Cannel and Bituminous Coals, by Mr. Lewis Thompson, though published as early as the year 1851, still constitute the most comprehensive and useful series of experiments (if we except those of Mr. James Paterson) that have appeared in this department of the science of Gas Lighting; and their general correctness and consequent value have frequently been proved.

It is to be noted that dry samples of coal were employed in each experiment. The importance of using dry material will be apparent when it is remembered that when coal in a wet or moist condition is placed in the retorts, the results are unsatisfactory in several respects. In the first place, the temperature of the retorts is reduced, and, as a consequence, extra fuel is consumed in restoring the temperature, and in drying the coal by evaporating the moisture and driving it off as steam before the coal is in a fit condition to undergo destructive distillation. Again, a portion of the moisture or steam is decomposed in contact with the sulphide of iron produced by decomposition from

the bisulphide of iron or iron pyrites contained in the coal.* The oxygen combines with the iron, forming the oxide of that metal, and the hydrogen with the sulphur, producing sulphuretted hydrogen. Bisulphide of carbon and other sulphur compounds are also formed in considerable volume. In this way the whole of the sulphur present in the coal is caused to pass off into the gas, and has to be subsequently removed in the process of purification, thus increasing the cost of manufacture. On the other hand, when the coal is distilled in the dry state, rather more than one-half of the sulphur present is left behind in the residuary coke.

Sulphur exists in Cannel in a free state, and in Bituminous Coals chiefly in combination with iron, as pyrites or bisulphide of iron, FeS₂, and this in the retort is converted into sulphide or protosulphuret of iron, FeS.

ANALYSES OF COALS.* (THOMPSON.) CANNEL COALS.

Name and		Coke.	Ash p	er Cent.		Sulphur in			
General Character of Cannel.	Vola- tile Matter		In Coal.	In Coke.	Nature of Ash.	Coal.	Coke.	Vola- tile Matter	
ARMISTON.—Resem bling lig- nite, and containing crys- tals of carbonate of lime, with impressions of leaves and deposits of iron py- rites. Compact. Principal fracture, slaty; cross frac- ture, irregular. Streak, dull brownish black. Thrown on the fire, it decrepitates, but does not fly. Colour of ash, a dirty grey; with nitrate of co- balt, greenish black. Spe- cific gravity of coal, 1-1967	45.5	54.5	4.18	7.66	Silicate of lime, alumi- na, and oxide of iron.	1.70	-95	•75	
BOSHEAD. — Brown, compact, and massive, containing a few impressions of sigillaria. Principal fract., slaty, conchoidal; cross fracture, irregular. Streak, yellow. Thrown on the fire, decrepitates alightly, does not fuse, but splits. Colour of ash, white; with nitrate of cobalt, blue. Specific gravity, 1.221.	68·4	31.6	22.8	72·15	Silicate of alu- mina.	•58	-08	-45	
CAPELDRAE.—Massive, dull black, impressions of sigillaria, with deposits of carbonate of lime and pyrites. Principal fract, conchoidal and slaty; cross fracture, distinctly conchoidal. Streak, yellowish brown. Thrown on the fire, decrepitates, splits, and flies, but does not fuse. Ash, white; with nitrate of cobalt, blue. Specific gravity, 1.2275.	54.5	45.5	10.5	23 · 07	Silicate of alumina.	•65	•20	-45	

^{*} From the Journal of Gas Lighting, Vol. II., pp. 203, 223, 243, 262.

NEWBIGGING'S HANDBOOK FOR

Warra and	Vols-		Ash p	er Cent.		,	Bulphur	in
Name and General Character of Cannel.	tile Matter	Coke.	In Coal.	In Coke.	Nature of Ash.	Coal.	Coke.	Vola- tile Matter
KIRENESS.—Massive and foliated, free from foreign matters. Dull brown. Principal fracture, slaty; cross fracture, conchoidal. Streak brown. Scarcely decrepitates on the fire. Colour of ash, whitish grey; with nitrate of cobalt, dull dark blue. Specific gravity, 1.208.	60-	40.	18.5		Silicate of alu- mina, limeand oxide of iron.	1.40	-58	• 82
KNIGHTSWOOD. — Compact, dull, black, massive, with deposits of carbonate of lime and iron pyrites. Principal fracture, slaty, conchoidal; cross fracture, conchoidal. Streak, shining black. Thrown on the fire, decrepitates and flies, but does not fuse. Colour of ash, pale umber, with nitrate of cobalt, dull black.	48.5	51.5	2.4	4.66	Oxide of iron and silicate of lime, with a-lumina.		-61	-49
LESMAHAGO.—Massive, dull black. Principal fracture, slaty, conchoidal; cross fracture, conchoidal and angular. Streak, black and somewhat shining. Thrown on the fire, decrepitates slightly, does not split or fuse. Colour of ash, white; with nitrate of cobalt, dirty blue. Specific gravity, 1 222.	49.6	50.4	9·1	18.05	Silicate of alu- mins and ox- ide of iron.	2.23	1.14	1.09
Lochgelly. — Colour, dull black and slaty. Fracture, inclining to slaty; cross fracture, irregular conchoidal. Streak, shining black. On the fire, decrepitates and flies. Ash, white; with nitrate of cobalt, blue. Specific gravity, 1°320.		66.5	18·1	19.7	Silicate of alumina.	.75	•25	-50

GAS ENGINEERS AND MANAGERS.

Action/ and			Ash p	er Cent.		Sulphur in		
Name and General Character of Cannel.	Vola- tile Matter	Coke.	In Coal.	In Coke.	Nature of Ash.	Coal.	Coke.	Vola- tile Matter
OLD WEMYSS. — Compact, dull brownish black; free from foreign matters. Principal fracture, slaty; cross fracture, angular, inclining to conchoidal. Streak, dull brownish black. Thrown on the fire, decrepitates and splits, but does not fly. Colour of ash, dull white; with nitrate of cobalt, clive green. Specific gravity, 1°3256.	52.5	47.5	15:1	31-78	Oxide of iron and silicate of alu- mina.	1.30	-60	-70
Wigan. — Compact, black and shining. Principal fract. conchoidal; cross fracture, conchoidal and cubical. Streak, shining black and waxy. Thrown on the fire, decrepitates, flies, and slightly fuses. Colour of ash, yellowish brown, inclining to red; with nitrate of cobalt, clive black. Specific gravity, 1.271.	37	63	3.	4.76	Oxide of iron and silicate of alu- mina.	1.25	-60	•65
Ransay's Newcastle.— Compact and massive, slightly tinged with oxide of iron. Black and shining. Principal fracture, highly conchoidal and resinoid; cross fracture, conchoidal and cubical. Thrown on the fire, decrepitates and flies to pieces, inclined to fuse. Colour of ash, reddish brown; with nitrate of cobalt, dull black. Specific gravity, 1 290.	36.8	63.2	6-6	10-44	Oxide of iron and silicate of lime, with alumina		-94	.81
BAND OF CANNEL IN Leverson's Wallsend Coal.—This is a dull black band, which runs through the mass of the coal. Fracture, slaty, con- choidal; cross fracture,		69.2	9.35	13.51	Oxide of iron and silicate of lime, with alumina		•50	-50

			Ash pe	r Cent.		8	ulphur	in
Name and General Character of Cannel.	Vola- tile Matter	Coke.	In Coal.	In Coke.	Nature of Ash.	Coal.	Coke.	Vola- tile Matter
cubical and conchoidal. Streak, black and shining. On the fire, splits, but does not fly or fuse. Ash, dull white, with shade of pink; with nitrate of cobalt, dull black. Specific gravity, 1.320.								
Band of Cannel in Pelton Main Coal.—Colour dull black, with a shade of brown. Structure, com- pact and uniform. Frac- ture, conchoidal and slaty; cross fracture, irregular, conchoidal, with deposits of iron pyrites. Streak, black and shining. On the fire splits, but does not fly; agglutinates and intumesces slightly. Ash, dirty white, with shade of pink; by nitrate of cobalt, black. Specific gravity, 1:320.	31.5	68.5	9.4	13.72	Oxide of iron and silicate of lime, with slumina	-95	-49	*46
Band of Cannel in Washington Coal.—This resembles Pelton and Leverson's bands. Colour, dull brownish black. Fracture, irregular, conchoidal; cross fracture, cubical and conchoidal. Streak, shining black. On the fire, splits and fuses slightly. Ash, dirty white, with shade of pink. Specific gravity, 1°326.	27-4	72.6	9-37	12-9		1.10	-56	.24
STAFFORDSHIRE. — Compact and uniform. Fracture, in all directions conchoidal, with deposits of carbonate of lime. Streak, shining black. On the fire, decrepitates and flies, but does not fuse. Ash, dirty white. Specific gravity, 1.220.	50.	50.	2.9	5.8		1.30	-52	-78

GAS ENGINEERS AND MANAGERS.

and the second second	200		Ash pe	r Cent.	Sulphur in			
Name and General Character of Coal.	Vola- tile Matter	Coke.	In Coal.	In Coke.	Coal.	Coke.	Vola- tile Matter	
New Brusswick.—Jet black, and pitchy looking. Fracture, highly conchoidal and resinoid in all directions. Streak, dull and pitchy. On the fire cracks and splits, then fuses and boils up with strong intumescence. Largely soluble in naphtha, oil of turpentine, and bisulphuret of carbon. Specific gravity, 1 098. The coke is light and friable, like that from pitch.	66.8	83.7	•6	1.78	·07	None.	•07	

BITUMINOUS COALS.

	11100		,,,,,				
Chashiae: Harcastle.—Structure, laminated, with numerous black bands. Principal fracture, slaty, inclining to angular; cross fracture, cubical, with deposits of carbonate of lime and iron pyrites. Streak, dull black. On the fire, agglutinates a little. Ash, dirty red. Specific gravity, 1 230.	31.5	68.5	5.	7.3	2.10	1.10	1.00
CUMBERLAND, No. 1.—Dull black, and coarse grained. Fracture, rough and hackley, inclining to cubical; cross fracture, slaty, and angular. Streak, dull black. On the fire, agglutinates and swells a little Ash, dirty white. Specific gravity, 1 294.	25.5	74-5	2.1	2.81	1.30	-70	-60
Cumberland, No. 2.—Coal black, with dull laminæ. Fracture, irregular, inclining to cubical; cross fracture, rough and angular, with charcoal deposits. Streak, black. On the fire, swells and fuses slightly. Ash, grey. Specific gravity, 1.275.	25.6	74-4	1.4	1.88	1.10	-60	-50
Cumberland, No. 3.—Coal black, and coarse grained, semi-crystal-line. Fracture, hackley and angular, with layers of charcoal; cross fracture, irregular and angular. Streak, brownish black. On the fire, swells and agglutinates. Ash, yellow white. Specific gravity, 1-290.	30-9	69-1	4	5.8	1.70	-80	-90

	200	1	Ash pe	r Cent.		Bulphu	in
Name and General Character of Coal.	Vola- tile matter	Coke.	In Coal.	In Coke.	Coal.	Coke.	Vola- tile Matter
DERBYSHIRE: Staveley.—Colour, jet black. Structure, splintry and prismatic. Fracture, slaty and columnar; cross fracture, irregular and cubical, with deposits of carbonate of lime and iron pyrites. Contains several black bands with charcoal. Streak, black. On the fire, crackles and splits; fuses slightly. Ash, dirty pale red. Specific gravity, 1.275.	40.9	59-1	2.7	4.57	1.20	-80	•40
GLOUCESTERSHIRE: Coal-Pit Heath. —Colour, coal black. Structure, granular and crystalline. Fracture, coarse grained and irregular in all directions, with numerous layers of charcoal and iron pyrites, and traces of carbonate of lime. On the fire, swells and fuses slightly. Ash, brick red. Specific gravity, 1.370.	30.1	69.9	5.8	8.3	4.10	2.20	1.90
Whitecroft, near Lydney.—Coarse grained and fibrous. Principal fracture, backley and slaty, with deposits of charcoal; cross fracture, uneven, inclining to rhomboidal, with deposits of carbonate of lime and iron pyrites. Streak, dull black. On the fire, fuses slightly. Ash, deep red. Specific gravity, 1 401.		65.7	11-1	16.89	3·10	1-90	1.20
LANCASHIRE: Arley.—Colour, coal black, with shining layers. Structure, massive. Fracture, inclining to slaty, with charcoal deposits; cross fracture, cubical, with traces of carbonate of lime. On the fire, splits slightly, and intumesces. Ash, dull fawn colour. Specific gravity, 1-270.		66.3	3.6	5.48	1.20	.60	-60
St. Helens.—Coal black and laminated. Principal fracture, slaty; cross fracture, cubical, with numerous deposits of charcoal in the principal fracture, and carbonate of lime in the cross fracture. Streak, dull black. On the fire, swells and agglutinates. Ash, fawn colour. Specific gravity, 1.285.		62.8	1.2	1.91	1.10	•54	.56

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GAS ENGINEERS AND MANAGERS.

W	***		Ash pe	r Cent.	8	ulphur	in
Name and General Character of Coal.	Vola- tile Matter	Coke.	In Coal.	In Coke.	Coal.	Coke.	Vola- tile Matter
NORTHUMBERLAND AND DURHAM: Blenkinsop.—Coal black; laminated. Fracture, coarse and granular; cross fracture, splintry, inclining to cubical. Streak, dull black. On the fire, fuses slightly, and intumesces. Ash, grey. Specific gravity, 1.298.	38.	62	5.1	8-22	1.60	-80	.80
Dean's Primrose.—Colour, brownish black, with shining layers. Frac- ture in all directions, cubical and somewhat irregular, with occa- sional deposits of iron pyrites. On the fire, splits and crackles slightly, swells, and intumesces. Ash, brick red. Specific gravity, 1.261.		70.75	2.4	3.4	1.40	-71	-619
Garesfield (Bute's).—Coal black and rather friable, with thin bands of dark lamine throughout. Fracture, uneven and cubical; cross fracture, angular and hackley, containing traces of charcoal. Streak, dull black. On the fire, swells and fuses together. Ash, light red. Specific gravity, 1-290.	28-3	71.7	3.2	4.46	-90	:40	*50
Garesfield (Cowan's).—Coal black and shining, with thin dark lamine. Fracture, irregular and cubical; cross fracture, angular, and affording deposits of charcoal. Streak, dull black. On the fire, agglutinates, swells, and partially fuses. Ash, pale cream colour. Specific gravity, 1'259.		70-6	-95	1.34	-85	-40	:45
Gosforth.—Coal black, with shining layers. Fracture, irregular, inclining to cubical; cross fracture, cubical, with indications of charcoal. Streak, dull black. On the fire, swells and agglutinates. Ash, dull yellow. Specific gravity, 1-260.		65*	1*	1:54	1.10	.50	-60
Eastings Hartley.—Jet black; laminated and splintry. Fracture, cubical and slightly conchoidal; cross fracture, cubical and irregular. Streak, black, with a shade of brown. On the fire, cracks and splits, with a trifling tendency to agglutinate. Ash, white, with red streaks. Specific gravity, 1.278.		63.4	2.	3.12	-95	-50	*45

		Coke.	Ash p	er Cent.	8	lalphur	in
Name and General Character of Coal.	Vola- tile Matter		In Coal.	In Coke.	Coal.	Coke.	Vola- tile Matter
Nobthumberland and Durham: West Hartley.—Jet black, with thin dull lamine in the direction of the principal fracture, and slight deposits of charcoal. Fracture, slaty, cubical, inclining to conchoidal; cross fracture, cubical, with layers of carbonate of lime. Streak, brown black. On the fire, splits and opens, but does not fuse. Ash, dull cream colour. Specific gravity, 269.		64.2	4.7	7.8	1.10	-60	-50
Leverson's Wallsend.—Colour, coal black, with shining layers. Frac- ture, cubical, and slightly slaty; cross fracture, cubical, with thin layers of iron pyrites. Streak, black and shining. On the fire, opens out, and agglutinates. Ash, brick red. Specific gravity, 1-278.	34.9	65·1	4.9	7.52	1.30	-65	•65
South Peareth.—Dull black, with bright lamine, coarse grained. Fracture, irregular, hackley, and inclining to cubical, with charcoal deposits; cross fracture, cubical. Streak, dull black. On the fire, intumesces and fuses partially. Ash, light yellow. Specific gravity, 1'266.	27.8	72.2	1.8	2.5	1.20	-60	· · 60
Pelaw Main.—Colour, coal black, inclining to jet in variable layers. Fracture, cubical in all directions, with deposits of pyritic charcoal and carbonate of lime. On the fire, opens out, agglutinates, and intumesces. Ash, pale fawn colour. Specific gravity, 1-271.	30.3	69.7	2.6	3.73	1.20	.70	.50
Petton Main.—Colour, coal black, with shining layers. Fracture, in both directions cubical, with thin deposits of carbonate of lime, and iron pyrites in the cross fracture. Streak, black and shining. On the fire, opens out and fuses slightly. Ash, pale ochry yellow. Specific gravity, 1-270.		71.6	1:41	1.96	1·10	·62	·48
New Pelton.—Colour, coal black, in- clining to jet in layers. Fracture, slaty and cubical: cross fracture, irregular and cubical. Streak, black and shining. On the fire, opens out, fuses slightly, and in- tumesces. Ash, light brick red. Specific gravity, 1-265.		69.8	1.75	25	1·10	•56	•54

GAS ENGINEERS AND MANAGERS.

CONT. 2 STATE TO THE		15	Ash pe	r Cent.	8	ulphur	in
Name and General Character of Coal.	Vola- tile Matter	Coke.	In Coal.	In Coke.	Coal.		Vola- tile Matter
Northumberland and Durbam: South Tyne.—Shining black, with dull lamins. Fracture, somewhat rhomboidal and irregular, with layers of charcoal and pyrites; cross fracture, angular. Streak, dull brownish black. On the fire, agglutinates and swells slightly. Ash, deep pink. Specific gravity, 1-339.		63.7	3-9	6-1	2.10	1-10	1.00
Urpeth.—Colour, coal black, with shining layers. Fracture, in all directions, cubical, with layers of carbonate of lime and iron pyrites on the cross fracture. Streak, black and shining. On the fire, opens out, swells and fuses slight- ly. Ash, dull ochry yellow. Spe- cific gravity, 1 271.		71.3	1*35	1.89	1-00	-60	-40
Washington.—Colour, coal black, with shining layers. Fracture, in all directions, cubical and irregular. On the fire, opens out and fuses slightly. Streak, shining black. Ash, reddish yellow. Specific gravity, 1'260.	31.25	68.75	2.2	8-2	1.30	•67	•68
Somensetshine Nailsea. — Dull black, coarse grained and fibrous. Fracture, hackley, inclining to rhomboidal, with numerous deposits of charcoal and iron pyrites; cross fracture, very irregular. Streak, brown black. On the fire, swells and fuses together. Ash, flesh-coloured, with red streaks. Specific gravity, 1:312.	34.9	65-1	8.	4-6	2.85	1.20	1.35
Radstock. — Colour, dull black. Structure, coarse grained and irregular. Fracture, slightly slaty; cross fracture, hackley, inclining to cubical, with layers of charcoal and iron pyrites, in cubical crystals; deposits of carbonate of lime. Streak, dull black. On the fire, alters but little, and intumesces slightly. Ash, dull yellow and flocculent. Specific gravity, 1-275.		61-75	8.5	5.66	3·10	1.80	1.80

			Ash p	er Cent.	s	ulphur	in
Name and General Character of Coal.	Vola- tile Matter	Coke.	In Coal.	In Coke.	Coal.	Coke.	Vola- tile Matter
STAFFORDSHIRE: Apedale, 4 ft.— Jet black, and in square, splintry fragments. Principal fracture, slaty, and slightly conchoidal; cross fracture, irregular, and nu- merous black bands. On the fire, decrepitates and opens; does not fuse. Ash, deep fawn colour. Specific gravity, 1.267.	40-	60.	•75	1.25	-80	•38	-42
Apedale.—Jet black and laminated; splintry and hard. Principal fracture, slaty; cross fracture, irregular and angular, inclining to cubical. Streak, shining black. On the fire, crackles and burns freely, but remains open, without any symptoms of fusion. Ash, deep red. Specific gravity, 1.307.		61.5	1.0	3.1	1.50	*82	-68
Heathern.—Colour, dull black, with shining layers. Fracture, slaty, containing deposits of charcoal; cross fracture, cubical, with thin layers of carbonate of lime and iron pyrites. On the fire, splits and fuses slightly. Ash, pale dull yellow. Specific gravity, 1.280.		57.1	1+75	3.06	1.50	•70	-80
Silverdale, 10 ft. — Splintry and laminated. Principal fracture, slaty; cross fracture, angular, and alightly conchoidal. Streak, dull black. On the fire, splits and orackles slightly; does not fuse. Ash, dull red. Spec. gravity, 1.301.	:	66.	1.95	2.95	1.30	·70	·60
Woodshutts, 7 ft., Banbury.— Fibrous and coarse grained. Principal fracture, hackley; cross fracture, irregular, inclining to rhomboidal, with layers of char- coal. On the fire, swells, but does not fuse. Ash, deep fawn colour. Specific gravity, 1.291.	; ;	59-8	1.22	2.04	-90	•54	•36
Wales (North): Ruabon, Top Yard Seam.—Coal black, with shining layers; laminated. Fracture, slaty and cubical, with charcoal de- posits; cross fracture, cubical. Streak, black. On the fire, swells, and agglutinates. Ash, pale fawn colour. Specific gravity, 1 269.		62 · 5	2.5	4.	1.40	-80	-60



Wasses and	V-1-		Ash p	er Cent.	8	ulphur	in
Name and General Character of Coal,	Vola- tile Matter	Coke.	In Coal.	In Coke.	Coal.	Coke.	Vola- tile Matter
Wales (North): Ruabon, Main Coal.—Coal black and laminated. Fracture, irregular, inclining to cubical; cross fracture, foliated and splintry, with numerous layers of charcoal, and some indications of iron pyrites. Streak, dull black. On the fire, swells and fuses together. Ash, pale yellow. Specific gravity, 1.284.	41.5	58-5	1.	1.71	*85	•45	-40
Ruabon, Yard Seam.—Coal black, with dull laminæ. Fracture, irregular, inclining to cubical; cross fracture, angular, with considerable deposits of charcoal, and thin layers of carbonate of lime. Streak, dull black. On the fire, agglutinates and intumesces. Ash, fawn colour. Specific gravity, 1.271.	34-	66*	1.4	2.12	1.10	-60	-50
Ruabon Nant Seam.—Shining black, and in columnar concretions. Fracture, coarse and hackley, with charcoal deposits; cross fracture, rhomboidal and crystalline, with thin layers of carbonate of lime. Streak, black. On the fire, agglu- tinates slightly and intumesces. Ash, cream colour. Specific gra- vity, 1.269.		62-1	1-4	2.25	1.10	*70	.40
	-		_			1	
Wales (South): Rhonda.—Colour, coal black. Structure, coarse grained. Fracture, slaty and irregular; cross fracture, hackley and angular. On the fire, swells slightly. Ash, light fawn colour. Specific gravity, 1.278.	22.8	77.2	2:7	8.5	2·30	1.20	1.10
Bkonda Low Main.—Colour, coal black; coarse grained and hackley. Fracture, irregular and slightly cubical; cross fracture, rough and angular. Streak, dull black. On the fire, intumesces and agglu- tinates feebly. Ash, pale red. Specific gravity, 1°280.	28·1	76-9	2.1	2.78	2.30	1.10	1.10

	***	100	Ash pe	r Cent.	8	ulphur	in
Name and General Character of Coal.	Vola- tile Matter	Coke.	In Coal.	In Coke.	Coal.	Coke.	Vola- tile Matter
YORKSHIBE: Elsecar Low Pit.— Colour, jet black, with dull layers. Structure, laminated. Fracture, slaty, inclining to cubical; cross fracture, cubical, with numerous deposits of charcoal, and traces of carbonate of lime. Streak, black. On the fire, swells and fuses with some intumescence. Ash, ochry yellow. Specific gravity, 1 258.	37.	63.	1-1	1.74	1.20	-63	-57
Grigleston Cliff, Soft.—Colour, coal black. Structure, splintry, and in layers. Fracture, slaty, with bands of charcoal; cross fracture, hack- ley and cubical, containing traces of carbonate of lime. Streak, black. On the fire, alters but little, and does not fuse or decrepitate. Ash, brick red. Specific gravity, 1-255,	35*6	64-4	1.6	2.48	1.40	.75	-65
Mortomly.—Coal black, with shin- ing layers, in splintry fragments. Fracture, laminated and cubical; cross fracture, cubical and irre- gular. Streak, dull black. On the fire, splits and opens, but after- wards agglutinates and intu- mesces. Ash, light fawn colour. Specific gravity, 1 '220.	87*	63.	1.6	2.54	1.10	-60	•60
Silkstone, No. 1.—Colour, jet black. Structure, laminated and prismatic. Fracture, slaty; cross fracture, cubical and irregular, with deposits of carbonate of lime and charcoal. Streak, black and shining. On the fire, splits and fuses slightly. Ash, fawn colour. Specific gravity, 1°260.	34.1	65.9	2.78	4.21	1.30	*80	-50
Silkstone, No. 2.—Colour, jet black. Structure, uniform. Fracture, in all directions, cubical; traces of carbonate of lime and charcoal. Streak, brownish black. On the fire, fuses slightly, and intu- mesces. Ash, yellowish fawn colour. Specific gravity, 1°259.	38*	62*	2.55	4.1	1.10	-60	•50
Stilkstone, No. 3.—Colour, coal black. Structure, laminated and prismatic. Fracture, slaty and columnar; cross fracture, irregular and cubical, with deposits of charcoal and traces of carbonate of lime. Streak, black. On the fire, alters little. Ash, pale fawn colour. Specific gravity, 1.262.	35.2	64.8	2.8	4.3	1.45	-75	-70

	l		Ash pe	er Cent.	8	ulphur :	in
Name and General Character of Coal.	Vols- tile Matter	Coke.	In Coal.	In Coke.	Coal.	Coke.	Vola- tile Matter
Yorkshire: Soap House Pit — Dull black and slaty, with impressions of leaves. Fracture, rough and hackley, inclining to conchoidal; cross fracture, irregular and angular. On the fire, splits, and then agglutinates and swells. Streak, dull brownish black. Ash, light brown. Specific gravity, 1.258.	85	65*	-8	1.23	•75	•40	*85
Woodthorpe.—Compact, black and uniform in appearance; resembles cannel coal. Fracture, conchoidal; cross fracture, splintry and conchoidal, with layers of carbonate of lime. Streak, black. On the fire, decrepitates slightly and splits, but does not fuse. Ash, dirty pink. Specific gravity, 1.847.	88.1	66.9	10.5	15.7	1.30	-70	.50
FRANCE: Denain (Valenciennes).— Colour, coal black. Structure, coarse grained and slightly fibrous. Fracture, irregular, inclining to cubical, with layers of charcoal; cross fracture, hackley and angular, with traces of iron pyrites. On the fire, but little affected, intumesces and agglutinates. Ash, fawn colour. Specific gravity, 1.265.	29.9	70-1	6.	8.56	2:40	1.80	1·10

COAL AND CANNEL.

Every-day experience shows that variations occur in the quality of the coal obtained from the same seam and in the same locality. The identical seam of coal also varies in quality in different districts. Coal got from those parts where the seam is thickest is more likely to possess uniformity of structure than that got near to the circumference of the basin.

Mr. E. W. Binney's observations led him to the conclusion the seams of coal are materially affected by the nature of the se imposed strata. If this is of an open character, such as sandstone

gaseous matter can readily escape; while, on the other hand, if the roof is of almost air-tight black shale or blue blind, the gas is retained. Further, it is not unreasonable to infer that the vegetable matter of which coal is composed would be deposited irregularly. For example, during the ages of primeval vegetable growth, a larger proportion of leaves would be deposited in some places than in others where the deposits of bark and cellular tissue would be in excess. These conditions would naturally tend to produce variations in quality. In seams of cannel there is more uniformity of quality than in those of ordinary coal, due to the circumstance, as is supposed, of their having been formed from vegetable matter long macerated in water, thus insuring a more intimate admixture of the vegetable substances.

It is well known that variations in the gas-producing qualities of coal are caused by the material having been stacked for a length of time at the pit's mouth.

The particulars contained in the following Tables, showing the Producing Power of various kinds of Coal and Cannel, have been derived from the standard works on Gas Lighting, from Parliamentary Returns, and from the recorded results of the different experimentalists, in whatever authentic form they may have appeared. There are evident discrepancies between some of the results, especially between the earliest and the most recent. The range of time, however, over which the several experiments have been made, embraces a period of more than fifty years; and it is doubtless to the imperfect apparatus used in the earlier trials that the difference between these and the later results may chiefly be attributed. In some instances the difference is only apparent, the distillatory process having been prolonged at the expense of the illuminating power.

It is exceedingly desirable, in recording the results of experiments with mixtures of various coals with each other, and along with other substances, that the exact proportions used should be stated. When these are not specified, the other particulars given are comparatively valueless. The worth of some of the information contained in the subjoined Tables would have been much enhanced had this necessary rule been followed.

The weight of the coke produced in the different trials should also be given in every instance. The absence of such information, so easily obtained, and of such obvious value, is always to be regretted.

COAL AND CANNEL.

Quantity of Gas obtained from Coal and Cannel per Ton; Illuminating Power of the Gas; Specific Gravity of the Gas; Weight of Coke in Pounds per Ton; and Percentage of Ash in Coke.

The results described in the third column of the following tables were obtained with the old burners, now discarded for the "Standard" burner; it is necessary, therefore, when desiring to ascertain the illuminating power which the latter burner would develop, to add about 15 per cent. to the figures here given.

10 mg

Name of Coal.	Cubic Feet of Gas Obtained per Ton,		fic Grav. of the Gas. Air	Wght. of Coke in lbs. per Ton.	Ash in Coke per Cent.	Authority.
CANNEL COAL.		1				
Arniston	12,600	22.5	-626	1221*	7.66*	Chartered Gas Co.
Boghead	13,334	45.		717		Mr. T. G. Barlow.
Ditto	15,000	37 - 75		708*		Chartered Gas Co.
Ditto	15,486	52.	.726	760	63.95	Dr. Fyfe.
Bridgewater	11,200			• •		Mr. J. Leigh.
Brymbo	6,650	20	504			,,
Capeldrae	14,400	19.75	.577	1019*	23.07*	Chartered Gas Co.
Ditto, No. 1	11,500	41.56	.644	999	17.26	Dr. Fyfe.
Ditto, No. 2	9,600	50	650	1256	43.7	Ditto.
Chapelside, Airdrie .	11.272	35.61		916	19.08	Dr. Wallace, 1869.
Coed Talon, shale	10,780	14.07		Nil.		Mr. J. Paterson.
Donibristle	9,923	37:55	.593	1220	7.85	Dr. Fyfe.
Dunkirk, Dukinfield .	10,875	22.75	i	1568	8.	Mr. Longworth.
Haywood, Scotch	11,400	30.2:		1157	17.8	Mr. F. J. Evans.
Kirkness	12,800	21.2	.562	896*	83.7*	Chartered Gas Co.
Ditto	9,620		.711		۱	Dr. Fyfe.
Knightswood	9,720		.590			Mr. Wright.
Ditto	13,200	19.	.550	1154*	4.66*	Chartered Gas Co.
Ditto	8,960		.557		٠	Dr. Fyfe.
Lesmahago, No. 1 Canl.	13,500	27.1	•642	1129*	18.05	Chartered Gas Co.
Ditto No. 2 do	13,200	24.8	.618			Ditto.
Ditto	10,176	44.12	•669	1360	6.58	Dr. Fyfe.
Ditto	12,750	35.55		1052	10.85	Mr. F. J. Evans, 1868
Ditto	11,500	34.5		1081	11.17	Prof. Penny, 1869.
	to	to	[1	[• • • • • • • • • • • • • • • • • • •
	12,000	85.25	il		1	
Ditto, 1st experiment .	11,681		•540	٠		Mr. Wright.

^{*} Mr. L. Thompson.

Name of Coal.	Cubic Feet of Gas Obtained per Ton.	Power of Gas in Stand.	Grav. of the Gas.	Wght. of Coke in lbs. per Ton.	Ash in Coke per Cent.	Authority.
CANNEL-continued.						
Lesmahago, 2nd expmt.	9,878		.650		22/10/	Mr. Wright.
Ditto	11,312		.737			Mr. J. Hedley.
Leverson	11,600	18*	.523	1550*	13.21.	Chartered Gas Co.
Lochgelly	9,123		.567	1490*	19.7*	Dr. Fyfe,
Lothian	10,000	133	556		2.7	Ditto.
Monkland	10,190	1000	.667	755	1:78	Ditto. Mr. L. Thompson.
Peasley Cross, St.			-	100	1 10	Mr. D. Thompson.
Helens	10,000	19.46	120	100	4.25	Mr. King.
Pelton	11,500	18.5	.520	1534*	13.72*	Mr. J. Hedley.
Ramsey	10,300	21.4	.548			Chartered Gas Co.
Ramsey's Newcastle .	9,746		.554 to			Dr. Fyfe.
Ditto	9,692	16.65		1520		Ditto.
Ditto	9,016		.604			Mr. Wright.
Ditto	9,333	**	-598			Mr. Kay, Dundee Gas
Ditto	9,667.		:731			Drs. Leeson, Miller, &c.
Ditto	9,151	27.2		1416	10.44	Mr. L. Thompson.
Scotch Parrot	9,500		640	**	**	Dr. Fyfe.
Scotch	14,000	**	.580	**	**	Mr. Clegg.
Ditto	13,813		*500	1120	5.8	Ditto. Mr. L. Thompson
Torryburn	11,200	**	-624	1120		Dr. Fyfe.
Washington	10,500	18.	.500	1626*	12.9*	Mr. J. Hedley.
Welsh	11,424	·	.737			Ditto.
Wemyss	10,976		.670	**		Mr. Wright.
Ditto	10,192	-:	-691			Ditto.
Ditto	14,300	24.5	.580	1064*	31.78	Mr. Evans, Chrtrd.Co
Ditto	9,500		·642	**	**	Dr. Fyfe. Ditto.
wigan	3,000	**	.520		**	Ditto.
Ditto	11,200		-606			Mr. J. Hedley.
Ditto	9,500		.580		100	Liverpool Gas Co.
Ditto, Ince Hall	11,673		.620	1474		Mr. J. Leigh.
Ditto, do	11,400	20.	.528	1411*	4.76	Mr. Evans, Chrtrd.Co
	11,500	**	**	**	••	Mr. J. Leigh.
Ditto, Blundell's	11,500	**	.470		**	Ditto.
Ditto	9,408 10,500	**	•478		***	Mr. Wright. Mr. J. Leigh.
Ditto	14,453	::	.640	- 11	:: 1	Mr. Clegg.
Ditto	14,267		.610			Ditto.
Ditto Dews-	100000000000000000000000000000000000000		7			
burys	11,300		***		**	Mr. J. Leigh.
Wyan	14,453		640	**	**	Mr. Clegg.
Yorkshire	11,500		451	**	••	Dr. Fyfe.
Co. West Ardsley,				4	00 1	
near Leeds	10,296	21.		1344		Mr. W. Hugon.
	20,000	-		2022	200	Territoria de la constanta de

^{*} Mr. L. Thompson.

Name of Coal.	Cubic Feet of Gas Obtained per ton.	Illum. Power of Gas in Stand. Sperm Cndls.	Specific floor Grav. of the Gas. Air 1 000.	Wght. of Coke in lbs. per Ton.	Ash in Coke per Cent.	Authority.
NEWCASTLE COALS.						
Benton Main	10,987	••	·400		••	Mr. Clegg.
Berwick & Craister's	10 507		·470	ł		Ditto.
Wallsend	12,507	•••	-521		::	Mr. J. Hedley.
Blenkinsopp	9,700	14:	•450	1389	8:22	Mr. L. Thompson.
Ditto	10,500	1	·480	1585	3.4	Ditto.
Ditto	11,120	::	•410			Mr. Clegg.
Ditto	10,500	12	490			Mr. Evans, Chrtrd. C
Eden Main	10,400		•400			Mr. Clegg.
Ellison's Main	11,200		·416			Mr. Clegg.
English caking coal .	8,000		1420			Dr. Fyte.
Felling Main	11,200	•••	•410	•••	••	Mr. Clegg. Mr. L. Thompson.
Garesfield	10,500	•••	•398	1606	4:46	Ditto.
Ditto, Bute's			•••	1581	1.84	Ditto.
Ditto, Cowan's	10,500	11.2	-398	1001	1 02	Mr. Evans, Chrtrd. C
Ditto	10,000	j .	1402	1456	1.54	Mr. L. Thompson.
Ditto	10,000	12:	•402	1	- 0-	Mr. Evans, Chrtrd. C
Hasting's Hartley	10,300	12.5	•421	1420	8.15	Mr. L. Thompson.
Heaton Main	10,400		•410	•••		Mr. Clegg.
Hutton Seam	8,700					Hartlepool Gas Co.
Leverson's Wallsend .	10,800		• 425	1458	7.52	Mr. L. Thompson.
Di tto	10,800	12.5	• 425	•••		Mr. Evans, Chrtrd. C
Newcastle	11,648		· 475			Mr. J. Hedley.
Ditto	9,450	13.2	••	•••	• • •	Brighton Gas Co.
Dit to	9,420	13.2	••	•••	i	Brighton and Hov Gas Co.
D/44 -	0.905	14.2				Sth. Metropolitan O
Ditto	9,395		••	•••	1 :: 1	Exeter Gas Co.
Ditto	10,500	12:	.415	1564	2.5	Mr L. Thompson.
Peareth's Wallsend	11,147		•410	1001		Mr. Clegg.
Ditto	9,700	12.		::		Cambridge Gas Co.
Pelton	11,000	14.	•430			Mr. Evans, Chrtrd. C
Disto	11,000	14.	•430	1604	1.96	Mr. L. Thompson.
Ditto	11,424		·487	••		Mr. J. Hedley.
Ditto	9,746	15.93		1563		Dr. Fyfe.
Pelaw	11,424	••	•444	•••		Mr. J. Hedley. Mr. L. Thompson.
Ditto	11,000	10.75	·420 ·420	•••		Mr. Evans, Chrtrd. C
Ditto	11,000	12.75	·420	1561*	8:78*	Mr. Clegg.
Pelaw Main Russell's Wallsend	12,400	••	•418		""	Ditto.
Kussell's Wallsend	9,000	12.5	410	::	::	Rochester Gas Co.
South Peareth	3,000	12.0	::	1617	2.5	Mr. L. Thompson.
South Tyne	::	::	::	1427	6.1	Ditto.
Urpeth	::	::	١	1597	1.89	Ditto.
Wallsend, Newcastle .	12,000		•490			RevolvingWeb Retor
Washington	10,000	14.	·430	1540	8.2	Mr. L. Thompson.
West Hartley	10,500	12.5	•420	1488	7.8	Ditto.

[•] Mr. L. Thompson.

Name of Coal.	Cubic Feet of Gas Obtained per Ton.	Illum. Power of Gas in Stand. Sperm Cndls.	Speci- fic Grav. of the Gas. Air 1-000.	Wght. of Coke in lbs. per Ton.	Ash in Coke per Cent.	Authority.
CUMBERLAND, YORK- SHIRE, LANCASHIRE, DERBYSHIRE, STAP- FOORDSHIRE, WELSH, AND OTHER KINDS OF COAL.		:				
Arley	10,200	18.	•462	1540	6.	Mr. J. B. Clift.
Ditto	10,200	. 10	102	1485	5.43	Mr. L. Thompson.
Ditto	11,200	13.8	•406	1460		Dr. Thompson.
Ashton - under - Lyme	1,	1			1	
coal slack	9,000	10.	۱	۱		Stafford Gas Co.
Barley Brook, Arley,	-,	1 -0	""	!	!	3
Wigan	9,500	16.7	•460	1459	4.59	Mr. Alfred King.
Bickerstaff, Liverpool.	11,424		.475		١	Mr. J. Hedley.
Bilston	7,100	9.5				Bilston Gas Company
Brancepeth	8,500	18		١	l	Harrogate Gas Co.
Brymbo, 2-yard coal .	8,800	i	•463	۱		Mr. Wright.
Ditto. main	10,500	15.	.540		l	Mr. L. Thompson.
Cheshire	1			1534	7.8	Ditto.
Cumberland, No. 1.	l			1669	2.81	Ditto.
Ditto, No. 2.		!		1667	1.88	Ditto.
Ditto, No. 3.				1548	5.8	Ditto.
Derbyshire	8,000	18.				Leamington Gas Co.
Ditto	8,500	13.				Leicester Gas Co.
Ditto	8,500	15.			!	Oxford Gas. Co.
Ditto, Staveley		1		1824	4.57	Mr. L. Thompson.
Ditto, deep main	9,400		•424			Mr. Wright.
Ditto, soft coal	7,500	1	.528	1	١	Leicester Gas Co.
Ditto, do	7,000		•448		1	Derby Gas Co.
Ditto, do	7,000	::	.424		•	Nottingham Gas Co.
Durham Fields, best	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	''			1	
seam	8,600	12.			1	Sunderland Gas Co.
Forest of Dean, 1st var.	10,188		350			Mr. Clegg.
Ditto, 2nd variety	10,133	1	.360		1	Ditto.
Ditto	9,000	8 to 9			1	Gloucester Gas Co.
France, Denain (Va-	1	1	1	1	1	
lenciennes)			١	1570	8.56	Mr. L. Thompson.
Garswood Hall topooal	"	''				•
Wigan	10,820	16.	.566	1346	5.79	Mr. J. Paterson.
Gloucestershire, Coal-	,				i	
Pit Heath	·		١	1566	8.3	Mr. L. Thompson.
Gloucestershire, White-			İ	1	1	-
croft, near Lydney .				1472	16.89	Ditto.
Hindley Field best coal	10,760	15.26	.450	1814	5.45	Mr. J. Paterson.
Leeds coal	6,500		•530	1		Leeds Gas Co.
Llanelly, Wales	5,000					Llanelly Gas Co.
•	to 8,000	1		1	i	1
Lumpcoal, West Brom-	1		ļ	1	!	l
wich	6,500	1	458	l	1	Birmingham Gas Co
Ditto, do	6,500		455		••	Birmingham and State fordshire Gas Co.

Name of Coal.	Cubic Feet of Gas Obtained per Ton.	Illum. Power of Gas in Stand. Sperm Cndls.	Speci- fic Grav. of the Gas. Air 1.000.	Wght. of Coke in lbs. per Ton.	Ash in Coke per Cent.	Authority.
VARIOUS COALS—contd.						•
Macclesfield Mynydd Bach-y-Glo-	6,720		••	••		
Colliery coal	7,000	9.		٠	l	Swansea Gas Co.
Neath, South Wales	11,200		•468		::	Mr. J Hedley.
Ormskirk or Wigan	,				''	
slack	8,200		·462			Liverpool Old Gas Co
Park Gate coal	7,500	11.		••		Rotherham Gas Co.
Platt Lane coal .	9,750	18.75	· 483	1412	2.94	Mr. J. Paterson.
Powell coal, 2 owt.						
charges every 5 hours Powell coal, 11 cwt.	10,165	••	•459	••		Mr. Wright.
charges every 5 hours	8,250		·470	••	l	Ditto.
Somersetshire coal.	8,000	••	••	••	l 1	Wells Gas Co.
Ditto, Nailsea		••	••	1458	4.6	Mr. L. Thompson.
Ditto, Radstock		••	• •	1383	5.66	Ditto.
Staffordshire, Apedale.	•••	••	••	1378	3.1	Ditto.
Ditto, 4-feet do		••	••	1844	1.25	Ditto.
Staffordsbire, Heath-				1000	اممما	1.5 T m
orn		••	• •	1279	3.06	Mr. L. Thompson.
Ditto, Silverdale, 10-ft.	••	••	• •	1478	2.95	Ditto.
Ditto, Woodshuts, Ban- bury, 7-feet	1			1840	2.04	Ditto.
Di tto	7,780	11to12	••	1		Bath Gas Co.
Ditto, South, 1st var	10,988		. 898	::	::	Mr. Clegg.
Ditto, 2nd do	10,667	::	•895	::	l :: i	Ditto.
Ditto, 3rd do	10,667	::	.890		::	Ditto.
Ditto. 4th do	9,600		.820			Ditto.
St. Helens			• •	1407	1.91	Mr. L. Thompson.
Stockport	7,800		.539			Stockport Gas Co.
Wales (North), Ruabon,	1			1		-
top yard seam			••	1400	4.	Mr. L. Thompson.
Ditto, main coal		••	• •	1810	1.71	Ditto.
Ditto, yard seam			• •	1478	2.12	Ditto.
Ditto, Nant seam	••	••	• •	1891	2.25	Ditto.
Wales (South), Rhonda	••		• •	1729	3.5	Ditto.
Ditto, low main	11:000	••	. 400	1723	2.78	Ditto.
Ditto, Neath.	11,200	••	468	••	••	Mr. J. Hedley.
Welsh coal, 1st variety Ditto, 2nd do	10,000	•••	· 385 · 380	••	••	Mr. Clegg. Ditto.
Wigan and St. Helens	1	30.05		••		
Yorkshire, best South	9,168	16·25 14·	••	••		Mr. J. Paterson.
Ditto, Elsecar Low Pit	9,000		••	1411	1:74	Sheffield Gas Co. Mr. L. Thompson.
Ditto, Grigleston Cliff,		••	••			_
soft	••	••	• •	1448	2.48	Ditto.
Ditto, Mortomly	0.000	10.6	• •	1411	2.54	Ditto.
Ditto, Silkstone	8,600	18.3	••	1470	4:5.	Great GrimsbyGasCo
Ditto, Silkstone, No. 1.	•••	••	••	1476	4.21	Mr. L Thompson.
Ditto, Silkstone, No. 2.	••	•••	••	1889	4.1	Ditto.
Ditto, Silkstone, No. 8.	••	•••	• •	1452	4.3	Ditto.

Name of Coal.	Cubic Feet of Gas Obtained per Ton.	Illum. Power of Gas in Stand. Sperm Cndls.	Grav. of the Gas.	Wght. of Coke in lbs. per Ton.	Ash in Coke per Cent.	Authority.
VARIOUS COALS—contd.						
Ditto, Silkstone, nuts, Thorncliffe Ditto, Soap House Pit. Ditto, Woodthorpe	10,800	15.85	::	1418 1456 1499	6· 1·23 15·7	Mr. F. J. Evans, 1870 Mr. L. Thompson. Ditto.
MIXTURES OF CANNEL AND COAL.						
Proportions specified.	!					
Boghead cannel 1-8th, Arley Mine coal 7-8ths	10,400	16.5		· ·		Blackburn Gas Co.
cent., Newcastle coal 95 per cent.	10,000	14.		! , ••		Devonport Gas Co.
Boghead cannel 1-4th, Pelton coal 3-4ths. Boghead cannel 1-10th,	12,800		••	••		Mr. T. G. Barlow.
Lochgelly cannel 9-10ths. Drighlington cannel	9,055	24.93	· • • · · ·	! 	••	Ditto.
1-4th, Halifax soft bed coal 3-4ths Ince Hall cannel 68 per	9,000	18.9		 	••	Shipley Gas Co.
cent., Arley coal slack 32 per cent. Lesmahago cannel 6	10,206	19.01	•527	1396	6.4	Rossendale Union Gas Co.
per cent., Cumber- land coal 94 per cent. Wigan coal and iron Co.'s cannel 72 per	7,000	15.		· ••	••	Carlisle Gas Co.
cent., Arley coal slack 28 per cent Wigan cannel 2-3rds,	9,967	19.65	•530	1462	5.2	Rossendale Union Gas
coal 1-8rd	9,600	17.	••	••		Heywood Gas Co.
coal 1 to 5	9,000	14.	••	••		Alliance Gas Co. Dublin.
black bed Half cannel, half coal .	9,000 9,450	16· 13·5			::	Pudsey Gas Co. St. Helens Gas Co.
Proportions not specified.				<u> </u>		
Wigan cannel and other coals Cannel and bett or bed	10,091	21 ·	••			Birkenhead Gas Co.
coals	9,250	18.	••			Bradford Gas Co.

Name of Coal.	Cubic Feet of Gas Obtained per Ton.	Illum. Power of Gas in Stand. Sperm Cndls.	Specific Grav. of the Gas. Air 1-000.	Wght. of Coke in lbs. per Ton.	Ash in Coke per Cent.	Authority.
MIXTURES OF CANNEL AND COAL—contd.						
Ramsey's cannel with Newcastle caking coal Cannel and best house	9,500 to 10,000	12.	••			Hastings Gas Co.
coal	9,000	12to14	••	••		Holmfirth Gas Co.
ooal	9,300	12.5	۱	٠		Phœnix Gas Co.
Ditto do	9,400	12.		••		Plymouth and Stone
Ditto do	8,000 to 9,000	12.	••			house Gas Co. Portsea Island Gas Co
West Riding cannel and common coal .	8,000	10to14				Scarborough Gas Co.
Oldham, Watergate, and Wigan cannel .	9,500		•584			Manchester Gas Wks
MIXTURES OF DIFFERENT COALS. Coal-Pit Heath, Forest						
of Dean and South	7,000	18.		۱		Bristol Gas Co.
Derbyshire and Staf- fordshire coal.	8,500	10to12	ľ	"		Warwick Gas Co.
Ditto do	9,000	9to10		l ::	::	Worcester Gas Co.
Derbyshire, Notting- hamshire, and York-	7,800 to	1 2t o15				Nottingham Gas Co.
shire best coal Derbyshire and Forest	8,200	i		}		
of Dean coal Low Moor mixed with	9,000	10.	••	••	••	Cheltenham Gas Co.
two kinds of slack . New Pelton and other	8,000		•420	••		Bradford Gas Co.
Newcastle coals Newport (Monmouth-	8,500 Newpirt	13.	••			Kingston-on-Thames _Gas Co.
shire coals	8,000 Somers. 5,500	9.	••	••	••	Weston-super-Mare Gas Co.
Ravensworth Pelaw & Newcastle coals Silkstone and Renshaw	9,000	13.	••	••		Beccles Gas Co.
coal	7,500	11.2	••	••		Lincoln Gas Co.
tol coal	7,500		••			Bridgewater Gas Co.
byshire coal	8,800	12.5	••	••		${\bf Birming ham Gas\ Co.}$

Name of Coal.	Cubic Feet of Gas Obtained per Ton.	Power of Gas in Stand.	of the Gas. Air	of Coke	Ash in Coke per Cent.	Authority.
MIXTURES OF COAL AND OTHER SUBSTANCES.						
Llantwit small coal, with 5 per cent. of Broxbourne shale oil Newcastle coal 80 per cent., Trinidad bitu-	9,750	21.5	••		! 	Mr. T. G. Barlow,
men 20 per cent Newcastle coal 90 per cent., Trinidad bitu-	10,600	17.6				Dr. Letheby and Mr Keates.
men 10 per cent. New Brunswick Albertite	10,200 9,166 to 10,200	15.6 28.66 to 35.42	1	:	·	Ditto do. Mr. Evans.

RECENT ANALYSES OF COALS AND CANNELS.

		GA	8.		co	KE.	
Name of Coal.	Gas per Ton of Coals, Cubic Feet.	Illumi- nating Power. Can- dles.	Ab- sorption by Bro- mine per Cent.	Car- bonic Oxide per Cent.	Per Ton of Coals. lbs.	Ash in Coke per Cent.	Authority.
CANNELS.		-			1		
Boghead	13,000	40.0	25.0	1.5	670	60.0	Mr. F. J. Evans.
Lesmahago .	12,000	32.0	14.0	8.0	980	7.0	
Lothian Cannel .	12,700	34.0	17.0	7.0	963	6.0	"
Cleugh Cannel	12,000	30.0	7:75	10.5	1182	12.8	"
Lochgelly	10,500	17.0	40.0	6.0	1232	15.0	"
Ince Hall (Wigan) .	10,200	20.0	12.0	3.5	1120	8.0	"
Wigan	10,000	20.0	13.0	4.2	1120	6.5	,,
Kirkless Hall	10,500	23.0	14.0	4.0	1232	9.5	"
Leeswood Curley	10,000	28.0	24.0	3.0	728	10.0	"
Ditto do. average	9,800	20.0	12.5	8.0	1120	8.0	"
Wemyss , .	11,000	26.0	17.0	1.0	1844	50.0	"
VARIOUS COALS.							
Pelton (Old)	11,500	13.5	5.0	5.0	1560	2.75	,,
" (New)	10,500	12.0	4.75	4.5	1568	2.5	,,
Pelaw	10,000	13.25	4.5	4.5	1568	2.5	,,
Waldridge	9,000	13.0	4.3	3.2	1568	8.0	,,

·		GA	8.		CO	KE.	
Name of Coal.	Gas per Ton of Coals. Cubic Feet.	Illumi- nating Power. Can- dles.	Absorption by Bromine per Cent.	Car- bonic Oxide per Cent.	Per Ton of Coals. lbs.	Ash in Coke per Cent.	Authority.
VARIOUS COALS—contd.							
Wearmouth	10,500	13.5	4.7	8.8	1500	2.5	Mr. F. J. Byans
Bute's Tanfield	10,100	13.2	4.0	8.7	1450	3.8	***
Dean's Primrose	10,500	13.2	5.0	4.7	1400	8.5	",
South Hetton	9,600	12.7	8.0	8.2	1470	3.7	**
Shincliffe	9,500	12.0	5.0	2.0	1500	8.8	,,
Lambton	10,500	14.0	4.8	8.8	1560	.2.8	,,
Haswell	10,300	18.0	3.4	8.1	1300	2.5	
P 25 12 12 12 12 12 12 12 12 12 12 12 12 12	10,400	15.64	6.25	6.25		3.0	•
Silkstone, three	10,866	15.84	6.5	6.25		2.0	**
samples	10,800	15.65	4.75	7.0	1480	6.1	••
Thorneliffe	10,500	16.5	5.5	6.5	1483	4.8	"
Rhos Lantwit, Caer-	10,000	10 0	"	•	1200	1 0	,,
philly.	9.780	15.07	7.8	8.2		l !	Mr. Fiddes.
Ditto do	9,675	18.69	4.55	7.3	::	::	
Powell's Lantwit	0,010	10 00	1 00		•••		••
large	11,079	15.16	6.05	10.1			
Ditto do. small	10,285	14.56	5.0	8.6	::	::	"
Lydney — Norchard Coal— Coleford, High Delf	·	15.40	4.75	10.0			"
Seam	9,215	15:46	4.75	10.8	•••	••	1)
Ditto do. Cannel — Varteg Hill	8,702	14.13	4.25	9.4	••	••	11
Colliery, Pontypool.	9,262	17 · 21	6.2	8.6	••		,,
Gas Coal from do	9,021	15 · 47	5.8	4.9		••	,,
Tyr Filkens, Newport,			i		İ		•
Mon	11,835	13.6	4.3	5.9			,,
Lydney — Tranchard			i	l	1	:	**
Seam	9,870	14.77	5· 4 5	8.6		'	,,
Pellowell, near Lyd-			. •		İ	i l	•
Llantwit Red Ash, Pontypridd small	9,785	13.84	4.25	10.15	••	••	"
coal	9,390	15.06	5.8	8.9		!	
Ditto do, large	9,708	16.33		8.33			,,
Dean's Primrose	9,800	16.0		1	::		Mr. G. Livesey
Holmside	9,800	16.0		::	::	:: ;	•
West Leversons	9,464	15.5		l ::			**
330000000 01 31	9,200	15.8	١ ::	::	::		"
Washington	9,200	16.9		::			**
Nettlesworth Prim-	0,200	10 0			••		,,
rose	9,500			١	۱	[
Mr. A D.L.	9,537		i	1		••	"
Norfolk Silkstone	10,000	17:5		•••	١ • •		**
					• • •	••	**
Teesdale	9,468						**

	NEWBIGGING'S HANDBOOK FOR
Authority	Hutchinson Brothers. Ditto. Dr. Macadam. Mr. G. F. Cusiter. Mr. G. R. Hislop. Mr. G. R. Hislop. Dr. Macadam. Mr. G. R. Hislop. Dr. Macadam. Mr. G. R. Hislop. Dr. Macadam. Dr. Macadam. Mr. G. R. Hislop. Ditto. Dit
Hydro- carbons absorbed by Bromine per Cent.	13:20 13:20 13:00 11:60 11:60 10:25 11:25
Sulphur in Coal per Cent.	1.00 1.00 1.00 1.00 1.00 1.00 1.00 1.00
Ash in Coal per Cent,	6 - 9 6 - 9 16 - 0 16 -
Coke per Ton of Coal in Ibs.	1308 1140 1140 1154 1102 11102 11103 11103 11103 11103 11208 11208 11208 11308
Value of One Ton of Coal in lbs. of Sperm.	865-45 739-13 886 8876 930 933 851 1347 967 820 820 820 820 820 1204 820 1204 1204 1204 1204 1204 1204 1204 12
Value of One Cubic Ft. of Gas in Grains of Sperm.	607 648 648 7757 757 757 757 757 757 757 757 757 7
Illumi- nating Power of Gas in Standard Candles.	22.22 22.22 22.22 23.22 23.22 23.22 23.23
Gas per Ton in Cubic Feet.	11,350 10,655 10,200 10,200 11,200 11,260 10,280 10,280 10,280 10,280 10,280 10,280 10,280 11,828 11,610 11
Specific Gravity.	1.287 1.284 1.284 1.286 1.286 1.412 1.514 1.277 1.284 1.287 1.287 1.287 1.284 1.284 1.284
Name of Coal.	Adwalton Stone Coal, Seam No. 1 Ditto, Seam No. 2 Billyford Billyford Blackhall and Calderbank, No. 2 Brachead Coppa Curly Ditto, Smooth Cornelloch and Milburn Cowdenbeath Craignethan Donibristle Cylinton Forlisset Eglinton Forlisset Grenhill Home Farm and Box Parrot Inchall Kirkness Kirkwood, No. 1 Lanemark Lesmahago, Duke of Hamil- ton Lochore Lochore

	GAS ENGINEERS AND MANAG		8
Authority.	Mr. G. F. Cusiter. Mr. G. B. Hislop. Mr. G. R. Hislop. Mr. G. F. Cusiter. Mr. J. Pattinson. Mr. G. F. Cusiter. Dr. Macadam. Mr. J. Hislop. Mr. F. M. Remington. Mr. G. R. Hislop. Mr. G. R. Hislop. Mr. G. R. Lislop. Mr. G. F. Cusiter. Mr. G. F. Cusiter.	Mr. J. Pattinson. Ditto. Mr. J. Hutchinson. Mr. W. Carr. Hutchinson Brothers. Mr. J. Hutchinson.	Ditto. Mr. A. Upward. Mr. W. King. Ditto.
Hydro- carbons absorbed by Bromine.	15.55 14.00 11.00		0:::
Sulphur in Coal per Cent.	0.70 0.61 1.82 0.73 0.54 0.67 1.72	0.83	1111
Ash in Coal Per Cent.	5.70 2.44 8.14 115.40 11.68 11.68 11.68 11.68 11.40 11.75	2.83 1.90 6.88 2.87	1.38
Coke per Ton of Coal in lbs.	1125 1125 1136 1136 1077 11250 1068 1410	1512 1520 1350 1578 1375 1872	1450 1476 1523 1500
Anue of Value of me Cubic One Ton Frost of of Coal Gas in of Coal Grains of Sperm.	1366 1404 11090 11090 11090 11090 11090 11090	:::89:99	
Value of one Cubic Foot of Gas in Grains of Sperm.	782 781 781 782 683 680 680 680		;
nating Power of Gas in Standard Candles.	82.60 14.22 31.72 81.72 88.47 88.47 88.44 88.44 88.44 88.47 17.00	14.40 15.40 15.96 18.70 16.74 17.03	16.75 17.56 17.40 18.30
Gas per Ton in Cubic Feet.	13,100 11,150 11,150 12,000 9,340 10,204 11,933 10,213 10,250 10,250 11,012	11,000 10,050 10,520 10,365 10,360	11,800 10,620 9,100 9,780
Specific Gravity.	1.218 1.226 1.226 1.250 1.250 1.257 1.257 1.268 1.268 1.268	1.273	1.269 1.283 1.279
Name of Coal.	Monkland Muirkirk, No. 1 Orrell Nuts. Old Wemyes Seton Parrot Stansey's Newcastle Caunel Roschall Stone Parrot Tannocheide Tannocheide Coals. Coals. Barnsley "Soft Coal" Farmsley "Soft Coal" Farmsley "Soft Coal" Farmsley "Soft Coal" Farmsley Sliktone	Main Silkst e. Soliks iks G	Coal Stanbope Silkstone Main Wigan Deep Yard Gas Coal Wigan, Arley Mine

RECENT ANALYSES OF COALS AND CANNELS—continued. COALS. (F. J. Evans.)

Name of Coal.	Gas per Ton in Cubic Feet,	Illumi- nating Power of Gas.	Value of One Cubic Foot in Grains of Sperm.	Coke per Ton of Coal. ibs.	Sul- phur in Coal per Cent.	Hydro- carbons con- densed by Bromine.	Value of One Ton in lbs. of Sperm.
Old Pelton	11,500	14.50	348	1545	•75	5.0	571
Pelaw	11,500	14.75	354	1568	*85	4.5	581
Washington	10,000	15.00	360	1523	.73	5.0	514
New Pelton	10,100	14.00	336	1456	.62	4.75	484
Leverson	11,000	14.00	336	1411	.69	4.00	528
Dean's Primrose	10,500	15.00	360	1456	.90	4.80	540
Londonderry	9.800	16.50	396	1545	1.64	6.50	554
Do. average of eight				1 2 4 4		(A-32)	
samples	11,000	16.80	403	1500	1.30	6.00	633
Gosforth	10,000	13.50	324	1456	1.10	4.CO	462
West Hartley	10,800	14.00	336	1411	1.20	4.20	518
Hastings Hartley	10,300	14.00	333	1344	1.50	4.30	494

CANNELS. (F. J. Evans.)

	1.	Con- densed	Specific	Specific Gravity of	Photogen	ic Power.
Name of Cannel.	Gas per Ton.	per Cent. by Bromine.	Gravity. of Gas.	Con- densed Matter.	Actual.	By Analysis
Boghead	15,000	30.0	.752	1.21	35.75	36.30
Lesmahago, No. 1.	13,500	16.0	-642	1.64	27.10	26.24
Ditto. No. 2.	13,200	17.0	•618	1.43	24.80	24.81
Capeldrae	. 14,400	16.5	.577	1.29	19.75	21.28
Armiston	12,600	17.0	•626	1.40	22.50	23.80
Ramsey	. 10,300	12.5	.548	1.82	21.40	22.95
Wemyss	14,300	14.5	•580	1.87	24.50	27.11
Kirkness	. 12,800	10.2	.562	1.95	21.20	19.88
Knightswood	. 13,200	9.6	•550	2.28	19.(0	21.66
Wigan (Ince Hall)	. 11,400	11.5	.528	1.77	20.00	20.35

RECENT ANALYSES OF COALS AND CANNELS—continued. COALS. (Mr. W. Fiddes.) Illuminating Power ascertained by the New "London" Argand.

Name of Coal.	Specific Gravity.	Gas per Ton in Cubic Feet.	Illuminating Power of Gas.	Value of one Cubic Foot of Gas in Grains of Sperm.	Value of Gas per Ton of Coal in lbs. of Sperm.	Coke per Ton of Coal in lbs.	Ash in Coal per Cent,	Sulphur in Coal per Cent.	Hydro- carbons absorbed by Bromine per Cent.
Welsh Coals.	1.271	10,285	16.56	897	889	1524	4.85	1.42	2.00
itto	1.277	11,079	17.16	411	650	1522	4.05	1.43	90.9
itto	:	11,092	16.38	393	623	1.00		:	:
hos Llantwit	1.282	9,730	17.07	409	899	1417	2.332	1.643	:
itto	1.805	006'6	16.86	404	571	1411	2.876	2.312	5.71
itto	1.303	9,675	15-69	376	619	1462	4.043	2.414	4.55
antwit Red Ash	1.272	9,708	18.33	439	609	1344	4.90	1.354	6.46
itto do	1.227	9,390	17.06	409	648	1306	9.82	1.34	2.80
itto do	:	9,180	15.94	385	109	:	:	:	;
lantwit Basin	:	8,325	16.93	406	483	:		:	:
Oitto do		7,300	16.76	401	418	:	:	:	:
Brw	1.326	167.6	16.64	839	558	1379	8.78	3.45	6.50
Bargoed		8,600	15.86	380	467	:	:	:	:
Winserchan	:	10,850	16.19	364	638			•	:
Rock Vein	:	9,399	18.52	444	969	:	6.45	:	:
Ditto	:	8,370	17.44	418	499	:		:	:
E Hill	1.467	9,262	19.51	461	609	1366	8.83	2.32	6.50
tto Gas Coal	1.305	9.021	17.47	419	539	1335	9.12	2.82	08.9
Ditto do		8,010	15.07	361	418	:	:	:	:
Ditto do.		10,080	15.65	875	540	:	6.70		
redegar	1.288	9,910	14.30	848	485	1716	1.615	3.50	4.83
Ditto		9,321	14.09	888	450	:			:
Energivn	1.312	9,960	17.85	428	609	1597	5.30	1.87	5.75
itto		10,464	16.86	898	250	•			
Aberbege		8,885	17.02	408	819	:			:
Holle Rush	1.089	10.577	10.61	008	459	1666	8.509	0.070	8.10

NEWBIGGING'S HANDBOOK FOR

Name of Coal.			Specific Gravity.	Gas per Ton in Cubic Feet.	Illuminating Power of Gas.	Value of one Cubic Foot of Gas in Grains of Sperm.	Value of Jas per Ton of Coal in lbs. of Sperm.	Coke per Ton of Coal in lbs.	Ash in Coal per Cent.	Sulphur in Coal per Cent,	Hydro- carbons absorbed by Bromine per Cent.
Welsh Coals—continued.	tinu	ed.			1						
Abercarn	,		;	12,300	16.91	883	673	:		:	:
thondda Valley				10,270	11.04	592	888	:			:
Lyr Filkens			1.368	11,835	16.60	874	682	1452	8.808	2.237	4.30
Blenavon				10,619	16.43	870	999	:	4.730	:	
Diendare			1.0.1	90,1	17.66	424	606		4.0.0	1.000	:
Abor Phondde			1.800	09,400	14.00	588	999	1505	019.1	9.675	
Wallsend			1.817	066.6	17.84	498	611	1478	4.890	1.860	6.10
Pontrowaith				8 800	16.59	879	479	2	6.790	-	2
Sryncoch			1.285	10.971	16-17	888	608	1585	1.860	: :	4.60
Ditto			1.369	9,849	15.44	870	494	1491	13.120	:	4.30
Спопсектевания	COALS	d					H.				
rd High Delf.			1.219	9,700	17.46	419	089	1428	8.050	2.062	4.75
Ditto do			1.354	9,785	15.84	380	681	1351	10.535	2.667	4.55
Ditto do			1.831	9,630	15.35	898	909	1338	9.510	2.370	4.40
Ditto do	,		1.313	9,150	16.13	387	909	1402	9.200	1.669	4.55
Trenchard's Lydney .			1.354	9,870	16.77	403	299	1419	4.800	1.271	2.45
Vew Bowson, Cinderf	pro		1.332	9,220	17.80	427	299	1803	4.760	1.940	6.50
Ditto do.			1.307	8,576	16.80	403	494	1326	4.530	0.860	4.93
Hanham			1.277	6,979	14.87	345	492	1318	11.480	2.440	4.76
Ditto			:	9,465	14.85	355	480	1416	7.430	:	4.00
Ditto			:	8,329	14.61	350	417	1416	8.200	:	4.00
Yate			:	10,360	19.91	374	653		6.980	:	:
			:	9,900	13.55	325	459		3.480		:
Coal Pit Heath				8,262	18.18	436	615		18.740	:	:
Š			:	8,800	16.70	400	203	:	:	:	:
			***	13,871	16.54	365	728	:		:	:
Ditto do				7,500	12.00	360	386	:			:
Warmley	,		1.304	8,990	15.50	872	478	1698	2.830	0.820	4.96
harlefold			1.074	0100	10:00	AGO	KOR	1000	002.0	1.400	100

	Na.	Name of Coal.	Ö	oal.				Specific Gravity.	Gas per Ton in Cubic Feet.	Illuminating Power of Gas.	Value of one Cubic Foot of Gas in Grains of Sperm.	Value of Gas,per Ton of Coal in lbs. of Sperm.	Coke per Ton of Coal in 1bs.	Ash in Coal per Cent.	Sulphur in Coal per Cent.	Hydraphy absorbed Brom per O
SOMERSETSHIRE COALS	RS	TE	1	0	1 4	I só										1
Paulton					ŀ			:	9,240	15.57	878	492	1949	17.20	:	4.5
Ditto .	,							:	11,288	17.16	411	662	:	6.48		:
Ditto .				٠			,	:	10,098	18.30	487	633	:	6.34		:
Ditto .	,								9,807	16.64	888	629	:	:		:
Ditto .								:	10,195	16.06	361	526	;			•
Ditto .								:	9,515	17.90	429	583		15.44	:	:
Radstock								:	10,270	18.82	489	644	1308	2.64	:	:
Ditto .								:	8.978	18.00	482	554		94.0	:	:
Ditto .								:	8,971	17-99	481	552	:	8.84		-
Midsomer Norton	LA	ort	100					:	10,850	16.91	403	969	:		:	:
Clutton		•	•					;	8,901	17.51	420	534	:	6.58	:	
Ditto .								:	11,520	16-39	888	647		:	:	:
Ditto .		•						:	10,530	14.13	883	610		:		:
Ditto .									9.720	15.79	379	526				
Timsbury			1				9		9.196	15.25	366	481			3	
Ditto									9.720	14.48	846	480				
Nailsea								1.320	9,334	16.61	868	530	1484	89.8	2.87	4.8

TABLE.—PRACTICAL ANALYSIS OF VARIOUS SCOTTISH CANNEL COALS, BY MR. G. R. HISLOP.

Description.	Parified Gas per ton of Cannel. Cabic Feet.	Specific Gravity of Gas Air 1000.	Illumi- nating Power of Gas in Sperm Candles,	of One Cubic Foot of Gas in grains of Sperm.	Value of Gas from Ton of Cannel in 1bs. of Sperm.	and CO ₂ in Foul Gas, per cent.	Weight of Coke in lbs. per Ton of Cannel.	Carbon in Coke, per cent.	Sulphur in Volatile Matters from Ton of Cannel, in lbs.	Sulphur in Coke from Tor of Canne in Ibs.
Cairntable , Ayrshire	11,480	602	92.83	787 - 90	1292.20	3.00	1164	94.04	18.76	4.08
ditto	10,602	574	29.23	701.50	1062.30	8.20	1241	89.20	22.84	9.41
pitto. No. 2 ditto	10,658	588	28.34	680.16	1035 60	4.50	1165	89.40	10.53	4.70
No. 1, Portobello, Edin	11,616	684	30.62	784.88	1219.87	4.25	1087	92.80	15.28	7.17
Ditto, No. 2, ditto ditto	11,650	572	27.34	656.16	1618.49	4.50	1139	85.80	16.94	7.13
	18,825	610	32.13	771.12	1522.96	3.80	1034	75.10	12.11	8.58
nyss	13,220	612	82.28	780 48	1482.28	4.80	1036	73.50	16.35	7.61
Hamilton La	10,561	518	22.32	585-70	808.50	4.75	1272	95.42	19.04	28.9
ar, Whitburn.	10,640	581	28.06	673.90	1024.30	00.9	1385	58.20	16.55	9.62
Bradisholm Railleston ditto	10,055	564	27.86	688.60	1087 - 25	4.50	1207	79.80	18.67	4.92
side, Airdrie	13,265	672	35.86	09.098	1630-22	2.52	978	81.11	3.38	2.52
Carnwath	11,894	586	28.15	675-60	1150.80	8.00	1193	88.80	10.75	5.83
West Calder .	10,535	516	25.82	89-209	914-56	3.35	1234	91.40	6.37	2.91
Airdrie	13,126	716	38.71	929.04	1742.08	2.75	1109	84.20	9.40	6.27
Carnwath	11,706	989	30.55	783.20	1226.10	3.15	1135	85.80	17.85	6.16
wood, No. 1, Coatbridge	11,615	593	30.04	722-10	1196-20	3.20	1002	87.40	90.8	4.95
No. 2, ditto	10,538	578	28.41	681.80	1026 - 40	2.75	1062	87.20	8.21	3.36
shago, Main coal .	12,420	889	34.26	824.24	1458.88	6.25	1060	08.98	13.66	10.75
Shieldmuir, Motherwell . ditto	9,520	586	23.13	555.10	754.96	4.50	1242	91.80	8.26	6.82
chside, Bellshill .	10,918	576	28.85	89-629	1059-62	8.75	1250	82.80	10.30	6.27
Tilsontown, Carnwath . ditto	11,120	587	99.04	896-968	1007-17	08.6	1979	06.66	7.84	8.86

Nore.—The above Table exhibits the results obtained from a few of the principal Cannels out of upwards of 130 kinds from different districts in Scotland. The market value of Cannels is largely affected by the jourlity of Cote produced. A large proportion of the above number contains only from 80 to 85 per cent. of carbon, which limits their use, and in the manufacture of gas renderes an admixture of such Cannels as yield a superior class of Coke for fring purposes indispensable, with the effect of greatly enhancing the price of the latter.

The filluminating power of the gas from the whole of these Cannels was tested with Union burners, No. 8 being used for 80 andle and under; above 100 enables, but the rate of consumption gradually reduced below the 5 cubic feet, to prevent smoking, as the scale of quality ascended; the 38-candle gas being tested while burning at the rate of 85 cubic feet per hour, and calculated to the 5 cubic feet,

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			Value of Value of
•			Value
NELE			_
CAN			
S ANI	TERBON.	'n	_
COALE	By Mr. JAMES PATERSON.	GAS COALS.	
GAB	IR. JAN	GAS	
OF	By M	•	
ANALYSES OF GAS COALS AND CANNELS.			
ANAI			

77. **38**

	GAS ENGINEERS AND MANAGERS.
Sai. Phur Per Cent.	11.864 1.864 1.864 1.828 1.828 1.828 1.828 1.828 1.828 1.828 1.828
Ges puri- ned by One Own. Lime.	19,000 15,000 15,000 11,000 14,000 15,000 15,000 15,000 16,000
Value of Gas per Ton of Coal in lbs. of Sperm.	676-17 698-37 688-37 688-69 694-91 696-69 699-69 677-66 678-39 67
Value of One Cubic Foot in grains of Sperm.	884. 8653. 870.33 870.33 870.33 867.93 867.93 886. 886. 888. 8
Illum. Power.	14.00 14.136 16.43 16.43 16.70 16.70 16.70 16.89 16.89 16.80
Conden- sation by Bromine.	8 - 75
Ash in Specific Coke Gravity per of Cent. Coal.	4. 1.288 8.21 1.288 8.21 1.264 1.76 1.265 7.62 1.204 8.85 1.274 8.85 1.274 8.86 1.267 4.16 1.274 8.666 1.267 4.16 1.274 8.76 1.206 6.66 1.267 6.66 1.274
Ash in Coke Per Cent.	6.05. 6.
Coke per Ton.	1336 1466 1411 1470 1460 1560 1680 1870 1836 1817 1438 1838 1838 1838 1838
Gas Per Ton.	12,800 11,026 11,026 9,500 10,000 11,860 11,860 11,800 11,800 11,868 11,800 11,868 11,800 11,868 11,868 11,868 11,868 11,868 11,868 11,868 11,868 11,868 11,868 11,868 11,868 11,868 11,868 11,868
Bituation.	Rotherham Ditto Ditto Ditto Ditto Wigan Monmouthshire Ditto Wigan Ditto Ditto Ditto Ditto Ditto Ditto Ditto Ditto Ditto Ditto Ditto Ditto Ditto Ditto Ditto Ditto Ditto Botherham Wigan Ditto
Name of Coal.	Denaby Main Colliery gas coal acreened Ditto Derbyshire Coal Co. gas coal Derbyshire Silkstone Duxbury Coal and Iron Co., Middle Monntain Mine Duxbury Park gas coal. Bebw Vale Coal & Iron Co., Medow Yein Ebbw Vale Coal & Iron Co., Rock Yein Coal Ebbw Vale Coal & Iron Co., Rock Yein Coal Ebbw Vale Coal & Iron Co., Rock Yein Coal Ebbw Vale Coal & Iron Co., Rock Yein Coal Ebbw Vale Coal & Iron Co., Rock Yein Coal Ebbw Vale Coal & Iron Co., Rock Yein Coal Ebbw Vale Coal & Iron Co., Rock Flacher, Burrows, & Co., Arley Flacher, Burrows, & Co., Arley Flacher, Burrows, & Co., Arley Flacher, Burrows, & Co., Arley Flacher, Burrows, & Co., Arley Flacher, Burrows, & Co., Arley Flacher, Burrows, & Co., Arley Flacher, Burrows, & Co., Arley Flacher, Burrows, & Co., Arley Flacher, Burrows, & Co., Arley Flacher, Burrows, & Co., Arley Flacher, Burrows, & Co., Arley Flacher, Burrows, & Co., Arley Flecher, Burrows, & Co., Orrell Garwood Coal & Iron Co., Orrell Garwood Little Delph Growenor Colliery, N. Wales, gas coal bottoms Guy Brothers, Amberwood gas coal.

GAS COALS.—continued.

NEWBIGGING'S HANDBOOK FOR

		GAS CC	ALS.	COALS.—continued.	nued.						1
Name of Coal.	Situation.	Gas per Ton.	Coke per Ton.	Ash in Coke per Cent.	Ash in Specific Coke Gravity per of Cent. Coal.	Conden- sation by Bromine.	Illum, Power,	Value of One Cubic Foot in Grains of Sperm,	Value of Gas per Ton of Coal in 1bs. of Sperm.	Gas puri- fled by One Cwt. Lime.	Sul phu Oen
Haddock, Little Delph Hazelwood Coal and Cannel Co. Hazelwood Coal and Cannel Co. Ditto do. Ellerbeek do. Ditto do. Peacock Mine Higgan, J. & P., Dukinfield Black Mine. Ditto do. Peacock Mine Hindley Field, gas coal Ditto do. Vigan 4-feet Hindley Green, Arley Ditto do. 5-feet Hindley Hall, King coal Ditto do. 5-feet Hindley Hall, King coal Ditto do. Golborne gas coal Lingste Colliery Mickless Yard Coal. Johnson, Edward, Wigan 4-feet Johnson, Edward, Wigan 6-feet Ditto do. Golborne gas coal Lingste Colliery Micklefield Colliery Micklefield Colliery Co. Milton Colliery Mirkled Coal Co. Coal and Cannel mixed Moss Hall, gas coal. Ditto delleg Coal Co. Lingste Colliery Mirklefield Colliery Mirklefield Colliery Mirklefield Coal Co. Lotto delleg Coal Co. Ditto delleg Coal Co. Milton Colliery Mirkled Coal Co. Miss Coal Co. Ditto delleg Coal Co. Miss Coal Co. Ditto delleg Coal Co. Ditto delleg Coal Co. Arley Montain Mine Coal Co.	St. Helens Liverpool Mold Wigan Ditto Chorley Dutto Ditto Di	8,896,010,000,000,000,000,000,000,000,000,00	18398 1470 1282 1282 1340 1870 1874 1874 1877 1877 1876 1886 1886 1886 1886 1886	200212300 20021	1.25 1.25 1.25 1.25 1.25 1.25 1.25 1.25	6. 10 8 8 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9	12. 12. 12. 12. 12. 12. 12. 12. 12. 12.	8853-30 8853-30 8852-1 8852-1 887-1 886-1 866-1 866-1 866-1 866-1 866-1 866-1 866-1 866-1 866-1 866-1 866-1	391. 518.34 522.28 522.28 522.28 665.4 667.14 667.28 667.28 667.38 689.38 689.38 689.4 687.7 687.7 687.7 687.7 687.8 689	15,000 16,000 16,000 17,000 17,000 17,000	

-		
Sul- phur per Cent.	17.168 17.016 17.016	0.738
Gas purified by One Cwt.	17,500 16,000 16,000 16,000 17,000 11,000 11,000 11,000 11,000 11,000 11,000 11,000 11,000 11,000 11,000 11,000 11,000	15,000
falue of Value of One Gas Cubic per Ton of Coal rains of in lbs. of Sperm, Sperm,	588 94 18 649 118 649 118 658 18 668 18 668 18 668 18 668 18 668 18 668 18 668 18 688	679.26 657.94
Value of One Cubic Foot in grains of Sperm.	396. 396. 397. 398. 399.	872. 874.64
Illum. Power.	16.98 14.95 14.19 16.19 16.19 16.19 16.19 16.19 16.19 16.19 16.19 16.19 16.19 16.19 16.19 16.19	16.50
Specific Conden- Gravity sation Dy Coal, Bromine.	5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	44:
Specific Gravity of Coal,	1.262 1.262 1.262 1.262 1.262 1.263	1.283
Ash in Coke per Cent.	0.4 6.8 6.0 0.1 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0	7.31
Coke per Ton.	1330 1049 1049 1049 1440 1440 1440 1440 144	1368
Gas per Ton.	10, 200 10,	10,900
Situation.	Cheshire Gloucester Thorneliffe Ditto Ditt	Ditto Ditto St. Helens
Name of Coal.	n Colliery (nt Cosl and not cost and cost and corfolk Slake on the likstone thi likstone thi likstone thi likstone thi likstone soft vincing, O do. Whining, O do. Whining, O do. K do. K do. K cosland, Wery Colliery on and Kno and Kno and Kno in Main, Che in Main, Che in Main, Che in Main, Che in Main, Che in Main, Che in Main, Che in Main, Che in Main, Che in Main, Che in Main, Che in Silkstone Silkstone K Pearson, & Pearson, & Pearson, & Pearson, & Pearson, Che in the control of	Ditto unscreened do

GAS COALS, -continued.

NEWBIGGING'S HANDBOOK FOR

Sul- phur per Cent.	0.482
Gas purified by One Owt. Lime.	18,000 17,000 18,000 18,000 11,000 11,000 11,000 11,000 11,000 11,000 11,000 11,000 11,000 11,000
Value of Gas per Ton of Coal in lbs. of Sperm.	628.24 650. 650. 650. 657.61 657.60 657.80 657.90 6
Value of One Cubic Foot in Grains of Sperm.	988-16 408-7 370-385-30 885-8 885-8 885-8 885-8 8114-72 889-414-72 889-408-84 408-24 408-24 408-24 408-66 981-9 408-66 981-9 408-68 881-9 408-84 881-8 8 8 8
Illum. Power.	15. 94 17. 94 16. 52 16. 53 17. 01 16. 68 17. 01 16. 68 17. 01 16. 68 17. 01 17. 01 18. 98 18. 98 19
Conden- sation by Bromine,	5.50 5.25 5.05 5.05 5.05 8.50 8.50 6.5 5.7 4.25 5.7 4.25 6.8 8.50 6.6 6.7 6.7 6.7 6.7 6.7 6.7 6.7 6.7 6.7
Specific Gravity of Coal.	1.24 1.242 1.243 1.273 1
Ash in Coke per Cent.	0.64 3.12 9.23 6.87 6.87 6.87 6.87 1.77 1.85 1.77 1.85 1.77 1.85 1.77 1.85 1.77 1.85 1.77 1.85 1.85 1.85 1.85 1.85 1.85 1.85 1.85
Coke per Ton.	1462 1462 1463 1315 1316 1316 1310 1428 1318 1428 1430 1430 1448 1430 1440 1440 1440 1440 1440 1440 1440
Gas per Ton.	11,850 11,000 11,150 11,150 11,200 11
Situation.	Farnworth Ditto Ditto Ditto Ditto Ditto Ditto Ditto Ditto Ditto Ditto Chesterfield St. Helens Alfreton Ditto
Name of Coal.	Roscoe & Lord, Mountain Mine Ditto One-foot Mine

		GAS ENGINEERS AND MANAGERS. 49
	Bul. Phur Per Cent.	0.118 0.881 0.865 0.8668 0.8668 0.8668 0.8668
	Gas puri- fied by One Cwt. Lime.	18,000 18
	Value of Gas per Ton of Coal in lbs. of Sperm.	511.38 528.7.28 528.7.38 528.7.3 528.7 52
	Value of One Cubic Foot in Grains of Sperm.	886. 886. 886. 886. 886. 886. 886. 886.
	Illum. Power.	14.888888888888888888888888888888888888
	Conden- sation by Bromine.	8
COALS.—continued.	Specific Gravity of Coal.	1.908 1.976 1.980 1.980 1.976 1.977 1.977 1.983
	Ash in Coke Per Cent.	00004440004400004000400000000000000000
	Coke Per Ton.	1468 1870 1870 1870 1870 1870 1870 1870 187
GAS C	Gas Per Ton,	9,750 9,750
,	Bituation.	Wigan St. Helens Ditto Ditto Barnsley Wigan Barnsley Ornaklirk Ditto Ditt
	Name of Coal.	Spring Colliery Smith coal Sk. Helens Colliery, Rushy Park. Ditto Ditto Ditto Swaley, Ras coal, tope Ditto Swale Colliery Co., Silistone. Syndall Hall, Arley. Tawd Vale Colliery Co., Rushy Park Ditto do. Rushy Park Ditto Ditto On Rushy Park Ditto On Rushy Park Ditto On Rushy Park Ditto On Crombouke. Ditto On Gas coal. Ditto On Gas coal. Ditto On Swale Colliery Warhall Colliery, Wall and Bench. Vactoria Colliery, Wall and Bench. Victoria Colliery, Wall and Bench. Victoria Colliery, Rushy Park Waterloo Main, Silkstone. Ditto Ditto On Silkstone Nuta. Soft coal. Ditto On Gas Coal. On Silkstone West Lancashire Coll. Co., gas coal. Ditto On Silkstone Ward Lancashire Coll. Co., gas coal. Ditto On Silkstone Ditto On Silkstone Ditto On Silkstone Ditto On Silkstone Ditto On Silkstone Ditto On Silkstone Ditto Ditto On Salkstone Ditto On Silkstone Ditto On Silkstone Ditto On Salkstone Ditto Ditto On Salkstone Ditto Ditto On Salkstone Ditto Ditto On Silkstone Ditto Ditto On Salkstone Ditto Ditto On Salkstone Ditto On Salkstone Ditto Ditto On Salkstone Ditto On Salkstone Ditto On Salkstone Ditto On Salkstone Ditto On Salkstone Ditto On Salkstone Ditto On Salkstone Ditto On Salkstone Ditto On Salkstone Ditto On Salkstone Ditto On Salkstone Ditto On Salkstone Ditto On Salkstone Ditto On Salkstone Ditto On Salkstone Ditto On Salkstone Ditto On Salkstone Ditto On Salkstone Salkstone Ditto On Salkstone Salkstone Ditto On Salkstone Salkstone Ditto On Salkstone Salkstone Salkstone Ditto On Salkstone Salkstone Ditto On Salkstone Salkstone Ditto On Salkstone Salkstone On Salkstone Salkstone On Salkstone On Salkstone Salkstone On Salkstone Salkstone On Salkstone Salkstone On Salkstone Salkstone On Salkstone On Salkstone Salkstone On Salkstone On Salkstone On Salkstone On Salkstone On Salkstone On Salkstone On Salkstone On Salkstone On Salkstone On Salkstone On Salkstone On S

NEWBIGGING'S HANDBOOK FOR

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	Sul- phur per Cent.	0.820 0.402 1.173		Sai- phur Cent	:::	0.909	0.239 :	0.727	98	<u></u> :88:			
	Gas puri- fied by One Cwt. Lime.	16,000		Gas puri- Gas puri- per Ton fied by of Coal One Cwt. In lbe. of Lime.	17,000 18,000 8,000	::	14,000	::		::			
	Value of Gas puri- igas puri- per Ton fied by of Coal One Cwt. In lbs. of Lime.	629.71 620.75 662.40 631.20 681.36 693.68 614.40			1483·21 911· 656·64	965·28 1017·57	1256·88 927·08	927. 9073:	1082.79	749.14			
	Value of One Cubic Foot in Grains of Sperm.	860° 867° 886°40 898°40 404°20 890°24 884°		Value of One Cubic Foot in Grains of Sperm.	701 · 52 497 · 487 · 76	368·40 547·92 497·	687·36 646·72	623·20 919·36	686.62				
	Illum. Power.	15 · 87 16 · 87 16 · 40 16 · 40 16 · 84 16 · 26			Illum. Power.	29.23 18.24 18.24	15.85 22.83	88 25 25	24 88 26 88 26 88	81 S	96 22 28 28		
	Ash in Specific Conden- Coke Gravity, sation of of by Cent. Coal. Bromine.	6.25 6.25 6.75 4.50 6.50		Conden- sation by Bromine.	90.25 9.52 6.50	6.25	16. 11.60	12.82 28.38	9.	} : <u>.</u>			
COALS.—continued.	Specific Gravity of Coal.	1.275 1.275 1.246 1.290 1.245 1.262 1.262	LŠ.	ērs.	ELS.	•	Ash in Specific C. Coke Gravity sper of Cent. Cannel. Br	1.184 1.264 1.812	1.274	1.176	1.277	1.81	1.988
	Ash in Coke per Cent.	1.87 1.79 1.79 5.90 6.80 6.80				Ash in Coke Per Cent.	60 4 6 8 6 6 8 6 6	86.98 80.88	8.95 9.95 9.95	88.93 8.93	6.525 8.91	. 4	
	Coke Per Ton.	1441 1449 1428 1436 1368 1368	CANNELS.	Coke Per Ton.		1248			188 188 188 188 188 188 188 188 188 188	88			
GAS C	Gas Per Ton.	10,300 11,840 11,200 11,200 10,650 12,200	75	G y Fi Hou	14,800 12,830 10,500	12,450 18,000	12.11 970 870	12,400 15,750	18,500	12,500			
	Bituation.	Prescot Wigan Ditto Ditto Ditto Ditto Leeds		Situation.	Wigan Ditto Ditto	North Wales Ditto	Manchester Wigan	Ditto Bathgate	St. Helens Leeds	Ditto Wigan			
	Name of Coal.	Wigan and Whiston, Ruahy Park. Wigan Coal and Iron Co., Arley. Ditto do. Lady Lane, Arley Ditto do. Hidlow, Arley Ditto do. Hidlow, Arley Winstanley Colliery Woodleford Coal		Name of Cannel.	Abram Coal Co., Wigan 4-feet cannel Alliance Coal Co., Wigan cannel . Ditto do. Scone cannel .	Bersham Coal Co., Bersham cannel. Ditto do. New Pit.	Bickershaw Coal Co. (4-feet) Blundell & Son, Wigan cannel	Ditto do. Pemberton cannel. Boghead, black variety.	Bournes & Robinson	Bower, T. & B., Woodleford cannel. Brancker & Co., Wigan cannel			

		GAS ENGINEERS AND MANAGERS.	4
	Bal. phur Per Cent.		:
	Gas puri- fied by One Cwt. Lifme.		13,000
	Value of Gas per Ton of Coal in lbs. of Sperm.	611. 988.66 1559.68 164.60 644.60 644.60 1089.7 1089.6 1089.7 1431.86 724.11 666.86 786.17 766.12 776.7 776.9 776.1 7776.1 7776.1 7776.1 7776.1 7776.1 7776.1 7776.1 7776.1 7776.1 7776.1 7776.1 7776.	.219
ļ	Value of One Cuble Foot in Grains of Sperm.	986.68 687.08 686.4	#03.68 89.30
	Illum. Power.	22,52,52,53,53,53,53,53,53,53,53,53,53,53,53,53,	78.91
	Conden- stion by Bromine.	26 - 26 - 26 - 26 - 26 - 26 - 26 - 26 -	36 26 26
CANNELS.—continued.	Specific Gravity of Coal.	1:978 1:978 1:978 1:988 1:288 1:288 1:288 1:288 1:188 1:214 1:214 1:272 1:288	1.276
	Ash in Coke Cent.	5 - 5 - 5 - 5 - 5 - 5 - 5 - 5 - 5 - 5 -	. 4
	Coke Per Ton.	1288 1340 1900 1900 1900 1900 1900 1900 1900 19	380
CANN	Ger Ton.	10,736 11,100 11,670 12,800 12,800 12,800 12,800 12,800 14,100 14,100 16,000 11,270 11,270 11,000 11	10,700
1	Situation.	Mold Mold Mold Ditto Sheffield Ditto Wigan Alfreton Mold Ditto Wigan	Ditto
	Name of Cannel.	ilow, D., de de de de de de de de de de de de de	Ditto do. semi-cannel

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		CANNELS.—continued.	SIS	contin	ned.	Conden		Value of	V	Value of
Name of Cannel.	Situation.	Gas per Ton.	Coke Per Ton.	Coke per Cent.	Gravity of Coal.	sation by Bromine,	Illum, Power,	Gree	Cubic Foot in Frains of Sperm.	Cubic per Ton fled by Foot in of Coal One Cwt. Sperm. Sperm.
Garswood Coal & Iron Co., C. F. Clark, Esq.	Wigan	10,620		6.87	1.292	2.00	22.00	528		
Ditto do. Glendon Iron-Works, Napperley.	Ditto	9,975	1170	19.47	1.384	07.9	22.06	629.44	24	-
Ditto Ditto Dunesdale.	Ditto	9,600		16.50	1.274	6.25	20.52	496.08	.08	.08 800
Haigh, John, and Sons, No. 1	Gildersome,	11,500		6.25	1.272	6.51	17.27	416	40	_
Ditto do, No.2	Ditto	10,800	1848	6.30	1.271	6.30	16.67	897-70	20	70 618
Talon cannel		14,200	1947	8.45	1.174	13.00	27.38	657	120	_
Hindley Field, Wigan 4-feet cannel.		12,800	1053	7.40	1.084	13.75	28.52	558	9	1027
Higson, J. & P., Dukinfield do.	Dukinfield	11,850	1276	8.65	1.978	9.20	24.	694		_
Ince Hall, Wigan cannel		12,780	1411	4.44	1.262	9.16	22.35	580		_
Ditto do.		12,825	1420	4.38	1.241	;	23.34	561.		_
Ditto	Ditto	11,550	1368	11.72	1.860	::	17.08	409 92		688.08
Lawton Colliery, Lawton cannel	Stoke-on-Trent	8,000	nil	4.88	1.978	8.65	16.50	583		609.
Lockwood, S.	Yorkshire	11,600		12.05	1.309	:	25.	.009		994.
Midland Coal Co.	Nottingham	11,425		18.30	1.984	9. nearly	_	426		695 . 30
Ditto do.	Ditto	13,260		9.80	1.206	11.0	_	653.28		1287-50
Mostyn cannel	Burton-on-Trent	12,400		28.27	1.206	01.0	28.96	695		1231 14
New South Wales cannel	Sheffeld	16,300	1886		1.184	5.15	38.43	922-82		2126.
Old Hall cannel	St. Helens	11,200		6.20	1.318	8.50	38	662		883.20
Pearson & Knowles, Wigan cannel .	Wigen	11,870	1416	4.87	1.562	11.60	22.78	546.72		927.08
Rocher's cannel	Ashton	11,800	1278	13.13	1.267		24.12	09.629	8	.22

		•	GA	B EN	GIN	eri	28 A	ND	MAI	NAGI	rs	•	47
	Sal- pbur per Cent.	176.	::	::	æ :	:	:	::8	15.64 26.68 26.68		::	1.184	
	Gas puri- fied by One Cwt. Lime.	:	18,000	::	::	::	:	::	:::	25			
	Value of Value of One One One Gas Cubo per Tool in of Coal Fred in in the of Sperm. Sperm.	.898	883 883	777.	712. 881.34 807.10	38	885.20	847.	710·11 1417·82		1188	719.	
	, 9	548	884. 493·44	628° 647°	511 · 20 549 · 50	.63	504.	459.60	282 282 283 383 383 383 383 383 383 383	F.E.	8	.99	 <u></u>
	Illum. Power.	89.88	16. 20.56	88 88	28 28 28 28 28 28	8 8 8 8	21.	19.18	18.08 17.08	90.78	27.50	19.	
	Ash in Specific Conden-Coke Gravity sation ber of by Conf. Bromine.	11.76	6.75 -925	9.5		9.6	÷ å	8.76	: 9:	Ġ	18.	81.0 81.0	
CANNELS.—continued.	Bpedflo Gravity of Coal.	1.968	1.884	1.255	1.286	1.178	1.286	983	1.986	1.064	1.279	1.280	
	Ash in Coke per Cent.	. 2	5.05 2.05 2.05 3.05 3.05	4.60	17·45 2.95	6.45	4.50	6.42	8. S. S.	4.80	. 6	8	
ELS.	Coke Per Ton.	1414	1416 1886	1180	1870 1800 1800	1088	1806	315	878	1400	1841	158	
CANN	Gas Ton.	11,126	11,850	10,800	9,750 10,600 78,750	12,600	11,600	121 186 186	11,500 12,600 18,600	11 580	12,600	11,100	
	Bituation.	Wigen	Farnworth Wigan		_	Wigan.	Ditto	St. Helens	Motherwell Newcastle-on-	Tyne	O C	Wornley, near Manchester.	-
	Mame of Cannel.	Rosco & Lord. Mountain Mine	cannel Boyal Colliery, Wigan cannel.	band of coal Scott Lane Colliery, Wigan cannel	Sheepbridge Coal and Iron Co. Shirland Coal Co., Shirland cannel.	Simpson & Co., Wigan 4-feet cannel	Smelturet, D. 11., & Co., Orbest seam,	Sutton Heath, cannel	Thomson, S., Ibstock cannel	Wigan Coal & Iron Company—	Curley cannel	• •	

CANNEL AND COAL NUTS AND SLACK OR DROSS.

Bequire high heats for carbonization. When the heat is not high they cake together in a mass, and at the end of the charge are drawn from the retort in a comparatively unspent condition. They cannot be used to advantage in iron retorts.

TABLE

Showing, by the Chlorine and Durability Test, the Comparative Value of Various Coals. (Dr. Fyfe.)

Coals.	Cubic Feet of Gas per Ton.	Condensa- tion by Chlorine in 100 parts:	Durability with Jet Flame, 5 inches, 1 ft, burns.	Value of Gas Accord- ing to Con- densation by Chlorine and to Durability.	Value of Coals ac- cording to Value and Quantity of Gas.
English caking	9,746	6.5	min. sec. 50 40	1.00	1.00
English parrot, average.	10,500	7.6	44 30	1.02	1.08
Marquis of Lothian's .	10,000	13.0	60 0	2.35	2.41
Lesmahago	10,176	17.5	70 0	3.72	3.87
Wemyss	10,000	19.5	75 0	4.44	4.55
Kirkness	9,620	20.75	80 18	5.06	4.99
Boghead	15,486	28.37	84 22	6.09	9.67

TABLE

Giving the Result of the Distillation for Gas and for Oil of One Ton of Newcastle Cannel Coal. (Gesner.)

Distilled for Gas, at 1000° to 1200°	Distilled for Oil, at 750° to 800°
Fahr.	· Fahr.
PRODUCTS.	· PRODUCTS.
Coal gas	Gas 1400 cub. ft. Crude oil 68 gals. Coke 1280 lbs.
PRODUCTS OF THE COAL TAR. Benzole 3 pints. Coal tar naphtha 3 gals. Heavy oil, naphthaline, &c. 9 gals.	PRODUCTS OF THE CRUDE OIL. Eupion 2 gals. Lamp oil 22½ gals. Heavy oil and paraffin . 24 gals.
Total 123 gals.	Total 481 gals.

WIGAN CANNEL AND COAL

Yield, on an average, per ton :-

Gas	24 sperm candles 1486 lbs	:	15 sperm candles 1517 lbs.
Tar	17 gallons		11 gallons.

NEWCASTLE COAL

	Yie	lds	, 0	n a	n av	7era	ge,	per ton:—
Gas .							٠.	9700 cubic feet.
Illumina	ting	p 0	W	er				15 sperm candles
Coke			•					1540 lbs.
								9 gallons.
Ammoni	iacal	lig	įuo	r				10 gallons.

AVERAGE YIELD OF BITUMINOUS COAL.

The average percentage yield, by weight, of good bituminous coal is as follows:—

_						er Cent.
Gas						18
Coke and breeze.						6 8
Tar						
Ammoniacal liquor	•	•	•	•	•	9
						100

TO DETERMINE THE SPECIFIC GRAVITY OF COAL.

Take a small piece of the coal, suspend it by means of a horsehair from the under side of the pan of a carefully adjusted balance (Fig. 1), and weigh it both in and out of water (fresh distilled); divide its weight in the air by the loss of weight in the water, and the quotient is the specific gravity.

EXAMPLE.

A piece of coal weighs, say 480 grains. Loss of weight when weighed in water . 898 ,,

Then $\frac{480}{898} = 1.206$ specific gravity of the coal compared with water as 1.000.



F16. 1.

Note.—Specific gravity is the relative weight of equal bulks of different substances; distilled water at 62° Fahr. being taken as the standard of comparison. At this temperature a cubic foot of water weighs 1000 ounces avoirdupois. Hence, the specific gravity of a body is also its weight in ounces avoirdupois per cubic foot; so that, knowing the specific gravity, the weight of any quantity of matter may be calculated by simple measurement. For example: In the instance just given, the specific gravity is shown to be 1.206; the weight of the coal per cubic foot is, therefore, 1206 ounces, or 75.4 lbs. avoirdupois.

TO FIND THE VALUE OF GAS IN GRAINS OF SPERM PER CUBIC FOOT FROM THE GIVEN ILLUMINATING POWER.

Rule.—Multiply 120 (the grains allowed per hour for the consumption of the standard sperm candle) by the illuminating power, and divide by 5 (consumption of gas in cubic feet per hour by the standard burner). The answer will be the value of the gas in grains of sperm per cubic foot.

Example.—What is the value of gas in grains of sperm per cubic foot, the illuminating power of which is 19.46 candles?

$$\frac{19.46 \times 120}{5}$$
 = 467 grains of sperm.—Answer.

TO FIND THE VALUE OF ANY COAL PER TON IN POUNDS OF SPERM, THE YIELD OF GAS AND ILLUMINATING POWER BEING KNOWN.

Rule 1.—Multiply the cubic feet produced per ton by the value of the gas in grains of sperm per cubic foot (ascertained by the previous rule), and divide by 7000 (the number of grains in 1 lb. avoirdupois). The answer will be the value of the coal in lbs. of sperm per ton.

EXAMPLE.—What is the value of a certain coal in lbs. of sperm per ton, whose yield of gas is 10,540 cubic feet, and illuminating power 19.68 standard sperm candles?

$$\frac{19.68 \times 120}{5} = 471.12$$
, value of the gas in grains of sperm per cubic ft.

Then
$$\frac{10,540 \times 471 \cdot 12}{7000} = 709.87$$
 lbs. of sperm per ton, value. Or by

RULE 2.—Divide the yield per ton by 5 (cubic feet of gas consumed per hour by standard burner), multiply by the ascertained illuminating power and by 120 (consumption of standard sperm candle per hour in grains); lastly, divide by 7000 (number of grains in 1 lb. avoirdupois). The answer will be the value of the coal in lbs. of sperm per ton.

Example.—What is the value of a certain coal in lbs. of sperm per ton, whose yield of gas is 10,540 cubic feet, and illuminating power 19.63 standard sperm candles? Then

 $\frac{10,540}{5} = \frac{2108 \times 19.68 \times 120}{7000} = 709.87 \text{ lbs. of sperm per ton, value.}$

TO ASCERTAIN THE RELATIVE VALUE OF DIFFERENT COALS AND CANNELS.

To ascertain the relative value per ton of different coals and cannels, attach approximate or actual market prices to the sperm pounds as ascertained above, and to the several residual products, cast up the various items, and compare them by the ordinary rule of proportion.

Example.—The two coals to be compared are—.

No. 1, yielding—	r		d.
10,600 c. ft. of gas per ton, 17½ candles value = 686 lbs.	~	о.	u.
sperm		16	
131 cwt. Coke			71
10 gals. Tar		1	
22 gals. Ammoniacal Liquor at 1d.	0	1	10
	£32		
	202		
No. 2, yielding—			
9700 c. ft. of gas per ton, 163 candles value = 557 lbs.	£	8.	a.
	07	17	۸
sperm		5	
9 gals. Tar at 1½d.		ŏ	
20 gals. Ammoniscal Liquor at 1d.	ŏ	ĭ	
	£28	5	
Е 2	_	_	_`

Assuming that No. 1 is 12s. 6d. per ton, the relative value of No. 2 will be found as follows:—
As £32 4s. 6d.: £28 5s. 5½d.: 12s. 6d.: 10s. 11½d. value per ton of No. 2.

TO FIND THE RELATION BETWEEN QUANTITY OF GAS PER TON AND ILLUMINATING POWER. (FARMER.)

If a coal yields a known volume of gas of a known illuminating value, to ascertain how much it will yield of another value :

RULE.—Multiply yield of gas by illuminating power, divide by the

required power, and the quotient is the quantity.

Example.—A coal yields 9600 cubic feet per ton of 16-candle gas; how much will it yield of 14 and 17 candle gas respectively? $9600 \times 16 = 153,600$. Then

$$\frac{153,600}{14}$$
 = 10,971 c. ft. and $\frac{153,600}{17}$ = 9085 c. ft.

The above presupposes that the period of distillation is extended or abridged, as the case may be. The rule, however, must not be assumed as absolutely correct, but only approximately so, and that only within a limited range.

WEIGHT OF COAL.

Anthracite, per cubic yard, solid . . . 2160 lbs. Bituminous ,, ,, . . . 2025 ,, Cannel ,, ,, . . . 2160 ,, Coal, stored in the usual way, per cubic yard 1400 ,,

ANNUAL CONSUMPTION OF COAL FOR GAS PURPOSES IN THE UNITED KINGDOM.

It is estimated that the present (1889) annual consumption of coal for the manufacture of illuminating gas in the United Kingdom is about 10,000,000 tons; about 2,000,000 tons (or 20 per cent.) of this quantity being cannel coal.

FOR ROUGHLY ESTIMATING THE QUANTITY OF COAL OR CANNEL REQUIRED TO PRODUCE A GIVEN QUANTITY OF GAS.

RULE.—Strike off the last four figures from the quantity of gas produced, and the figures remaining will represent the coal and cannel in tons.

Thus: 20 0,000 cubic feet = 20 tons.

This will be evident when it is remembered that a ton of coal or cannel produces about 10,000 cubic feet of gas. If the production rise to 11,000, or fall to 9000 per ton, one-tenth must be deducted from, or added to, the coal, as the case may be.

THE STORAGE OF COAL.

COAL AND CANNEL SHEDS.

In gas making it is economical to use the coal as fresh as possible from the pit, but to be prepared for emergencies, the covered storage room for coal and cannel should be of capacity sufficient to contain from six to eight weeks' stock of the material, reckoned on the basis of the heaviest day's consumption in winter. An exception to this rule may be made in the case of gas-works situated in the immediate vicinity of the coal-fields from whence the supply is derived. Under such circumstances, provision for two or three weeks' stock is ample.

In storing coal, 48 cubic feet of space per ton is required.

When coal is exposed to the weather, being stored in the open air without any protecting covering, it is not only liable to be wetted by rain on its outer surface, but it also absorbs and retains moisture

within its structural interstices.

The effect of this excess of moisture is to produce disintegration, reducing the size of the lumps, and converting them to a considerable extent into dust and culm. The exposure of the coal in the winter season in this climate is, of course, the most objectionable as regards disintegration. In hot climates the intense heat of the sun produces disintegration. The ill-effects of this absorption of moisture do not end there. Oxidation of the particles of the coal also ensues; and as this is only another name for eremacausis or slow-burning, the material is not only reduced in weight, but its gas-producing power, both as regards quantity and quality, and its coking qualities, are greatly impaired.

All kinds of coal suffer deterioration by exposure to the weather, both as regards their heating, coking, and gas-yielding qualities. The extent of this deterioration is from 20 to 50 per cent. within a brief period of time. An absolute loss of weight due to the evaporation or slow combustion of the more volatile constituents, is also experienced. This is particularly the case with bituminous or caking coal; cannel suffers next in degree; and anthracite the least. Varrentrapp found in one instance that coal which had been exposed for some years to the weather had diminished in weight to the extent of 38.03 per cent.

Wet or damp coal not only yields less gas, but gas of an inferior quality. The sulphur impurities given off from it are more, thus

augmenting the cost of purification; whilst some of the sulphur compounds—notably, bisulphide of carbon—are not removable, except by a greatly increased area of purification beyond what is to be found at most gas-works.

SPONTANEOUS IGNITION OF COAL.

Coal containing a large proportion of iron pyrites (bisulphide of iron), commonly called "brasses," when stored in a compact mass in a wet or humid state, is liable to spontaneous ignition. This is not an unusual occurrence in the experience of gas managers. The indications that combustion has commenced are a sensible rise in the temperature of the coal-store, a sickly odour, and a choking or smothering sensation on drawing breath.

There is this liability to spontaneous ignition in almost all bituminous coals of a friable nature. It is due to more than a single cause. It may arise from the condensation of oxygen within the pores of the carbonaceous particles, just as oily cotton waste will fire spontaneously in the same way by the rapid absorption of oxygen. According to Professor Abel and Dr. Percy, water or moisture does not accelerate, but rather retards spontaneous ignition under these circumstances.

The danger of firing is greatest with those coals which contain a large proportion of iron pyrites in the shape of nodules, or "brasses," as they are called, and which are stored in a mass in the wet condition. These "brasses" become oxidized by the atmospheric oxygen dissolved in the water with which the coal is saturated; and the heat thus

generated raises the coal to ignition point.

Notwithstanding a conflict of opinion on the subject, we believe that the best remedy for this is ventilation. Various expedients are resorted to for effecting this object, amongst which may be mentioned the insertion of perforated iron pipes amongst the coal, leaving the ends exposed; coarse wicker-work baskets, without bottoms, are used with good results; and ventilating-shafts of brick, or venetianed shafts of wood, both horizontal and vertical, have proved efficient. Unless the ventilation is thorough however, the admission of air will do more harm than good, as a sluggish current will not reduce the temperature, but rather tend to develop and increase it.

A thermometer let down through the pipes or shafts will indicate any rise of temperature, and iron rods thrust into the mass of coal, when withdrawn and touched by the hand, will answer the like

purpose.

When the pyrites are present to a serious extent, the coal should be hand-picked, either at the colliery or when discharging at the gasworks. It is only sheer necessity, however, that will justify the employment of coal of this character for gas-producing purposes.

THE GASES OCCLUDED IN COAL.

Besides the liability to spontaneous combustion or ignition, there is another strong reason why coal should not be stored in the open air, nor, indeed, under cover, for a longer time than is absolutely necessary. In all bituminous coals a constant chemical change is in progress by which gas is being liberated. This gas, though frequently several times the volume of the coal, is condensed within the solid substance, being occluded or enclosed therein, until by diffusion it escapes into the air, and to such extent the coal is depreciated for gas making. In warm weather and in hot climates, this deterioration proceeds more rapidly than in low temperatures.

Dr. Lyon Playfair and others in this country, and Dr. E. von Meyer in Germany, have investigated the subject; and the subjoined table by the latter shows the quantity and composition of the gas so occluded, obtained from freshly raised samples of coal submitted to him for

analysis.

The plan adopted was to place 100 grammes of the coal in hot deaërated water, which was then boiled as long as any gas continued to be given off, and the gas collected was analyzed by Bunsen's methods.

	Samples of Coal Submitted.											
No.	1.]	Low Main Seam,	Bewick Colliery,	Newcastle.				_				
	2.]	Maudlin Seam,	ditto	ditto.								
	8.]	Main Coal Seam.	Urpeth Colliery,									
		Five-fourth Sean		ditto .				80				
		Ditto	Wingate Grange	Colliery, D	urh	ım		74				
	6.]	Low Main Seam,		ditto .								
		Harvey Seam,		ditto .		•		148				
	8.		Emily Vil, Wood	house Close	Col	lier	y	25				
			•				•					

ANALYSIS. PERCENTAGE COMPOSITION OF THE GAS.

	oal bor			CO ₂	CH ₄ Marsh Gas.	0	N	Cubic Centimetres of Gas from 100 Grammes of Coal.		
No. 1	•	•		5.22	6.2	2.28	85 · 65	25.2		
2			.	8.54	26.54	2.95	61.97	80.7		
8				20.86		4.88	74.81	27.4		
4			.	16.21	Trace.	5.65	77.84	24 · 4		
5				0.84	85.80	Trace.	13.86	91.2		
6	_			1.12	84.04	0.19	14 62	238.0		
7		·		0.28	89.61	0.55	9.61	211.2		
8	Ċ	:	. 1	5.81	50.01	0.68	44.05	84.0		

¹ cubic centimètre = 610.28 cubic inches. 1 gramme = 0.0022 lb. avoirdupois, 100 = 0.22 lb.

TESTING COAL FOR ITS PRODUCING QUALITIES.

It is almost impossible to judge from the appearance of a coal whether its gas and coke yielding qualities are good, bad, or indifferent. So far as outward indications go, nothing is so deceptive to the inexperienced in such matters; and even to those who have had large practice in coal-testing, it is very difficult to forecast with any certainty

the result of a trial of any particular sample.

Some of the poorest coals and cannels have a fatty unctuous appearance, suggestive of richness in gaseous properties. Again, the most valuable cannels and shales, yielding gas in extraordinary abundance, have a dull earthy cast, which might readily be taken as indicating poverty of composition and yield. The rich Boghead (Scotland), Sydney (New South Wales), and Cloverport (Kentucky) cannels or shales are striking examples of this latter kind. On the other hand, this does not hold good of the Brazilian shales or "Turba." have a dull clayey appearance, and are very indifferent both in the yield and in the illuminating power of their gas. The importance of being able to test samples of coal and cannel, or of having them tested by a specialist in whom reliance can be placed, before entering into a contract for the material in bulk, is therefore obvious.

A test may be made either on a working scale, or in the experimental apparatus in the gas manager's laboratory. In the former case several tons of the material have to be used; and the trial of a single sample is a formidable and tedious process, extending over many days, until the old gas in the apparatus and holder has been replaced by the new. It is obviously impossible to test a variety of samples in this manner within a reasonable period. Besides, such a method of testing is not always satisfactory. The manager has to take a good deal for granted; he is largely dependent on subordinates for the attention and care that ought to be exercised, because his constant personal supervision throughout the time occupied by the test is out of the

question.

The experimental test is to be preferred for many reasons. The small apparatus is more under the command of the operator. Full justice is done to the material. The best results it is possible to obtain are secured. Time is economized in making the tests, because a number of samples can be tried in the course of, say, ten or fourteen

It may be urged against the experimental, or laboratory test, that, in practical working, equal results are unattainable. If this be the fact, it only proves that either the practical working is at fault to the extent of the difference in result, or that the bulk of the material is not equal to the sample tested. Assuming, however, that the sample is a fair average of the whole, whatever the deficiencies of practical working may be, the coal at least should not be depreciated below its intrinsic value through defective heats and other faulty methods of carbonization, and although the actual every-day working of the material may afterwards fall short of the results obtained in the trial apparatus, these latter are a standard at which to aim. As a general rule, the difference between the results of actual use and the experimental results, with efficient plant and careful supervision, will not exceed 5 to 7 per cent. in favour of the experimental test.

To argue that the quality of a coal should be judged and determined solely by the results yielded in actual working, is just about as reasonable as to say that the illuminating power of gas should be decided by the methods of consumption through possibly defective fittings, and some of the burners largely in use by consumers. Whether coal or gas, the means best calculated to develop its intrinsic qualities should

be adopted.

In the apparatus described and shown (Fig. 2), the charge to be used is the 1000th part of a ton—viz., 2.24, say, 21 lbs.

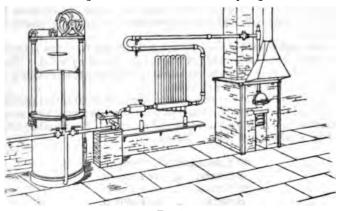


Fig. 2.

Description.

RETORT.—Cast iron; D-shaped; 5 in. wide, 41 in. high inside; 2 ft. 3 in. long outside; ASCENSION-PIPE.—2 in. wrought tube.

Condensed.—12 vertical 1½ in. wrought tubes, each 3 ft. 6 in. long.

Washer.—1 ft. long, 6 in. wide, 6 in. deep.

Purifier.—1 ft. 2 in. square, 12 in. deep, with 2 trays of lime.

Gabrolder.—Capacity 12 cubic feet, with graduated scale attached.

Care should be taken to obtain a fair average sample of the coal to be operated upon. For that purpose at least half a cwt. of the material should be broken up into small pieces and thoroughly intermixed; and from this three several charges are to be taken without selection.

The retort should be got up to, and maintained throughout the charge, at a bright red heat. If from any cause the temperature is much reduced, the test will not be satisfactory. This is especially the case in testing cannel and the rich shales. The time required to work off the charge of 2½ lbs. will range from 40 to 60 minutes, according to the character of the coal.

The illuminating power of the gas given out from each charge should be ascertained by the Bunsen photometer; no other being sufficiently trustworthy for that purpose. The average of the three tests is then taken, both for yield of gas and coke, and for the illuminating power of the gas, and this fairly represents the capabilities of

the coal.

The further conditions to be observed are that the holder be entirely emptied of air or of the previous charge of gas; and that the condenser be drained of its contents. The test charge may be continued until the whole of the gas is expelled, or otherwise, depending on circumstances. In comparing two coals, an equal production from both may be obtained, and the comparative illuminating power then ascertained.

The coke and breeze should be carefully drawn from the retort into a water-tight receptacle made of sheet iron closed by a lid. This is then placed in a bucket or other vessel of cold water, and, when suffi-

ciently cooled, the coke is weighed.

For ascertaining the quantity of tar and ammoniacal liquor produced, drain the yield of the three charges from the condenser and washer, and measure this in a graduated liquid measure. The number of fluid minims in a gallon is 76,800. Thus—

60 fluid minims = 1 dram. 8 drams. . = 1 ounce. 20 ounces . = 1 pint. 8 pints . . = 1 gallon.

Then-

lbs. lbs. per ton.

As 6.75 (The weight: 2240:: The number of: The total number of the three charges of coal.)

The total number of: The total number of minims of tar and liquor obtained.

And this ÷ 76,800 gives the gallons of tar and liquor produced per ton.

RETORT HOUSE.

The house may be adapted for either a single or double stack of retorts, and may be of the ground-floor or stage-floor type of erection, according to circumstances. In ground-floor houses provision should, if possible, be made for the application of generator furnaces by taking the foundation of the retort stack to a depth of 9 ft. 6 in. below the floor-line, and making an underground passage, at least 7 feet wide, in front of the stack.

Dimensions.

For a single stack of retorts-Width inside, 80 feet. Height to wall plate, 20 feet. For a double stack of retorts-Width inside, 60 feet. Height to wall plate, 26 feet.

Wrought-iron trussed roof, slated, tiled, or covered with corrugated

galvanized-iron sheets, with ventilator.

The ventilator should extend from one end of the building to the other, and be of ample capacity. Suitable openings should be left in the walls, above the height of the retort-bench, for the admission of air and light. Ventilating tubes or towers may be used alone or in connection with the louvre ventilator. They are efficient, and present a good appearance.

Corrugated-iron sheeting, being lighter than slates or tiles, admits of the principals and purlins being placed wider apart, so reducing their number. The first cost of a roof of this description is less; it is less affected by wind; but its durability is inferior to a slated roof.

The sheets should not be thinner than No. 20 gauge.

The clear space in front of a retort stack should not be less than 18 feet. When it is intended to employ machinery for charging and

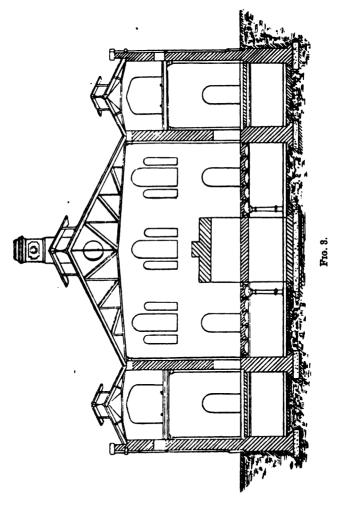
drawing the retorts, 22 feet may be allowed.

About 8 feet of the width of the floor, immediately in front of the stack, may be paved with fire-bricks set on edge; the remainder of the floor flagged with 4-inch flags. Blue Staffordshire bricks or tiles, 4 inches thick, make an excellent paying for a retort-housefloor; and, when these are used, the fire-bricks in front may be dispensed with.

A slight inclination—say, 6 inches in the whole width—towards the stack should be given to the floor. This allows the waste water from the slaked coke to run into the ash-pans, and is also handier for the

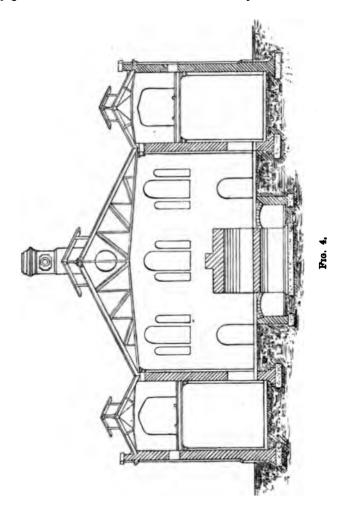
stokers in charging.

A stage-floor retort-house, Fig. 8, costs in erection from 50 to 75 per cent. more than a ground-floor house, Fig. 4, (dependent on



the character of the site and subsoil); but it can be worked with more economy, and the advantages it offers for the removal of the

coke, the application of generator furnaces, and in other ways, are very great. In all cases where the site naturally favours this form of



construction, it should be adopted. The stage-floor is usually formed of brick or concrete arches, or cast-iron plates, laid on girders having

their ends built into the wall of the house and the division piers of the retort-stack foundation, and supported also near to this latter by cast-iron columns.

THE RETORT STACK.

This necessarily varies in size and mode of construction according to the number of retorts, their dimensions, and arrangement in the settings. The following details will be found adequate for the erection of a stack with benches of seven large retorts of any shape, and either single or throughs, set as shown in Fig. 5.

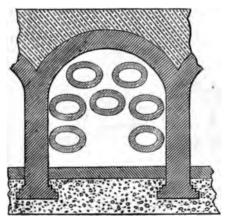


Fig. 5.

The ovens are 8 ft. 6 in. wide, 8 feet high from floor-line, and 20 feet through, inside measure.

Height to top of bench, 10 ft. 8 in.

Excavation for bench, 3 feet deep. For generator furnaces, 9 ft. 6 in. deep.

Place therein bed of hydraulic lime or Portland cement concrete, 14 inches thick.

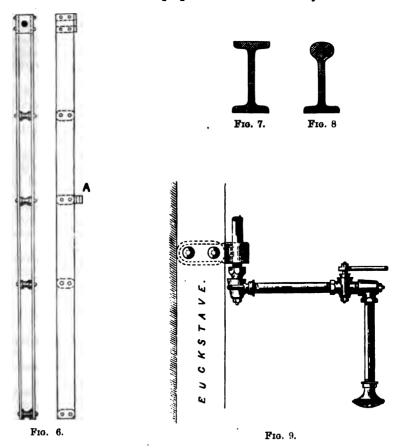
Upon this build the brick footings of the division walls of ovens, of good hard common bricks, set in lime mortar.

When these are built, fill up between with a further layer of concrete, 18 inches thick.

Division walls of ovens above footings, 18 inches thick, built of best fire-clay bricks, set in fine, well-tempered fire-clay.

Floor of ovens paved two courses on edge with fire-bricks set in fire-clay.

Arched roof of ovens, 14 inches thick, formed of three rings of fire-bricks moulded to the proper radius set in fire-clay.



Two flue-holes in crown of arch, 12 inches square, communicating with main flue on stack. Damper tiles to be provided for these, 27 inches long, 16 inches wide, 8 inches thick.

End or buttress walls of stack, 3 ft. 4½ in. thick, of common bricks, built in with the fire-brick work of stack, and faced with fire-bricks

laid in good lime mortar.

The whole of top of stack haunched up five courses above the top of the arches, so as to make the total height of 10 ft. 3 in. from floorline, of good common bricks faced with fire-bricks, laid solid, with close joints, in good lime mortar. Finish with cornice or coping as desired.

Double main flue on the stack, built of fire-bricks, set in fire-clay, and continued to the opening provided in the chimney. Dimensions of each flue, not less than 30 inches deep, 15 inches wide, inside measure. Outside walls and division wall, 9 inches thick, covered

with fire-clay tiles 2 ft. 41 in. wide, 4 inches thick.

Buckstaves of wrought iron, either rolled girder (Fig. 7) or railiron (Fig. 8), or, what is still better, formed of two flat-iron bars 6 inches wide, and 1 inch thick, with five cast-iron distance pieces between (the upper one being square in form), through which the

plates are riveted together with 3-inch rivets (Fig. 6).

The boss, A, with hole therein, is intended to receive the wroughtiron pipe, 1 inch diameter, leading from the 3-inch water main on the top of the retort stack. To the end of this pipe a brass swivel is attached; and from this again a piece of 1-inch steam-tubing, 11 inches long, projects, having a brass swivel cock at its end. A tube 3 of an inch diameter is screwed thereto, and terminates in a 4-inch brass rose jet, through which water is discharged for slaking the coke as it is drawn from the retorts (Fig. 9).

Tie rods of 1½-inch square bar, or 2-inch round iron; screwed 6 inches at each end, and furnished with strong hexagon nuts and

washers.

RETORTS.

Materials of which Retorts are made.

The materials of which retorts for the distillation or carbonization of coal are made are fire-clay and iron exclusively.

In the early days of gas lighting, and for many years after, cast-

iron retorts only were used.

The fact of the iron retorts not being capable of standing a heat sufficiently high for the distillation of coal in the most economical manner, and their liability to rapid oxidation, and even fusion, in the furnace, operated to cause the adoption of clay in the manufacture of retorts.

The clay retorts, in the face of much prejudice and opposition, gradually advanced in popularity as their merits became known, until at the present time, their use is all but general.

Single clay retorts are burnt better and more uniformly when the ends are left open in the kiln. The backs are easily jointed in setting; care being taken to butt them close up against the mid wall.

Clay retorts when once heated do not bear "letting down" and "standing off" like those made of cast-iron, owing to their liability to crack when cooling; and for this reason a setting of one or two iron retorts is useful in very small works during the minimum gas production in the summer season.

Different Forms of Retorts.

Retorts are made of three different shapes in cross section-viz., round, oval, and D-shaped. Formerly, rectangular or square, earshaped, and kidney-shaped retorts were made; but these are now entirely discarded.

The round, by reason of its shape, is the strongest and most durable;

but it is not equal to the oval and D as a carbonizer.

The oval ranks next to the round in strength and durability, and

exceeds it in carbonizing capabilities.

The D is the shape most commonly in use, and is considered by many gas managers to be equal to the oval as regards its power of carbonizing.

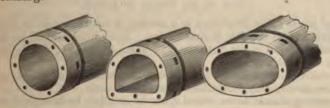


Fig. 10.

After a lengthened experience in the use of both round, oval, and D-shaped retorts, the writer prefers the oval, as being the most efficient and economical, producing during its lifetime the greatest quantity of

Dimensions of Clay Retorts.

Clay retorts are usually made 23 to 3 inches thick; the flange to which the mouthpiece is bolted being 4 inches thick and 8 inches broad, the neck tapering down to the thickness of the body.

The following are useful and convenient sizes of clay retorts:-

Bound . . 15 in. díam. Oval . 21 × 15 in. ,,

Inside measure, and 9 ft. 4 in. long outside. D-shaped, 18 × 15 in. ,,

The weight of a clay retort of the above sizes is from 14 to 16 cwt.

For very small works the following sizes are more suitable:

Round . . 14 in. diam.

Oval . . 18 × 12 in. ,,

D-shaped, 16 × 14 in. ,,

"Through" Retorts.

"Through" or double clay retorts, with a mouthpiece at each end, are made 18 to 20 feet long, being jointed together in three or four

pieces.

The advantages gained in using this kind of retort are important. The accumulation of carbon is less, owing to the absence of backs. The current of air which is drawn through their interior every time they are charged tends to loosen any carbon deposit that takes place. More heating surface for carbonization is obtained without additional expense, and that in the hottest part of the oven. They are also drawn with greater facility.

As they require to be drawn and charged at both mouthpieces simultaneously, they cannot conveniently be worked in establishments where the stokers are fewer than six in number. The scoop is gene-

rally used in charging these retorts. (See Fig. 21.)

Hints on the Setting of Retorts.

The joints of the brickwork in a setting of retorts should be as close and fine as it is possible to make them. Each brick should be dipped in water, placed in its position, and then gently, but firmly bedded home with the hammer.

A cutting heat from the furnace can be prevented, or greatly modi-

fied, by having ample nostrils in the furnace arch.

A setting should never, when it can be avoided, be brought into use immediately on completion, as the application of strong heat to the damp clay is liable to crack the joints of the brickwork, and so hasten its destruction.

The setting ought to be allowed to stand at least fourteen days, in order that it may be gradually and thoroughly dried and hardened.

Dimensions for a setting of three large sized clay retorts, 8 ft. 6 in. long:—

Width of oven, 5 ft. 2 in.; height, 6 ft. 3 in.; depth, 8 ft. 7 in.

Width of furnace at grate bars, 9 in.

Width of furnace at springing of arch, 16 in.

Length of furnace, 30 in.

Height from floor-level to underneath the flanges of the two bottom retorts, 2 ft. 3 in.

Number of grate bars, two; 30 in. long each, made of 2 in. square bar-iron.

Dimensions for a setting of five large sized clay retorts, 9 ft. 4 in.

Width of oven, 8 ft.; height, 7 ft. 6 in; depth, 9 ft. 5 in.

Width of furnace at grate bars, 10 in.

Width of furnace at springing of arch underneath the middle retort, 18 in.

Length of furnace, 80 in.

Height from floor-line to underneath the flanges of the bottom retorts, 2 ft. 8 in.

Number of grate bars, two; 30 in. long each, made of 2 in. square bar-iron.

Dimensions for a setting of seven large sized clay retorts, 9 ft. 4 in.

Width of oven, 8 ft. 6 in.; height, 8 ft.; depth, 9 ft. 5 in.

Width of furnace at grate bars, 12 in.

Width of furnace at springing of arch, 20 in.

Length of furnace, 36 in.

Height from floor-line to underneath flanges of two bottom retorts 16 in.

Number of grate bars, three; 86 in. long each, made of 2 in. square bar-iron.

To prevent radiation, the front wall of the oven should be a brick and a half, or 14 inches thick. The division walls between the ovens, two bricks, or 18 inches thick. The back wall when the retorts are not "throughs," a brick and a half, or 14 inches thick.

Quantity of Brickwork in Retort Settings.

The retorts in a setting should be firmly supported by transverse walls, so that they may satisfactorily bear the wear and tear of working during the time they are expected to last. It is an error to suppose that the brickwork causes a diminution in the heat. Take the case of two benches of retorts set: the one with as much brickwork as is required for proper support without obstructing the draught, or unnecessarily covering the retort surfaces; and the other having the least possible quantity of brickwork, supporting (say, for example) the retorts only at their extremities. In getting these benches in action for the first time, there can be no doubt the latter would be the first to attain the desired temperature; but although the former would require a little longer time, and the expenditure of more fuel at first, the superior regularity of its action over the other in distilling the gas firm coal will scarcely be questioned.

No doubt the thinner the retorts themselves, compatible with strength, the better, so that the heat may the more readily pass to their interior. But the circumstances attending the retort as the

vessel containing the material for distillation are not to be confounded with those appertaining to the adjacent brickwork. This, of course, need not be more than is reasonable; but it is better to err on the side of excess than too little.

Clay retorts are best 2\frac{3}{4} to 3 inches in thickness, according as they are made by machine or by hand; and the chief point to be observed in setting them, is to let the heat have free scope for circulating throughout the oven. With this object in mind, there should be no mistaken contraction of the nostrils leading out of the furnace. It is here where the evil in some settings exists, obstructing the passage of the heat as it is generated, producing cutting draughts, and hastening the destruction of the furnace bag.

Clay retorts, 9 ft. 4 in. long, are adequately supported by four transverse supports, in addition to the back ledge and the front wall, and only one of these four need be 9 inches thick. With a setting of this description, having ample space left for the exit of the heat from the furnace into the oven, and through the flues, the best results, both as

regards heating and economy of fuel, are obtained.

" Gaiting " Retorts.

On putting a bench or oven into action, the heat should be applied gently at first, the damper being gradually opened a little more each day, until the proper temperature is attained.

When the retorts have reached a dull red heat, a light charge of coal thrown into them will assist the development of the required temperature, as well as tend to preserve them in good condition.

By carefully attending to these points, the cracking of clay retorts

on first "gaiting" may be entirely avoided.

Furnace Ash Pan.

Ash pan of wrought plate-iron, 5-16ths inch, or cast-iron, 7-16ths inch thick. For a setting of seven large retorts, the length over all is 5 feet, or 4 feet not including the mouth part; 12 inches wide, and 10 inches deep, outside. (Fig. 11.)



Fig. 11.

The pan should always be kept charged with water raised to boiling point by the glowing coke. The water gives off steam in considerable volume; and this, rising underneath and between the furnace bars, contributes to the durability of these by keeping them in a state of comparative coolness. In its passage through the hot coke, the

steam is decomposed into its constituent gases, the hydrogen adding to the furnace fuel, and the oxygen promoting combustion. A tidy fire about, with the ash-pans charged with water, and reflecting the bright fire between the bars, is one of the indications of good stoking.

Duration of Clay Retorts.

The duration of clay retorts, of course, greatly depends on the setting. When the lower retorts in an oven are properly and continuously protected by seating tiles or brick arches from the direct action of the furnace, the setting will last from three to four years; otherwise—and this is nearer their average life—they will be burnt out in 15 to 18 months.

In moderate sized and in large works, each single retort should be of sufficient capacity to hold a charge of from $2\frac{1}{2}$ to 8 cwt. of coal. And if Newcastle, or other caking coal of fair quality, is used, with five or six hours' charges, the yield of gas per mouthpiece should be at the rate of 5500 to 6500 cubic feet per diem of 24 hours.

Now, 18 months' continuous production, at the average rate of, say, 5500 cubic feet per mouthpiece per day of 24 hours, is equal to a total production of about 8,000,000 cubic feet of gas.

For clay retorts the heat generally ranges from 2010° Fahr. (orange)

a little upwards.

Usual Number of Retorts in a Bed.

In average sized works, settings of five, six, seven, and eight retorts are usually adopted. In some of the large metropolitan and provincial works, as many as ten are placed together in one bed, with an elevated travelling stage in front, from which the higher retorts are charged and drawn.

Flues and Draught.

For a double stack, containing ten or twelve ovens or benches on each side, the main flue should also be double, and the internal dimensions of each division not less than 30 inches in depth by 15 inches in width. For even a lesser number of ovens, the size of the flue should not vary greatly from the above.

An insufficient draught, whilst it invariably results in diminished heats, causes a waste of fuel, from the consequent incomplete combustion in the furnace, and the usual hard firing that accompanies it. The flame which is occasionally seen at the top of a retort-house chimney is significant of this defect. The flame is produced by the unconsumed carbonic oxide uniting with its due proportion of oxygen on coming in contact with the atmosphere, and by combustion being converted into carbonic acid. When the proper quantity of air is supplied to the furnace, the carbonic oxide produced is there converted

into carbonic acid, and the heat thus generated is utilized for the

distillation of the coal contained in the retorts.

An excessive draught through the ovens is to be avoided, as well as an obstructed one. If too much air is drawn in between the grate bars, its effect is to reduce the heat, as well as to cause the consumption of an excess of fuel. Hence the importance of being able to control the draught by means of a damper placed at the entrance of the cross flue into the main flue on the bench.

According to the experiments of Dulong,

1 lb. of hydrogen, burning to water, yields 62,535 units of heat.

1 lb. of carbon, burning to carbonic acid, yields 12,906 ditto.
1 lb. of carbon, burning to carbonic oxide, yields 2495 ditto.
1 lb. of carbonic oxide, burning to carbonic acid, yields 4478 ditto.

Note—The English standard unit of heat is the quantity of heat necessary to raise the temperature of a pound avoirdupois of water 1° Fahr. The French calorie is the quantity of heat required to raise 1 kilo. (2.2 lbs. avoirdupois) of water 1° centigrade.

As a rule, when firing with coke, cleaning off the fire bars once in 12 hours is sufficient. Too frequent cleaning entails a waste of coke,

besides reducing the heat of the oven.

Instead of the tall chimney-stalk at the end of the retort-house, it has become the custom to erect chimneys or shafts of less altitude immediately over the bench, or between the benches, rising a few feet above the roof, and serving for four or more double ovens on each side. These are found to produce a sufficient draught, they are more uniform and regular in their action, and their cost is necessarily less. But as they deliver the products of combustion into the atmosphere at a low level, their use should be restricted to neighbourhoods where the nuisance is unobjectionable.

When the room can be spared, it is best to erect the chimney between, and apart from, the retort-benches; so that, when the latter need to be taken down and rebuilt, the chimney, being a more permanent structure,

remains undisturbed.

In some works each bench is supplied with a small shaft for its own use. This is scarcely necessary, though Mr. Valon has found the arrangement useful in the facility it affords for controlling the draught

where generator furnaces are used.

In many American gas-works the main flue and chimney are dispensed with altogether; the opening in the crown of the bench being found sufficient, it is said, to afford the requisite draught. Even assuming the draught to be ample for ensuring perfect heating and carbonization (which may be doubted), the objections to allowing the hot fumes to escape into the retort-house underneath the roof, are sufficiently obvious to cause the practice to be condemned.

RULE for size of retort-house chimneys under 70 feet in height: 1\frac{1}{2} square inches of area for each lineal foot of retort, or, say, 15 inches per mouthpiece.

EXAMPLE.—Required the internal sectional area of a chimney shaft serving twelve double benches of seven retorts, or fourteen mouthpieces, each (six benches on each side of chimney); retorts 20 feet through, total, 168 mouthpieces. Then

$$168 \times 15 = \frac{2520}{144} = 17.5$$
 square feet area.

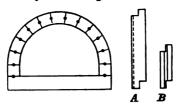
Cost of Ovens and Settings.

The cost of a double retort-stack, with benches or ovens to contain settings of five, six, or seven clay retorts (whether single or double), including hydraulic main, stand-pipes, and all other ironwork, retorts, brickwork, and labour, amounts (at present prices) to from £20 to £26 per mouthpiece.

The cost of renewing a bench of five, six, or seven clay retorts is £7 10s. to £9 per mouthpiece; a bench of three clay retorts, about £6 10s. per mouthpiece.

Fire-brick Retorts.

Retorts made of fire-bricks and tiles, rebated or grooved together and jointed with fire-clay, are in use; but their general economy as regards the percentage of fuel required for heating, is not considered equal to that of the ordinary clay retorts. In the matter of durability, however, brick retorts possess a clear advantage, their life being three to four times that of the other; and though their first cost is more, this is compensated for by the saving in wear and tear. Fig. 12 is a



F16. 19.

section of a brick retort. A is the bottom tile, 18 inches long by 8½ inches thick, and B, one of the bricks, 9 inches by 3½ inches.

Large retorts, 40 to 50 inches wide, are objectionable for many reasons: A large area is exposed to the cold air every time the charge is drawn, and the time occupied is necessarily considerable. Again, there is a tendency to allow carbon to accumulate in such retorts, because in the ample space the inconvenience of the presence of a

thick body of carbon is not felt by the men in drawing and charging. If the required temperature, however, is kept up under these circumstances, it must be at an excessive expenditure of fuel and labour. The greater depth of the coal, and the constant inequality of carbonization between the inner and outer portions of the charge, is also a serious drawback to their use.

Cast-Iron Retorts.

Cast-iron retorts are now only employed in very small works, where the gas making is intermittent; here they are useful, as they bear letting down frequently without suffering damage. As carbonizers they are not economical, because the heat which they will stand is not high enough to produce the best results in the yield of gas from the coal. They are usually made 1\frac{3}{8} inch thick, with an ordinary flange to which the mouthpiece is attached.

The round, 15 inches diameter, and D-shaped, 15 × 13 inches, are the handiest, and 7 ft. 6 in. is a convenient length. Their weight



Frg. 13.

is 16 to 18 cwt. Fraser's ribbed retort (Fig. 13) is an improvement on the ordinary form. In setting iron retorts a space of about 3 inches should be left in the rear, to allow for the expansion of the metal, and prevent their being forced out beyond the front wall, with the possible breakage of the ascension pipes.

Fire-clay tiles are invariably used to protect iron retorts from the

direct action of the furnace heat.

Oxidation proceeds rapidly on the outer surface of iron retorts, and the scale should be frequently removed, otherwise the proper temperature will not be maintained. For facility in doing this, sight holes should be left in convenient positions in the front wall of the bench.

Iron retorts should always be scurfed before being let down, otherwise the unequal contraction of the incrusted carbon and the metal of the retort in cooling might cause fracture in the latter.

The duration of an iron retort is equal to the production of about

700,000 to 800,000 cubic feet of gas.

The best heat for iron retorts is that ranging from 1650° Fahr. (cherry red) to 1830° Fahr. (bright cherry red). Any temperature beyond this is apt to burn or soften, and so cause distortion of the retort.

Combined Settings of Clay and Iron.

In some works, combined settings of clay and iron retorts have been used, the latter being heated by the surplus heat from the former. The benefits arising from their adoption are questionable.

THE SLAKING OR QUENCHING OF HOT COKE.

In the slaking or quenching of hot coke, water is a necessity. It is true that if the coke is drawn from the retorts into iron barrows, and a close cover placed over it, the confined gases, in the absence of atmospheric oxygen, will gradually arrest combustion in the mass; and this method of dealing with the coke is sometimes adopted with a view to abating the nuisance of the escape of steam charged with sulphurous vapours from the retort-house, and to preserve the coke for sale in a dry and bright condition. Where the production of coke is great, however, as in the case of large works, this is an inconvenient, if not impossible, method of dealing with the material.

The quantity of water absorbed by the coke when it is slaked in the ordinary way is comparatively small, not exceeding, on the average, 15 per cent. of the weight of coke in the first instance; and the bulk of this evaporates when the coke is deposited outside the retort-house in the open air—about 8 per cent. of moisture being

permanently retained.

FUEL FOR CARBONIZING.

Coke.

In moderate sized works, skilfully conducted, about 3.44 cwt. of coke, or 25 per cent. of the production (say, 18½ cwt.) of coke per ton from Newcastle and other high-class bituminous coals, is used as fuel to carbonize one ton of coal.

In large works, under the most favourable conditions, and with the ablest management, the consumption of coke for heating the ovens may be reduced as low as 18 to 20 per cent. of the production.

In small works, one-third the production of coke is nearer the aver-

age consumption.

For the heating of brick retorts, owing to their greater thickness, 10 to 15 per cent. more fuel is used than is required for clay retorts.

Radiation from the bench is reduced, and fuel economized to an extent greater than might be supposed, by temporarily bricking up the furnace doors and the mouths of all retorts in beds not in use in proximity to others in action.

Tar as Fuel.

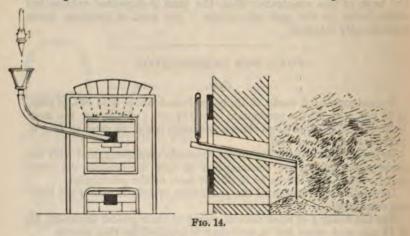
Where tar is unmarketable, or but of low value, and there is a ready sale for coke, the former should be employed in heating the retort ovens.

Its application is exceedingly simple. When applied to an ordinary furnace, the ash pan is first filled up with breeze; the door is then

removed and the door space bricked up, leaving two holes, one above the other, about 4 by 3 inches. The tar is supplied through the top hole, the bottom hole being for the admission of air, and to allow of the fire being stirred when required. A piece of 2-inch angle-iron, or a grooved fire-clay slab, or other convenient channel, is inserted into the furnace through the top hole, and down this the tar is made to flow in a stream about 3-16ths of an inch thick.

The tar can be taken direct from the hydraulic main, in the bottom of which a 1-inch wrought iron ferrule, having a stop-cock attached, is screwed. A ½-inch reducing coupling is then put on, and this size of pipe brought down to the side of the oven, where the tar is supplied to the trough through a nozzle of the proper dimensions. (See Fig. 14.)

As the hydraulic main will not supply all the tar necessary, a pipe should also be brought from a tank or cistern erected in some convenient place outside the retort-house. If this tank is placed inside



the retort-house, the dust arising from the coal mixes with the tar and hinders its flow. Into this tank a supply of tar should be pumped from the tar well as required.

The great objection to the use of tar as fuel, as above applied, is that the intense heat which is generated at the point of combustion, soon destroys the arch or tiles underneath the middle retort, breaking the latter down.

As this retort, in the ordinary setting of fives and sevens, is the one usually first burnt out, it is advisable to restrict the use of tar to those benches that have been at work for a length of time, and in which the middle retort is either much burnt or already destroyed.

To obviate the above-mentioned drawbacks, Mr. George Anderson has invented a furnace specially adapted for the consumption of tar as fuel, which admirably answers the purpose intended.

About 50 gallons of tar used as fuel will carbonize 2½ tons of bituminous coal, or a mixture of bituminous coal and cannel, in 24 hours.

At this rate about 6 gallons of tar are equal to a sack (8 bushels) of coke.

Numerous other expedients for firing by means of tar have been put forward, but the above has the merit of efficiency with cheapness and extreme simplicity. In the event of a deficiency in the supply of tar, this furnace is readily reconverted for coke firing.

GENERATOR FURNACES AND REGENERATION.

The use of gaseous fuel for heating retorts may be said to have emerged from the experimental stage. On the Continent more has been done in this direction than in this country, stimulated, perhaps, by the comparatively higher value of fuel there. Mr. Webber, Mr. G. E. Stevenson, Mr. Valon, Mr. Foulis, and others have done much to spread a knowledge of the value of these furnaces amongst the gas engineers of this country.

From a scientific point of view, generator furnaces have everything to recommend them. The saving in fuel by their adoption is variously estimated at from 10 to 80 per cent. on the best results obtained by direct coke firing. But they offer other marked advantages. "Clinkering" is avoided, and consequently wear and tear of settings is reduced; the heats are higher and steadier, and, being more easily regulated, they save manual labour; the charges in the retorts are carbonized more rapidly, and thus the production of gas per mouthpiece is increased, and retort-house space economized.

In the generator furnace, the solid fuel is converted into carbonic oxide gas, and if the regenerative system is not super-added, the gas produced is mixed with the entering air whilst the latter is at the ordinary, or at but a slightly higher temperature, unassisted by the waste heat from the flue. In some instances where the air is heated, the heat is derived from the active heat within the furnace, and so to this extent (as compared with the regenerative method) detracts from the temperature therein.

In the regenerative system invented by Siemens, the heat, after it has done its work in the oven, and which, under ordinary circumstances, is allowed to escape up the chimney, is utilized in heating the air required for combustion.

There is quite a variety of generators in actual use, and though vary in the details of their construction, and in their position (

within the arch of the retort bench, or outside of it, the principle of

action in each is identical.

The following are the chief generators:—Siemens'; Liegel's, the latter well known from the description given of them by Mr. G. E. Stevenson, who introduced them into this country; Hasse's; Oechelhäuser's; Schilling's; Dietreich's, in use in some American gas-works; Klönne's, the "Didier," the "Munich," Valon's, and Livesey's, the last-named being in successful operation at the South Metropolitan and other gas-works.

Mr. Webber gives the following concise description of generator furnaces ("King's Treatise," Vol. III., p. 879 et seq.):—

"There is much difference in the details of generator furnaces as at present constructed by various engineers; but their main features are always alike, and are remarkably simple. The usual form of the generator itself is that of a kiln, generally sunk underground or beneath the level of the charging floor of the retort-house; the capacity of the kiln, of course, varying with the amount of work it is intended to perform; but it is usually about one-and-a-half diameters in height. The form of cross-section of the generator may be either rectangular or round, the former being easier of construction, although, according to Grahn, the latter gives better results. The generator is fed through a hole in the top, covered with an air-tight cap. The gas is usually taken off by an opening near the top. The lower part of the generator, in which the initial combustion commences, is subject to the greatest wear, especially from the formation of clinker. The air is admitted either by a grate at the bottom of the generator, as in an ordinary furnace, or by openings in the brickwork, which may be either at the sides, or in the bottom—which in that case is tapered down to the size of the opening-or by a combination of the two, as designed by Liegel, who puts a fire grate underneath the opening in the bottom of the generator. The generator should be lined with at least 9 inches of the best fire-bricks, between which and the surrounding walls of common brickwork, about 18 inches thick, a space of about 6 inches is left to be filled with a comparatively non-conducting material, such as asbestos, or even powdered fire-bricks, in order to diminish the loss of heat by radiation.

"The gas channel, by which the products of combustion leave the generator, varies according to circumstances, from the short connecting chamber of Liegel or Livesey, whose generators are virtually one with the retort settings, to a pipe of considerable length; but the former, or some similar plan, is obviously preferable when it is convenient to adopt it. In all cases the passage, when of any length, must be pro-

vided with a damper.

"In most cases a generator is about 3 feet to 3 feet 6 inches square, which is sufficient for heating two large settings of retorts. For one setting half this area will suffice. The body of incandescent coke is usually about 3 feet deep, although it might be reduced to half that depth without vitiating the gas produced. Still it is best to keep a considerable margin, in order to avoid risk of interruption in working, which might otherwise be caused by irregularity in charging the generator, which operation would, with the sizes of apparatus above specified, be necessary at four or five hours' intervals.

"The generator may be situated anywhere in the neighbourhood of the retort bench. The furnace gases are admitted to the interior of the retort stack, guarded as much as possible from loss of their acquired heat while in transit, and there mingle with the proper quantity of previously heated air; the mixture being attended with instant com-

bustion."

It may be mentioned, incidentally, as a matter of experience, that where this class of furnace is used, retorts constructed of fire bricks and tiles do not answer as well as the ordinary moulded retort, as they are more liable to become deformed by the intense heat acting upon them.

Dry air, though diathermanous to radiant heat, takes up heat with extreme rapidity when brought in contact with a hot surface. It is not necessary, therefore, that the hot flue passage through which the secondary air is caused to travel in order to be heated before coming in contact with the combustible gases from the generator should be

long-extended and tortuous in its course.

The advantages of the so-called regenerative arrangements as applied to retort furnaces are due not only, or chiefly, to the heating of the secondary air, which is readily accomplished, but largely to the circumstance that the heat of the waste gases, as the latter traverse the passages constructed alongside the furnace, is at a potential higher than that to which the brickwork in the base of the setting, and in the sides of the generator in the absence of the waste-gas flues, could possibly attain. The effect of this is to insulate, as it were, the heat of the furnace, minimizing outward radiation and conduction.

Heat, like water and electricity, tends to establish an equilibrium; and the lower the temperature of a body in contact with another at a higher temperature, the greater the abstraction of heat from the latter

by the former.

From this it will be evident that the function fulfilled by the heat of the waste gases cannot properly be considered as "regenerative." Their temperature is necessarily lower than that of the furnace and the inside of the oven. Heat cannot travel from a lower to a higher potential any more than water under normal conditions can travel uphill; and therefore it is not possible for the lower temperature to

"regenerate" the higher. The chief function of the heat of the waste gases is by insulation, as already explained, to conserve, in the ratio of their own temperature, the heat generated by combustion in the furnace. If it were possible to enclose the heated ovens of a retort-stack on all sides with an envelope of heat, it is obvious that the heat of the ovens would be conserved, a higher and steadier temperature maintained, and that economy of fuel would result.

SCURFING RETORTS.

In the distillation of coal a deposit of carbon takes place within the retorts, which, if allowed to go on accumulating, eventually seriously contracts their internal area, and causes a diminution in the heats.

This deposit is due principally to the pressure produced by the resistance offered to the passage of the gas through the different apparatus.

Its removal by scurfing with chisel bars in the ordinary way is always more or less attended with damage to the retorts; the more so as they require to stand off for 6 or 12 hours, to loosen the carbon by the admission of air, before applying the bar.

Different methods of scurfing have been tried with varying success; the best probably being that by which a current of air and steam is made to impinge upon the carbonaceous deposit. The latter plan is the invention of Mr. G. W. Edge, of the Jersey City (U.S.A.) Gas-Works. The process is thus described by Mr. E. Goddard:—

"The apparatus consists of a steam-pipe connected with the steam-boiler, and passing along the top of the retort benches, to which is connected a 1-inch pipe, extending out to the face of the retort mouth-piece; to this is connected a ½-inch pipe, having on it a stop-cock and union joint to connect and disconnect the pipe readily. This steam-pipe terminates at the end of a pipe 3 inches in diameter, and about 5 feet long, resting on the bottom of the retort, into which the steam rushes through a nozzle having a 3-16ths of an inch outlet, at the same time drawing with it a current of atmospheric air. A retort-lid is cut out to fit closely round the 3-inch pipe. The lid is luted on tight, and the plug removed from the top of the ascension-pipe, the retort being at a good working heat, and the apparatus is ready to perform.

"The steam should be used at a pressure of from 25 to 40 lbs. to the square inch. The rush of steam carries with it a current of atmospheric air, the cast-iron pipe becomes heated, and the steam and air rushing through it become superheated, and thus we have a compound blowpipe of immense power, the current of which strikes with great energy

on the thick portion of the carbon at the rear of the retort, but with diminished force as the returning current partially charged with the products of combustion approaches the front end of the retort, where the carbon is thin, in order to pass out through the ascension-pipe. If the retorts are thickly coated with carbon (say, several inches thick), on the first application of the apparatus, it will require several hours to clean them out; but when the retort is once decarbonized, one hour's application every thirty days will be found amply sufficient to keep the retort clear of extraneous carbon."

After all, the best plan of obviating the nuisance is to prevent the deposit as much as possible, by minimizing the dip, by employing an exhauster to reduce the back pressure; and in very small works where this is not available, by cleaning the surface of the retorts with a rounded steel scraper every time they are drawn.

TABLE OF COLOURS

Corresponding to Various High Temperatures. (Pouillet.)

•					Fahr.	•	Fahr.
Faint red .					977°	White heat	28700
Dull red					1290°	Bright white heat	25500
Brilliant red					1470°	Dazzling white	2780°
Cherry red						Melting point of cast iron—	
Bright cherry	TO:	đ			1830°	White 1920° to	
Orange						Grey 2010° to	2190°
Bright orange					2190°		

The effect of an excessively low heat in the retorts is to diminish the gaseous products, the chief results of the distillation being the production of tar.

TABLE,

By Miller, exhibiting the amount and specific gravity of the gas obtained from two bushels of coal during each of five hours' heating in an ordinary retort; showing the importance of restricting the time during which the coal is subjected to the action of heat in the manufacture of gas. The rich hydrocarbons diminished, and carbonic oxide and hydrogen increased in quantity as the experiment progressed.

		Cubic Feet.					Specific Gravity.			
In the first hour .			845				•	·677		
In the second hour			208					· 4 19		
In the third hour								·400		
In the fourth hour								·822		
In the fifth hour .			20					_		

With cannel the carbonization takes place in considerably less time than with ordinary coal.

TABLE

Exhibiting the Qualities of Gas at different Periods of Distillation. (Dr. Henry.)

From Half a Ton of Wigan Cannel.

	of Imp	easures oure Gas itain		Measure Purified G consist of	100 Measures of Purified Gas			
Time from Commencement of Distillation.	Sulphu- retted Hydro- gen.	Other Com- pounds of Nitrogen and Hy- drogen.	Olefiant Gas.	Other Inferior Gases.	Nitrogen.	Consume Oxygen.	Give Carbonio Acid. 94 112 106 94 88 78 54 36	
½ an hour. 1 hour. 8 kours. 5 " 7 " 9 " 10 " 12 "	3 2½ 2½ 2½ 2 1	5½ 3½ 2½ 2½ 2½ 2½ 2½ 2½	16 18 15 13 9 8 6 4	64 771 80 72 76 77 74 76	20 43 5 15 16 16 20 20	180 210 200 176 170 150 120 82		
From H	Talf a T	Con of C	Common	Wigan	Gas C	oal.		
1 hour. 8 hours. 5 " 7 ", 9 ", 11 ",	8 2 8 1 1	3 2 2 3 21 1	10 9 6 5 2	90 91 94 80 89 85	15 9	164 168 182 120 112 90	91 93 70 64 60 48	

RATE OF PRODUCTION OF GAS

FROM 2 CWT. OF WIGAN COAL IN AN EXPERIMENTAL RETORT.

									Cı	ubic Feet.
1	hour									275
1	,,									245
11	hours									200
2	,,									140
24	"									80
8	"				-					40
31	"								·	20
1½ 2 2½ 3 3½ 4	"									15
	••						•	•	•	
				1	'ota	ıl				1015

THE DINSMORE SYSTEM OF GAS MAKING.

The Dinsmore system (so called after its inventor) of enriching gas by the conversion of a portion of the hydrocarbons present in the tar into permanent gas of a high illuminating power, has been adopted at Widnes under the supervision of Mr. Isaac Carr, who has introduced various improvements in the method of its application, by which results of an important character have been obtained. The chief obstacle to the success of all previous attempts in a similar direction was the blocking of the ascension-pipes and hydraulic and foul mains with pitch. This difficulty has now apparently been overcome. With one-third of the carbonizing plant at work on the new system, about 10,000 cubic feet of gas per ton, of an illuminating power equal to 19 standard candles are obtained from an inferior class of coal.

RETORT MOUTHPIECES.

The following are the details of a mouthpiece for an oval retort 21 in. by 15 in., and will serve as a model for any other size and shape, allowance being made for varying dimensions. (See Figs. 15 to 18.)

Depth from front to back, over all, 15 in.

Thickness of metal in front portion, & in.

Thickness of metal in front portion, § in.

Ditto in lip, 1 in., and planed level.

Ditto in flange, 1 in.

Width of flange in front, 3\frac{3}{8} in.

Ditto at back, 4 in.

Number of bolt holes, eight; diameter, 1 in. Ear-box on each side, with slot 2 in. by $\frac{5}{5}$ in.

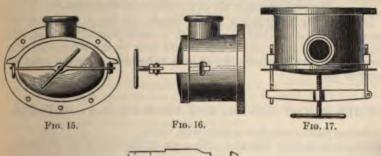




Fig. 18.

Socket, to receive end of ascension-pipe, 5 in. in height, and 61 in. diameter inside; centre 5 in. from front.

Bolts, for securing mouthpiece to retort, eight; diameter, 7 in.;

screwed and nutted at both ends.

Lugs of wrought-iron, 14 in. long, 2 in. broad, and § in. thick; one with jaws and pin for hinging cross-bar, the other cranked and notched as in Fig. 18. Slit at opposite end, 2 in. long, § in. wide; wedged to ear-box.

Cross-bar of wrought-iron, 25 in. long, 2 in. broad at each end, and $\frac{1}{2}$ in. thick. Middle part $2\frac{1}{2}$ in. broad, swelled out to 2 in.

thick, with 1 in. screwed hole through centre.

Screw, 10 in. long, with square thread 7 in. of its length.

Cross handle, 14 in. long, 3 in. round-iron.

Lid, 1 in. thick, plate-iron, dished, with lug on each side.

Various devices for dispensing with the screw and its slow action have been introduced. Amongst these Box's retort-lid fastener, made by Geo. Waller and Co., Storer and Pugh's lever handle, and King's patent fastener, made by West's Gas Improvement Company, may be specially named.

CEMENTS FOR JOINTING RETORT MOUTHPIECES.

For clay retorts-

Three-fourths by weight of fire-clay. One-fourth by weight of iron borings.

When ready to connect, mix with ammoniacal water. Use no sulphur.

20 lbs. gypsum (sulphate of lime) made into a pulp with water. 10 lbs. iron borings saturated with a strong solution of sal ammoniac.

Mix well together till of a consistency fit for use.

In fixing the mouthpieces to clay retorts, the flange or face of the retort should be notched all over with a sharp-pointed hammer, or a slight channel cut all round (this is best done by the retort maker in course of manufacture), for the cement to bed into when the bolts are screwed up.

CEMENTS FOR JOINING THE ENDS OF CLAY RETORTS.

10 lbs. gypsum made into a pulp with water.

20 lbs. iron borings saturated with a strong solution of sal ammoniac.

Mix well together till of a consistency fit for use.

Some engineers use fire-clay alone, mixed with water to the consistency of mortar.

For iron retort mouthpieces-

2 lbs. fine clean iron borings.

1 oz. sal ammoniac.

· 1 oz. flowers of sulphur.

Mix together and keep dry. When required for use, add water to bring the mixture to a proper consistency.

CEMENTS OR LUTING FOR RETORT-LIDS.

Ordinary lime, or spent lime from the purifiers mixed with fire-clay or common clay, and worked up into mortar.

The following makes a tough persistent luting: -

1 part lime.

2 parts moulding sand.

Ground up together, with water, in a mortar mill.

SELF-SEALING RETORT-LIDS.

The self-sealing retort-lid invented by Mr. Morton, with Holman's eccentric fastener, is extensively used. The lid is not removed from the mouthpiece in charging the retort, but swivels round with the hinged cross-bar, to which it is secured. It is made in any form to suit the shape of the retort, with upturned semicircular edge, faced true. This, pressing against the flat edge of the mouthpiece, which is also faced, makes a gas-tight joint without the intervention of any kind of luting.

Other self-sealing retort-lids are Tassie's, made with a steel ring let into a groove in the face of the mouthpiece; Parlby's and Grice's, having a projection on the edge of the lid fitting into a recess on the face of the mouthpiece; Somerville's, which consists in the contact of the outside of the rim of the lid with the inner conical lip of the mouthpiece; and Ruscoe's, with steel cross-bar and fastener.

RETORT-HOUSE TOOLS.

Shovels with riveted handles are not good in or about a retorthouse. The heat soon causes the wood to dry in, and the rivets give way and become jagged, lacerating the hands of the men who use them. Socketed handles are much the best.

A good handy-sized shovel for charging retorts of the ordinary size is one 16 inches long by 11 inches wide. Firing shovels (for coke) are best made an inch wider. Both should be well turned up at the sides.

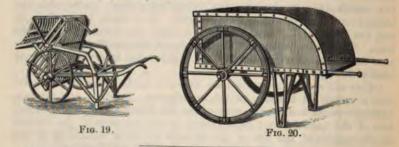
For charging through retorts, the scoop (Fig. 21) is frequently

employed.

This in section is a semicircular trough of sheet-iron, the length of half the through retort, and large enough to contain about 1½ or 1¾ cwt. of coal. It is inserted twice into the retort at each end. Six men are required to charge a through retort with the scoop—i.e., three at each mouthpiece. The method of using it is as follows:—On its being filled with coal, one man takes hold of the handle at the end, raises it slightly, the saddle is placed underneath by a second man, and a third grasps the opposite side. The three then raise the scoop and insert its end into the retort mouth, whereupon the saddle is released, and the man having hold of the handle pushes the scoop with its charge right into the retort, turns its round, and withdraws it, leaving the charge inside. This operation is repeated a second time; the scoop on the first insertion being turned to the left, and on the second to the right.

Other retort-house tools consist of the discharging rake, Fig. 22; auger, Fig. 26; ash-pan rake and shovel, Figs. 23 and 24; fire tongs, Fig. 27; and pricker, Fig. 25. [See next page.] Price's coke and coal barrow, Fig. 19, and Cockey's charging barrow, Fig. 20, are

useful and serviceable adjuncts to the retort-house.

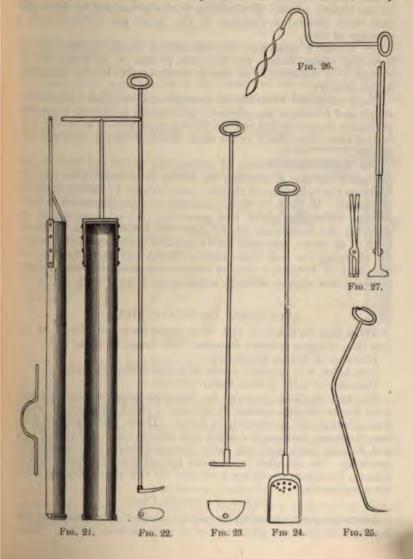


CHARGING AND DISCHARGING RETORTS BY MACHINERY.

The difficult problem of applying machinery to the charging and drawing of retorts is one which has occupied the minds of gas engineers from the very introduction of gas-lighting, and its solution has been attempted with varying success. Out of about twenty different contrivances that have been invented for the purpose, not more than four or five remain in use at the present time, and these only to a limited extent,

The hydraulic stoker invented by Mr. W. Foulis and the combined hand and machine stoker of Mr. J. West are both in use at the Manchester Corporation Gas-Works. The latter has also been adopted

at Maidstone, Portsea, Ipswich, Burnley, Bury, and other works. Mr. West has also patented the application of compressed air to the propelling of his machinery; and this is successfully at work at the Manchester and the South Metropolitan Gas-Works. More recently



he has adopted the plan of driving by means of a wire rope running the whole length of the retort-house, and actuated by a stationary engine placed at one end. This latter is in use at Blackburn. Mr. West's machines, both for charging and drawing, and the plan which he has latterly adopted of obtaining motive power, are so admirable, that their general application in the larger gas-works is only a question of time.

Mr. Warner's machinery is employed at South Shields; and the ingenious steam stoker, the invention of Mr. A. Q. Ross, of Cincinnati, U.S. America, is in use at various works in the States and

in this country.

Clegg attempted to perfect an arrangement by which a continuous supply and discharge was effected; and though he did not succeed in producing an economical and satisfactory apparatus, it is greatly to be desired that other efforts in the same direction may be crowned with

The latest improvements of carbonizing plant and methods are revivals of the idea of inclining the retorts at an angle, with a view to facilitate the operations of charging and drawing by calling in the aid of gravity. M. Coze, of Rheims, claims to have succeeded in overcoming difficulties which had previously proved insuperable, by adopting the inclination of 80° from the horizontal for a flattened form of \square retort, combined with a peculiar design of tipping wagon for charging the coal from above. Mr. J. Elliott, of Ludlow, has also revived Brunton's idea of carbonizing coals in small charges pushed into a sloping retort by a traversing arrangement.

ASCENSION OR STAND-PIPES.

These may be either of cast or wrought-iron, and should be not less than 5 inches internal diameter, with flange at upper end.

Diameter of flange, 101 inches.

Bolt-holes, 4 in number, centre to centre across, 81 inches.

Diameter of bolts, 3 of an inch.

The best caulking material for Ascension-pipes at their junction with the mouthpiece socket, is ordinary ground fire-clay, or slaked lime, made of the consistency of putty. These, when pressed down into the space between the spigot and socket, make a perfectly tight and durable joint, and are easily removed when the retorts need renewing. On the other hand, when the joints are caulked with iron cement, the labour in cutting it out and the risk of splitting the socket are considerable.

Choking of Ascension-Pipes.

Ascension-pipes occasionally become choked, to a greater or less degree, with thick tar, pitch, and other carbonaceous matter. When

this occurs, let as many as can be spared at once stand off for a shift (provided the retorts are in condition to admit of this), drawing the charge, and removing the bonnet or plug from the top of the bridgepipe. The heated air making its way through the smallest aperture will thoroughly clear them of the obstruction.

Preventive of Choking.

Keeping the pipes cool is the best preventive of choking. This may be accomplished to a great extent by making the front walls of the ovens 11 bricks thick, so preventing undue radiation from the bench, and having the mouthpieces of the retorts so constructed as to allow of the pipes standing 6 or 8 inches away from the front wall of the

BRIDGE AND DIP PIPES.

Internal diameter of bridge and dip pipes, 5 inches.

Height of bridge-pipe, 16 inches.

Width, centre to centre, 21 inches.

Connecting flanges, diameter 101 inches.

Bolt-holes, four in number, centre to centre across, 81 inches.

Diameter of bolts, 3 of an inch. (See Fig. 28.)



Frg. 28.

HYDRAULIC MAIN.

Dimensions and Form.

The hydraulic main, as a general rule, even in small works, should not be less than 18 inches in width at the water-level.

In section it may be either D-shaped (with the flat side upwards), square, oblong, or round. The three former shapes are usually adopted in preference to the round, allowing more gas space than the latter. (Figs. 29, 30, and 31.)

The Livesey Hydraulic.

This, in section, resembles the frustum of a cone, but is slightly convex at the sides, and dished at the bottom to the extent of 2 inches

below the end of the dip-pipe. It is smaller, and consequently lighter, than the mains generally in use; but at the water-level the area is equal to the old forms. The chief object of the modification in form is to prevent the accumulation of thick tar. This is accomplished by allowing only a shallow depth of liquid; and this being kept in motion or circulation by the issuing gas, deposit to any great extent is prevented. (Fig. 32.)

With the same object in view, Mr. Livesey has reduced the bottom space in his existing old-fashioned D-shaped mains, by placing therein a plate of No. 10 gauge sheet-iron, also dished to the extent of 2 inches below the end of the dip; the space underneath being

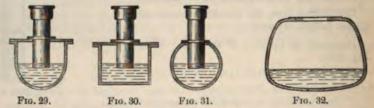
first filled up with sand.

Wrought-Iron and Steel Hydraulic Mains.

Hydraulic mains of wrought-iron 5-16ths of an inch thick, or mild steel plates ‡ inch thick sides and bottom, and 7-16ths of an inch top, are being generally adopted, owing to their lightness and strength, and are an improvement on those made of cast-iron, which are usually 3-4ths of an inch thick.

Position of the Hydraulic Main.

The hydraulic main may be either erected on standards placed on the retort-bench; on girders attached to the buckstaves, which are



lengthened so as to reach above the bench for that purpose; or on cast-

iron pillars in front, and quite detached from the brickwork.

When placed upon the bench, it is liable to be disturbed by the contraction and expansion of the materials composing the latter; and when the bench needs rebuilding, it is an obstacle to the progress of the work. On the other hand, when erected on pillars in front, these are slightly in the way, though placed opposite the walls dividing the several ovens; and the main itself is more exposed to the heat of the flame from the retorts in charging.

In some instances the hydraulic main is placed against the retorthouse wall, being supported on brackets or cantilevers attached thereto. This plan necessitates a strong wall to bear the weight of the main and its contents, and also a long length of pipe overhead, fixed in an inclined position, attached at one end by a bend to the

ascension-pipe, and at the other to the dip-pipe on the main.

In addition to the hydraulic main, a second main is sometimes laid along the bench, and connected to the former at the water-level, at each bench or oven, by a branch with a valve upon it for closing when necessary. This secondary main conveys the gas and fluid products from the retort-house, and admits of the isolation of the hydraulic main over each setting of retorts. By this arrangement it is easy, in case of any disturbance of the bench through settlement or otherwise, to restore the several short lengths of hydraulic main to the true level.

The Liquid Products in the Hydraulic Main. The Effect of Keeping the Gas in Contact with the Tar. The Hydraulic Dip.

A simple gas is usually described to be a permanently elastic fluid under the ordinary conditions of temperature and pressure. Coal gas, as it is compound in character, does not answer to that description. When it has been distilled from the coal by the agency of heat, and issues from the retort up the ascension-pipe into the hydraulic main, there is carried in suspension, along with the permanently gaseous fluids, a number of hydrocarbon and other vapours, which condense

at temperatures varying from about 200° Fahr. downwards.

The water which is found in the hydraulic main is due to the condensation of the vapour or steam which, coming from the retorts, is carried up the ascension-pipes along with the permanent gases and the heavy hydrocarbons; the latter being deposited as tar. presence of the water is accounted for by its previous existence in the interstices of the apparently dry coal. It is also produced synthetically by the combination, brought about by the heat of the retorts, of a portion of the oxygen and hydrogen-two constituents of the solid coal. The quantity of water thus yielded varies with different coals; but the average yield may be set down at 16 gallons per ton. It has previously been explained (see page 5) that a portion of the steam from wet coal is decomposed in the hot retorts, being resolved into its constituent gases. It will be seen, therefore, assuming the correctness of this hypothesis, that two opposite processes are being carried on simultaneously in the retorts - the analytical and the synthetical—and this apparent inconsistent action may be explained by the original character of the substance acted upon—the steam in the one instance, and the gases, oxygen and hydrogen, in the otherand their proximity to, and period of contact with, the hot surface traversed by them.

The strong affinity which exists between this water and the ammonia impurity in the crude gas, causes the absorption of much of

the latter by the former, producing what is, roughly speaking, a solution of ammonia. This again, by reason of its affinity for suphuretted hydrogen and carbonic acid, absorbs a proportion of the gases named, reducing the amount of these impurities in the gas, and thus is pro-

duced the complex liquid designated "ammoniacal liquor."

The hydrocarbons contribute largely to the illuminating power of the gas; and it is therefore desirable to retain them in the permanently gaseous form. Some of them, especially such as are of the greatest density, are reduced to the liquid state by the mere mechanical reduction of their temperature; whilst others of equal specific gravity, and many of those of lower density, undergo a change from the gaseous to the liquid condition, by reason of the solvent or absorbent action of the liquid contents of the hydraulic main, through which, by reason of the dip, they have to pass, or with which, in the absence of the dip, they come intimately in contact. The former may be classed as hydrocarbon vapours; the latter, as gaseous hydrocarbons. It is thus evident that the process of condensation begins at the hydraulic main; the results there produced materially affecting the quality of the gas.

Those hydrocarbons that are changed to the liquid form by this slight diminution of temperature, it is probably impossible to retain in the gas under any circumstances whatsoever. With the more volatile, though still heavy, hydrocarbons, the case is different; the power of retaining them in the permanently gaseous form is within the bounds of possibility, and these are, therefore, of the greatest

interest to the gas manufacturer.

A further class of hydrocarbons are not liquefied at all under ordinary conditions; and there should never be any difficulty experienced

in keeping them in the gaseous state.

Of the second class of hydrocarbons—viz., those which, though of high specific gravity, it is practicable to retain in the gaseous form—we shall now speak. Their retention in the gas, and how this is most likely to be accomplished—or at least how best to remove all impediments to that end—greatly concerns the gas-maker. It has been assumed that the mere reduction of temperature between the retortmouth and the hydraulic main will not affect their gaseous condition. Under what other circumstances, then, are they condensed in the hydraulic main, and in the subsequent mains leading to the condenser? The answer is clear, and is what has been already indicated—viz., by the affinity which exists between them and the already liquefied hydrocarbons present in the mains.

Some remarkable notes corroborating these views in several important particulars are recorded by Mr. W. Young, being the result of a number of experiments made by the late Mr. Cusiter in 1868, on the absorption of the light-giving constituents of coal gas by the heavy

hydrocarbon oils, his attention being drawn thereto when experiment-

ing with glycerine as a substitute for water in gas-meters.

After having satisfied himself that the disadvantages attending its use were not compensated by its advantages, he turned his attention to other liquids which might, he thought, be suitably applied for the like purpose. One of them was mineral oil of 840° specific gravity. The effect of this with 28-candle gas was to reduce the illuminating power to 14 candles; and with gas of 35 candles, to 16·1. During the winter of 1873-4 he repeated the experiments, and made some additions to the number. Mr. Young deduced from these experiments various facts of general interest, having reference to the means afforded of ascertaining the percentage of hydrocarbons in a given quality of gas.

In a further communication on the same subject, Mr. Young showed that so great is the solvent action of heavy hydrocarbon oil (boiling point 180° Fahr.) that hydrocarbons, such as olefant gas, which are permanent gases at ordinary temperatures, may be reduced to the liquid form in passing through it. He further showed that if, instead of allowing the gas and mixed hydrocarbons to cool together, the gas, saturated with the vapour of the lighter hydrocarbon liberated by heat from the mixed fluids, were transferred into a separate vessel, thereby preventing the heavy hydrocarbons from coming into contact with, and reabsorbing the lighter, the gas would remain saturated with the vapour from the more volatile fluid.

These important facts lead to but one conclusion—viz., that the practice of allowing the whole of the tar to flow along with the gas through an extensive range of pipes to the condenser, both being gradually cooled together in the passage, is founded on an erroneous estimate of the results that follow thereon, is highly objectionable, and

must be condemned.

The late Mr. R. H. Paterson, with that wise insight which characterized his investigations, gave expression to his views on this subject in an able article "On Keeping Gas in Contact with Tar," in which the objectionableness of the practice is very clearly shown.

The cooling of the gas gradually is a provision the wisdom of which is unquestionable, and the plan of causing it to make the circuit of the retort-house in pipes is probably the best method of accomplishing that object; but the deposited tar in the hydraulic main and in the foul main at the point, as near as can be ascertained, when its temperature has fallen to about 110° or 100° Fahr.—the temperature at which its absorbent powers come into most active operation—should be drained away direct to the tar-well by its own separate conductor.

The chief advantages believed to accrue from lengthened contact of the gas with the tar are, first, the absorption by the latter of naphthaline that would otherwise be carried forward to be deposited, by reason of the decrease in temperature and other causes, in the mains on the works, and even in the street mains, service-pipes, and the internal fittings on the premises of consumers; and, secondly, the absorption also of a considerable portion of the obnoxious sulphur and other com-

pounds.

These advantages will not be forfeited by the direct removal of the bulk of the tar, because sufficient light tar will be left in the circuitous gas-main to absorb any excess of naphthaline vapour present, and even to assimilate a portion of the sulphur and other impurities. Besides this, as the general effect will be to leave a larger proportion of the gaseous hydrocarbons in the gas, these, by virtue of the power which they possess in common with the liquid hydrocarbons, of assimilating—and, in this special case, of suspending—other hydrocarbons, will necessarily assist in retaining in the permanent form a portion of the naphthaline that would, in presence of the greater bulk of tar, have been liquefied and deposited. By a similar train of reasoning, the fact of the inferior quality of the tar produced from the richer cannels, as compared with that from coal, may be explained.

In dealing with this subject, it has been assumed by some that no absorbent action is likely to result so long as the tar with which the gas is in contact is at a temperature of about 100° Fahr., and above : and that, therefore, the dip in the hydraulic main causes no diminution in the amount of hydrocarbon gases present. It has even been assumed that the tar in the main gives off a proportion of hydrocarbon vapour; and in this way increases the illuminating power of the gas. On reflection, however, it will be plain that this argument is altogether untenable, for it is scarcely possible to conceive that hydrocarbons which have already been liquefied at a high temperature, can again, at a lower temperature, assume the gaseous or vaporous form. There can be no doubt that the heavy tars have an absorbent action, less or more, at all temperatures, being greatest at the lowest; and this being so, the passage of the gas through such tars by reason of the dip in the hydraulic main, must have a prejudicial effect upon the illuminating constituents of the gas. On the other hand, where means are employed for removing the heavy tars from the main as rapidly as possible after they are deposited, the disadvantages of the dip into the lighter liquors contained therein are reduced almost to nil. This is especially true where the arrangements are such that, by careful adjustment, and an adequate area at the water-level, the dip is limited to about three-fourths of an inch.

It is desirable that the ends of the dip-pipes in the hydraulic main should be sealed with the ammoniacal liquor in preference to the tar; the latter not only robbing the gas to some extent of its richest illuminating substances, but offering greater resistance to its passage. Various expedients to accomplish this end have been devised and are

in use in well-regulated gas-works.

Such being the case, considering the easy application of the dip, its economy, its self-acting regularity, its comparative immunity from failure, and the safety attending its use, it is questionable whether any of the many appliances for dispensing with it, offer sufficient inducements to compensate for the advantages enumerated.

TEMPERATURE OF GAS IN THE RETORTS.

The reason of the comparatively low temperature of coal gas as it ascends to the hydraulic main, after being in contact with the intensely heated surfaces of the retorts in which it is generated, is not apparent at a cursory glance.

At first sight it would appear as though the action upon the gas in a retort would be similar to the effect upon air by the ovens of blast furnaces, where a million cubic feet are heated in the space of an hour

to 633° Fahr.—the melting point of lead.

So far from this being the case, the permanent gas at its highest temperature does not probably exceed 135° Fahr., though generated in

a heat usually reaching 2200°.

The reason of the difference in the effect produced in the two instances given is explained by the fact of the rapid absorption of heat by the volatile constituents of the coal in assuming the gaseous form; this heat becoming latent in the gas as in the case of the formation of steam in an open boiler.

The following is a record of experiments made by the writer to determine the temperature of the gas as it issues from the retort:—

Experiment No. 1.

This experiment was conducted entirely under the usual conditions of working.

Clay retort, 20 feet through, one in a setting of seven.

Heat, bright cherry red.

Hole drilled in both ascension-pipes 3 feet above the mouthpiece.

Retort charged with 4 cwt. of cannel.

Temperature indicated on insertion of thermometer through the hole on one side of bench, 193° Fahr.

Temperature indicated on insertion of thermometer through the

hole on the other side, 510° Fahr.

The temperatures indicated were clearly not those of the gas. In attaining the higher temperature, especially, the mercury rose by starts at the rate of 3° to 5° at once, evidently caused by hot particles

of solid carbon, or other solid or semi-fluid substances coming sud-

denly in contact with the bulb of the thermometer.

The remarkable difference in the temperature of the two sides is accounted for in this way: On the side in which 198° was indicated the dip-pipe was probably sealed to a greater depth in the hydraulic main, and consequently the flow of gas was neither so abundant nor so rapid on that side as on the other. This was evidenced by the thermometer on withdrawal being found less thickly coated with tar than in the other case. The gas was in a more quiescent state, and therefore there was not the same rush of hot solid particles against the bulb to raise the temperature abnormally.

It may be noted incidentally here, that indications of temperature thus obtained would prove whether the ascension-pipes at the two ends of a through retort were each taking their due share of the gas

being produced.

Experiment No. 2.

The conditions were the same as in the previous instance; but instead of inserting the thermometer directly through the hole in the ascension-pipe, the end of a piece of india-rubber tube, 12 inches long, \(^3_4\) inch bore, was pressed against the orifice, and the gas allowed to flow in a stream through the tube. The object of employing the tube was to obviate, if possible, the contact of the semi-solid or semi-fluid substances previously referred to.

The result was: Temperature indicated on one side 250°, ditto on

the other side 324°.

The rise of the mercury was still somewhat irregular, and the instrument, so much as was inserted, was again thickly coated with tar.

Experiment No. 3.

One end of the through retort was now bricked up, being made perfectly gas-tight, the gas passing away by one only of the ascension-pipes;

in point of fact, the retort was made single instead of through.

In a short, double-flanged piece of the ascension-pipes, within

In a short, double-flanged piece of the ascension-pipes, within 8 inches of the top of the mouthpiece, were inserted six layers of iron wire netting, cut into discs, accurately fitting the bore of the pipe. Three of these discs had meshes one-eighth, and the other three three-sixteenths of an inch gauge, and the discs were kept three-fourths of an inch apart by sheet-iron rings, inserted edgeways into the pipe.

The charge, 2 cwt. of cannel, thrown into the retort, happened to be taken from a heap that had been exposed to the rain, and there was

considerable moisture present.

The hole through which the thermometer was inserted, as in the previous experiments, was 8 feet above the mouthpiece.

The follo	owing	were tl	ie temperati	ires indicat	: bec		
Time. Minutes. 10	,		omp. Fahr. Degrees. 200	Time. Minutes. 55		3	emp. Fahr. Degrees. 177
	• •				• •	•	
15	• •		198	60			174
20			195	65			172
25			192	90			160
80			190	105			158
35			188	120			150
40			184	180		• •	150
45			182	140			148
50			179	150			142

Through all the higher temperatures, down to 172°, steam was condensed into drops upon a piece of paper held in the stream of gas issuing from the hole. Tar, though not entirely absent, was nearly so, the instrument on each withdrawal being but slightly coated. The temperature, with but few exceptions, rose with great regularity from that of the atmosphere of the retort-house (74°) to the rates observed, showing that the semi-solid particles, which were evidently the cause of the high temperatures previously indicated, had been nearly all arrested by the wire netting.

The higher temperatures, I am of opinion, were due to the presence of steam in the gas in varying proportions, and this latter would be caused by the moisture in the coal.

Experiment No. 4.

The retort was again charged, this time with 2 cwt, of cannel in a drier state. All the other conditions were as in the previous trial.

The following were the results obtained: -

Time. Minutes.	T	emp. Fahr. Degrees.	Time. Hours.		Te	emp. Fahr. Degrees.
2	 	158	1 3			129
7	 	174	2^{-}			128
12	 	177	$2\frac{1}{4}$			122
17	 	172	$2\frac{1}{2}$			119
22	 	171	$2\frac{3}{4}$	• •		118
27	 	169	8		• •	116
32	 	168	8 1		• •	118
75	 	141	8 <u>1</u>			110
90	 	184	_			

During the first half-hour of the charge, the presence of steam, mixed with the issuing gas, was indicated as before, but less abundantly, though still, doubtless, affecting the results obtained. When

the temperature of the gas within 3 feet of the mouthpiece was at 174°, it stood at 182° in the bridge-pipe, 14 feet higher up.

Temperature of the Gas in the Bridge-Pipe, 14 feet from the Retort Mouthpiece.

Experimen	at.		wt. Char		Te	mp. of the	Gas.
No. 1		 retort (charged 1	hour	 	135° Fa	hr.
,, 2		 **	,, 1	3 hours	 	116°	3
3		 		11 hours	 2.5	119°	

It may be suggested that the effect of passing the gas through the wire netting would be to lower the temperature of the gas, just as the wire gauze on a Davy lamp reduces the temperature of the flame impinging against it. The conditions of the two cases, however, are entirely different. The meshes were sufficiently large to admit of an easy passage for the gas, and the metal would be immediately covered with a thick coating of tar, virtually producing insulation. In addition to that, the temperature within 6 inches of the front of the bench was 208°; and the metal of the ascension-pipe, as well as the inserted wire netting, would, as a rule, be above the temperature of the gas. The results of these researches will be found to confirm, in a remarkable manner, the deductions of earlier investigators.

CONDENSATION.

Extent of Condensation.

The degree of condensation to which coal gas should be subjected after leaving the retorts, and before entering the purifiers, has never been determined with that scientific accuracy which the importance

of the subject demands.

The axiom that "thorough condensation is half the purification," is too sweeping in character to be serviceable or safe as a guide. The term "thorough," as applied to the condensation of coal gas, still remains an indefinite quantity, though the well-directed and carefully conducted inquiries of the first Referees in the metropolis (the results of which are embodied in their admirable and valuable reports) have led to a more exact knowledge on this and the other branches of gas purification.

With respect to one point there cannot be two opinions—viz., the necessity of guarding against a lower temperature in the gas than 50° Fahr. If condensation is carried beyond this, the lighter hydrocarbons are in danger of being deposited, and the gas im-

poverished.

In the following table the bad effects of excessive refrigeration are shown.

TABLE

Exhibiting the Loss of Illuminating Property in Coal Gas on Exposure to the Temperature of Freezing Point, 32° Fahr.

Name of Gas,		10	ubic		ondensed fr as on Expo	
Boghead cannel .			1	4.42 cu		
Ince Hall ditto .				+37	22	
Methyl ditto				*88	**	

From the above it appears that the richest gas suffers the greatest deterioration on being subjected to cold.

Rapid or Sudden Condensation.

Experience has sufficiently proved that rapid or sudden, as well as excessive, condensation, is an evil to be avoided; and that to prevent the deposition of naphthaline in the pipes, and preserve some of the richer illuminants, the gas should be allowed to travel in contact with the lighter tars until the latter are reduced in temperature to about 100° Fahr, before separation takes place.

With this object in view, the pipe leading from the hydraulic main may be carried with a gradual inclination round the interior of the retort-house or other convenient building, and from thence to the condenser; provision, of course, being made to allow the thicker tar to run off at a point near to the hydraulic main. By this arrangement the gas is slowly reduced in temperature, and some of its most valuable light-giving hydrocarbons, which would otherwise be condensed, are retained within it in the permanent state.

Livesey and Tanner's Differential Tar and Liquor Overflow and Tar Screen is a useful provision for separating the tar and liquor by means of a perforated screen, preventing the oscillation of the liquor in the main and allowing of a minimum of seal. The arrangement for adjusting the difference of seal required for drawing off the tar and liquor separately according to their specific gravities, is also very ingenious and useful.

Temperature as affecting Registration.

The make of gas, as indicated by the station-meter, is materially affected by the temperature at which it is registered.

At the temperature of 60° Fahr., with the barometer at 80 inches, gas is at its standard volume; and as all aëriform bodies expand $\frac{1}{480}$ of their bulk at 32° Fahr. for every additional degree of temperature, or about 1 per cent for 5°, it follows that a quantity of gas, say 10,000 cubic feet, registered at 60°, would at 70° become 10,196, and at 80° 10,393.

The quantity of heat which will raise a cubic foot of water one degree, will raise 2850 cubic feet of gas or atmospheric air to the same extent.

In instituting a comparison between the production per ton of material at different works, and in testing the productive value of different coals, it is, therefore, necessary to take into account the temperature of the gas at the time of measurement. In ascertaining the specific gravity of gas, and in conducting photometrical observations, the same care should be taken to note the temperature of the gas at the time and place of making the experiment.

TABLE.—Expansion of Air and Permanent Gases by Heat.

Temp. Fahr.	Expansion.	Temp. Fahr.	Expansion.	Temp. Fahr.	Expansion.	Temp. Fahr.	Expansion
32	1000.0	52	1041.6	72	1083-3	92	1125.0
33	1002.1	58	1043 - 7	73	1085 4	93	1127.1
34	1004.2	54	1045 · 8	74	1087.5	94	1129.1
35	1006.2	55	1047-9	75	1089.6	95	1131.2
36	1008.3	56	1050.0	76	1091.6	96	1133-3
37	1010 · 4	57	1052.1	77	1093.7	97	1135.4
38	1012.5	58	1054.1	78	1095.8	98	1137.5
39	1014.6	59	1056-2	79	1097 9	99	1139-5
40	1016.6	60	1058 · 3	80	1100.0	100	1141-6
41	1018 · 7	61	1060.4	81	1102.1	110	1162.5
42	1020.8	62	1062.5	82	1104.1	120	1183.3
43	1022 · 9	63	1064.5	83	1106.2	130	1204 - 1
44	1025.0	64	1066.6	84	1108.3	140	1225.0
45	1027 1	65	1068 - 7	85	1110.4	150	1245 . 8
46	1029 1	66	1070.8	86	1112-5	160	1266 6
47	1031-2	67	1072.9	87	1114.6	170	1287-5
48	1033 · 3	68	1075.0	88	1116.6	180	1308 - 3
49	1035 · 4	69	1077 1	89	1118.7	190	1329 - 1
50	1037.5	70	1079 1	90	1120.8	200	1350.0
51	1039.6	71	1081.2	91	1122.9	212	1375-0

TABLE

Showing the Relative Effects of Water and Air as Cooling Agents for the Condensation of Gas. (Peclet.)

1	of Tempe in the Gas e Atmosp	8				ien	of E Radi	xte	rior	Pip	by a Square Unit be Surface. When plunged in Water.
For an	excess o	f 10°			100		8		4	-	88
93	31	20°		-	141		18				266
.55	11	30°	00			*	29				5,353
17	14.	40°	4	*	+		40		2		8,944
**	**	50°	-				53				13.487

Water is thus shown to be the superior cooling agent, requiring the exposure of much less radiating surface than air; but, for the reasons already adduced, the latter is found to be the more suitable medium for the condensation of gas, except under the special conditions noticed hereafter.

TABLE

Giving the Mean Temperature (Fahr.) of every Tenth Day in the Year in the Central District of England. (Box.)

Month.	1st.	11th.	21st.	Month.	1st.	11th.	21st.
January February March April May June	Deg. 36.5 37.2 40.1 43.6 50.0 56.4	Deg. 35·6 37·5 41·0 45·0 51·3 57·5	53.8	July	Deg. 61·2 62·5 58·8 53·5 46·4 41·7	Deg. 61·5 61·7 57·4 51·4 44·0 40·2	Deg. 62.0 60.6 55.5 49.0 42.0 38.4

CONDENSERS.

Atmospherical Vertical Condenser.

The ordinary Atmospherical Condenser (Fig. 33) consists of a series of pipes, usually 18 feet long, put together in two lengths, and placed upright, through which the gas passes up and down alternately. These enter a rectangular cistern at bottom, in which the condensed vapours are deposited, and from whence they flow to the tar well. At the top is another cistern, containing water to seal the movable hoods covering each pair of pipes, and for further refrigeration, should such be required, in warm or sunny weather; small streams being made to trickle down the exterior surface of the pipes.

Atmospherical Annular Condenser.

The Annular Condenser is one of the most efficient Atmospherical condensing apparatus for gas that has yet been devised. In Kirkham's Condenser, as improved by Wright (Fig. 34), the pipes are placed in the vertical position, and are of large diameter, each one enclosing a smaller pipe; the two forming an annular space through which the gas is made to flow. Other pipes, placed diagonally, connect the top and bottom of the condensing columns alternately. By this arrangement the gas passes through the annular space always in the downward

direction, whilst the current of air moves upwards through the interior ventilating pipe. In cold weather movable covers are placed over the latter, or butterfly valves are fixed at the foot, for closing, to regulate the air draught, which might otherwise reduce the temperature of the

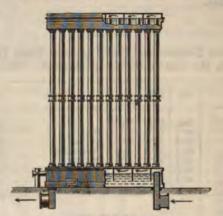


Fig. 33.

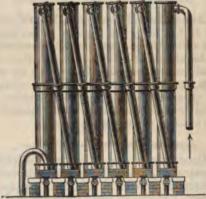


Fig. 34.

gas below the desired standard. A small pipe is connected to the bottom of each column to carry away the deposited tar and water into a main laid alongside the Condenser, and leading into the tar well.

Instead of the diagonal pipe, extending from the top to the bottom of each column alternately, Mr. Warner has inserted a mid-feather or partition, within the annular chamber. This reaches to within a short distance of the top and bottom; the space at the lower end being sealed by the deposited fluids, and a short connecting piece joins the several columns at the base. By this modification a free passage is obtained from end to end for the condensed fluids, and the separate tar main is dispensed with.

Cleland's Slow-speed Condenser.

This consists of a series of vertical pipes, connected together at the top by a tubular cornice or cap, which serves as the common inlet to the whole series. The stream of gas being thus divided equally amongst the several columns, travels through them in a downward direction and at a comparatively slow speed.

In the lower part of each column, to about a fifth part of its length, is inserted a "bottle brush" of wood or other material, with a drip ledge above it to divert the descending liquor on to the centre of the brush, which has the effect of converting the apparatus, to that extent, into a scrubber.

The general result is superior efficiency in condensing, and the yield of a high strength of liquor.

Atmospherical Horizontal Condenser.

The Atmospherical Horizontal Condenser (Fig. 35) is one of the earliest forms of the apparatus. Its efficiency has not been generally



Fig. 35.

recognized, owing to the want of a correct estimate of the conditions on which the condensation of coal gas ought to be conducted; and this has led to its being generally discarded in favour of the vertical form. The earlier method of construction was to fix it against the outside of the wall of the retort-house or other convenient building; the several pipes rising nearly parallel, one above the other, their ends being con-

nected by >-shaped bends.

An improvement, on strictly scientific principles, has been effected in the apparatus by Mr. D. A. Graham. A Condenser designed by him consists of two series of 16-inch cast-iron pipes, 65 feet long, in ten of such 65-feet lengths, arranged in pairs side by side, and supported on framework, the end of each length being joined to that of the next. From the inlet at the top, through the entire run of the Condenser to the outlet at the bottom, there is a gradual inclination, so that it is simply a flat screw or spiral, such as might be represented by winding

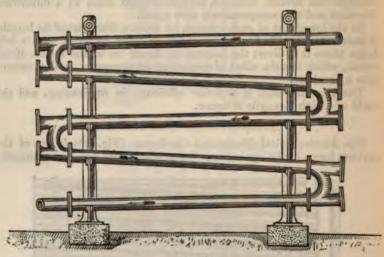


Fig. 36.

a length of soft wire five times round a piece of board, in which case the two ends of the wire would answer to the inlet and outlet of the Condenser. Blank flanges are bolted on the end of each length for

convenience in cleansing.

In this arrangement there is a recognition of the fact that *length* rather than *height* is the desideratum in a Condenser. In the ordinary vertical form of the apparatus, the cooling effect of the air on the surface of the upper parts of the pipes is almost *nil*. This will be obvious when it is considered that the air contiguous to the lower part of the

Condenser, being assimilated to the temperature of the latter, expands, and so, becoming lighter than the surrounding air, ascends in contact with the pipes, extracting less heat in proportion as it rises.

In addition to the other advantages, the ammoniacal liquor on leaving the Horizontal Condenser is of a strength equal to 5° Twaddel—a result which it is impossible to obtain from the ordinary vertical form.

A somewhat similar form of Condenser was previously designed and used by Mr. George Livesey.

Fig. 86 shows a useful form of the Horizontal Condenser suitable for small works.

Combined Atmospherical and Water Condenser.

Cutler's Horizontal Condenser has one or more small tubes passing through the interior of the larger pipes. Through these tubes a stream of water flows in the opposite direction to the gas; so that by the time the water reaches the inlet of the Condenser, by absorbing the heat of the gas, it has attained a moderately high temperature, and thus any sudden cooling of the gas at the entrance is prevented.

The Tubular or Battery Condenser.

An excellent apparatus (atmospherical) is that known as the Battery Condenser (Fig. 87). This is an oblong vessel, 12 to 24 inches wide,

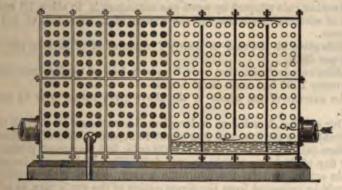


Fig. 37.

12 to 18 feet in height, and of length suitable to the requirements of the works. It is divided by internal plates or mid-feathers, placed at distances, equal to the width, apart, extending to within a few inches of the top and bottom of the chest alternately; and the gas passes from the inlet, up and down each division, till it arrives at the outlet. To augment its condensing power, small tubes, 2 inches in diameter, through which the air has free circulation, are passed through from side to side of the vessel, and there securely jointed. These transverse tubes serve the double purpose of cooling the gas; and, by breaking it up and retarding its progress, inducing a natural settlement of the heavy condensable vapours.

Rules for Calculating the Area required for Atmospherical Condensation.

It is stated in "Clegg" (4th edition, p. 173), that "the different states in which crude gas enters the Condensers make it impossible to give any fixed rule for the determination of the area of the exposed surface. It may be dangerous even to venture on a general one; but it may be stated from experience that a surface of 150 square feet for every 1000 cubic feet per hour is about sufficient when the stratum of gas has not exceeded 3 inches in thickness, and this without the application of a water shower."

This is at the rate of 61 square feet of condensing surface for every 1000 cubic feet maximum production of gas per diem of 24 hours.

The superficial area of the original Condensers designed by Mr. Croll for the Great Central Gas Company was 4 feet per 1000 cubic feet maximum production per diem, or at the rate of 96 square feet for every 1000 cubic feet of gas produced per hour.

Another rule adopted by some gas managers is to allow 10 square feet of condensing surface for the cooling of 1 cubic foot of gas per

minute.

This gives at the rate of nearly 7 square feet of surface per 1000

feet per diem.

Others again insist that only 5 square feet of surface are needed for every 1000 feet made in 24 hours.

An average of the whole of the above gives rather over 51 square

Our opinion, founded on a lengthened experience, is that all these estimates are too low, and that about 10 superficial feet of condensing surface (atmospherical) for each 1000 cubic feet maximum production per day of 24 hours should be provided. This includes the length of main extending from the hydraulic main; moreover, the Condenser should be protected from the direct action of the sun's rays, or otherwise water should be made to trickle down the outer surface of the pipes during sunshine.

Dry Scrubbers as Condensers.

In some works condensation is effected by means of dry scrubbers—cast-iron vessels of large diameter—charged with coke, drain tiles, or other material, breaking up the gas into minute streams, which, being thus cooled, deposits its tar and water.

A natural settlement of the condensable matter also takes place, irrespective of the action of the contained material, owing to the velocity of the flow of the gas being reduced on entering the larger

The rapid fouling of these vessels, however, necessitating frequent changing of the filling material to prevent undue back pressure, and maintain their efficiency, renders their use objectionable.

Precipitating chambers of large size are also employed, without any filling material, in which the gas, as it were, sleeps, and deposits its condensable particles. A vessel of this kind is useful in other respects, because the large volume of gas serves as a cushion to counteract pulsatory action between the exhauster and the retorts.

Underground Condenser.

In this arrangement the pipes are placed in the ground, out of the reach of the fluctuations of temperature in the atmosphere, with a view to obtaining uniformity of action in the process of condensation. By this system, however, a much longer length of piping is required than by any other, owing to the small amount of radiation from the surface of the buried pipes.

There is an advantage in this process of gradual condensation; but it is advisable, wherever in use, to supplement it by finally passing the gas through one of the other forms of Condensers made of less than the usual area.

Water-Channel Condenser.

Mr. Livesey, at the South Metropolitan Works, has adopted the plan of placing the condensing pipes in a tank divided into channels, through which a stream of water is made to flow, and which can be regulated according to the make of gas. The water enters the tank at the point where the condensed gas makes its exit, and, flowing in the opposite direction to the gas in the pipes, is gradually raised in temperature by the latter till it reaches its outlet, where the crude gas enters. By this means a more uniform condensation is obtained than is possible in the atmosphere.

Pelouze and Audovin's Condenser.

The principle of this is different to any of the other apparatus described. In construction it consists of an outer cylindrical castiron chamber, with the usual inlet for gas, and outlets for gas and liquids, and contains a cylinder of perforated sheet-iron constituting the Condenser. The sides of the condensing chamber are two thin sheets of iron with a concentric space between. The inner sheet is perforated with holes 1-20th of an inch in diameter, and the outer with slots of larger size; the outer sheet being so arranged as to offer a blank surface opposite the small holes in the inner sheet. The gas and condensable vapours pass through the small perforations, the vapours being as it were wire-drawn, and striking against the opposite solid surface are deposited thereon, and flow down into the receptacle below, and thence to the tar well.

The gas passes on through the slots in the outer cylinder to the

outlet pipe.

The condensing cylinder is so balanced as to rise and fall in an annular space containing tar or liquor which acts as a seal. As the make of gas increases or decreases, the cylinder rises or falls; and consequently a larger or less number of openings are uncovered for the passage of the gas. The result is a more complete separation of the tar from the gas than is attainable by any other form of Condenser.

Carburetting Condensers.

The Aitken and Young Analyzer, and the St. John and Rockwell apparatus, may both be included under this head, as they are each designed by their inventors to enrich the gas by carburetion. The tar and gas are both conveyed direct from the hydraulic main to the apparatus, their temperature at the inlet being maintained as high as possible, and means are even adopted of raising the temperature, if required, in order that the heavier hydrocarbons present in the crude gas and tar may be permanently suspended, and so become fixed illuminants in the gas, notwithstanding the subsequent reduction of temperature in the ordinary course of purification. At the works where the respective processes have been adopted a good account is given of their efficiency.

Exhibiting the Total Condensing Surface, Maximum Quantity of Gas Passing per Hour, and Condensing

(Compiled from the Referees' Report on the Ammonia Impurity in Gas, June 1, 1871.) Surface per 1000 Cubic Feet per Diem of 24 Hours, at the several London Works named.

Name of Company.			Chartered	Chartered Company.			Imp	Imperial Company.		South Metropolitan Company.
Manufacturing Station, Beckton.	Beckton.	West- minster.	Brick Lane.	Curtain Road.	Black- friers.*	Bow Common.	Fulham.	St. Pan- oras.	Haggers- Old Kens ton. Road,	Old Ken Road.
Total condensing sur- face 82,842	+ Sq. Ft. 82,842	Sq. Ft. 14,866	8q. Ft. 7,744	Sq. Ft. 1,967	Sq. Ft. 18,470	Sq. Ft. 10,864	8q. Ft. † 16,761	Sq. Ft. 98,958	Sq. Ft. 18,564	Sq. Ft. 14,666
Maximum quantity of gas passing per hour 125,000	Cub. Ft. 125,000	Cub. Ft. 200,000	Cab. Ft. 95,000	Cub. Ft. Cub. Ft. 19,000	Cub. Ft. 125,000	Cab. Ft. Cab. Ft. Cab. Ft. Cab. Ft. Cab. Ft. 120,000 860,000 280,000 260,000 130,000	Cub. Ft. 850,000	Cub. Ft. 280,000	Cub. Ft. 250,000	Cub. Ft
Condensing surface per 1000 cubic feet of gas produced per diem of 24 hours	84. Ft. 10·78	84. F	Sq. Ft. Sq. Ft	88. F. E.	8q. Ft.	86 84 85 84 84 85 84 84 84 84 84 84 84 84 84 84 84 84 84	Sq. Ft.	Sq. Ft.	84. F.	Sq. F.

The condensing surface, as given in the table, includes not merely the superficial area of the Condensers proper, but also the whole length of pipes between the hydraulic main and the scrubbers.

* These works are now closed.

† Pipes placed in the ground.

† Pipes placed in a tank of water arranged in channels as before described.

In connection with the subject of Condensation, the following Table, comparing the English and French Thermometers, will be found useful:—

ahr.	Reau.	Cent.	Fahr.	Reau.	Cent.	Fahr.	Reau.	Cent.	Fahr.	Reau.	Cent.
212	80.0	100.0	160	56.8	71.1	108	33.7	42.2	56	10.6	13.8
211	79.5	99.4	159	56.4	70.5	107	83.8	41.6	55	10-2	12.7
210	79.1	98.8	158	56.0	70.0	106	32.8	41.1	54	9.7	12.2
209	78.6	98.3	157	55.5	69.4	105	32.4	40.5	53	9.3	11.6
208	78.2	97.7	156	55.1	68.8	104	32.0	40.0	52	8.8	11-1
207	77.7	97.2	155	54.6	68.3	103	31.5	39.4	51	8.4	10.5
206	77.3	96.6	154	54.2	67-7	102	31.1	38.8	50	8.0	10.0
205	76.8	96.1	153	53.7	67.2	101	30.6	38.3	49	7.5	9.4
204	76.4	95.5	152	53.3	66.6	100	30.2	87.7	48	7.1	8.8
203	76.0	95.0	151	52.8	66.1	99	29.7	37.2	47	6.6	8.9
202	75.5	94.4	150	52.4	65.5	98	29.3	36.6	46	6.2	7.7
201	75.1	93.8	149	52.0	65:0	97	28.8	36.1	45	5.7	7.2
200	74.6	98.8	148	51.5	64.4	96	28.4	85.5	44	5.3	6:6
199	74.2	92.7	147	51.1	63.8	95	28:0	35.0	43	4.8	6.1
198	78.7	92-2	146	50.6	63.3	94	27.5	34.4	42	4.4	5.5
197	73.3	91.6	145	50.2	62.7	98	27.1	33.8	41	4.0	5.0
196	72.8	91.1	144	49.7	62.2	92	26.6	83.8	40	3.5	4.4
195	72.4	90.5	143	49.3	61.6	91	26.2	82.7	39	3.1	8.8
194	72.0	90.0	142	48.8	61.1	90	25.7	32.2	38	2.6	3.8
193	71.5	89.4	141	48.4	60.5	89	25.3	31.6	37	2.2	2.7
192	71.1	88.8	140	48.0	60.0	88	24.8	31.1	36	1.7	2.2
191	70.6	88.3	139	47.5	59.4	87	24.4	30.5	35	1.3	1.6
190	70.2	87.7	138	47.1	58.8	86	24.0	80.0	34	0.8	1.1
189	69.7	87.2	137	46.6	58.3	85	23.5	29.4	33	0.4	0.5
188	69.3	86.6	136	46.2	57.7	84	23.1	28.8	32	0.0	0.0
187	68.8	86.1	135	45.7	57.2	83	22.6	28.3	31	- 0.4	- 0.5
186	68.4	85.5	134	45.3	56.6	82	22.2	27.7	30	- 0.8	- 1.1
185	68.0	85.0	133	44.8	56-1	81	21.7	27.2	29	- 1.3	- 1.6
184	67.5	84.4	132	44.4	55.5	80	21.3	26.6	28	- 1.7	- 1.6
183	67.1	83.8	131	44.0	55.0	79	20.8	26.4	27	- 2.2	- 2.7
182	66.6	83.3	130	43.5	54.4	78	20.4	25.5	26	- 2.6	- 3.8
181	66.2	82.7	129	43.1	58.8	77	20.0	25.0	25	- 3.1	- 3.8
180	65.7	82.2	128	42.6	53.3	76	19.5	24.4	24	- 3.5	- 4.4
179	65.8	81.6	127	42.2	52.7	75	19.1	23.8	23	- 4.0	- 5.0
178	64.8	81.1	126	41.7	52.2	74	18.6	23.3	22	- 4.4	- 5.5
177	64.4	80.2	125	41.8	51.6	78	18.2	22.7	21	- 4.8	- 6.1
176	64.0	80.0	124	40.8	51.1	72	17.7	22.2	20	- 5.8	- 6.6
175	63.5	79.4	123	40.4	50.5	71	17.3	21.6	19	- 5.7	- 7.9
174	63.1	78.8	122	40.0	50.0	70	16.8	21.1	18	- 6.2	- 7.7
178	62.6	78.3	121	39.5	49.4	69	16.4	20.5	17	- 6.6	- 8.8
172	62.2	77.7	120	39.1	48.8	68	16.0	20.0	16	- 7.1	- 8.8
171	61.7	77.2	119	88.6	48.3	67	15.2	19.4	15	- 7.5	- 8.8
170	61.3	76.6	118	38.2	47.7	66	15.1	18.8	14	- 8.0	-10.0
169	60.8	76.1	117	37.7	47.2	65	14.6	18.8	13	- 8.4	-10.5
168	60.4	75.5	116	87.8	46.6	64	14.2	17.7	12	- 8.8	-11.1
167	60.0	75.0	115	36.8	46.1	63	13.7	17.2	11	- 9.8	-11.6
166	59.5	74.4	114	36.4	45.5	62	13.3	16.6	10	- 9.7	-12.2
165	59.1	78.8	113	36.0	45.0	61	12.8	16.1	9	-10.2	-12
164	58.6	73.8	112	35.5	44.4	- 60	12.4	15.5	8	-10.6	-13
	58.2	72.7	111	35.1	43.8	59	12.4	15.0	7	-11.1	-13
168											-14
62	57.7	72.2	110	84.6	43.3	58 57	11.5	14.4	6	-11.5	
61	57.3	71.6	109	34.2	42.7	01	11.1	13.8	5	-12.0	-15

To convert Decrees of Fahrenheit into those of Centigrade and Reaumur, and conversely.

To convert Fahr, into Cent.

RULE 1st.—Substract 82, and divide the remainder by 1.8, thus: Fahr. $\frac{167 - 82}{} = 75$ Cent.

or by-

RULE 2nd.—Subtract 82, multiply the remainder by 5, and divide the product by 9, thus :-

Fahr. $(\frac{167 - 82) \times 5}{9} = 75$ Cent.

To convert Cent. into Fahr.

Rule 1st.—Multiply by 1.8, and add 82, thus:— Cent. $75 \times 1.8 + 82 = 167$ Fahr.

or by-

RULE 2nd.—Multiply by 9, divide by 5, and add 82, thus :— Cent. $\frac{75 \times 9}{5} + 82 = 167$ Fahr.

To convert Fahr. into Reau.

RULE 1st.—Subtract 82, and divide by 2.25, thus:—

Fahr. $\frac{118-82}{2\cdot 25} = 86$ Reau.

or by-

RULE 2nd.—Subtract 32, multiply by 4, and divide by 9, thus:— Fahr. $(118-82) \times 4 = 86$ Reau.

To convert Reau. into Fahr.

RULE 1st.—Multiply by 2.25, and add 82, thus:— Reau. $86 \times 2.25 + 82 = 118$ Fahr.

or by-

RULE 2nd.—Multiply by 9, divide by 4, and add 32, thus:-Reau. $\frac{86 \times 9}{4} + 82 = 118$ Fahr.

NAPHTHALINE.

In dealing with the subject of Condensation, that of the formation or deposition of Naphthaline may be appropriately discussed. This hydrocarbon when deposited in the solid state in the apparatus and mains of a gas-works and in the distributing pipes in the streets, is exceedingly troublesome; sometimes entirely blocking the passage of the gas, and entailing much labour and expense in its removal.

It is generally believed that the presence of Naphthaline in gas is due, principally, to the high heats necessarily used in the carbonization of the coal, owing to the partial distillation of a portion of the tar. In the early days of gas lighting, when iron retorts were used exclusively, and the heats were comparatively low, Naphthaline as now found in the mains in the solid state was almost unknown. It was not until clay retorts came to be employed, and the heat of carbonization was increased, that Naphthaline made its appearance.

It is well known by its flaky crystalline structure, and its peculiar ethereal odour. It is not soluble in water, but easily so in naphtha; hence its removal is effected by steaming with naphtha vapour, or by

pouring that liquid into the obstructed mains and apparatus.

Naphthaline is deposited most freely from gas produced from bituminous coal. Some kinds of coal yield it in greater abundance than others. By using a proportion of cannel along with the coal, the gas being enriched is enabled to retain some or the whole of the Naphthaline in suspension within it in the gaseous condition. The richer the gas, the more capable it is (under ordinary conditions) of retaining the constituents which contribute to its enrichment and vice versa.

In the year 1877 M. Brémond published an account of a series of valuable researches made by him on the question of the formation of Naphthaline and its deposition, in which he showed that (to use his own words) "Naphthaline is produced wherever there is condensation of the aqueous vapours contained in the gas; that its deposition is preceded by the phenomenon of the condensation of the water; and that gas absolutely deprived, as far as possible, of aqueous vapour does not deposit Naphthaline under the ordinary conditions of temperature

and pressure."

It is clear, therefore, that the subject of condensation is one of the utmost importance if Naphthaline, or an excess of it, is to be got rid of. But however perfect the ordinary condensing apparatus may be, it is almost impossible to deprive gas of its aqueous vapour by this M. Brémond therefore adopted other means of drying the means. gas; and for this purpose he employed an ordinary lime purifier, but instead of filling it with slaked or hydrated lime, he charged it with unslaked lime in lumps. By passing the gas through this unslaked lime he completely desiccated the gas, with the interesting result that the aqueous vapour, and consequently the excess of Naphthaline also, was arrested. The gas thus deprived of its moisture was found to have increased in illuminating power to a considerable extent.

This remarkable result of drying the gas had previously been

observed by the first London Gas Referees. They found that the gas

made at Beckton actually gained in illuminating power in traversing the long length of mains from Beckton to London; and they remark as follows: "In considering the satisfactory result of the novel and somewhat perilous enterprise, the Referees are inclined to account for it [the increase in the illuminating power] mainly by the slow and gradual withdrawal of aqueous vapour from the gas in its long journey. This condensation is very different in character from the sudden withdrawal of aqueous vapour produced by the application of great cold, for it takes place very gradually, so that the water is deposited without any appreciable portion of the hydrocarbons being condensed along with it. In order to ascertain the effect of withdrawing the aqueous vapour from gas, we made several experiments by passing the gas through porous chloride of calcium; the result showing that dry gas has a superiority in illuminating power over ordinary gas, to the extent of from 6 to 8 per cent."

The remedy for the objectionable deposit of Naphthaline is thus in the gasmaker's own hands to a great extent. If the gas be dried either by means of chloride of calcium or oxide of calcium (unslaked lime), or by careful and gradual condensation through a considerable length of mains, not only will the after-deposition of Naphthaline be prevented, but there will be a sensible increase in the illuminating power of the

gas so treated.

THE EXHAUSTER.

Wherever the make of gas exceeds 8 millions of cubic feet per annum, an Exhauster becomes a useful adjunct to the other apparatus of a gas-works; the invariable result of its use being to increase the production per ton, to improve the quality of the gas (provided air is not drawn in), and to lengthen the duration of the retorts, by preventing, in a great measure, the deposition of carbon, the removal of which with the ordinary chisel bars is so destructive and unsatisfactory.

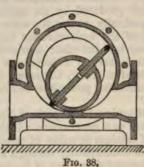
Mechanical Exhausters are of two kinds, the rotatory and the reciprocating. Both descriptions have their advocates, and much may be said in favour of each. The rotatory is certainly steadier in its action, producing less oscillation, the gas flowing more equably through the

mains and apparatus.

Beale's (the early form of which is shown in Fig. 38), Jones's (Fig. 39), and Laidlaw's (Fig. 40) are on the rotatory principle; Methven's, Musgrave's, Anderson's (Fig. 41), and Dempster's are reciprocating.

The steam-jet Exhauster (Fig. 42), invented by Mr. Cleland, and improved by Körting Brothers, is another form of exhausting apparatus. This operates by projecting a jet of steam, at about 45 lbs.

pressure, through an arrangement of pipes or nozzles, without the intervention of any other mechanical appliances—the steam being afterwards extracted by condensation. The capacity of the Exhauster is regulated by the adjustable screw and spindle at the end; and by a movable inner sleeve, opening or closing the port holes by means of the screw and nut at the side.



Mr. R. O. Paterson found a gain in illuminating power equal to 3ths of a candle from using this Exhauster, which he attributed to the steam having volatilized some of the liquid hydrocarbons.



Fig. 40.

Beale's form of Exhauster is the one now usually adopted and whilst the original type is retained, great improvements have been effected in its construction and working by various makers of recent years—notably by Gwynne and Co., B. Donkin and Co., W. H. Allen and Co., and G. Waller and Co.

The essential features of a good Exhauster are that it should

work with a minimum of friction and power, that it should give the steadiest possible flow of gas, and that the parts should be

perfectly gas-tight. Beale's Exhauster, when well constructed, satisfies these conditions. The commonest fault is the want of tightness, and when it is remembered that, under a pressure equal to a 14-inch column of water, about 9000 cubic feet of gas will pass per hour through an opening of only one square inch in area, the absolute necessity of the best workmanship only, being used in Exhausters, will be evident.

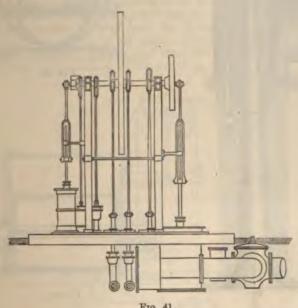
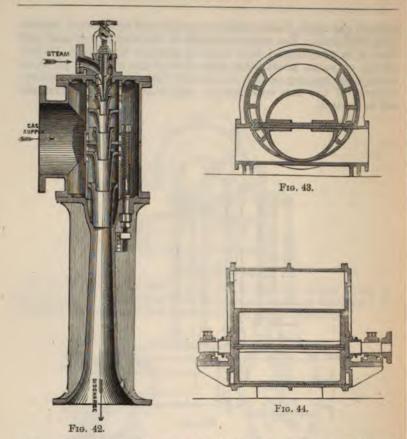


Fig. 41.

The apparatus (Beale's) consists of a cylinder, inside which a drum revolves, and is provided with pistons on slides which have a radial motion. The drum is smaller in diameter than the inside of the cylinder, and the centre lines or axes of both are parallel and horizontal; but the drum is placed eccentrically in the cylinder, so as to be in contact with it at the bottom without resting on it. The inlet and outlet passages are on the two opposite sides of the cylinder, and as the slides are guided by segments in the end plates, so that their outer ends are always in contact with the inside of the cylinder, the gas enters one side, is carried round over the drum to the other side, and is forced out at the outlet.



The illustrations Figs. 43 and 44 show sections of a Beale's Exhauster as made by Gwynne and Co. under their patents, and containing several improvements on the machine as first invented, by which the areas of wearing surfaces have been augmented so as to greatly increase the durability of the machine. These include the double slides, large segments, steel pins fastened in the segments and extending through the whole length of the slides, and the outside bearings for the axle.

The apparatus may be driven either by a strap from a line shaft actuated by a steam or gas engine, or, what is preferable, by a steamengine coupled direct. By employing two Exhausters, and working

them from one engine, the slides of the Exhausters being placed at right angles to each other, a perfectly steady vacuum and pressure are maintained.

Exhauster Governor.

When an Exhauster is employed, it is necessary to supplement its use by a gas Governor, acting either on a throttle valve within the steam feed-pipe, in this case increasing or diminishing the speed of the engine, or on a valve within a bye-pass connected to the inlet and outlet mains leading to and from the Exhauster, the opening of which, when the exhaust is too active, allows a portion of the gas to return through the Exhauster, and thus prevents the formation of a partial vacuum in the retorts. (See Fig. 45.)

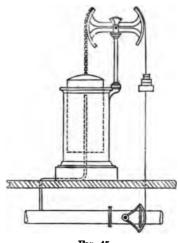


Fig. 45.

STEAM BOILER AND ENGINE.

These should be provided of ample size, allowing a margin over and above the actual power needed. An Engine and Boiler barely fit to do the work required of them are a nuisance.

The Engine, besides turning the exhauster, may be used in pumping water and tar; and the Boiler, in addition to supplying steam

for the Engine, is useful for steaming the mains and apparatus on the

Duplicate Boilers of the required size should be provided, to allow for periodical cleaning and examination.

For firing the Boiler, breeze may be used, mixed with a portion of

coke or coal.

One pound weight of coal of average quality requires 150 cubic feet of air for its perfect combustion. In actual practice, however, about double this quantity of air passes through the furnace of steam Boilers.

Wherever practicable and convenient, the Boiler should be set in such a position as to allow of its being heated with the waste heat from the retort-stack.

In small works, if a steam Boiler cannot be employed for want of space, or should a Boiler be considered objectionable on other grounds, the Exhauster can be driven by a Gas-Engine.

The kind of Boiler most suitable for a gas-works of moderate size is the cylindrical, with flat ends, and single internal tube containing the

furnace. The nominal horse power of such a Boiler is found by multiplying the sum of the diameters of the outer shell and internal flue by the length, and dividing the product by 6.

Example.—Required the power of a Boiler whose diameter is 4 ft. 6 in., diameter of tube 2 ft. 6 in., and length 12 ft.

$$(\frac{4' \ 6'' + 2' \ 6'') \times 12'}{6} = 14$$
-horse power.

Again-

Required the power of a Boiler whose diameter is 6 ft., diameter of tube 3 ft., and length 20 ft.

$$\frac{(6' + 3') \times 20'}{6} = 80$$
-horse power.

Cement for Stopping Leaks in Boilers.

By Weight. Powdered fire-clay . . 6 parts. Fine iron filings . . Made into a paste with boiled linseed oil.

In high-pressure or non-condensing Engines, with-

Steam at 25 lbs. per square inch, $13 \cdot 6$ circular inches on piston = 1 horse-power Do. 30 lbs. do. do. do.

The diameter of the piston in inches, squared = circular inches. The following table gives the diameter of cylinders for high-pressure (non-condensing) Steam-Engines, from 3 to 16 horse power, with steam at 25 lbs. and 30 lbs. per square inch respectively, and the length of stroke for the different sizes—

Nominal		of Cylinder iches.	Length	Nominal		of Cylinder ches.	Length
Horse Power.	Steam per 8	Square Inch.	Stroke.	Horse Power,	Steam per S	quare Inch.	Stroke.
-	25 lbs.	80 lbs.	Inches.	Parcel of the Pa	25 lbs.	30 lbs.	Inches.
3 34 4	6½ 6¾ 7¾	6 61 62	12 12 14	8 8 9	10½ 10½ 11½	9½ 9½ 10½	20 20 22 22
4½ 5 5½	63 74 72 84 84	7½ 7½	14 16 16	10 11 12	11½ 12½ 12½ 12¾	101 111 119	22 24 24 26
6 64 7 74	9 94 94 101	71 81 81 81 9	18 18 18 20	18 14 15 16	13¼ 18¾ 14½ 15	12± 12± 13 13±	26 26 28 30

Cement for Metallic Joints.

Equal weights of red and white lead, mixed with boiled linseed oil to the consistency of putty.

THE WASHER.

The Washer was one of the very earliest appliances used in the purification of coal gas, and naturally so, owing to the cooling and condensing property of water, and its power of absorbing ammonia and of arresting the tar.

Its construction, however, was often faulty at first, and the limits of its functions misunderstood; so that the misuse, or overuse, of the apparatus, resulting in reduced illuminating power to the gas exposed

to its action, caused it to fall for a time into disrepute.

The principle of its action is that of causing the gas to pass in finely-divided streams through a body of water contained in a vessel, so that a portion of the ammonia and other gaseous impurities, and the whole of the floating particles of tar which have escaped condensation, may be removed before the gas enters the scrubbers.

The Washer should always be used in conjunction with the scrubber,

and the gas passed through it in the first instance.

When the Washer is exposed to outside atmospheric influence, it is necessary in winter to employ means to prevent the water from falling below a temperature of 50° Fahr.; otherwise the gas, especially a rich

gas, passing through it will suffer deterioration.

The Washer is generally employed as a separate and distinct apparatus; but sometimes it is placed at the bottom of the tower scrubber, of which it constitutes a part.

All Washers give an amount of back pressure, varying from 1 to 4 inches, according to the depth of water traversed. There are numerous

designs of Washers, but the principal ones are here described.

Anderson's Washer.

The persistent advocacy of Mr. George Anderson has done much to restore the Washer to favour, and his form of the apparatus is still one of the best.

It consists of a cast-iron outer vessel, containing a number of trays, having on their under side a series of serrated bars extending from side to side; these dip into the water or liquor, and the gas, in passing through the serrations is divided into minute globules. The pressure given can be regulated by raising or lowering the overflow with which the apparatus is provided. A four-way valve is used for shut-off and bye-pass. Weak liquor from the condenser is run in at the top, and drips from tray to tray till it reaches the bottom. The Washer is made either single or double as required.

Cathels' Washer.

The usual oblong or square vessel in this case is divided into sections as many as may be desired, each elevated higher than the others in the form of steps. The gas enters at the bottom, passes in divided streams through a number of curtain serrations extending the full length of the vessel, and so on through the rest, and out at the top of the higher compartment. When the liquor in the lowest section is of the strength required, it is run off, and the contents of the several sections transferred one step lower, the last or uppermost being charged with fresh water.

This Washer is also arranged in the vertical form to occupy less

ground space.

Livesey's Washer.

This is a compact and efficient apparatus, occupying less room for

the work done than any other.

In a rectangular cast-iron box of any size (depending on the make of gas) is a series of rectangular tubes of wrought-iron, to which wrought-iron perforated plates are fastened, turned down at the sides till they dip into the liquor. The perforations are 1-20th of an

inch diameter, and 1-5th of an inch apart.

The gas passes down between the tubes and through the side perforations into spaces filled with liquor, and, bubbling upwards, is again broken up by finding its way through the horizontal perforations into the open space above, and so along to the outlet of the apparatus. Means are provided for securing an active circulation of the liquor, which is constantly flowing through it from the adjacent scrubber, and away by an overflow to the well.

THE SCRUBBER.

The Tower Scrubber (Fig. 46) is a cast-iron vessel, either rectangular or cylindrical (the latter shape being preferred), erected on end, through which the gas is made to pass in an upward direction after issuing from the washer.

Its primary use is to entirely purify the gas from ammonia by the aid of water; advantage being taken of the well-known great affinity

of ammonia for that liquid.

Water, at mean temperature and pressure (60° Fahr., barometer 30'), dissolves 783 times its volume of ammoniacal gas—that is, undiluted ammoniacal gas. When the latter is mixed with other gases, as in the case of coal gas, the power of water to arrest it is not nearly so great.

It also arrests a considerable proportion of the sulphuretted

hydrogen and carbonic acid.

This is accomplished by filling the vessel wholly or in part with either coke, boulder-stones, brick-bats, roof or draining tiles, furze, or layers of thin boards set on edge, about 5 to 7 inches in width, \$\frac{3}{8}\$ths of an inch thick, and from \$\frac{1}{2}\$ to \$\frac{3}{4}\$ of an inch apart; the material being kept constantly moistened by a stream of water trickling from a suitable distributing apparatus fixed in the crown.

When the coke or other material is placed in layers, it is supported on grids fixed at convenient distances apart; and opposite each space a manhole, secured by a movable lid or cover, is provided, so as to afford access to the interior, either for examination or renewal of the

contained material.

The original Livesey Scrubber is fitted with boards of an inch thick, 11 inches wide, placed on edge, and kept apart by strips or blocks of wood \(^3\) of an inch square; thus making one board to 1 inch. The tiers are separated by 2-inch square cross sleepers.

The first cost of filling with boards is greater than when coke or

other material is employed; but it possesses the marked advantage of not fouling up, and will rarely or never need renewing. The gas cannot form narrow channels in its passage through the vessel, but is constantly being broken up, and brought in contact with the water that drips from all sides.

Open Scrubbers are also used without any of the materials above mentioned. In such cases the column of gas in its upward progress

is met by a descending shower of spray from a Gurney jet.

The most efficient kind of Scrubber is the cylindrical, standing in height about six or seven times its diameter.



Fig. 46.

The superiority of the Tower Scrubber is due, principally, to the fact that in this apparatus, more than in any other, there is lengthened contact of the gas with the water or liquor in a minute state of sub-division. Height is therefore an important factor in a Scrubber.

Tower Scrubbers are most economical and effective when they are used in duplicate (Fig. 46); the gas being made to pass through

first one, and then the other.

Where more than one pair of Scrubbers is employed, as is the

case in many considerable works, the gas should be distributed in equal quantities through the several pairs simultaneously—not through each in succession.

Experience has proved that the best filling material is thin roughsawn boards, as before described, placed in alternate layers, on edge,

one over the other.

When coke is used as the scrubbing material, it may be placed in six or eight layers, with a space of about 6 inches between each.

Whatever material is used in filling the Scrubber, it is important that all parts of its surface should be wetted as equally as possible. The proper action of the Scrubber depends on this.

The necessity of a good water-distributing apparatus is therefore apparent. Not only should this be of good construction in the first instance, but it should always be maintained in efficient working

order.

The gas enters at the bottom of the vessel, and the water or liquor at the top. The gas in travelling upwards is completely broken up, fresh surfaces being constantly presented to the descending drip, and to the wetted sides of the filling material, against which it is rubbed or "scrubbed" all the way up, until it emerges by the outlet at the top. A trapped overflow at the bottom conveys the liquor either to the washer or to the tar well.

The gas, before entering the Scrubbers, should have the whole of the tar eliminated from it; and to insure this, a washer may be employed. The washer can be conveniently placed at the bottom of the first

Scrubber.

The weak ammoniacal liquor from the hydraulic main and condenser, and from the second Scrubber, should be employed in the first Scrubber. The object of this is to arrest a proportion of the carbonic acid and sulphuretted hydrogen, as well as the other sulphur compounds, for which ammonia has a strong affinity, thus relieving the lime and oxide purifiers, and saving labour and purifying materials. The weak liquor is also by this means brought up to the requisite commercial strength.

Fresh water, in the proportion of two to three gallons per 1000 cubic feet of gas passing, is used in the second Scrubber, to remove the last vestige of ammonia. It also takes up a considerable pro-

portion of the deleterious gases above named.

One method frequently adopted of applying the water or liquor is by a pipe passing through the crown or side of the vessel, from which pipe smaller tubes, pierced with holes, radiate towards the circumference. This may be either fixed or revolving; the latter being the most efficient.

Mr. Mann, who has bestowed much attention to this subject, with

most satisfactory results, makes the uppermost part of his Scrubbers about 2 or 3 inches wider than the rest, in order that the sides of the vessel may be wetted as well as the contained material. In this wider portion of the Scrubber, and underneath the distributing tubes, he has a revolving layer of birchwood twigs lessening in depth towards the circumference, and the water falling upon this is equally distributed throughout. This arrangement requires the use of a small engine and gearing to produce the slow rotary motion.

To obviate the necessity for an engine, a Barker's mill or other similar appliance is sometimes used for producing the required motion; but as the stream of water necessary to keep this in constant action would be too great for scrubbing purposes, the mill is usually fed intermittently from a tilting box, or a vessel holding several gallons of water, and fitted with a valve and float. Where the quantity of liquor passing is large, as may be the case in the first Scrubber.

a small turbine may be adopted for turning the distributor.

Note.—The action of the Barker's mill is due to the pressure of water being equal and acting in contrary directions. The rotary portion of the machine revolves about its vertical axis. This consists of a shaft or spindle working in suitable bearings, and passing through a cylinder open at the upper end, which is fed by a stream of water. Near to the bottom of this cylinder, horizontal radiating tubes are fixed, and on one side of these, holes are drilled for the outlet of the water. The pressure at these points being removed, acts only on the opposite side, so causing the mill to revolve, the velocity increasing with the height of the liquid and the size of the apertures.

Tower Scrubbers should have an aggregate cubical volume of at least 9 feet for each 1000 cubic feet of gas made per day of 24 hours, taking the maximum production as the basis of the calculation. For example, take a works producing in the depth of winter 600,000 cubic feet of gas per day of 24 hours:—

Then.

 $600 \times 9 = 5400$ feet, cubical volume required.

This would be supplied by

2 Scrubbers, each 8 ft. diameter, and 56 ft. high.

Or again, take a works producing 1,000,000 cubic feet per day:

Then,

1000 × 9 = 9000 feet, cubical volume required.

This would be supplied by

2 Scrubbers, each 10 ft. diameter, and 58 ft. high.

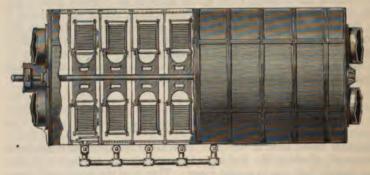
ANDERSON'S COMBINED WASHER AND SCRUBBER.

A combined Washer and Scrubber, the invention of Mr. George Anderson, consists of a rectangular cast-iron vessel, standing on end, and in height about five times its width. The vessel is divided into compartments, each of which contains a drum caused to revolve by suitable gearing. The circumference of each drum is fitted with a brush of whalebone or other fibre. These fit exactly into the space allotted for them, and, in revolving, dip into the liquid which partially fills the several divisions. The Scrubber stands on one of Mr. Anderson's Washers, previously described (p. 117). A small stream of pure water, at the rate of 10 to 12 gallons per ton of coal carbonized, is kept flowing into the top compartment through a funnel and sealing tube. and gradually descends by way of the gas-pipes connecting the chamber till it enters the Washer, from which there is an overflow pipe to the well. The gas enters the Washer at the bottom, and is first relieved of the tar remaining after condensation; thence it passes through the revolving brushes, meeting different strengths of liquor in each division, till it reaches the upper one containing pure water, and away by the outlet. By this means the whole of the ammonia, and a large proportion of the other impurities, is removed.

THE WASHER SCRUBBER.

Another useful form of Scrubber, or Washer-Scrubber as it has been designated, of which Mr. Paddon's apparatus is the original type, has come largely into use in recent years. This is of the horizontal form, rectangular in sectional plan, and consists of a cast-iron tank or vessel, usually in sections, containing water or liquor, in which a series of perforated discs, or volutes of sheet-iron, or chambers containing wood balls, or other filling medium exposing a large surface, are made to revolve on a central shaft, at a slow speed. These, as they rise from the liquid, are completely wetted on both sides, and the crude gas passing through or amongst them, coming in contact with the wet surfaces, is deprived of its ammonia and a portion of the other objectionable compounds. The clean or fresh water entering at one end, and flowing through the different divisions, is met by the gas which enters at the opposite end, and gradually increases in strength till it issues from the final compartment as 10 or 12 ounce (5° or 6° Twaddel) ammoniacal liquor. Kirkham, Hulett, and Chandler's Standard" Washer-Scrubber, Fig. 47, and Laycock and Clapham's "Eclipse" Washer-Scrubber, Fig. 48, are of this type.





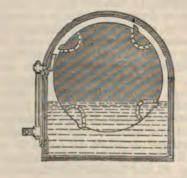
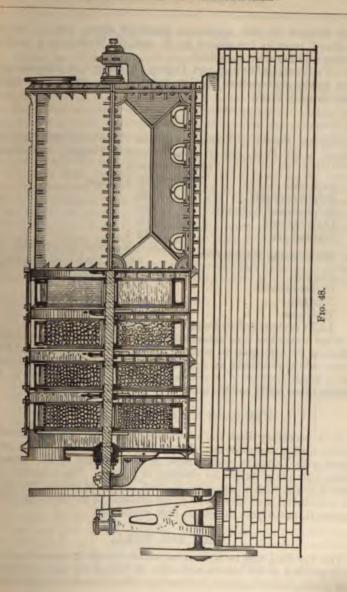




Fig. 47.



In addition to the apparatus described above, the "Purifying Machine" recently introduced by C. and W. Walker, is a powerful Washer and Scrubber combined.

Ford's Scrubber-Washer and Cockey's Washer are compact apparatus, producing excellent results, and these do not require motive

power to work them.

TABLE

Showing the Number of Volumes of Various Gases which 100 Volumes of Water, at 60° Fahr. and 30 inches Barometric Pressure, can absorb.

(Dr. Frankland.)

Ammonia			78,000 volumes.
Sulphurous acid.			3,300 ,,
Sulphuretted hydro	ogen .		253 ,,
Carbonic acid .			100 ,,
Olefiant gas			12.5 ,,
Illuminating hydro	carbon	s	Not determined, but probably more soluble than olefiant gas.
Oxygen			3.7 volumes.
Carbonic oxide .			1.56 ,,
Nitrogen			1.56 ,,
Hydrogen			1.56 ,,
Light carburetted	hydrog	en	1.60 ,,

When water has been saturated with one gas, and is exposed to the influence of a second, it usually allows a portion of the first to escape, whilst it absorbs an equivalent quantity of the second. In this way a small portion of a not easily soluble gas can expel a large volume of an easily soluble one.

BYE-PASS MAINS AND VALVES.

It is necessary that the condenser, exhauster, washer, scrubber, station-meter, and governor, should be provided with Bye-pass mains, closed with Valves or water-traps, to allow of any of the apparatus being put out of action for cleaning or repairs. The exhauster Bye-pass is closed with a flap-valve, so that, in case of sudden stoppage of the machinery, the Valve opens by the pressure of the gas being thrown against it, and allows the gas to flow unchecked.

THE TAR WELL.

The Tar Well may be built either of bricks laid in cement, and carefully puddled at the bottom and sides, or formed of cast or wroughtiron plates, bolted together, and having either planed or caulked joints.

The iron vessel is preferable where the construction of a good foundation is likely to be a question of great expense.

It should be of capacity sufficient to contain six weeks' make of

material, reckoning from the maximum daily production.

Another Well of smaller dimensions, the size depending on the magnitude of the works, ought to be provided, to serve as a lute or seal, into which the tar-pipes from the different apparatus should dip. From this, at a depth of about 15 or 18 inches below the surface of the ground, an overflow-pipe or channel conveys the condensed products

into the larger reservoir.

In some works the tar-pipe is taken direct from the hydraulic main into the large Well, and there sealed by being made to dip into a vertical pipe secured to the bottom of the tank. This is objectionable, as, in case of stoppage, it is difficult of access. Again, there is always the liability of an escape of gas from that portion of the pipe within the Well; further, where flushing of the hydraulic main is practised, the rushing liquor carries with it a quantity of gas which is liberated within the Well. It is also important that the tar should be cooled somewhat before entering the larger receptacle, because hydrocarbon vapour is given off from it at a temperature of about 90° Fahr.

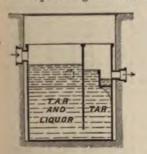


Fig. 49 .- VERTICAL SECTION.

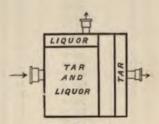


Fig. 50.—Plan.

and above. In each of these cases the gas or vapour, mixing with the contained air within the Well, would explode with disastrous consequences on contact with a light. Accidents which have occurred have been due to one or other of these causes.

In all cases the Wells should be covered over to exclude surface and rain water, and prevent the possible loss of ammonia by evaporation.

In addition to the underground Tar Well, an elevated cast-iron Cistern is indispensable in a well-appointed gas-works. Into this the tar and liquor are pumped from the underground Well, and suitable draw-off pipes, furnished with stopcocks or valves, serve to discharge

the material into the barrels, trucks, or barges of the purchasing contractor.

The Cistern may be divided in two by means of a partition plate reaching to within about 6 inches of the top, over which the ammoniacal liquor will flow, separating itself from the tar by reason of its

lower specific gravity.

A tar and liquor Separator, for placing in the ground in any convenient position near to the underground Well, is shown in sectional elevation and plan in Figs. 49 and 50. It consists of a cast-iron vessel, about 4 feet square and $4\frac{1}{2}$ feet deep, for a considerable sized gas-works. The division plate extends from the top of the vessel to within 4 inches of the bottom; the diaphragm, over which the tar escapes into its separate Well, being placed $1\frac{1}{2}$ inches lower than the other diaphragm for the ammoniacal liquor.

TABLE.

Contents of Circular Tanks or Wells in Gallons for each Foot in Depth.

Diameter, Ft. In.	Gallons for each Foot in Depth.	Diameter. Ft. In.	Gallons for each Foot in Depth.	Diameter, Ft. In.	Gallons for each Foot in Depth.
9 0	397.6	16 6	1336-4	24 0	2827 • 4
9 3	420.0	16 9	1377-2	24 3	2886 - 7
9 6	443.0	17 0	1418-6	24 6	2946.5
9 9	466.6	17 3	1460.7	24 9	3006.9
10 0	490.9	17 6	1503.3	25 0	3068-0
10 8	515.7	17 9	1546.6	25 8	3129.6
10 6	541.2	18 0	1590.4	25 6	3191.9
10 9	567.3	18 3	1634.9	25 9	3254.8
11 0	594.0	18 6	1680.0	26 0	3318.3
11 3	621.3	18 9	1725.7	26 3	3382.4
11 6	649.2	19 0	1772.1	26 6	3447 2
11 9	677.7	19 3	1819.0	26 9	3512.5
12 0	706.9	19 6	1866.6	27 0	3578.5
12 3	736.6	19 9	1914.7	27 3	3645.1
12 6	767:0	20 0	1963.5	27 6	3712.2
12 9	798.0	20 3	2012.9	27 9	3780.0
13 0	829.6	20 6	2062 • 9	28 0	3848.5
13 3	861.8	20 9	2113.5	28 3	3917.5
13 6	894.6	21 0	2164.8	28 6	3987.1
18 9	928.1	21 3	2216.6	28 9	4057.4
14 0	962.1	21 6	2269 1	29 0	4128 3
14 3	996.8	21 9	2322.1	29 3	4199.7
14 6	1032 · 1	22 0	2375.8	29 6	4271.8
14 9	1068.0	22 3	2430.1	29 9	4344.6
15 0	1104.5	22 6	2485.0	30 0	4417.9
15 8	1141.6	22 9	2540.6	80 8	4491.8
15 6 15 9	1179.3	23 0	2596.7	30 6 30 9	4566 4
	1217.7		2653.5		4641 5
16 0 16 3	1256·6 1296·2	23 6 23 9	2710·8 2768·8	31 0 31 3	4717·3 4793·7

PURIFICATION.

The Impurities in Coal Gas.

The chief impurities present in coal gas, in its crude or raw and unpurified state, at the time it leaves the retorts, are tar vapour, ammonia, carbonic acid, sulphuretted hydrogen, and other sulphur compounds, notably bisulphide of carbon.

The first-named impurity, tar vapour, begins to condense and is partially removed in the hydraulic main and pipes leading to the condensing apparatus, where, if this is of sufficient capacity, and otherwise adapted to the performance of the work required of it, it is nearly all removed. What remains is taken out by the washer.

The ammoniacal gas, of which there is about 1 per cent. by volume, also begins to separate from the crude coal gas in the hydraulic and toul mains, combining with the moisture distilled from the coal. In the condenser and washer a further portion is removed; and in the scrubbers, if these are as efficient as they ought to be, or can easily be rendered, the whole of the remaining ammonia (amounting to shout 15 per cent) is extracted

about ·15 per cent.) is extracted.

The hydraulic and foul mains, condensers, washers, and scrubbers are also efficacious in removing a portion of the carbonic acid (existing in the gas to the extent of about 2·5 to 3 per cent.), sulphide of hydrogen or sulphuretted hydrogen (from 1 to 2 per cent. of which is contained in the gas), and bisulphide of carbon; but the bulk of these three latter impurities still exists in the gas after leaving the scrubbers,

and is carried forward to the Purifiers.

These are charged either with hydrate of lime or hydrated peroxide of iron, or a combination of both substances, arranged in separate layers or tiers within the several vessels.

Purification by means of Lime (Oxide of Calcium).

The lime has a perfect and strong affinity for carbonic acid and sulphuretted hydrogen, and accordingly it entirely removes these compounds from the gas, without leaving the slightest trace of their presence. The lime, however, in its state of oxide of calcium, has no affinity for the bisulphide of carbon, so that the greater proportion of this impurity (all, except such part as is removed by the foul lime when in the state of sulphide of calcium), is carried forward into the holders.

Preparation of the Lime.

Cream or milk of lime was used in Purifying in the early days of gas manufacture, and though this was thoroughly efficient, and is

probably the most economical method of employing the lime, it has been generally discarded on account of the obnoxious character of the refuse material, "blue billy," as it was called, and the difficulty of getting rid of it. Lime in the hydrated state is now generally

adopted.

The lime should be prepared by being slaked with clean water a day or two before it is required for use. If placed in the Purifiers before this necessary interval has elapsed, it is liable to cake or become more compact than it otherwise would. On the other hand, hydrate of lime absorbs carbonic acid from the atmosphere, and its Purifying power is nullified in proportion to the extent of such absorption. It should not, therefore, be prepared for any great length of time before it is needed.

It is a common mistake to place the prepared lime in the Purifiers in a comparatively dry and almost powdery state. Lime used in this condition is less effective than when thoroughly moistened. It is also a wasteful method of using the lime, as a large proportion of the material will be found unspent and almost untouched by the impurities, when the vessel requires to be changed. The finely-divided lime is also more liable to cake than the other, and thus increase the back pressure. When the production of gas is great, as in the depth of

winter, these disadvantages are strongly felt.

Mr. Forstall's instructions for preparing the lime are excellent. After it has been thoroughly well watered, "a simple and effective means of gauging the proper degree of moisture, and securing its uniformity throughout the whole charge of lime operated upon, is to pass the slaked lime through a wire screen, with an open mesh of one square inch area, placed at an angle of 70° with the floor. screening reduces the lumps to granular pellets of irregular form and size, the largest not exceeding the bulk of a small hickory nut. The proper degree of moisture is that beyond which any excess will cause the 'dough' to adhere to the screen instead of breaking through. Slight variations of moisture in different portions of the charge are corrected by the thorough mingling of the whole in the screening. The pellets do not adhere to one another spontaneously, but can be shovelled into barrows, and reshovelled into the Purifiers without losing their independence; but the slightest compression and working in the hand resolves them immediately into adhesive putty. The lime in this state is so penetrable to gas, that lumps as large as walnuts are thoroughly saturated, even when lying loosely upon the surface of the layers." The weight of the lime prepared in the manner described, and ready for the Purifiers, is 92 lbs. to the bushel.

Quick lime nearly doubles in bulk on being slaked.

From 90 to 140 lbs. of quick lime, reduced to a hydrate, are required

in the Purification of the gas produced from 1 ton of cannel, and from

60 to 80 lbs. of that produced from 1 ton of coal.

Mr. Hislop has patented a process of calcination in suitable kilns, by which the spent lime is converted into quick lime to an almost unlimited extent, and at considerably less cost than new lime. A nuisance is thus got rid of, and further economy in Purification effected.

Purification by means of Hydrated Peroxide of Iron.

Oxide of iron possesses the property of combining with the sulphuretted hydrogen, but it has no affinity for carbonic acid and bisulphide of carbon; hence when this oxide is used exclusively, the two latter named impurities are still present in the gas as supplied from the holders. This remark, however, needs some qualification. As oxide of iron, pure and simple, it has no affinity for bisulphide of carbon and other sulpho-carbon compounds, but, from the observations made at the several metropolitan gas-works, Mr. R. H. Patterson (one of the Referees) deduced the interesting fact that the sulphur which is present in a state of minute division in the oxide of iron, after the latter has been in use for some time and frequently revivified, possesses the power of arresting a portion of the bisulphide of carbon.

The hydrated peroxide of iron may be either the natural oxide, bog iron ore, as it is called, found largely deposited in some of the bogs in Ireland and elsewhere; or the artificial oxide, obtained as a waste

product from various processes of the manufacturing chemist.

Oxide of iron possesses this advantage over lime: After it has been in the Purifier, and has taken up its quantum of sulphuretted hydrogen, it can be revivified on exposure to the air. Accordingly, when this material is used, a floor has to be provided on which it can be spread out, and turned over for revivification. At the Manchester Gas-Works, a horse and plough are employed for turning over the foul oxide.

When taken out of the Purifier it is sulphide of iron, of a dense black; and after exposure it changes to its original reddish brown colour, oxygen having been taken up, and sulphur deposited in the free state in the mass. When the sulphur is found in it to the extent of about 40 to 60 per cent. by weight (the proportion depending on the quality of the oxide), the material is sold to the manufacturing chemist, and replaced by fresh oxide.

In using fresh oxide of iron, it is necessary to exercise certain precautions. The foul material, on its exposure to the air for the first two or three times, absorbs oxygen so rapidly as often to generate very intense heat, the whole mass frequently becoming red hot. Should this occur in the Purifiers, the danger is considerable, and

the wood grids may be completely destroyed. Whenever, therefore, a Purifier containing such new oxide has been put out of action, it should be *emptied without delay*. The danger of ignition may be overcome by mixing the new oxide with a proportion of the spent.

Foul oxide should not be spread out immediately on being removed from the Purifiers. If it is allowed to remain in the heap for a space of 12 to 24 hours, and then distributed over the floor, the revivification is more complete, whilst the liability to ignition is reduced.

Average Composition of the Richer Descriptions of Native Bog Ore for Purifying Purposes, dried at 212° Fahr. (King's Treatise):—

As generally used, the material contains 30 to 40 per cent of water.

Purification by means of Oxide of Calcium (lime), Sulphide of Calcium (foul or spent lime), and Oxide of Iron.

Lime alone, or the lime and oxide of iron, when properly applied, are capable of freeing the gas entirely of the whole three impurities—carbonic acid, sulphuretted hydrogen, and bisulphide of carbon. This brings us to the method of Purifying expounded by the Referees in their Report to the Board of Trade on Sulphur Purification at the Beckton Gas-Works, January 31st, 1872; and also by Dr. Odling, somewhat more in detail, in his lecture on Sulphide of Carbon, delivered at the Annual Meeting of the British Association of Gas Managers, held in London, in June, 1872.

To accomplish this perfect Purification in accordance with the suggestions made by Dr. Odling, three sets of Purifiers are required; the gas passing through the first set into the second, and on to the third, from which it makes its exit through the station-meter into the

holders. The modus operandi is as follows :-

Let it be assumed that three sets of Purifiers, consisting of four vessels each, are employed. Nine of these are constantly in action, three being at rest (one from each set), for the purpose of changing or revivifying the Purifying material.

The first and second sets are charged with lime, the third set with

oxide of iron.

Say the whole nine are newly charged. On the gas from the scrubbers entering the first set, the lime is acted on by the carbonic acid and sulphuretted hydrogen simultaneously, leaving the bisulphide of carbon at the beginning of the process to pass unabsorbed. After they have worked for some time, the sulphuretted hydrogen in the first set is gradually expelled by the incoming carbonic acid, for which the lime has a stronger affinity. The second set is now being fouled with sulphuretted hydrogen, the lime being wholly or in part changed in character, having become sulphide of calcium, in which state it has an affinity for, and consequently arrests, the bisulphide of carbon; whilst the unabsorbed sulphuretted hydrogen passes on to be taken up by the oxide of iron with which the final set of Purifiers is charged. By the application of the proper tests at the several sets of Purifiers, the time for changing the material is ascertained.

The question of supplying gas entirely free from sulphur in any form is a formidable one for gas companies; not so much because of the cost (though that is considerable) of erecting the additional sets of Purifiers, as from the difficulty of providing the necessary ground space for their erection. In new works about to be constructed, the thing is easily arranged; but in the majority of works already established, it would not be easy to carry the system into effect.

As regards the question of cost, a careful estimate shows that to adopt the extended method of Purifying as enunciated, would entail an outlay of additional capital equivalent to close upon 2d. per 1000

cubic feet of gas sold.

The property of absorbing or arresting bisulphide or disulphide of carbon possessed by the sulphide of calcium, was known by chemists and some observant managers of gas-works for a period considerably anterior to the date of the publication of either the able report of the Referees, or of the valuable lecture of Dr. Odling, and the principle of Purification, therein recommended, acted on to some extent. Dr. Letheby, in a paper communicated to the British Association of Gas Managers in 1870, speaking of the mode of Purification pursued at the Great Central Works, after referring to the scrubbers, goes on to say, that "the gas is then passed through a series of dry lime Purifiers, which present a very large surface for absorption; and the lime is purposely left in the Purifiers after it has become foul, and until a good deal of the sulphuretted hydrogen first absorbed is displaced by carbonic acid. In this manner the natural affinity of sulphide of calcium for bisulphide of carbon is permitted to act, and much sulphur, in this objectionable form, is retained. Leaving the lime Purifiers, the gas, which is still charged with more or less of sulphuretted hydrogen, is passed through oxide of iron The chemical effect of these operations is very intelligible, for sulphide of ammonium (in the scrubbers, &c.) and sulphide of calcium

are both endowed with the power of combining with bisulphide of carbon, and therefore of absorbing and fixing this objectionable impurity. It is manifestly then of the greatest importance that coal gas should be kept in contact with these substances as long as possible during the process of Purification . . . In the case of sulphide of calcium, it should be permitted to act for some time after the lime has become foul, for it is in this condition that it is most effective, and a lime Purifier should not be changed until the sulphuretted hydrogen of the foul lime is largely displaced by the carbonic acid of the raw gas. If it be necessary to use oxide of iron on account of the difficulty of disposing of foul lime, it should be used after the lime."

It remained, however, for Mr. R. H. Patterson to show, which he did conclusively, that this complete Purification can only be successfully attained by first extracting the carbonic acid, as, until that is entirely removed from the crude gas, it is impossible to obtain the sulphide of calcium in sufficient quantity or condition to arrest the

bisulphide of carbon.

CLASSIFICATION

Of the best known Limestones of this Country, in the Order of their Purity and which Order also expresses their Value for the purpose of Purifying Coal Gas. (Hughes.)

1. The white chalk limestone of Merstham, Dorking, Charlton, Erith, and other parts of the chalk range surrounding the metropolis.

The grey chalk limestone, from the lower beds of chalk.
 The blue beds of the upper and middle Oolites.

4. The lower white and grey limestones of the Oolites.

5. The most calcareous and crystalline beds of the carboniferous or mountain limestone, colours grey and bluish.

6. The magnesian limestone of Yorkshire and Derbyshire.

7. The white lias limestone.

8. The blue lias limestone.

9. The Silurian limestone of Wenlock, Dudley, &c., and the coralline limestones of Plymouth and the neighourhood.

The value of limestone as a Purifying agent is in inverse proportion to the amount of earthy or foreign matter it contains; that which leaves the smallest proportion of insoluble sediment on being dissolved in diluted acid is the best.

Limestone is the carbonate of lime found in its natural state, from which the oxide of calcium (quick or caustic lime) is produced by the expulsion of the carbonic acid by means of heat in the limekiln.

Quick or Caustic Lime (oxide of calcium) is lime in the solid state,

before absorbing, or being slaked with, water.

Hydrate of Lime is lime in a moist state. It is a chemical compound of lime and water in the proportion of one part of water to three parts of lime.

Milk of Lime, or Cream of Lime, is a mixture or solution of hydrate

of lime and water.

WEIGHT AND MEASUREMENT OF LIME.

1 bushel of quick lime weighs about 70 lbs.

1 cubic foot of ,, ,, 54 , 1 ,, yard of ,, ,, 1460 , 1 ton of ,, is equal to about 32 54 ,,

is equal to about 32 bushels.

TABLE

Showing the Composition of Different Limestones and their Specific Gravity. (Government Commission.)

Quality of Limestone and Locality.	Carbo- nate of Lime.	Carbo- nate of Magnesia.	Silica (Flint.)	Iron Alumina (Clay.)	Water and Loss.	Specific Gravity (Dry.)
Ancaster, Lincolnshire Bath Box, Wiltshire Portland, Dorsetshire Ketton, Rutlandshire. Barnack, Northamptonshire. Chilmark, Wiltshire Ham Hill. Somersetshire.	93·59 94·52 95·16 92·17 93·40 79·00	2·90 2·50 1·20 4·10 8·80 8·70	1.20	-80 1·20 ·50 ·90 1·30 2·00	2·71 1·78 1·94 2·83 1·50 4·20	2·182 1·839 2·145 2·045 2·090 2·481
A trace of bitumen	79·30 was obs	5·20 erved in ea	4.70 ch of th	8.30 ne above.	2.50	2.260
Bolsover, Derbyshire	51·10 54·19 57·50 55·70	40·20 41·37 39·40 41·60	3.60 2.53 .80	1.80 .80 .70 .40	3·30 1·61 1·60 2·30	2·816 2·147 2·134 2·138

Hawkins's Air Process for Revivification of the Oxide of Iron in Situ.

Mr. J. G. Hawkins discovered that by drawing in from 21 to 3 per cent. of air at the inlet to the condenser, revivification of the oxide of iron in situ can be effected to a large extent.

The Purifiers are thus made to continue in use for a greater length of time without changing; whilst it is remarkable that the oxide by this process can be charged with as much as 75 per cent. of free sulphur.

Purifiers with a proportionately large area in comparison with the make of gas are required to obtain the full advantage of this process.

In adopting the air process, two layers of oxide are preferable to one deep layer. Owing to the heat generated by chemical action, as well as to the deposition of the sulphur, a considerable increase or expansion in the bulk of the material takes place in the Purifiers; and it is necessary, therefore, to allow ample room for the oxide to expand. A space of several inches should be allowed between the two layers, and the surface of the upper layer should be at least 3 inches below the edge of the water lute.

To counteract the effect of the nitrogen passing into the gas, (the oxygen having entered into combination with the purifying material), and reducing the illuminating power, Mr. Hawkins has devised an apparatus for carburetting the air. This consists of a closed cast-iron box, oblong in shape, which is constantly supplied with tar from the hydraulic main or condenser, the tar being heated, by means of steam pipes at the bottom of the box, to a temperature of 176° Fahr. the boiling-point of benzole. Air is forced, by means of a steam pump, through the box over the surface of the tar, being made to pursue a tortuous course by means of a series of baffle plates, and is then permitted to join the stream of gas at the condensers; so that any subsequent condensation of hydrocarbon vapour is returned to the tar well.

The Use of Pure Oxygen in Purification.

The chief objection to the use of air for revivifying the oxide of iron in situ is the importation of a considerable volume of the inert gas nitrogen into the coal gas, reducing the luminiferous value of the latter, unless counteracted by the carburetting process above described.

It is obvious that if pure oxygen is employed instead of atmospheric air, the objection stated will be overcome. The cost of producing oxygen, however, rendered its use prohibitory for this purpose until the advent of Brin's process for the production of pure oxygen from atmospheric air on a commercial scale and at a cheap rate.

In a valuable paper read before the Gas Institute in 1888, Mr. Valon gave an interesting description of a series of careful experiments

carried out by him to test the value of the system of adding pure oxygen to the gas in the process of Purification by oxide of iron or lime.

The oxygen was admitted at the exhauster outlet by a pipe connected to a wet meter to register the quantity passing, and to a small holder in which the oxygen was contained.

The quantity of oxygen passed into the oxide was 1 per cent. by volume for every 100 grains of sulphuretted hydrogen per 100 cubic feet of gas.

There was found to be an increase in luminosity of about 5 per cent., whilst the Purification was conducted with less than the usual quantity of Purifying material and Purifying space.

Using lime only in the Purifiers, the results were still more satisfactory. It was found that the sulphur was deposited in the solid form, the lime being perfectly carbonated.

The sulphur compounds were kept down to an average of 6 to 8 grains per 100 cubic feet; and the illuminating power of the gas was raised by 1.25 per cent.

In order to obtain the pure oxygen by Brin's process, air is first deprived of its carbonic acid and moisture by being drawn by a pump through chambers containing lime and caustic soda, and the same pump forces it, under a pressure of about one atmosphere, through barium oxide, contained in steel retorts 8 inches in diameter, heated in brick furnaces to a dull red heat by producer gas. At this temperature the barium oxide absorbs a large proportion of the oxygen contained in the air, and is converted into barium peroxide; the nitrogen, and any unabsorbed oxygen, escaping through a relief-valve at the other end of the retorts. When the barium oxide is sufficiently peroxidized, the temperature of the retorts is raised to bright red, and the pumps, by the changing of the valves, are converted into vacuum pumps; thereupon the absorbed oxygen, under the influence of the higher temperature and reduced pressure, is given off again, and discharged by the pumps into the gasholder. The retorts containing the restored barium oxide are allowed to cool to their previous dull red temperature, when the barium oxide is again ready to abstract a fresh supply of oxygen from the air. With due care, and under proper conditions, there seems to be practically no limit to the number of operations which may be effected by the one charge of barium oxide. The cost of the oxygen obtained by the method described, including interest on capital for plant, wear and tear, and all manufacturing expenses, is given by Brin's Company at 5s. per 1000 cubic feet.

Purification by means of Caustic Soda and Sulphide of Sodium.

The late Mr. R. H. Patterson patented a process of Purifying by washing or scrubbing the gas in solutions of caustic soda and sulphide of sodium, extracting the carbonic acid and sulphur impurities, and so dispensing altogether with the ordinary lime and oxide of iron Purifiers. The soda solutions, when saturated with the impurities, possess the important quality of being easily and perpetually revivified or restored to their original state on the gas-works, whilst the whole of the sulphur is secured for sale. The plan, however, has not been tried on an adequately large scale.

Purification by means of Caustic Ammonia, and Carbonate of Ammonia.

Attempts have been made by Mr. Laming, Mr. Livesey, Mr. F. C. Hills and others, to purify the gas in closed vessels by employing the ammonia found in the gas for arresting the other impurities. Unfortunately, the loss of ammonia at each time of desulphurating the liquor, owing to its extreme volatility, prevented success in this direction under the conditions adopted.

Claus's Process of Purification by Ammonia Gas.

This process of continuous Purification in closed vessels, though not hitherto largely adopted, is of such importance as to merit a detailed description.

The crude ammoniacal liquor, consisting of sulphide of ammonium and carbonate of ammonia, is passed through a series of towers, wherein it is exposed to the action of carbonic acid (obtained as described below), whereby the sulphide of ammonium is decomposed, sulphuretted hydrogen being liberated, and carbonate of ammonia remaining alone.

The sulphuretted hydrogen passes through and out of the towers in the opposite direction to that in which the crude liquor travels, and is disposed of in the manner described hereafter; whilst the carbonate of ammonia solution passes forward into other towers in which it is heated to a temperature of 180° to 200° Fahr.

At this temperature the carbonate of ammonia, of a strength equal to 10 or 15 ounce liquor, loses two-thirds or three-fourths of its carbonic acid, and a corresponding quantity of caustic ammonia remains in the liquor passing from these towers.

As only a portion of the carbonic acid evolved in the heating vessel or towers is required for the above-mentioned decomposition of sulphide of ammonia, the surplus is allowed to escape in a regulated quantity, and may be used for other purposes forming part of the process.

The sulphuretted hydrogen, after leaving the towers, is conveyed to a closed furnace charged with oxide of iron, where a low-incandescent heat is generated and maintained by the admission of a regulated supply of air.

The oxide of iron, once heated, continues to absorb the sulphuretted hydrogen, which, owing to the continual admission of air, is evolved in the form of sulphur, in finely-divided particles, which is carried off and caught in chambers, so that the oxide does not require revivification, and the same quantity, kept hot by continual working, goes on indefinitely decomposing the sulphuretted hydrogen sent through it.

The purified ammoniacal liquor is then passed down distilling towers, into which steam is admitted, driving off the ammonia gas at the top, which is passed through cooling chambers, in which any carbonate of ammonia carried with it deposits in crystals.

Thence, as much of the ammonia gas as is required for the purposes of purification, passes with the coal gas into a chamber, where they are allowed sufficient time to mix.

The gas is then passed through scrubbing towers, where all the impurities are washed out in the liquor, which may be obtained of 40 to 50 oz. strength if required.

Any surplus ammonia, being perfectly pure, can be used for making any of the salts of ammonia desired.

The liquor flowing from the bottom of the distilling towers contains sulphocyanide of ammonium, and may be used over and over again in the scrubbers instead of water, until the sulphocyanide accumulates to such a strength as to make it marketably valuable for chemical manufacture.

PURIFYING HOUSE.

The house to contain the Purifiers should be lofty and well ventilated, not only for the comfort of the workmen employed therein, but to lessen or entirely remove the risk of explosion from any leakage of gas that might occur. The house should also be arranged with a view to future extension.

It is a convenient plan to build the house with a ground and upper floor, and to place the Purifying vessels on the latter with the

connections and centre-valve underneath and fully exposed and accessible. The ground floor can thus be used for revivifying the oxide of

iron, if that material is employed, or for other purposes.

The vessels are discharged through an opening in the bottom of each, closed by a gas-tight lid, and the fresh material is raised by means of an endless chain ladder, or other suitable elevating apparatus, to the floor above.

PURIFIERS.

Construction and Arrangement of the Purifiers.

The Purifying vessels are almost invariably made of cast-iron, with sheet-iron covers secured with suitable fastenings, to prevent their being lifted by the incoming gas pressing on their under surface.

Malam's arrangement of four in the set, with connections and a centre-valve (Fig. 51), by which three of the vessels are kept in action, and one out of use for renewal of the Purifying material, is still generally adopted, and is the simplest and most convenient. In some works a second set of two Purifiers is used in addition to the series of four, and these are connected together, and to the others, with single or four-way valves. (Fig. 51). Under this arrangement the set of four is charged with oxide to arrest the sulphuretted hydrogen, and the set of two with lime to take up the carbonic acid, the gas passing through them in the order shown.

Depth and best Form of Purifiers.

In determining the size of Purifiers, where either dry lime or oxide of iron is intended to be used, it is of the utmost importance to provide a liberal superficial area, and to make ample allowance for increased gas-make.

One of the greatest sources of discomfort to a gas manager is having his Purifiers so cramped and confined in their area as to be incapable

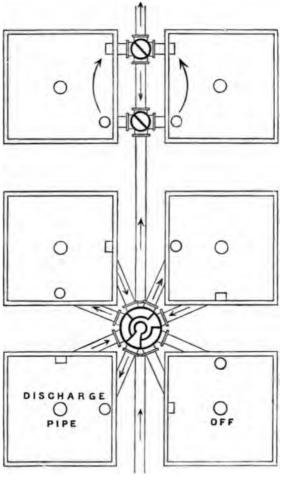
of doing the work required in an efficient manner.

The ordinary and best form of Purifier is the square or oblong; this shape is the cheapest, affords the largest area for the space occupied, and is also the most convenient as regards the placing of the trays or grids.

The usual depth of Purifiers is 5 feet; in some large gas-works they

are 6 feet deep.

Large Purifiers, say, 20 feet square and upwards, should have two or more tie rods of round wrought-iron, stretching across them from side



F16. 51.

to side, at the upper part of the lute, to support the sides under the strain to which they are often subjected by the expansion of the

contained oxide of iron, especially where the air process, previously described, is in operation. These ties should be removable, having an eyelet hole at both ends, fitting into a forked piece, also furnished with eyelet holes, bolted to the vertical flanges, and secured by an

easy fitting bolt or pin.

The capacity or Purifying power of the vessel is determined more by its superficial area than its cubical volume. There is, however, a mutual relation between the two, as, when the depth is increased and fully utilized, the surface area has to be proportionately augmented, on account of the resistance offered by the deeper material to the flow of the gas. It is more strictly correct, then, to say that the superficial area, in proportion to the depth of the Purifying material, is the gauge of the capacity or Purifying power of the vessels; and the maximum hourly or daily gas-make of which the works are capable should form the basis of any calculation to determine their size.

One of the chief conditions for securing satisfactory Purification is the use of vessels of large area. If economy and efficiency are to be considered, time is an important element, and must not be disregarded. The mere passing of the gas through the Purifying media is not sufficient to insure good results; time is required for chemical affinity to

operate.

Rules for Determining the Size of Purifiers.

It is stated in Clegg (4th ed., p. 200) that "the usual calculation with gas makers in France is that an area of about 1 foot is required for every 250 lbs. of coal carbonized in 24 hours, each Purifier being supposed to contain three sieves, which would amount to about three square yards of surface to each ton of coal carbonized." This is not very explicit.

The same also states "that for every 150 cubic feet of gas per hour which can be generated, each Purifier should present one superficial foot of surface." This allowance is absurdly small, and in practice, with anything near the maximum production, would be found altogether inadequate.

The rule given in Hughes (3rd ed., p. 158) is much to be preferred—viz., "Allow one superficial yard of sieve for every 1000 cubic feet of

gas produced per diem."

Adopting this rule, a works capable of producing a maximum of 220,000 cubic feet of gas per day of 24 hours will require four Purifiers, each 10 feet square, and having five tiers of lime sieves each.

Another rule, agreeing closely with the above, is to allow 10 square yards of sieve for every ton of coal and cannel that can be carbonized in 24 hours.

I venture on another rule which experience has taught me to regard with more favour than any of the above—viz., that where there is intended to be four Purifiers, three always in action, the maximum daily (24 hours) make of gas, expressed in thousands, multiplied by the constant 6, will give the superficial area in feet of each Purifier.

Example.—Required the superficial area of each of the four Purifiers in a works equal to the production of 500,000 cubic feet of gas per diem of 24 hours.

 $500 \times .6 = 300$ feet superficial area of each Purifier. $\sqrt{300} = 17.3$ (say, 18) feet side of square of Purifier.

For very small works where there is no exhauster, the constant '8 may be employed with advantage.

Water Lute for Covers and Hydraulic Centre-Valve.

The evils of contracted area in Purifiers are aggravated by having a shallow seal to the lids or covers and the hydraulic centre-valve.

In small works the water lute should never be less than 12 inches deep by $4\frac{1}{2}$ inches wide; and in medium sized and large works, from 18 to 24 inches by 6 to 8 inches in width.

Ample depth of water lute is especially important where the back

pressure is increased by the use of telescopic holders.

Number of Layers of Purifying Material.

In Purifiers charged with hydrate of lime, there may be two or four tiers of sieves. The lime spread upon their surface may be from 4 to 8 inches in depth.

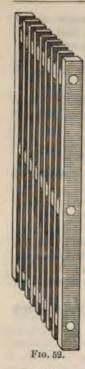
When oxide of iron is used, the layers may be two in number, and

the material 15 to 20 inches deep on each.

It is a mistake to adopt the plan of placing either the lime or oxide in a single deep layer. The gas is apt to form passages through the deep material; whereas when there are two or more layers of less depth, it recovers itself, and changes its course through each.

Sieves, Trays, or Grids for Lime and Oxide of Iron.

Round wrought-iron rods, $\frac{3}{8}$ of an inch thick, bound together with a framing of angle or flat-iron, make an excellent tray, especially where lime is used. They are less suitable for oxide of iron, which



destroys them by corrosion, though when made of the strength named, they last for many years. They possess a great advantage over most other travs in the smaller space which they occupy in the Purifier, and the larger Purifying area obtained by their use. Perforated cast-iron and wood trays are suitable for either lime or oxide. The latter are usually made with strips of wood (yellow pine, pitch pine, or red deal, the prices being as 3, 2, 1) of any convenient length; the strips are $1\frac{7}{8}$ inch broad, $\frac{1}{2}$ an inch thick, and slightly tapered, the outer pieces of frame being of harder timber (hickory, beech, oak, or ash), and 11 inches thick; the whole bound together with a inch bolts and nuts, having the heads, washers, and nuts countersunk in the side frames, and the holes plugged with wood or cement. The strips are kept 1 an inch to 5 of an inch apart by pieces of wood of that thickness, and 17 inches square, put between them at the places where the bolts are inserted (Fig. 52).

Apparatus for Raising the Lids or Covers.

For raising the lids or covers of the Purifiers, various contrivances are employed; the most common being a double purchase crab, travelling on iron rails laid on either wooden beams or iron lattice girders, having their ends inserted in the walls of the building; or, in the absence of walls, supported on pillars.

The lifting machine, sometimes called a "Goliath," first constructed by Messrs. Cockey and Sons, is a useful and compact contrivance for the same purpose. This consists of two standards, one on each side of the Purifier, connected across the top by two girders a few inches apart. The standards, having grooved or flanged wheels, or rollers attached, traverse the purifying house from one end to the other on rails laid on the floor. The covers are raised by means of two long vertical screws, with an eyelet-hole at the end of each, in which the hooks on the lid are inserted, and moved by a winch and cog-wheels put in motion by means of a handle at one of the sides. When the apparatus is not in use, it can be wheeled out of the way, leaving the space above the Purifiers to the tie-rods or beams of the roof entirely unobstructed.

Mr. Reid employs a somewhat similar travelling carriage; but, instead of the wheel gearing and screws, he uses hydrostatic pressure for accomplishing the same object. A full description, with drawing

of his ingenious apparatus, was submitted by him to the North British Association of Gas Managers, at their meeting in July, 1872, and appears at length in the *Journal of Gas Lighting* for Aug. 27 of the same year.

Centre and other Change Valves.

The dry Centre-valve, with surface faced to fit gas-tight, is now extensively adopted, and, as a rule, is preferred to the old hydraulic Centre-valve. The chief advantages it possesses over the latter are the greater ease and facility in changing from one Purifier to another; one man being able to accomplish this with a few turns of a handle, thus minimizing to the utmost extent the passage of unpurified gas during that operation. It occupies less space, is entirely beneath the Purifying-house floor, and presents a dead resistance to pressure, admitting of greater steadiness in the flow of the gas where an exhauster is at work.

Four-way valves are adopted by some managers in preference to the Centre-valve; their chief recommendation being that by their use the connections are simplified. The advantages which they possess over the ordinary single Valve are more apparent. When the latter are employed, twelve are needed for a set of four Purifiers, and six for a set of two; whereas, with the four-way valves, only one-third that number is required,

Size of Connecting-Pipes.

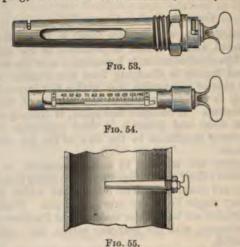
With respect to the size of the Connecting-pipes, the rule is to make their internal diameter, in inches, equal, as nearly as possible, to the square root, in feet, of the area of the Purifiers.

Thus, Purifiers 10 feet square, giving an area of 100 square feet, have Connecting-pipes 10 inches in diameter; and Purifiers 16 feet by 12 feet, having an area of 192 square feet, have their Connecting-pipes 14 inches in diameter. With the larger proportionate sizes of Purifiers now being employed over those formerly erected, a deduction of \(\frac{1}{2} \) may safely be made from the result obtained by the above rule. Thus (see rule on p. 143), a works capable of producing 500,000 cubic feet of gas per day requires four Purifiers, having each an area of 300 square feet [500 \times '6 = 300], the square root being 17.3; deducting \(\frac{1}{6} \), or 2.2, we have 15.1, or say 15 inches, the diameter of the Connecting-pipes.

DRORY'S MAIN THERMOMETER.

The illustrations (Figs. 53 to 55) show the improved arrangement invented by Mr. Drory, for ascertaining the temperature of the gas

passing through the condenser and other apparatus, and the mains. It consists of an outer shell fitted with a conical hollow plug having an aperture corresponding to that in the outer shell. The Tester, which fits into the plug, contains a Thermometer, which, on being turned



opposite to the apertures, is in immediate contact with the gas, and on withdrawal the temperature is ascertained. For attaching the Tester, a hole suitable for a 1-inch wrought-iron pipe is drilled and tapped in the pipe or side of the apparatus, and the instrument is screwed therein.

TESTS

For the Detection of Impurities in Coal Gas after the Ordinary Processes of Purification.

Ammonia.

Expose yellow turmeric paper slightly moistened with water, or litmus paper first reddened by any weak acid, to a jet of unlighted gas for about a minute. If the yellow colour of the turmeric be turned to brown, or if the blue of the litmus be restored, Ammonia is present.

Turmeric and litmus papers may be purchased at the chemists, or

they can be prepared as follows :-

Turmeric Paper.—Six parts by weight of spirits of wine are added to one of turmeric powder in a stoppered bottle, and well

shaken up occasionally for three days. A portion of the clear fluid is then poured on a plate, and pieces of unsized white filtering paper well soaked therein. These are then dried in air, cut into strips half an inch wide and 2 inches long, and kept for use in a bottle away from the light.

LITMUS PAPER.—Six parts by weight of water to one of powdered litmus, shaken well together, allowed to stand for several days, and then filtered. Pieces of white filtering paper are then thoroughly soaked in the solution, dried, and cut into strips, which should be kept in a close stoppered bottle, excluded as much as possible from the air and light. Should it be desired to redden the solution, add (after filtration) a small quantity of very dilute sulphuric acid, gradually, drop by drop, until the pink or neutral tinge is obtained.

Carbonic Acid.

Make a solution of pure barytes, and pass the gas through it. If Carbonic Acid be present, carbonate of barytes will be precipitated; or pass the gas through clear lime water, and carbonate of lime will be precipitated.

It may also be detected by adding to water impregnated with the gas a few drops of sulphuric acid, when minute bubbles of Carbonic

Acid gas will be rapidly disengaged.

Lime Water is prepared by agitating slaked lime with distilled water in a bottle or other vessel. It is then allowed to stand until the excess of lime has been deposited, when the clear liquid

is poured off, and filtered through filtering paper.

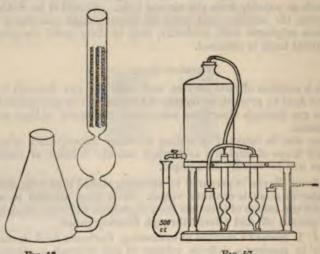
Mr. J. T. Sheard's method of estimating Carbonic Acid in coal gas consists in passing a definite volume of gas through a solution of barium hydrate of known strength, which absorbs the Carbonic Acid out of the gas; the amount of free hydrate remaining after the operation being determined by titration with deci-normal hydrochloric acid. Either the volume or the weight of impurity that has been absorbed can thence be calculated.

The gas absorption tube is of the form shown in Fig. 56; the

straight part above the bulbs being filled with glass beads.

To make a test, two absorption tubes are charged with 20 or 80 cubic centimetres each, of a barium hydrate solution, the strength of which has been accurately determined by titration with deci-normal acid, and which should be approximately of equal strength with the acid. The apparatus being connected up as shown, Fig. 57, 500 c.c. of gas are drawn by means of the aspirator slowly through the liquid, and followed immediately, without stopping the current,

by an equal quantity of air, which is done by slipping off the indiarubber tube at the inlet of the apparatus, as the water running from the aspirator passes the mark of a 500 c.c. flask, and then running out a further quantity of 500 c.c. into another flask held in readiness. The bulbs are then washed down with water free from Carbonic Acid, a few drops of the phenol-phthalein (sufficient to impart a distinct purple red colour to the liquid) added, and the whole titrated with deci-normal hydrochloric acid—the acid being added a few drops at a time, with frequent agitation of the liquid until the colour is The amount of barium hydrate that has been neutralized destroyed.



Frg. 56.

is equivalent to the amount of Carbonic Acid absorbed from 500 c.c. of gas; from which the percentage of the impurity present, or its

weight per cubic foot of gas, can be determined.

Example.—Two gas absorption tubes charged, respectively, with 30 c.c. and 20 c.c. of barium hydrate solution. One cubic centimetre of the barium hydrate having previously been found by experiment as equivalent to 1.09 of $\frac{N}{10}$ acid.

. 32.7 c.c. Equivalent of barium hydrate employed 21.8 c.c. acid required to neutralize resultant liquid. 21.6 c.c. .. 21.4 c.c.

> 11.1 c.c. 0.4 c.c.

11.5 c.c. × 0.0022 grm. × 100 = 2.77 per cent, by volume of CO. 0:914 grm.

11.5 c.c. × 0.0022 grm. × 15.482 grs. × 28,815 c.c. 500 c.c.

grains of CO, per cubic foot of gas.*

These calculations may be shortened by employing the factor 0.241 for percentage by volume, and 1.92 for grains per cubic foot. Thus-

> $11.5 \times 0.241 = 2.77$ per cent. by volume of CO₂ 11.5 × 1.92 = 22.1 grains of CO, per cub. ft. of gas.

A complete test can be made in fifteen minutes, and perfectly accurate results obtained.

The apparatus is equally applicable to the estimation of Ammonia in gas, by employing acid of suitable strength as the absorbent.

Sulphuretted Hydrogen.

Moisten a piece of writing-paper with a solution of acetate of lead in distilled water, and expose it for not less than a minute to a jet of unlighted gas. If Sulphuretted Hydrogen be present, the paper will be browned or blackened.

A solution of nitrate of silver is a more delicate test than the above. This requires to be kept in a bottle coated outside with tinfoil, and placed in a drawer or other dark place to protect it from the influence of the light.

Lead Paper may be made of white filtering paper soaked in the acetate of lead solution, then dried, cut into slips, and kept in a well-corked bottle for use. But the solution applied to the paper at the time of making the test is preferable.

The following are the regulations given in Schedule A of the Gas-Works Clauses Act, 1871, in respect of the apparatus and mode of testing for Sulphuretted Hydrogen :-

Apparatus for Testing the Presence in the Gas of Sulphuretted Hydrogen.

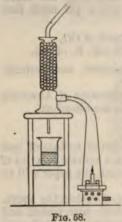
A glass vessel (Fig. 60) containing a strip of bibulous paper moistened with a solution of acetate of lead, containing 60 grains of crystallized acetate of lead dissolved in one fluid ounce of water.

[&]quot;It may be explained that-

^{0.0022} grm. is the weight of CO2 to which 1 c.c. of $\frac{N}{10}$ acid is equivalent.

^{0.914} grm. is the weight of 500 c.c. of CO_2 saturated with moisture. 15.432 grs. is the value of 1 gramme. 28,315 c.c. is the value of 1 cubic foot.

Mode of Testing for Sulphuretted Hydrogen.—The gas shall be passed through the glass vessel containing the strip of bibulous paper moistened with the solution of the acetate of lead for a period of three minutes, or such longer period as may be prescribed; and if any discolouration of the test paper is found to have taken place, this is to be held conclusive as to the presence of Sulphuretted Hydrogen in the gas.



Sulphur.

The Sulphur present in gas, due to compounds other than Sulphuretted Hydrogen, notably Bisulphide of Carbon, is estimated by burning a jet of the gas at the rate of one cubic foot, or half a cubic foot, per hour, for 24 hours, from a Leslie or other burner arranged within the wide end of a trumpet tube whose upper and smaller end is inserted in a condenser, from the opposite end of which a tube carries off the uncondensed vapour, and creates a current through the apparatus. (See Fig. 58.) Through the lower and wide end, where the burner is fixed, a supply of air, to support combustion, enters, carrying with it the vapour of ammonia from liquid ammonia or pieces of the carbonate contained in a suitable receptacle surrounding the burner. The ammonia com-

bining with the sulphurous acid from the gas-flame, is deposited within the condenser as sulphite and sulphate of ammonia, from which the quantity of Sulphur per 100 cubic feet of gas is calculated.

Illuminating Power and Impurities.

The illuminating power of gas may be high, and at the same time a good deal of Sulphur and other impurities may be present. Purity is not always in a given ratio with illuminating power.

Harcourt's Colour Test.

This is one of the most useful apparatus in the gas manager's laboratory for determining with ease and celerity the amount of Bisulphide of Carbon, Sulphuretted Hydrogen, and Carbonic Acid in coal gas. The following is a description of the test, and directions for its use.

Testing for Bisulphide of Carbon.

The arrangement of the colour test is shown in Fig. 59; the fire-clay cylinder being represented by dotted lines.

The bulb, which is filled with platinized pumice, is to be so adjusted

that it may be about an inch above the burner, and in the middle of the

cylinder.

To use the apparatus, turn on first the upper stopcock, sending gas through the bulb at the rate of about half a cubic foot an hour, as may be judged by lighting the gas for a moment at the end of the horizontal arm, when a flame about an inch in length should be produced. Raise the cylinder, which will be supported by the pressure of the wires, light the burner, and turn down the flame till it forms a blue non-luminous ring. Lower the cylinder, and place the small clay pieces upon it round the neck of the bulb.



Fig. 59.

A testing may be made five minutes after the burner is lighted, except when the apparatus is first used, when the gas should be allowed to flow through the bulb for a quarter of an hour, or a little longer, and any number of testings one after another as long as the heat is continued.

The mode of testing is as follows:—Lay a piece of white paper on the table by the side of the burner, and fix a piece of cardboard upright in the brass clip; the cardboard serves as a background against which to observe the colour of the contents of the glasses, and should receive a side light, and be as clear as possible from shadows. Fill one glass (once for all) up to the mark with standard coloured liquid, and cork it tightly. Dilute some of the lead syrup with twenty

times its volume of distilled water, and fill the other glass up to the mark with a portion of the liquid thus prepared. Insert the caoutchouc plug with capillary-tube and elbow-tube, and connect, as shown in the figure, with the bulb and aspirator, placing the two

glasses side by side.

The aspirator should be full of water at starting, and the measuring cylinder empty. Turn the tap of the aspirator gradually; a stream of bubbles will rise through the solution of lead. Turn off the tap for a minute, and observe the liquid at the bottom of the capillary-tube. If it gradually rises, the india-rubber connections are not air-tight, and must be made so before proceeding. Avoid pressing the plugs into the glass or the aspirator while they are connected, which would drive up the lead solution into the inlet-tube. When the connections are air-tight, let the water run into the measuring cylinder in a slender stream until the lead solution has become as dark as the standard. As the ascending bubbles interfere somewhat with the observation of the tint, it is best to turn off the tap when the colour seems almost deep enough; compare the two; turn on the tap, if necessary, for a few moments, then compare again; and so on, till the colour of the two liquids is the same.

The volume of water which the measuring cylinder now contains is equal to the volume of gas which has passed through the lead

solution.

This volume of gas contained a quantity of Sulphur as Carbon Bisulphide which, as Lead Sulphide, has coloured the liquid in the test-glass up to the standard tint. The standard has been made such that, to impart this tint to the volume of liquid, 0·0187 grain of Lead Sulphide must be present, containing 0·0025 grain of Sulphur. Hence, supposing the measuring cylinder, each division of which corresponds to 1-2000th cubic foot, to have been filled to the 30th division, 30-2000ths cubic foot of gas contained 0·0025 grain of sulphur. From this ratio the number of grains of Sulphur existing as Bisulphide in 100 cubic feet of the sample of gas tested can easily be calculated.

The following table gives the relation between (V) the divisions of the measuring cylinder filled with water, and (S) the grains of Sulphur existing as Bisulphide in 100 cubic feet of gas. Since gas contains besides Carbon Bisulphide, some other Sulphur compounds which are not transformed into Sulphuretted Hydrogen by the action of heat, and which contain Sulphur amounting ordinarily to 7 or 8 grains in 100 cubic feet, this quantity must be added to that found by the test, if it is wished to know approximately the total amount of

Sulphur.

									TAI	BLE	I.								
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	13			38.5		36			13.9		59			8.5	82	7	10	6.1	
	14		100	35:7		87	100		13.5		60			8:3	83			6.0	
	15	а	100	33.3		38	3300		18.2		61	-	-	8.2	84		-	6.0	
	16	ш		31.3		89	NO.	8	12.8		62	10	120	8.1	85	30	30	5.9	
	17	81	1	29.4		40	Tier	101	12.5		63	15	1	7.9	86	-		5.8	
	18	2	0	27.8		41	100	-	12.2		64	-	-	7.8	87	-	10	5.7	
	19		131	26.3		42	34		11.9		65	U.		7.7	88	101	131	5.7	
	20	80	181	25.0		43	-	15	11.6		66	IO.	160	7.6	89	100	œ	5.6	
	21	100	0	23.8		44	-		11.4		67			7.5	90	0		5.6	
	22	61	133	22.7		45	2	10.	11.1		68			7.4	91	-	5	5.5	
	23	91	ш	21.7		46	101	100	10.9		69	101	120	7.2	92		10.	5.4	
	24	0	-	20.8		47	16		10.6		70	-	-	7-1	93	30	1	5.4	
	25			20.0		48	12	-	10.4		71			7.0	94			5.3	
	26	91		19.2		49	70	8	10.2		72			6.9	95			5.3	
	27		100	18.5		50		(3)	10.0		73	30	000	6.9	96	9	iğu	5.2	
	28			17.9		51	1	16.	9.8		74	*	-	6.8	97			5.2	
	29	5		17.2		52			2.6		75	-		6:7	98	1		5.1	
	30		101	16.7		58	14	*	9.4		76	*		6.6	99	1	*	5.1	
	31	3	3	16.1		54	100	5	9.2		77	100	13	6.5	100	137	1	5.0	
	32			15.6		55	-		9.1		78	-	-	6.4	150			3.3	
	92	2	181	10.0		00			9.1		10	10		0.4	TOO		1	0.0	

For the next testing, the test-glass is to be disconnected and re-charged. The water in the measuring cylinders is poured back into the aspirator.

The colour of the standard is unaffected by exposure to light, but deepens if the liquid is warmed, returning to its original shade as the liquid cools. If, therefore, the glass containing the standard has

been in a warm place, it must be let cool before testing.

The liquid which has been used becomes colourless after being exposed to the light for a few hours, and may thus be used over and over again for 20 times or more, if it is not allowed to absorb carbonic acid from the air. The best mode of working is to have two well-corked flasks, into one of which the coloured liquid is emptied while the glass is re-charged from the other.

Testing for Sulphuretted Hydrogen and Carbonic Acid,

The apparatus may also be used without the bulb-tube and stand to test the amount of Sulphuretted Hydrogen or Carbonic Acid in gas at

any stage in its purification.

The gas is led in this case directly into the test-glass, which is charged with lead solution for Sulphuretted Hydrogen, and with a saturated solution of barium hydrate (baryta water) for Carbonic Acid.

When the gas contains more than 50 grains of Sulphur as Sulphuretted Hydrogen in 100 cubic feet, a smaller cylinder, containing 1-200th cubic foot, is used to measure the volume of liquid run from the aspirator. The divisions on the smaller cylinder are tenths of the corresponding divisions on the larger cylinder; therefore when it is used the numbers under S in Table I. must be read as whole numbers

by omitting the decimal points.

To estimate Carbonic Acid a standard liquid containing a definite amount of suspended barium carbonate is used for comparison. The glasses are placed side by side on a blackened board or piece of paper and with a black background behind them. The passage of the gas should be interrupted, and the test glass slightly shaken once or twice to wash down any particles of carbonate which may cling to the sides of the glass above the surface of the liquid. The standard should also be shaken before the comparison is made, in order that the precipitates may be in a similar condition. When the two liquids are judged to be equally white and opaque, the volume of water in the measuring cylinder gives the volume of gas which has precipitated a known weight of barium carbonate. Table II. gives the relation between (V) the divisions of the large measuring cylinder filled with water, and (C) the volume of Carbonic Acid in 100 volumes of gas. When the gas contains more than 72 per cent. of Carbonic Acid, the smaller measuring cylinder should be used, and the values of (C) multiplied by moving the decimal point one place to the right.

TABLE II.

V			C	V			C		V			C	V		C
10			.72	33		40	.22		56			.13	79		.09
11	- 3	1	.65	84	2	100	.21		57	100	19	.13	80	3	.09
12		0	.60	35	Č.		-21		58	13	-	.12	81		-09
13			:55	36			.20		59			.12	82		-09
			.51			*	.20	-			*	12	83		.09
14				37					60	*	*-				
15			.48	38			.19		61			-12	84		-09
16			.45	39			.18		62			-11	85		.08
17			.42	40			.18		63			.11	86		.08
18			-40	41			.17		64		4	*11	87		.08
19			.38	42			.17		65			•11	88		.08
20			.36	43			.17		66			.11	00		.08
21			.34	44		3	-16		67	1	-	.11	00		-08
22			.33	45			.16		68			•11	0.1		-08
23		*	.31	46	*		.16		69	*	185	-10	92		-08
		*			*	1.8							93	2	.08
24			.30	47			.15		70		4	.10		6 6	.00
25			.29	48			'15		71			.10	94		.08
26			-28	49			*15		72	10		.10			.08
27			.27	50			*14		78			.10			*07
28			-26	51			'14		74			.10	97		.07
29			.25	52	0		.14		75	2		.10	98		.07
30	12	1	-24	53	A	1	-14		76		467	.09	99	1 3	.07
31		-	-23	54	1		.13		77			.09	100		-07
32			-22	55			.13		78			.09	150		.05
02			22	99			10		10	*		00	100		00

After each testing the glass and capillary-tube should be cleaned with a little dilute hydrochloric acid and well rinsed with distilled water. The turbid liquid is poured into a flask, which should be kept well corked, containing an excess of crystallized barium hydrate. After the suspended precipitate has subsided, the clear liquid is poured off, or, if necessary, filtered, into another flask, also kept well corked, from which it may be poured into the test-glass when required. Care should be taken not to expose the solution to the air longer than necessary.

Instructions of the London Gas Referees as to the Times and Mode of Testing for Purity.

The testings for purity shall extend over twenty hours of each day, and shall be made upon ten cubic feet of gas, which shall be tested successively for each of the following impurities:—

I .- Sulphuretted Hydrogen.

The gas shall be passed as it leaves the service-pipe through an Apparatus (Fig. 60) in which are suspended slips of bibulous paper,

impregnated with basic acetate of lead.

The Test-paper from which these slips are cut is to be prepared from time to time by moistening sheets of bibulous paper with a solution of one part of Sugar of Lead in eight or nine parts of water, and holding each sheet while still damp over the surface of a strong solution of Ammonia for a few moments. As the paper dries all free Ammonia escapes.

If any discoloration of the slip of Test-paper is found to have taken place, this is to be held conclusive as to the presence of Sulphuretted Hydrogen in the gas. Fresh Test-slips are to be placed in

the Apparatus every day.

In the event of any impurity being discovered, one of the Test-slips shall be placed in a stoppered bottle and kept in the dark at the Testing-place; the remaining slips shall be forwarded with the daily Report.



Fig. 60.

II .- Ammonia.

The gas which has been tested for Sulphuretted Hydrogen shall pass next through an Apparatus consisting of a glass cylinder filled with glass beads, which have been moistened with a measured quantity of standard Sulphuric Acid. A set of burettes, properly graduated, is provided.

The maximum amount of Ammonia allowed is 4 grains per 100 cubic feet of gas; and the Testings shall be made so as to show the exact

amount of Ammonia in the gas.

Two Test-solutions are to be used—one consisting of dilute Sulphuric Acid of such strength that 25 measures (septems) will neutralize 1 grain of Ammonia; the other a weak solution of Ammonia, 100 measures of which contain 1 grain of Ammonia.

The correctness of the result to be obtained depends upon the ful-

filment of two conditions :-

1. The preparation of Test-solutions having the proper strength.

2. The accurate performance of the operation of testing.

To prepare the Test-solutions the following processes may be used

by the Gas Examiner :-

Measure a gallon of distilled water into a clean earthenware jar, or other suitable vessel. Add to this 94 septems of pure concentrated Sulphuric Acid, and mix thoroughly. Take exactly 50 septems of the liquid and precipitate it with Barium Chloride in the manner prescribed for the Sulphur Test. The weight of Barium Sulphate which 50 septems of the Test-acid should yield is 13.8 grains. The weight obtained with the dilute acid prepared as above will be somewhat greater, unless the Sulphuric Acid used had a specific gravity below 1.84.

Add now to the diluted acid a measured quantity of water, which is to be found by subtracting 13.8 from the weight of Barium Sulphate obtained in the experiment, and multiplying the difference by 726. The resulting number is the number of septems of water to be added.

If these operations have been accurately performed, a second precipitation and weighing of the Barium Sulphate obtainable from 50 septems of the Test-acid will give nearly the correct number of 13.8 grains. If the weight exceeds 13.9 grains, or falls below 13.7 grains, more water or Sulphuric Acid must be added, and fresh trials made, until the weight falls within these limits. The Test-acid thus prepared should be transferred at once to stoppered bottles, which have

been well drained and are duly labelled.

To prepare the standard solution of Ammonia, measure out as before a gallon of distilled water, and mix with it 50 septems of strong solution of Ammonia (sp. gr. 0.88). Try whether 100 septems of the Test-alkali thus prepared will neutralize 25 of the Test-acid, proceeding according to the directions given subsequently as to the mode of testing. If the acid is just neutralized by the last few drops, the Test-alkali is of the required strength. But if not, small additional quantities of water, or of strong Ammonia solution, must be added, and fresh trials made, until the proper strength has been attained. The bottles in which the solution is stored should be filled nearly full and well stoppered.

The mode of testing is as follows :- Take 50 septems of the Test-

acid (which is greatly in excess of any quantity of Ammonia likely to be found in the gas), and pour it into the glass cylinder, so as to well wet the whole interior surface, and also the glass beads. Connect one terminal tube of the cylinder with the gas supply, and the other with the meter, and make the gas pass at the rate of about half a cubic foot per hour. Any Ammonia that is in the gas will be arrested by the Sulphuric Acid, and a portion of the Acid (varying with the quantity of Ammonia in the gas) will be neutralized thereby. At the end of each period of testing, wash out the glass cylinder and its contents with distilled water, and collect the washings in a glass vessel. Transfer one-half of this liquid to a separate glass vessel, and add a quantity of a neutral solution of hæmatoxylin or litmus just sufficient to colour the liquid. Then pour into the burette 100 septems of the Test-alkali, and gradually drop this solution into the measured quantity of the washings collected, stirring constantly. As soon as the colour changes (indicating that the whole of the Sulphuric Acid has been neutralized), read off the quantity of liquid remaining in the burette. To find the number of grains of Ammonia in 100 cubic feet of the gas, multiply by 2 the number of septems of Test-alkali remaining in the burette, and move the decimal point one place to the left.

The remaining half of the liquid is to be preserved for a week in a bottle duly labelled.

III.—Sulphur Compounds other than Sulphuretted Hydrogen.

The gas which has been tested for Sulphuretted Hydrogen and Ammonia shall pass next through a meter, by means of which the rate of flow can be adjusted to half a cubic foot per hour, and which is provided with a self-acting movement for shutting off the gas when ten cubic feet have passed.

The testing shall be made in a room where no gas is burnt other

than that which is being tested for Sulphur and Ammonia.

The apparatus to be employed is represented by the diagram (Fig. 58), and is of the following description:—The gas is burnt in a small Bunsen burner with steatite top, which is mounted on a short cylindrical stand, perforated with holes for the admission of air, and having on its upper surface a deep circular channel to receive the wide end of a glass trumpet-tube. On the top of the stand, between the narrow stem of the burner and the surrounding glass trumpet-tube, are to be placed pieces of commercial Sesqui-carbonate of Ammonia weighing in all about 2 ounces.

The products both of the combustion of the gas and of the gradual volatilization of the Ammonia salt go upwards through the trumpettube into a vertical glass cylinder, packed with balls of glass, to break up the current and promote condensation. From the top of the cylinder there proceeds a long glass pipe or chimney, serving to effect some further condensation, as well as to regulate the draught and afford an exit for the uncondensable gases. In the bottom of the cylinder is fixed a small glass tube, through which the liquid (formed during the testing) drops into a beaker placed beneath.

The following cautions are to be observed in selecting and setting up

the apparatus :-

See that the inlet-pipe fits gas-tight into the burner, and that the holes in the circular stand are clear. If the burner gives a luminous flame, remove the top piece, and, having hammered down gently the nozzle of soft metal, perforate it afresh, making as small a hole as will give passage to half a cubic foot of gas per hour at a convenient pressure.

See that the tubulure of the condenser has an internal diameter of not less than 3 inch, and that its outside is smooth and of the

same size as the small end of the trumpet-tube.

See that the short piece of india-rubber pipe fits tightly both to

the trumpet-tube and to the tubulure of the condenser.

The small tube at the bottom of the condenser should have its lower end contracted, so that when in use it may be closed by a drop of water.

The india-rubber pipe at the lower end of the chimney-tube should fit into, and not simply rest upon, the mouth of the condenser, and the upper extremity of this tube may with advantage be given a downward curvature.

At the end of each period of testing, the cylinder and trumpet-tube are to be well washed out with distilled water. Fresh pieces of Sesquicarbonate of Ammonia are to be used each day.

The Gas Examiner shall then proceed as follows:-

The liquid in the beaker and the water used in washing out the Apparatus shall be put into the same vessel, well mixed, and measured. One-half of the liquid so obtained is to be set aside, and preserved for a week, properly labelled, in case it should be desirable to verify the

correctness of the testing.

The remaining half of the liquid is to be put into a flask, or beaker covered with a large watch-glass—treated with Hydrochloric Acid sufficient in quantity to leave an excess of acid in the solution—and then raised to the boiling point. An excess of a solution of Barium Chloride is now to be added, and the boiling continued for five minutes. The vessel and its contents are to be allowed to stand till the Barium Sulphate settles at the bottom of the vessel, after which the clear liquid is to be as far as possible poured off through a paper filter. The remaining liquid and Barium Sulphate are then to be poured on to the filter, and the latter well washed with hot distilled water.

(In order to ascertain whether every trace of Barium Chloride and Ammonium Chloride has been removed, a small quantity of the washings from the filter should be placed in a test-tube, and a drop of a solution of Silver Nitrate added; should the liquid, instead of remaining perfectly clear, become cloudy, the washing must be continued until, on repeating the test, no cloudiness is produced.) Dry the filter with its contents, and transfer it into a weighed platinum crucible. Heat the crucible over a lamp, increasing the temperature gradually, from the point at which the paper begins to char, up to bright redness. When no black particles remain, allow the crucible to cool; place it when nearly cold in a desiccator over strong Sulphuric Acid, and again weigh it. The difference between the first and second weighings of the crucible will give the number of grains of Barium Sulphate. Multiply this number by 11 and divide by 4; the result is the number of grains of sulphur in 100 cubic feet of the gas.

This number is to be corrected for the variations of temperature and atmospheric pressure in the manner indicated under the head of Illuminating Power (see post), with this difference, that the readings of the Barometer and Thermometer are to be taken for the day on which the testing commenced and also the day on which it closed:

and the mean of the two is to be used.

This correction may be made most simply and with sufficient

accuracy in the following manner :-

When the Tabular Number is between 955-965, 966-975, 976-985, 986-995, increase the number of grains of Sulphur by $\frac{1}{100}$ ths, $\frac{2}{100}$ ths, $\frac{1}{100}$ ths, $\frac{1}{100}$ ths, $\frac{1}{100}$ ths, $\frac{1}{100}$ ths.

When the Tabular Number is between 996-1005, no correction

need be made.

When the Tabular Number is between 1006-1015, 1016-1025, 1026-1035, diminish the number of grains of Sulphur by 100th, 100th, 100ths,

EXAMPLE: Barometer (mean). Thermometer (mean). Tabular Number. Grains of Barium Sulphate from 5 cubic feet of Gas. Multiply by 11, and divide by 4.	29·4 58 985	4.8
	4	1)47.3
Grains of Sulphur in 100 cub. ft. of Gas (uncorrected) Add $11.8 \times \frac{2}{100} =$		11:02
Grains of Sulphur in 100 cub. ft. of Gas (corrected) .		12:06

[Result: 12.1 grains.]

As to the Maximum Amounts of Impurity in each Form with which the Gas shall be allowed to be Charged.

Sulphuretted Hydrogen.

By the Acts of Parliament all gas supplied must be wholly free from this impurity.

Ammonia.

The maximum amount of this impurity shall be 4 grains per 100 cubic feet.

Sulphur Compounds other than Sulphuretted Hydrogen.

The maximum amount of Sulphur with which gas shall be allowed to be charged shall be 22 grains of Sulphur in every 100 cubic feet of gas.

STATION METER HOUSE.

The Station Meter House, if conveniently situated on the works, and made sufficiently large, may contain in addition to the meters, the station governors, exhaust and pressure register, a range of pressure gauges, and a jet photometer.

When thus arranged, they are all within the purview, and imme-

diately under the control, of the workman in charge.

The Meter-House is susceptible of ornamentation, and should have a little bestowed upon it, besides being kept scrupulously clean and well ventilated.

STATION METER.

The quantity of gas manufactured, as it passes into the holders, after its purification has been completed, is measured and recorded

by the Station Meter.

This is invariably of the "wet" description—that is to say, the measuring wheel or drum is caused to revolve by the elastic force of the gas pressing upon the surface of a body of water, with which the vessel is charged up to a certain line.

In construction it differs slightly from the wet meters used by

consumers, but its principle of action is identical with these.

The Meter case, which is of cast-iron, is made either cylindrical (Fig. 61), or rectangular (Fig. 62); the former shape being generally adopted for sizes up to 20,000 cubic feet per hour. When it is rectangular in form, the roof is composed of wrought-iron plates, usually No. 10 B.W.G.

The measuring wheel or drum is made of charcoal annealed tinned

plates, riveted and soldered together in segments, and the shaft or

axle is supported by anti-friction wheels.

The registering mechanism consists of a series of enamelled dials, with wheel-work and pointers indicating from 100 to 100,000,000 cubic feet at each of their revolutions. The dial figures, unlike those

on the consumers' meters, all run in the same direction.

An eight-day clock and tell-tale apparatus are placed in front, above the index. On a circular plate, a graduated disc of card paper is fixed; and a lead pencil attached to a rod, which again is attached to and actuated by the minute finger of the clock, pressing upon the paper, indicates the uniformity or otherwise of the gas production during each hour of the day and night.



Fig. 61.



Fig. 62.

The size or capacity of a Station Meter is designated by the quantity of gas in cubic feet which it is capable of passing per hour, the measuring wheel making 120 down to 70 revolutions, as a maximum, in that time (the number of revolutions depending on the size of the instrument), with a loss of pressure not exceeding 5-10ths of an inch between the inlet and the outlet. Thus, if the drum have a capacity of 50 cubic feet, $50 \times 120 = 6000$ cubic feet, the size of the Meter. If the capacity be 200 cubic feet, then $200 \times 100 = 20,000$ cubic feet, the size of Meter, and so on.

It is thus easy to determine the capacity of the wheel or drum required to measure any given production. Say the maximum hourly

make of gas in a works is 30,000 cubic feet; then,

$$\frac{30,000}{100} = 300$$
 cubic feet

the required capacity of the measuring wheel or drum. In all cases a reasonable margin in size should be allowed for growing production.

When a Meter wheel is driven beyond the speed above named, the friction is increased, more pressure is absorbed in working the wheel, and the registration is falsified.

The Station Meter should be placed perfectly level on a substantial

foundation, with raised stone base.

It should be fitted with bye-pass and hydraulic trap, with outlet cock; shut-off valves; adjustable overflow pipe; water-line gauge; an ordinary pressure gauge each for the inlet and outlet pipes (Fig. 64), and a differential pressure gauge (Fig. 66); a thermometer; a filling tube and funnel, with stopcock, and a flushing cock.

TABLE.
Station Meter Details.

Quantity Measured per Hour.	Capacity per Revolution.	Number of Revolutions of Measuring Drum per Hour.	Pressure Absorbed in Actuating the Meter.	Diameter of Measuring Drum.	Depth or Length of Measuring Drum, minus Hollow Cover.
	Cubic Feet.		Inch.	Ft. In.	Ft. In.
600	5	120	70	2 6	1 32
900	7.5	120	n	2 101	1 8
1,200	10	120	rb or	3 04	2 01
1,500	12.5	120	10	3 51	2 01
1,800	15	120	10	8 51	2 5
2,400	20	120 120	10	3 64	2 10
3,000	25 30	120	To a	4 0	3 0
3,600 4,800	40	120	******	4 3	4 2
6,000	50	120	10	4 74	4 44
7,200	60	120	10	4 11	4 64
9,600	80	120	. 10	5 6	4 11
12,000	100	120	. 10	5 8	5 61
15,000	150	100	3	6 8	6 3
20,000	200	100	A		6 3
25,000	250	100	A A	8 0 8 0 8 1± 9 6	7 0
80,000	300	100		8 11	7 0 8 1
40,000	400	100	A		8 5
50,000	500	100	10 10 10		9 8
60,000	750	80	10	11 6	10 2 11 7
80,000 100,000	1,000 1,430	80 70	10	12 10 15 4	11 7 12 6

THE PRESSURE GAUGE.

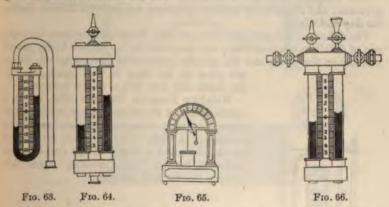
The ordinary Pressure Gauge (Figs. 63 and 64) has its tubes, which are of glass, charged with water to the zero line on the ivory or boxwood scale between. This is graduated into inches and tenths. It is made of any length as required, and the scale may be figured either in inches or tenths of an inch, as shown.

On the Gauge being attached to the main or service pipe, either directly or by means of a short connecting tube, the difference between the two water levels represents the gas pressure.

A series of these Gauges, to indicate the pressure existing between the different apparatus of the gas-works, should be fixed in some posi-

tion convenient for frequent inspection.

King's Gauge (Fig. 65) is constructed on the same principle as the above, but it indicates slighter variations of pressure; the finger having a long sweep for small differences of water level, and the dial being graduated into finer divisions.



The Differential Gauge (Fig. 66) is commonly attached to the inlet and outlet pipes respectively of station meters; the indications of the instrument being the difference in pressure between the two, showing the pressure absorbed in actuating the meter.

Coloured water for Pressure Gauges is made by infusing a little pounded cochineal in hot water. It is then filtered, and a few drops of nitric or hydrochloric acid added, to prevent the bright scarlet colour from fading.

The glass tubes of Pressure Gauges, when foul, may be cleansed with a weak solution of sulphuric acid in water.

PRESSURE AND EXHAUST REGISTERS.

The principle of action of these instruments (Fig. 67), invented by Crosley, is the same as that of the foregoing, but they are made to record as well as indicate the pressure or exhaust, as the case may be.

This is accomplished by means of a float in water, to which a vertical spindle is attached, having a lead pencil at the upper end, pressing upon a cylindrical graduated roll of paper upon a drum, which is caused to revolve by clockwork once in the 24 hours. The paper roll is renewed daily.

The Exhaust Register is connected to the mains on the works, at a point between the hydraulic main and the exhauster, and the record shows whether, in the absence of the manager, the exhauster has been

kept working with regularity.

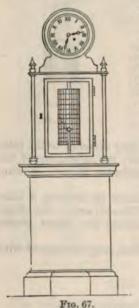
The Pressure Register is attached to the street main beyond the governor, and records the various pressures maintained therein during

the day and night.

The difference between the Exhaust and Pressure Registers is simply one of detail in construction; the zero line in the former being placed midway on the scale, and the spindle lengthened to correspond, whilst

the area of the float is also increased. In the latter the zero line is at the bottom.

Wright's Pressure Register (Fig. 68) is a combination of the King's gauge, with a time-piece, having a circular plate and paper disc instead of a dial. The 24 hours are printed on the disc, and a pencil at the end of a rod actuated by the float, pressing upon this, records the varying pressures.



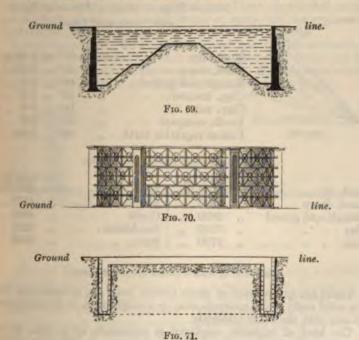


Mr. W. H. Cowan has invented a neat and compact instrument which records the pressures by photography upon sensitized sheets on the revolving cylinder, instead of by the markings of the usual lead pencil.

GASHOLDER TANKS.

The Tank is that portion of the storage reservoir for gas which contains the water in which the floating vessel or holder rises and descends. (Figs. 69 to 71).

It may be constructed either wholly or partially under the ground level, or (as in the case of iron Tanks) entirely above ground. (Fig. 70).



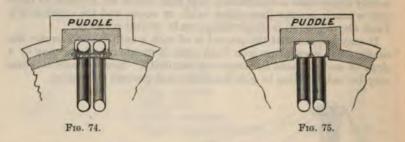
In excavated Tanks, wherever the substratum is favourable, it is economical to leave a circular or conical mound in the centre.

This is called the "dumpling" or "cone" (Fig. 69)

This is called the "dumpling" or "cone." (Fig. 69.)

Tanks are occasionally formed by making a circular cutting in the ground, and erecting therein an iron or brick annular channel to contain the water, the intervening central space being also covered with water, but only to a few inches depth. These are called "Annular" Tanks. (Fig. 71.)

that where the inlet and outlet pipes pass through the wall at the bottom. The instances of failure here are so numerous as to justify the plan, sometimes adopted, of placing the pipes in a recess built in the Tank wall. The objection to this recess is that it breaks the circle of the wall, and consequently weakens its power of resistance to outside pressure; but continuity of the circle can be secured by strutting the opening with cast-iron struts as in Fig. 74.



Or the pipes can be made square in section, and built in with the wall, as in Fig. 75.

When a brick or stone Tank built in blue lias lime mortar is of large dimensions, the walls may be strengthened at intervals of 2 or 3 feet apart, by rings 2 or 3 feet in width, of the brick or stone laid in Portland cement mortar.

Hoop-iron, or flat wrought-iron rings, built at intervals into the masonry or concrete, are occasionally used for giving strength to the walls of a Tank. When the diameter is great, and particularly in Tanks where no puddle is employed, flat bar-iron hoops, braced or tightened by screws or cotters, are also sometimes placed round the outside.

When from any cause it is found impracticable or undesirable to construct a masonry Tank, whether of stone, brick, or concrete, with its coping on a level with the adjacent ground, circumstances may require that the raised portion of the wall should be strengthened, in addition to the support given by the earth backing, either by flat wrought-iron rings built into it, or by outside wrought-iron hoops. One such ring or hoop will suffice for every 4 feet in height of the Tank wall above the natural ground level. The strength of the iron will, of course, be determined by the dimensions of the Tank; but it may be stated, by way of guidance, that for a Tank of 102 feet in diameter, the iron should be 5 inches wide and \(\frac{3}{4} \) of an inch thick. The flat ring is made continuous throughout the circle by riveting, and the hoop by screw-bolts or cotters.

The bricks used in building a Tank should be thoroughly well wetted before being laid, to cause the mortar to adhere.

In time of severe frost all brick and stone work should cease.

To prevent injury in time of rain, and especially in winter, when a sudden frost might supervene, the top of the new walling should be covered with weather boards.

Concrete.

Blue lias lime concrete (for foundations)—	By measure
Gravel, shingle, broken stone, bricks, or old retorts,	
1½ to 2 inches cube	6 parts.
Clean sharp sand	2 parts.
Blue lias or other hydraulic lime	1 part.
Portland cement concrete (for Tank walls)—	
Gravel, shingle, broken stone, bricks, or old retorts.	
1½ inches cube	7 parts.
Clean sharp sand	2 parts.
Portland cement	

Mr. J. Douglas gives the following useful instructions for mixing or preparing the concrete:—"A platform, about 20 feet square, of deals, should be laid on the ground to ensure the clean mixing of the materials. The measure for the material is simply a square box without top or bottom, and should contain, as a convenient quantity, about half a yard. It should be twice as many inches deep as the proportions of cement and ballast. For instance, if the cement is 1 in 8, it should be 16 inches deep. Inside, at 2 inches from the top, nail a lath all the way round; and after placing the measure at one end of the platform, fill the box with shingle or ballast to the level of the lath, and complete with cement, striking the cement level with a straight-edge. The box measure can then be lifted up and removed, when the cement will fall down over and among the aggregate, and the whole mass should be twice turned over dry. Water can then be added through a rose, and the whole turned twice over again. As little water should be added as possible, but enough to thoroughly moisten the whole mass. The concrete is then fit for use. In dry weather it is necessary to keep the work damp, as, if there is not sufficient water to enable the cement to set—about 11½ per cent.—the concrete will be useless. It is also important to thoroughly wet the previous work on which the fresh concrete is to be laid."

Concrete is best placed in position from barrows wheeled close up; it should then be well and solidly rammed down. To tip it from a

height (as was formerly the practice) is objectionable, as tending to

disintegrate the ingredients of which it is composed.

Asphalte or tar concrete has never (so far as I am aware) been tried for a holder Tank; but there is no reason why it should not answer admirably for that purpose. Its composition is as follows:-

Coal tar						6 parts.
Sifted lias lime						2 parts.
Gravel, shingle,						
retorts, not m						7 parts.
Clean, sharp san	ıd					2 parts.

The tar and lime to be first mixed together, and the other materials added. All to be thoroughly dry.

The kind of Mortar employed.

In the construction of brick or stone Tanks, hydraulic mortar or cement mortar, either one or the other, or both, is invariably used. The following is their composition:-

	H_{y_0}	dra	ulic .	Mo	rtar			-
	-							By measure
Best blue lias lime								1 part.
Clean sharp river sa								~ -
A STATE OF THE PARTY OF THE PAR			or,					75/64
Best blue lias lime				- 7				1 part.
Burnt clay								21 parts
			or.					
Best blue lias lime		4				10		1 part.
Puzzolana								
Clean sharp sand								
THE PARTY OF THE P			. ,	, .				-
	C	eme	ent A	Lort	ar.			
Cement, Portland								1 part.
Clean sharp sand								3 parts.

The lime should be fresh burnt, and not more than sufficient of the mortar for a day's work prepared at once. The cement mortar should only be made as it is being used.

The characteristics of good Portland cement are thus succinctly stated by Mr. Faija:—"In colour it should be of a dull bluish grey; and should have a clear, sharp, almost floury feel in the hand; it should weigh from 112 lbs. to 118 lbs. per striked bushel (87 to 92 lbs. per cubic foot), and when moulded into a briquette, or small testingblock, and soaked in water for seven days, should be capable of resisting a tensile strain of from 300 to 400 lbs. per square inch. The cement should, during the process of setting, show neither expansion nor contraction."

Asphalte	or	Tar	Mortar.	
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The tar and lime to be mixed together, and sand, in a thoroughly dry state, to be afterwards added.

Puddle.

For puddle, clay mixed with one-third sand, silt, or soil free from vegetable fibre, is preferable to pure clay, being firmer in texture, and less liable to crack when dry. It should be prepared outside of the trench, put in in thin layers as the wall of the Tank is built, kept moistened, trodden well in with the feet, and backed up with earth carefully pounded. A cubic yard of puddle weighs about 2 tons.

Iron Tanks.

In iron Tanks the flanges of the bottom plates should always be *inside*; whilst those for the sides may be *outside*, and the plates should break joint with each other throughout.

Iron piers, or piers of brick, stone, or concrete, are erected at equal distances apart round the outside of iron Tanks, for the purpose of supporting the gasholder columns or standards. If the Tank is of small dimensions, the standards may be bolted to strong brackets secured to the upper tier of side plates.

Leakages from Iron Tanks.

Leakages of water from iron Tanks may often be greatly reduced or altogether stopped by emptying a bushel or two of horse dung into the water contiguous to the escape. A handful of fine iron filings sprinkled lightly over the dung will be found of advantage. By this simple expedient, very heavy escapes have frequently been reduced to a mere drip within the space of a few minutes.

Dry Wells, and Inlet and Outlet Pipes.

The dry or stand pipe well is not necessarily the invariable accompaniment of a Gasholder Tank. Some engineers prefer to dispense with it altogether.

Many of the largest Tanks are made without dry wells, the inlet and outlet pipes being of such ample diameter as to admit of their examination and repair, if need be, from the inside.

The advantage supposed to be gained by providing a dry well is the facility which it affords of access to the inlet and outlet pipes, both vertical and horizontal, in case of fracture, without disturbing the puddle or other backing of the Tank wall.

In small Tanks it is not unusual to form a recess in the Tank wall in

which the inlet and outlet pipes are placed, and are thus accessible when the Tank is emptied of water. (Fig. 74.)

The inlet and outlet pipes, especially when of wrought-iron, should be securely anchored or bolted down to the stone or concrete base on which they rest within the Tank. If this is not done, the water, by reason of its floating power, is liable to raise them slightly, and so disturb and cause a leakage through or past the middle or concrete in disturb and cause a leakage through or past the puddle or concrete in which the horizontal portions of the pipes are embedded.

Thickness of Tank Walls.

The walls of masonry Tanks (brick, stone, and concrete) are never required to resist, unsupported, the pressure of the water acting upon their sides; but are invariably built under the surface level of the ground within the space of an excavation made for that purpose, and having a backing of earth carefully rammed all round them. This earth backing usually offers a resistance to the pressure of the water within the Tank, greater than the combined weight of the wall and the cohesive nature of its component ingredients; and consequently in designing a Tank wall, this fact is allowed for, and a deduction made from the calculated unsupported thickness of the masonry.

In the well-known Mémoire by M. Arson, a translation of which, by Dr. Pole, is given in "King's Treatise" (Vol. II., p. 181 et seq.), the author investigates this subject with his usual ability. After some preliminary observations on the nature of the ground, and the choice and placing of material, he proceeds to a consideration of the forces and resistances in a Gasholder Tank of masonry, and deduces the

following formulæ:-

As to the Pressure of the Water.

(1) S D
$$\frac{H^{0}}{6}$$
 = the total force of the water.

Then as to the threefold resistance to this force.

(1) C
$$D^1 \frac{H^2}{2}$$
 = the resistance of the earth backing.

(2)
$$\frac{P E^2 D^1 H}{2}$$
 = the resistance of the weight of the masonry.

(3) K H2 E = the resistance due to cohesion.

Adding the combined resistance from the three sources together, we have-

$$C D^{1} \frac{H^{2}}{2} + \frac{P E^{2} D^{1} H}{2} + K H^{2} E.$$

And to produce stability of the Tank these must be greater than the effect of the pressure of the water-

$$S\;D\;\frac{H^n}{6}$$

where D = Internal diameter of the Tank in feet.

E = Thickness of the wall (average) in feet. D'= External diameter of the Tank in feet.

H = Height of wall in feet.

S = Weight of a cubic foot of water.

C = Resistance of the earth backing in lbs. per sq. foot.

P = Weight of a cubic foot of the masonry.

K = Cohesive force per sq. foot.

Applying these formulæ to one of the examples of Tanks actually constructed, let us see how they work out. Take the Tank described on p. 180 :-

D = Internal diameter of tank, 122 feet.

E = Average thickness of wall, 21 feet.

D' = External diameter, 127 feet. H = Height (or depth), 24 feet.

S = Weight of a cubic foot of water, 62.5 lbs.
C = Resistance of the earth backing per sq. foot, clay and earth, say average 1200 lbs.

P = Weight of a cubic foot of the masonry, 112 lbs.

K = Cohesive force per sq. foot, bricks in 1 Portland cement to 3 sand, mortar, 31,680 lbs.

Then-

(1) S D
$$\frac{H^3}{6}$$
 = 62.5 × 122 $\frac{24^3}{6}$ = 17,568,000 = total force of the water in lbs.

(1) C
$$D^{1}\frac{H^{2}}{2}$$
 = 1200 × 127 $\frac{24^{2}}{2}$ = 48,891,200 = resistance of earth backing.

(2)
$$\frac{P E^2 D^1 H}{2} = \frac{112 \times 2 \cdot 5^2 \times 127 \times 24}{2} = 1,066,800 = \text{resistance of weight of masonry.}$$

(3) K H² E =
$$31680 \times 24^2 \times 2.5 = 45,619,200 = \text{resistance due to cohesion.}$$

90.577.200 = total resistance in lbs.

or about five times the pressure of the water, which is an ample

margin for safety.

It has already been pointed out that the walls of brick Tanks, which are porous in some degree, having a backing of clay puddle behind and over the Tank bottom, are placed in equilibrium by the water on both sides, and therefore do not require to be of as great a thickness as those with an internal lining of cement impermeable to water. In the latter case special care should be taken to see that the earth backing is thoroughly consolidated behind the wall, so that the pressure of the water against the Tank may be transmitted thereto direct, without danger of rupture to the masonry.

When it is required to ascertain the thickness of any portion of a Tank wall to resist the force of the water pressing against it, the

formulæ as under is applicable :-

PD K-P=thickness in inches.

Where P = the pressure of the water in lbs. per square inch.

D = the radius of the Tank in inches.

K = the safe cohesive force in lbs. per square inch.
Example.—A brick and puddle Tank set in Portland cement mortar is 122 feet in internal diameter and 24 feet deep to the surface of the rest stones. Required thickness of wall immediately above footings.

The pressure of the water on each square inch will therefore be-

$$\frac{62.5 \times 24}{144} = 10$$
 lbs. pressure of water per square inch.

The safe cohesive strength of the brickwork in Portland cement mortar (1 cement, 3 sand) may be taken at 220 ÷ 2 = 110.

 $\frac{PD}{K-P} = \frac{10 \times 732}{110-10} = \frac{7320}{100} = 74$ inches, nearly, or 6 ft. 2 in. the required thickness of the wall. It will be seen, however, that in

this calculation no account has been taken either of the resistance offered by the weight of the masonry, or of the support given by the earth backing; so that the result obtained is the theoretical thickness of the wall to resist the pressure of the water without any backing. And as this latter may be taken as fully equal to the other, the thickness obtained by the calculation may be reduced by one-half—i.e., to 3 ft. 1 in .- which will be the required thickness of the wall above the footings. The required thickness at any other depth may be found in like manner. The pressure of the water, which varies in proportion to the depth, may be represented by a right-angled triangle A B C. A

and, therefore, the thickness at the top would work It must not be overlooked, howout to nothing. ever, that the Tank sides act as a retaining wall to the earth both during construction and at any time afterwards, when the water is withdrawn; and consequently the thickness should be graduated from the ascertained thickness at the base to about 21 or 3 bricks width at the coping.

The thickness of 31 feet at the base of the wall is too thin by more than one-half for an ordinary retaining wall of that height (24 feet); but it must be remembered that this apparent weakness is counterbalanced by the circular form of the structure, possessing as it does all the qualities of the arch, and being built up, both wall and backing, gradually throughout the complete circle from base to coping.

The conditions as regards backing of cast and wrought-iron Tanks are different. These being generally erected above ground, the resistance offered to the bursting force of the contained water is entirely

due to the cohesive strength of the metal.

B

The same formula, however, is applicable here, as will be seen from the next example of a cast-iron Tank, where the safe cohesive strength of the iron is taken at 4000 lbs. per sectional square inch, its ultimate tenacity being 16,000.

Example. - A cast-iron Tank is 80 feet in internal diameter and Required the thickness of the lower ring of plates. 18 feet deep. These are generally 3 to 4 feet in depth, but the water pressure on the lowest foot may be taken.

Here
$$\frac{62.5 \times 18}{144}$$
 = 7.8 lbs. pressure of water per square inch.
Then—
$$\frac{P D}{K - P} = \frac{7.8 \times 480}{4000 - 7.8} = \frac{3744}{3992.2} = .937, \text{ or say 1 inch.}$$

the required thickness; and so in like manner the required thickness of the several higher rings may be ascertained. This thickness may be slightly reduced by making allowance for the assistance given to the lower ring of plates by their attachment to the plates forming the bottom of the Tank, and especially if iron hoops are employed round the outer circumference to give rigidity to the structure.

The safe cohesive strength of wrought-iron plates may be taken at

10,000 lbs. per sectional square inch.

Examples of Construction.

The following are examples of Gasholder Tanks constructed under moderately favourable circumstances. It will be found advisable in practice, in some instances, to increase the strength of the walls and footings, and even to put a bed of concrete below the latter where the underlying strata are of an unsatisfactory character.

BRICK TANKS.

Diameter, 21 ft. 6 in. Depth, 10 ft.

> Footings, 3 single courses; width respectively, 3, 21, and 2 bricks.

> Wall, 11 bricks thick for half the height, diminishing by an offset on the outside to 1 brick for the remainder.

Coping of wall, bricks set on edge, in cement.

Piers to support gasholder columns, 4 in number, brought up from foundation, and built in with the wall, each capped with a stone 2 ft. square, 8 in. thick, having 3 holes drilled in each for the holding-down bolts.

Rest stones, 8 in number, 15 in. square, 6 in. thick, laid on footings built at bottom, bound in with the wall-footings.

Puddled with clay, mixed with one-third fine sand, or soil free from vegetable fibre, 2 ft. thick at bottom; and at the sides, tapering from 2 ft. at the base to one foot at the top.

Bottom, flagged with 3-in. flags. Bricks, best hard-burnt stocks.

Mortar, lias lime one-third, sharp river sand two-thirds.

Diameter, 38 ft. 6 in. Depth, 12 ft.

Footings, 2 double courses, width 3 and 2½ bricks. Wall, 2 bricks thick for 8 ft. high, and 1½ bricks for the remaining 4 ft., set off on outside.

Coping of wall, bricks on edge, laid in cement.

Piers, 4, bound in with wall, and brought up from foundation, each capped with a stone 2 ft. square, 9 in. thick, with 3 bolt-holes.

Stones at bottom, for bottom curb of holder to rest on when down, 8; each 16 in. square, 6 in. thick, let into face of

wall 2 in.; laid on footings.

Puddled with clay puddle, composed of two-thirds clay and one-third fine sand, trodden well together, 2 ft. thick at bottom and sides, tapering to 1 ft. 6 in. at top.

Bottom, flagged with yard flags, 3 in. thick.

Bricks, best hard-burnt stocks.

Mortar, composed of best lias lime, mixed with two-thirds sharp sand.

Diameter, 39 ft. Depth, 14 ft.

Footings, 2 double courses, $3\frac{1}{2}$ bricks wide at base, diminishing by offsets to commencement of wall.

Wall, $2\frac{1}{2}$ bricks at bottom to height of 6 ft.; next 4 ft., 2 bricks; remaining 3 ft. 6 in. to underneath coping, $1\frac{1}{2}$ bricks thick. Coping stones, 6 in. thick, laid in cement, and cramped together

on the outside.

Piers, 5, brought up from foundation, each capped with a stone 2 ft. 6 in. square, 9 in. thick, with 4 bolt-holes.

Rest stones, 10, let 3 in. into face of wall, 18 in. square, 6 in. thick on footings.

Puddled with clay, mixed with one-third sand, 2 ft. thick at bottom and at the sides, tapering to 1 ft. 6 in. at top.

Bottom, brick paved.

Bricks, best hard-burnt stocks.

Mortar, lias lime, mixed with two-thirds sharp river sand.

Diameter, 51 ft. 6 in. Depth, 16 ft.

Footings, 2 double courses, 31 and 3 bricks wide.

Wall, thickness at base to height of 7 ft., 2½ bricks; next 5 ft., 2 bricks; and remaining 4 ft., 1½ bricks.

Coping, bricks on edge, set in cement.

Piers, 5, carried up from foundation, each pier capped with a stone 3 ft. square, 9 in. thick, having 4 holes for holding-down bolts.

Rest stones, 10, 18 in. square, 6 in. thick, laid on footings, and let 3 in. into face of wall.

Puddled with clay, mixed with one-third sand, 2 ft. thick at bottom and sides, diminishing to 1 ft. 6 in. at top.

Bottom flagged with yard flags 3 in. thick, bedded on the puddle.

Bricks, best hard-burnt stocks.

Mortar, lias lime, mixed with two-thirds sharp river sand.

Diameter, 62 ft. Depth, 14 ft.

Footings, 4 courses; width respectively 4½, 4, 3½, and 3 bricks. Wall, thickness at base to height of 5 ft., 2½ bricks; next 5 ft., 2 bricks; remaining 3 ft. to underneath coping, 1½ bricks.

Coping stones, 1 ft. thick, dressed to the proper radius, and laid in cement.

Piers, 6, brought up from foundation, bound in with tank wall, each capped with a stone 3 ft. square, 10 in. thick, with 4 boltholes.

Rest stones, 12, 18 in. square, 8 in. thick, laid on footings.

Mound left in bottom of tank, 8 feet less in diameter than the latter, flagged round the base, other part pitched with random stones.

Puddled with clay two-thirds, intimately mixed with one-third sand; 2 ft. thick at bottom; the sides, 2ft. at base to 1 ft. 6 in. at top.

Bricks, best hard-burnt stocks.

Mortar, lias lime, mixed with two-thirds sand.

Diameter, 62 ft. Depth, 20 ft.

Footings, 5 courses, first course, double, 5 bricks in width; others single; 4½, 4, and 3½ bricks wide respectively.

Wall thickness at base to height of 9 ft., 3 bricks; next 6 ft., 21 bricks; remaining 5 ft. to underneath coping, 2 bricks.

Coping stones, 1 ft. thick, dressed to the proper radius, and laid in cement.

Piers, 8, brought up from foundation, bound in with tank wall, each capped with a stone 3 feet square, 12 in. thick, with 4 bolt-holes.

Rest stones, 16, 2 ft. 6 in. long, 12 in. wide, 10 in. thick.

Mound left in bottom of tank, 11 feet less in diameter than the latter, covered with concrete 6 in. thick.

Puddled with clay; 18 in. thick at bottom; the sides, 2 ft. at base to 1 ft. 6 in. at top.

Bricks, best hard-burnt seconds.

Mortar, 1 Portland cement to 2 of sharp sand.

Diameter, 83 ft. 6 in. Depth, 20 ft.

Footings, 4 courses; first course, double, 5 bricks in width; others single; 4½, 4, and 3½ bricks wide respectively.

Wall, from base to height of 7 ft., 3 bricks; next 7 ft., 2½ bricks; and remaining 6 ft., 2 bricks thick.

Coping, bricks set on edge, and laid in cement.

Piers, 9, brought up from foundation, each capped with a stone 4 ft. square, 10 in. thick, with 4 holes for holding-down bolts of columns.

Rest stones, 18, 24 in. square, 10 in. thick, laid on footings, and let 3 in. into sides of tank.

Puddled with clay, mixed with one-third sand, 2 ft. thick at bottom; the sides, 2 ft. at base, tapering to 1 ft. 6 in. at top.

Centre pillar, to support crown of gasholder when down, built of brick, coated with cement.

Bottom, flagged with Yorkshire flags, 4 in. thick.

Bricks, best hard-burnt stocks.

Mortar, lias lime, mixed with two-thirds sharp river sand.

Diameter, 102 ft. Depth, 24 ft.

Footings, 6 bricks wide at base, diminishing by offsets to the bottom of wall.

Wall, thickness at base to 7 ft. in height, 4 bricks; next 7 ft., 3½ bricks; next 5 ft., 3 bricks; and remaining 4 ft. to coping, 2½ bricks thick.

Coping of stone, 1 ft. thick.

Piers, 12, carried up and built in with wall from foundation. Each capped with a stone 4 ft. square, 15 in. thick, with 4 bolt-holes.

Rest stones, 24, 2 ft. 6 in. square, 12 in. thick, let 4 in. into bottom of wall, and resting on footings.

Stones, 72 in number, 18 in. long, 12 in. by 12 in., built into tank wall, against which the channel guides are fastened.

Puddled with clay, mixed with one-third sand, 2 ft. thick at bottom; the sides, 2 ft. 6 in. at base, tapering to 1 ft. 6 in. at top.

Bottom, concreted over the puddle to the depth of 10 in.

Centre pillar, to support gasholder crown.

Bricks, best hard-burnt stocks.

Mortar, lias lime, mixed with two-thirds sharp river sand.

Diameter, 102 ft. 6 in. Depth, 30 ft.

Footings, 1 double and 4 single courses, respectively 6, $5\frac{1}{2}$, 5, $4\frac{1}{2}$, and 4 bricks wide.

Wall, 3 bricks wide for 10 ft. high; next 10 ft., 2½ bricks; and remaining 9 ft. to coping, 2 bricks.

N 2

Coping of stone, 12 in. thick, not less than 4 ft. long each stone, Strengthening rings, of brickwork, laid in cement, 5—

1st ring, 2 ft. 6 in. from bottom, 7 bricks deep.
2nd do. 8,, 6,, ,, 6 do.
3rd do. 14,, 0,, ,, 6 do.
4th do. 19,, 6,, ,, 5 do.
5th do. 24,, 0,, ,, 4 do.

Piers, 12, brought up from foundation along with and bound into the wall, each capped with a stone 4 ft. 6 in. square, 15 in. thick, with 4 bolt-holes.

Rest stones, 24, 27 in. square, 12 in. thick, on footings, and let 4 in. into tank wall.

Puddled with clay, mixed with one-third sand, 2 ft. thick throughout.

Centre pillar, of brick, to support gasholder crown, cemented

Bottom concreted to the depth of 12 in. over the puddle.

Bricks, best hard-burnt stocks.

Mortar, lias lime, mixed with two-thirds sharp river sand.

Diameter, 122 ft. Depth, 24 ft.

Concrete under footings of wall and rest stones, 12 in. thick and 10 ft. wide.

Footings, 8 bricks wide at base, diminishing by 8 offsets to the bottom of the wall.

Wall, thickness at base to 8 ft. 9 in. in height, 4 bricks; next 7 ft., $3\frac{1}{2}$ bricks; next 4 ft. 6 in., 3 bricks; and remaining 3 ft. to coping, $2\frac{1}{2}$ bricks thick. Batter of wall 1 in 100.

Coping of stone, 9 in. thick, by 24 in. wide, and not less than

3 ft. 4 in. long.

Piers, 14, each 7 bricks square carried up and built in with wall from foundation, and capped with a stone 5 ft. 4 in. square, 18 in. thick, and with 4 holding-down bolts to each.

Rest stones, 28, 3 ft. 6 in. by 2 ft. by 12 in. thick, let into wall

41 in., and resting on footings.

Guide rail stones 56 in number, built into tank wall, 28 of which are 2 ft. by 1 ft. 6 in. by 1 ft. 6 in., the remaining 28 being 2 ft. 6 in. by 1 ft. 6 in. by 1 ft.

Brick ring or apron extending 6 ft. from inside of tank wall at the bottom to form a floor, 3 courses of bricks thick laid flat.

Centre pillar of brickwork, 4 ft. diameter.

Mortar Portland cement, 1 part; sand 3 parts.

Bricks, picked common.

Puddle behind wall of tank, 24 in, thick at bottom, tapering t 18 in. at top. On cone in tank bottom 18 in. thick. Concrete over surface of puddled cone in bottom, 6 in. thick.

Diameter, 145 ft. Depth, 55 ft.

Top of tank, 4 ft. above ground level.

Footings, 4 double courses, respectively 5 ft., 4 ft. 8 in., 4ft. 41 in.,

and 4 ft. wide.

Wall, to height of 10 ft. above footings, 3 ft. 7 in., or 41 bricks thick; next 10 ft., 4 bricks; next 10 ft., 31 bricks; next 15 ft., 3 bricks; next 5 ft., 21 bricks; remaining 4 ft., exclusive of coping, 2 bricks thick.

Strengthening rings, or courses, 6 courses in every 5 ft. of height; also the 3 finishing courses, and the corresponding courses in piers, set in cement. The brickwork at no part carried higher than 5 courses of bricks, until the circle up to that level is completed, puddled, and backed up.

Coping of stone, 12 in. thick, bedded in cement.

Piers, 16, 4 ft. 3 in. wide, each capped with a stone 5 ft. square, 18 in. thick, for supporting columns; 4 holes in each for holding-down bolts; the said holding-down bolts, with castiron plate, built into each pier, 10 ft. below level of coping.

Rest stones, 32, let 41 in. into face of wall, and resting on piers

of brickwork forming part of the general footings.

Blocks of stone, 18 in. by 12 in. by 12 in., inserted in wall opposite each pier, for securing guides.

Cone in centre of tank, 6 ft. less in diameter at the base than the interior of tank; lower part, to height of 20 ft., paved with 4 courses of brickwork; upper part, of clay only.

Puddle, not less than 18 in. in thickness, and kept constantly well moistened; the earth being firmly pounded in behind.

Bricks, best hard-burnt stocks.

Mortar, composed of 1 part fresh burnt lias lime, to 3 parts of clean, sharp river sand; not more than sufficient for one day's work made at one time.

Cement, fresh burnt, with equal proportions of sand, mixed as it

is being used.

Dry, or stand pipe well, 15 ft. diameter, 63 ft. deep, paved with 3 courses of brickwork on edge, set in cement.

Diameter, 154 ft. Depth, 40 ft. 6 in.

Foundation of concrete 12 in. thick, 18 ft. wide under piers, and 11 ft. wide under walling.

Wall, starts from concrete foundation without footings, 5 bricks thick for a height of 16 ft. 10 in.; next 4½ bricks for 6 ft. 5 in. deep; next 4 bricks for 6 ft. 5 in.; next 8½ bricks for 6 ft. 5 in., and 3 bricks the remaining height.

Coping of stone, 12 in. by 2 ft. 3 in., in lengths not less than

4 ft. 6 in.

Piers, 16 in number, 6 ft. square from bottom to top, capped with hard Yorkshire stones, 6 ft. square and 2 ft. thick, with 4 bolt-holes in each.

Rest stones, 32, 4 ft. 10 in. by 2 ft., by 1 ft., built 4½ in. in tank wall.

Guide rail stones, 144 in number, 112 of which are 2 ft. by 1 ft. 9 in. by 1 ft., and the remaining 32 being 2 ft. by 1 ft. 9 in. by 1 ft. 6 in.

Puddled with clay 24 in. thick over surface of mound in bottom,

and behind tank wall.

Brick apron, 2 ft. thick and 6 ft. wide, round bottom of tank wall inside, upon which the rest stones are set.

Centre pillar of brick, 6 ft. square at bottom and 6 ft. 3 in. square at top, capped by a stone 12 in. thick.

Mortar, Portland, cement, 1 part; sand, 3 parts.

Bond, English; alternate courses of headers and stretchers throughout.

Dry well, 10 ft. in diameter, 48 ft. 6 in. deep.

Diameter, 182 ft. Depth, 40 ft.

Footings, 3 ft. deep below tank bottom, in 3 equal set-offs; placed on elm sleepers, 9 in. by 4 in.

Wall, thickness at base to 15 ft. in height, 4½ bricks; next 15 ft., 4 bricks; next 5 ft., 3 bricks, and remaining 4 ft., 2½ bricks

thick.

Coping, Bramley Fall stone, 12 in. thick, and 24 in. wide.

Piers, 28, 6 ft. thick from inside tank to outside pier, and 8 ft. 9 in. wide side to side, capped with granite blocks, 5 ft. 3 in. square and 2 ft. thick, with 4 bolt-holes in each.

Rest stones, 28, built in wall 12 in., are each 4 ft. by 2 ft. 6 in.

by 12 in. thick.

Guide rail stones, 112 in number, 18 in. by 12 in. by 12 in.

Puddled with clay on cone in bottom of tank, under footings, and behind tank wall a uniform thickness of 24 in.

Cone at bottom covered over the clay with 9 in. of concrete, and paved with a layer of bricks on edge, set in cement.

Centre pillar of brickwork, 7 ft. 6 in. square, capped with granite block, 2 ft. thick, the whole on a foundation of concrete.

Bricks, best hard-burnt stock bricks.

Mortar, blue lias lime mortar.

Brick ring or apron, 3 ft. thick, extending 6 ft. 6 in. from inside of tank wall at the bottom, to form a floor.

Diameter, 200 ft. Depth, 36 ft.

Footings, laid on elm boards 11 in. thick, placed on the puddle, are 9 bricks wide at base, diminishing by 21 in. offsets to

bottom of wall.

Wall, thickness at base to 12 ft. in height, 5 bricks; next 6 ft., 4½ bricks; next 5 ft., 4 bricks; next 5 ft., 3½ bricks; next 5 ft., 3 bricks, and the remaining portion, 2½ bricks; being finished at top, to form a coping, with Staffordshire blue bricks set on edge in cement.

Piers, 22 in number, 5 ft. 6 in. from inside tank to outside the pier, and 7 ft. wide from side to side, surmounted by Bramley Fall column stones, 6 ft. by 5 ft. 6 in. by 1 ft. 4 in. thick, with

4 holes in each.

Piers, intermediate, 22 in number, 5 brick lengths square, brought up from bottom, and capped with stones, 2 ft. square, and 1 ft. 6 in. thick.

Rest stones, 44, 4 ft. 6 in. by 3 ft. by 1 ft. 3 in. thick, set into wall 4½ in. and bedded on concrete.

Guide rail stones, 44, 2 ft. square by 1 ft. 6 in.

Puddled with clay, over cone in centre, and under footings 2 ft. 6 in. thick, behind tank wall 2 ft. thick at bottom, tapering to 1 ft. 6 in. at top.

Concrete apron, 2 ft. thick, extending 9 ft. from tank wall all round. Cone, covered with 6 in. of concrete over the clay puddle.

Bricks, well burnt Oldbury brown bricks. Mortar, blue lias lime, 1 part; sand, 2½ parts.

Bond, English, alternate courses of headers and stretchers

throughout.

Hoop-iron bond, every sixth course in height, 1½ in. by 1-16th in. is inserted as follows:—In the 5 bricks thick part, 5 rows are laid in the thickness of the wall at equal distances apart; in the 4½ and 4 bricks thick part, 4 rows; 3½ and 8 bricks part, 3 rows; and 2 rows for the remaining height.

Shallow dry well, 12 ft. diameter, 20 ft. deep.

Diameter, 203 ft. 6 in. Depth, 38 ft.

Footings, bottom course, 7 bricks wide, 4 bricks deep, and 4 single courses, respectively 6, 5\frac{1}{2}, 5, and 4\frac{1}{2} bricks wide.

Wall, thickness for a height of 20 ft., 4 bricks; next 9 ft., 8½ bricks; next 8 ft., 8 bricks.

Coping stone, 24 in. wide, 12 in. thick.

Strengthening rings of brickwork laid in cement, 5, divided equally throughout the depth of tank wall, 10 bricks each in depth.

Piers, 18, on foundations brought up from bottom of tank footings and bound in with wall, each capped with a stone 6 ft. square, 18 in. thick, 4 holes for bolts, the latter with plate built into pier, 10 ft. below the top of coping.

Rest stones, 36, 4 ft. square, 12 in. thick, on footings brought up

from bottom of wall footings.

Puddled with clay, mixed with one-third sharp sand, and not less than 2 ft. thick in any part.

Bottom concreted over the puddle to the depth of 12 in.

Bricks, best hard-burnt stocks.

Mortar, 1 part lias lime to 2 parts sharp river sand.

Diameter, 218 ft. Depth, 44 ft. 6 in.

Foundation of concrete 2 ft. thick, 9 ft. 5 in. wide, including apron. Wall, thickness at base to 20 ft. in height, 5 bricks; next 5 ft., 4½ bricks; next 5 ft., 4½ bricks; next 5 ft., 8½ bricks; next 5 ft., 3 bricks, and the remaining portion 2½ bricks; 7 circular bands of brickwork, 6 courses deep each, and extending through the full thickness of the wall, are built in equidistantly in the height of the wall set in Portland cement mortar, the intervening portions of the wall being set in hydraulic lime mortar all in English bond.

Coping of Yorkshire stone, 2 ft. 5 in. by 6 in., in 5 ft. lengths,

projecting 1 nch over wall.

Piers, 24, each 7it from inside tank wall to outside of pier, and 5 ft. 6 in. wide, side to side, capped with Bramley Fall stones, 7 ft. by 5 ft. 6 in. by 2 ft., having 7 bolt-holes in each.

Piers, intermediate, 24, each 3 ft. 10 in. square, capped with

stones 4 ft. by 4 ft. by 6 in.

Rest blocks of concrete, 48, each 4 ft. 6 in. long by 2 ft. wide, and standing 6 in. above the concrete apron.

Guide rail stones, 288, each 18 in. by 12 in. by 12 in., projecting 1 in. from face of tank wall.

Puddled with clay, not less than 18 in. at any part.
Truncated surface of cone paved with stones.
Mortar, blue lias hydraulic lime, 1 part; sand, 3 parts.
Cement mortar, ortland cement, 1 part; sand, 3 parts.
Concrete, Portland cement, 1 part; river ballast, 7 parts.
Shallow dry well, 12 ft. diameter, 26 feet deep.

COMPOSITE TANK.

Diameter, 152 ft. Depth 31 ft.

Footings, 8 ft. 6½ in. wide at bottom, including apron, 2 ft. 6 in. thick.

Wall, brick faced, 9 in. thick, in English bond; backing of concrete; thickness at base, including the backing, to 13 ft. 9 in. high, 3 ft. 4½ in.; next 8 ft. 6 in., 3 feet thick; and the next 8 ft. 6 in., 2 ft. 8 in., to the underside of coping.

Coping of stone, 1 ft. 10 in. by 12 in., in 3-ft. lengths.

Piers, 16, are 8 ft. from inside tank wall to outside pier, and 4 ft. 6 in. wide, from side to side, formed of 9-in. brickwork on three sides, and filled in with concrete, the whole being capped with a stone 8 ft. by 4 ft. by 1 ft.

Rest stones, 2 to each pier, or a total of 32, each 4 ft. by 1 ft. 6 in.

by 9 in.

Guide rail stones, 48, each 2 ft. by 1 ft. by 9 in.

Puddled with clay, 2 ft. thick throughout.

Cone, concreted over the clay puddle to a depth of 12 in. and rendered.

Centre pillar, solid brickwork, 6 ft. 6 in. diameter at top, the sides having a batter of 1 in 40; built on a foundation of concrete 10 ft. square and 8 ft. deep. Stone cap, 6 ft. diameter by 1 ft. thick, on which is placed a double layer of 4-in. oak planking.

Hoop-iron bond, tarred and sanded, 11 in. wide, 1-12th in. thick is placed every 41 ft. in height, in the proportion of 1 strip to

to every 41 in. in thickness of the wall.

Mortar, Portland cement, 1 part; sand, 3 parts.

Concrete, Portland cement, 1 part; sand, 3 parts; coarse screened stones, 1½ in. diameter, 4 parts.

Dry well, 11 ft. diameter, 40 feet deep to floor.

CONCRETE TANKS.

Diameter, 82 ft. Depth, 28 ft.

Wall, 3 ft. 8 in. thick at bottom, tapering on the outside to 2 ft. 4 in. at the top, built entirely of concrete, and rendered on inside with neat Portland cement \(\frac{1}{4} \) in. thick.

Piers, 10, each 4 ft. by 8 ft. 8 in. of concrete.

Rest blocks of concrete 21 ft. long, 18 in. wide, 6 in. thick.

Backing composed of sand.

Cone, concreted over surface, 18 in. thick, and rendered with neat cement \(\frac{1}{2} \) in. thick.

Centre pillar, 4 ft. square, 8 ft. high.

Concrete, Portland cement, 1 part; sand, gravel, old retorts, and clinkers, 5 parts.

Diameter, 184 ft. Depth, 47 ft.

Wall, 5 ft. thick at bottom, tapering on the outside to 2 ft. 3 in. at the top, built entirely of concrete, and rendered on inside with neat Portland cement 3 in. thick.

Piers, 20, each 8 feet thick, of concrete entirely.

Rest blocks of concrete, 6 ft. long.

Puddle, none.

Cone, concreted over surface, 12 in. thick, and rendered with neat cement 3/4 in. thick.

Centre pillar, hollow, external diameter 14 ft., internal ditto, 10 ft.

Concrete, Portland cement, 1 part; gravel, sand, ballast, burnt clay, old retorts, and clinkers, 7 parts.

Dry well, 10 ft. diameter, 53 ft. deep, built of concrete 2 ft. thick, and rendered outside with neat cement.

STONE TANK.

Diameter, 89 ft. Depth, 20 ft.

Footings, 2 courses. First course composed of stones at least 3 ft. 6 in. square and 9 in. thick; second course, 3 ft. square, 9 in. thick, breaking joint at least 1 ft. on the vertical joint.

Wall, to underneath coping, built of stones not less than 16 in. on the inner face, dressed to the proper radius; no stone having less than 10 in. of a square joint, nor less than 18 in. on the bed, and 5 in. thick. Walling carried out in horizontal courses throughout the circumference of the tank, and backed up with good strong random. Two throughs to every superficial yard. Thickness of wall at base, random included, 2 ft. 8 in., gradually diminishing to 1 ft. 8 in. at top.

Coping of stones, 1 ft. 11 in. broad, 8 in. thick, and not less than 3 ft. 6 in. long, dressed to the proper radius, and laid in

cement.

Piers, 9, bound in and built up along with the tank wall; a through of entire size every vertical yard, and capped with a solid cover 3 ft. 6 in. square, 15 in. thick, having 4 holes for foundation bolts of columns.

Rest or bearing stones, 18, throughs 2 ft. wide and 1 ft. thick built in along with wall footings, and projecting 1 ft. 9 in. into the tank.

Mound or cone in bottom of tank, covered with puddle to the depth of 24 in., its base flagged with a course of yard flags 4 in. thick, the remainder pitched with dry rubble.

Pillar in centre of tank, capped with a solid stone 4 ft. square, 15 in. thick, for supporting crown of gasholder when down.

Mortar, lias lime, one-third; sharp clean sand, two-thirds.

CAST-IRON TANKS.

Diameter, 33 ft. Depth, 15 ft.

Plates, not more than 4 ft. in length or width. All, except top course or tier, strengthened with diagonal ribs. Lowest tier, \(\frac{3}{4}\) in. thick; top tier, \(\frac{1}{2}\) in. thick; intermediate and bottom plates, \(\frac{5}{4}\) in. thick. Small brackets or snugs, projecting 4 in., cast \(1\frac{1}{2}\) in. below centre of side plates, to support the strengthening hoops.

Flanges, 3 in. wide, with brackets between the bolt-holes. Bolt-holes, square, § in. and ½ in., and 6 in. apart, centres.

Bolts of bottom plates and two lower tiers of sides, 5 in.; all the others, 1 in. square under head.

Hoops of flat wrought-iron, 3 in. by 5 in., bound round each tier of side plates with jaws and screws.

Joints, 1 in. thick, caulked with iron cement.

Diameter, 61 ft. Depth, 17 ft.

Plates, bottom, 1 in. thick, except outside row, 1\frac{1}{8} in. thick. Sides, first tier, 1\frac{1}{8} in.; second, 1 in.; third, \frac{7}{8} in.; and 4th, \frac{3}{4} in. thick. Depth, 4 ft. 3 in.; width, 4 ft. 9 in. Say, 40 plates in each tier. Snugs, projecting 4 in., cast on each plate, 2 in. below centre, to support the binding hoops.

Flanges, 3 in. wide, not less than \(\frac{3}{4} \) in. thick; brackets \(\frac{1}{2} \) in. thick between the bolt-holes.

Bolt-holes, square, 3 in.; 7 in. apart, centre to centre.

Bolts, 3 in., square under head.

Hoops of flat-iron, 3½ in. by ¾ in., with suitable jaws and tightening screws bound round each tier of side plates.

Joints, 1 in. thick, caulked with iron cement.

Diameter, 101 ft. Depth, 22 ft. 8 in.

Plates, bottom, outside row, 11 in., and remainder 1 in., except

centre plate, $1\frac{1}{2}$ in. Sides, first and second tiers, $1\frac{1}{4}$ in.; third tier, $1\frac{1}{8}$ in.; fourth and fifth tiers, 1 in. thick. Width, 4 ft. $2\frac{3}{4}$ in. (say 75 plates in each tier); depth, 4 ft. $6\frac{1}{2}$ in. Bearing bracket, projecting 5 in., cast on each plate, $2\frac{1}{2}$ in. below centre, to support the strengthening hoops.

Flanges, 31 in. wide, equal to plates in strength; brackets, 3 in.,

between the bolt-holes.

Bolt-holes, square, 1 in.; 7 in., centre to centre.

Bolts, 1 in., square under head.

Hoops, flat-iron, 5 in. by 11 in., with jaws and screws, bound

round each tier of side plates.

Joints, ½ in. thick, caulked with iron cement.

WROUGHT-IRON TANK.

Diameter, 51 ft. 4 in. Depth, 14 ft.

Plates, 3 in. thick, both sides and bottom, with the exception of the outer row in the latter, and those to which the guide rails

are fixed up the sides, which are 1 in. thick.

Curbs, of angle-iron, extending round the entire circumference of the tank outside; top curb, 4 in. by 4 in. by ½ in.; two intermediate curbs or rings the same size, and bottom curb ¼½ in. by ½½ in., all butt-jointed, and with lapping pieces not less than 18 in. long, riveted to the side plates of the tank with ½ in. rivets 6 in. apart.

Vertical stays, 12 in number, serving as guides for the holder, 14 ft. long, formed of two 3 in. by $2\frac{1}{2}$ in. by $\frac{3}{8}$ in. angle-irons placed thus: \parallel and riveted to the $\frac{1}{4}$ in. plates up the sides

before mentioned with rivets 6 in. apart.

Lap of plates, not less than 1½ in., riveted hot with § in. rivets, 1½ in. centres.

Masonry standards or iron brackets to support columns.

ANNULAR OR RING TANKS.

Cast-Iron.

Diameter, 75 ft. Depth, 19 ft.

Plates, bottom or ring plates, 3 ft. 6 in. wide, 1 in. thick. Inner circles, 1 tier of plates only, 4 ft. deep, 1 in. thick; strengthened with 2 horizontal ribs 2 in. deep by 3 in. thick on side next

centre of tank, and on other side with 2 vertical brackets. 9 in. at bottom, diminishing to nothing at top, \$\frac{3}{2}\$ in. thick, with foot, 9 in. by 6 in. by 3 in., on bottom of each bracket. Outer circle, 4 tiers, 4 ft. 9 in. deep, and 1 in., 7 in., 3 in., and § in. thick respectively. 55 plates in the circumference. Snug. projecting 43 in. 2 in. below centre, to support binding hoops.

Flanges, 33 in. wide, equal to plates in strength, with brackets between the bolt-holes.

Bolt-holes square, 7 in., 6 in. centre to centre.

Bolts, 7 in. square under head.

Hoops, flat-iron, 4 in. by 1 in., with suitable jaws and screws. bound round each tier of outside plates.

Joints, 1 in. thick, caulked with iron cement.

Diameter, 103 ft. Depth, 22 ft.

Plates, bottom or ring, 5 ft. wide, 1 in. thick. Inner circle, 1 tier of plates only 4 ft. deep, 1 in. thick; strengthened with 2 horizontal ribs, 2 in. deep by 3 in. thick on side next centre of tank, and on other side with 2 vertical brackets, 9 in. at bottom, diminishing to nothing at top, 3 in. thick, with foot on bottom of each, 9 in. by 6 in. by 3 in. Outer circle, 5 tiers, 4 ft. 5 in. deep, and 11 in., 1 in., 7 in., 3 in., and 3 in. thick respectively. 66 plates in the circumference. A snug or bearing bracket cast on each of the outside plates, 21 in. below centre, and projecting 4 in. for supporting the binding hoops.

Flanges, 3 in. wide, 1 in. thick, with brackets between the bolt-

holes.

Bolt-holes, 2 in. square, 6 in. apart, centre to centre.

Bolts, 3 in., square under head.

Hoops, flat-iron, $4\frac{1}{2}$ in. by $\frac{3}{4}$ in. for bottom tier, $4\frac{1}{2}$ in. by $\frac{5}{8}$ in. for the others, with jaws and tightening screws. Joints, & in. thick, caulked with iron cement.

Diameter, 110 ft. Depth, 24 ft, 2 in.

Plates, bottom or ring, 3 ft. 10 in. wide, 3 in. thick. Inner circle 1 tier of plates only, 4 ft. deep, \(\frac{3}{4} \) in. thick; strengthened with 2 horizontal ribs, 2\(\frac{1}{4} \) in. broad by \(\frac{3}{4} \) in. thick on side next centre of tank, and on the other side with 2 vertical brackets, 9 in. at bottom, diminishing to nothing at top, 3 in. thick, with foot on bottom of each, 9 in. by 6 in. by 3 in. Outer circle, 5 tiers, 4 ft. 10 in. deep, and 11 in., 1 in., 7 in., 3 in., and 3 in. thick respectively, 66 plates in the circumference. A bearing bracket cast on each of the outside plates, 21 in. below centre, and projecting 4 in., for supporting the binding hoops.

Flanges, 3 in. wide, and same strength as the respective plates; brackets between the bolt-holes.

Bolt-holes, 7 in. square, 6 in. apart, centres.

Bolts, 7 in., square under head.

Hoops, flat-iron, 5 in. by $\frac{3}{4}$ in. for the bottom tier, and $4\frac{1}{2}$ in. by $\frac{5}{8}$ in. for the others, with suitable jaws and tightening screws. Joints, $\frac{1}{2}$ in. thick, caulked with iron cement.

Wrought-Iron.

Diameter, 127 ft. Depth, 20 ft. 8 in.

Annular space, 3 ft. 9 in. wide.

Plates, bottom or ring plates $\frac{1}{2}$ inch thick; sides five rows deep: first and second row of plates from bottom $\frac{1}{2}$ in. thick; third and fourth rows, 7-16ths in. thick, and the fifth or top row $\frac{3}{8}$ in. thick; lap of plates, 3 in.; the top of the inner row of plates being 8 in. lower than the outer row; angle-iron curbs in bottom, 4 in. by 4 in., by $\frac{5}{8}$ in. thick; the $\frac{1}{2}$ in. and 7-16ths in. plates riveted with $\frac{7}{8}$ in. rivets, $2\frac{1}{2}$ inches apart, and the $\frac{3}{8}$ in. plates by $\frac{3}{4}$ in. rivets, 2 in. apart.

Curbs, top outer curb of angle-iron 5 in. by 5 in. by ½ inch.; top inner curb of angle-iron 3 in. by 3 in. by ½ in.; both riveted

with 3 in. rivets, 6 in. apart.

Standards, 18, box form, 15 in. by 9 in., of $\frac{3}{3}$ -in. plates on three sides, 3 in. by 3 in. by $\frac{1}{2}$ in. angle-iron to secure the same to side sheets, and extending round the bottom of the standard at its lower end, and 5 in. by 5 in. by $\frac{5}{3}$ in. angle-iron round the top to form a base for the columns, all riveted at 6 in. apart with $\frac{3}{4}$ -in. rivets. Two of these standards form the inlet and outlet pipes, for which purpose they are continued under the annular space and up the inside of the inner ring of side sheets, and riveted with $\frac{3}{4}$ -in. rivets as before, but only 2 in. apart.

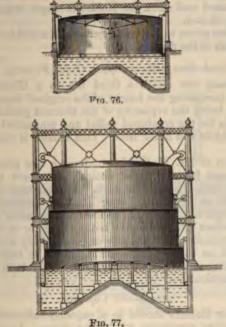
GASHOLDERS.

The Holder or floating vessel (Fig. 76) is the storage reservoir for the gas, and it serves the all-important purpose of equalizing the distribution of the gas under pressure, and ensures an unbroken continuity of supply. In form it is invariably cylindrical, like an inverted cup, and works freely up and down in the tank.

The Holder may be either single (Fig. 76), or telescopic (Fig. 77), and the latter may be in either two or more lifts. Two lifts are generally

adopted; but some of the largest Holders now constructed are in three lifts.

When the Holder is made in the telescopic form, its capacity is nearly double or treble (as the case may be) the capacity of the singlelift Holder for equal dimensions of tank. Ground space and capital are thus economized by its adoption.



Telescopic Holders require great care in construction and workingfirst, to ensure accuracy in the "cupping" of the water-lute or seal, and, second, to prevent the water in the lute from freezing, which endangers the action of the vessel, or causes distortion, and imperils the lighting of the district.

Holders, whether single or telescopic, are counterbalanced or not. as is found desirable or necessary. When the diameter of the Holder is more than twice the depth, counterbalance weights are not required, especially where an exhauster on the one hand, and a governor on the other, are employed, as is the case in all but the smallest gas-works. When the diameter and depth more nearly approximate, it will

generally be found of advantage to reduce the pressure by counter-

balancing.

The crown or roof of a Holder may be either trussed (Fig. 76), or untrussed (Fig. 77). In the latter case the top curb requires to be made sufficiently strong to resist the pressure of the gas exerted on the underside of the roof which tends to distort the curb. A framework of wood or iron is required to be erected within the tank to support the untrussed roof when the Holder is empty of gas, and resting on the landing stones.

The usual rise given to the roof or crown of a Holder is 5 per cent.

or one-twentieth of the diameter.

Gasholders without Upper Guide-Framing.

Mr. G. Livesey has added a third lift to a Holder at Rotherhithe, without increasing the height of the original framing; the only addition made being the replacing of the channel guides with H-iron to furnish paths for the combined radial and tangential rollers on the grips of the middle and outer lifts. This Holder is working success-

fully.

The invention of Mr. W. Gadd introduces a new principle of guiding; the elevated framing being entirely dispensed with, and the vessel guided from the bottom curb. The channel or rail guides within the tank, or within the lower lift of a telescopic Holder, are placed at an angle like the thread of a screw, instead of in the vertical plane. The rollers attached to the bottom curb, or to the cup of the inner lift, are ranged either radially or tangentially with the sides of the vessel; and as they work in the channels or rails provided for them, the floating vessel rises and descends in the tank with a helical or screw-like motion.

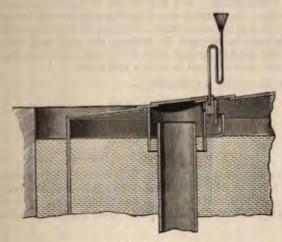
Gasholder Capacity.

The Holder or Holders should be of capacity sufficient to contain at least the 24 hours' maximum production of gas. An excess in capacity, though not absolutely necessary, is found advantageous in point of convenience and economy, where the rate of consumption is liable to fluctuations by the non-lighting of the public lamps during the hours of moonlight; and where, as in manufacturing towns and districts, the large manufactories, generally the heaviest gas consumers, being closed on Saturday nights and Sundays, the production for these two days (unless Sunday labour is partially avoided) is greatly in excess of the consumption.

Precautions to be observed in the Working of Gasholders.

Telescopic Holders in winter are liable to be thrown out of order by

the freezing of the water in the cup between the lifts. When the lower lift is down, the upper lift in its progress downwards rolls the ice and snow in the lute into lumps, often, if not removed, throwing the vessel out of plumb, and even fracturing the columns. Great care should therefore be taken to keep the water-lute clear; and where steam can be readily applied, it is of the utmost service in accomplishing this object in time of frost. Messrs. S. Cutler and Sons have devised an apparatus for preventing freezing of the water in Gasholder cups, by admitting steam or hot water at intervals round the circumference of the vessel. The arrangement is self-acting, compact, and trustworthy.



F10. 78

Another important precaution is to keep the top or crown of the Holder, whether single or telescope, clear of snow, especially when the latter is drifting. Nothing will sooner break down a Holder and its guide framing than allowing a mass of snow to collect and lie on one side of the roof.

The oscillation of a telescope Holder during strong winds is greater when uncupped than when the lifts are joined. Its liability to damage from wind is also greater when uncupped, even although less surface is presented to the wind's action.

Mr. G. Livesey's hydraulic seal (Fig. 78), for attaching to the underside of the roof of a Gasholder over the inlet and outlet pipes,

is an ingenious device for allowing access to the pipes without having

to discharge the gas contained in the crown.

The sheeting of a Holder, being thin and the portion most liable to wear out by oxidation, should be coated outside at least once a year with good oxide of iron or other suitable paint or tar. All rust should be removed before laying on the paint, and for this purpose the sheets should be scrubbed with a brush made of short steel wires. For re-

moving tar a steel scraper may be employed.

It happens not unfrequently that the roof of a Gasholder becomes pitted with small pin-holes from which there is a considerable and constant escape of gas. This may arise from the inferiority of the iron in the first instance; or from allowing the sheets to become oxidized before fixing; or it may be due to neglect to paint the vessel when in use. In districts where there are numerous chemical works, the impurities in the atmosphere affect the thin sheets in this manner. The leaks may be stopped by coating the roof with warm tar, and riddling dry sand or cement over it through a sieve, at the same time rubbing the mixture well in with a stiff brush.

RECIPE for coating a Gasholder :-

1 gallon of tar.

½ lb. of slaked lime.
½ lb. of pitch.
½ lb. of tallow.
½ pint of coal naphtha.

Dissolve the pitch and mix the lime in the tar by heating them in a boiler, being careful not to boil them; ladle out the hot liquid into a bucket, and then add the tallow and the naphtha. Stir the mixture occasionally, and with a brush paint it on the Holder before it grows cold.

TABLE

Giving the Capacity of Gasholders in Cubic Feet for every Foot in Depth, and from 40 to 150 Feet in Diameter, advancing Half a Foot at a Time.

no.	Capacity	Die	Capacity	Dia-	Capacity	Dia-	Capacity	This	Capacity
Dia-	in Cub.	Dia- meter	in Cub. Ft. for	meter	in Cub. Ft. for	meter	in Cub. Ft. for	Dia- meter	in Cub.
meter	every	of		of	every	of	every	of	every
Holder	Foot in	Holder	Foot in	Holder	Foot in	Holder	Foot in	Holder	Foot in
in Ft.	Depth of	in Ft.	Depth of	in Ft.	Depth of	in Ft.	Depth of	in Ft.	Depth of
	Holder.		Holder.		Holder.		Holder.		Holder.
40	1256 • 64	621	3067.96	841	5607.95	1061	8908 - 20	1284	12968 - 72
404	1288 25	63	3117.25	85	5674.51	107	8992.04	129	13069.84
41	1320.25	631	3166.92	851	5741 47	1074	9076 27	1291	13171 35
414	1352.65	64	3216.99	86	5808.81	108	9160.90	130	13273 26
42	1385 44	641	3267:46	861	5876 55	1081	9245 92	1301	13375.55
424	1418.62	65	3318.31	87	5944.09	109	9331.33	131	13478 24
43	1452.20	65½	3369.56	871	6013.21	1091	9417.14	1311	13581.33
431	1486 17	66	3421.20	488	6082-13	110	9503.34	132	13684 . 80
44	1520.53	661	3473 23	881	6151 44	1104	9589 93	1321	13788 67
441	1555.28	67	3525.66	89	6221-15	111	9676.91	133	13892 . 94
45	1590 43	671	3578 47	891	6291 25	1111	9764 28	1331	13997 - 59
454	1625 97	68	3631 68	90	6361 - 74	112	9852.05	134	14102 64
46	1661-90	681	8685 29	901	6432.62	1124	9940.21	1344	14208 . 08
461	1698 23	69	8739 - 28	91	6503.89	113	10028 . 77	135	14313.91
47	1784 94	693	3793 - 67	911	6575 - 56	1131	10117.71	1851	14420 - 14
47%	1772.05	70	3848 • 46	92	6647 62	114	10207 05	136	14526 . 75
48	1809 - 56	704	3903 · 63	921	6720 07	1145	10296 . 79	1364	14633 . 76
484	1847 45	71	3959 20	93	6792 92	115	10386 91	137	14741 . 17
49	1885 - 74	714	4015.16	931	6866-16	115%	10477 43	1374	14848 96
494	1924 - 42	72	4071.51	94	6939 - 79	116	10568 34	138	14957 - 15
50	1963 - 50	724	4128 - 25	944	7013.81	1163	10659 64	1384	15065 . 73
50%	2002 96	73	4185 39	95	7088 - 28	117	10751.34	139	15174 . 71
51	2042 - 82	784	4242.92	951	7163 04	1171	10843 - 42	1394	15284 . 08
511	2083 - 07	74	4300.85	96	7238 24	118	10935 90	140	15393 84
52	2123 - 72	743	4359.16	961	7313 84	1184	11028 - 78	140+	15503 - 99
521	2164.75	75	4417.87	97	7389 - 82	119	11122.04	141	15614.53
53	2206 · 18	754	4476 - 97	971	7466 - 20	1194	11215 . 70	1411	15725 47
531	2248 · 01	76	4536 47	98	7542 98	120	11309 - 76	142	15836 . 80
54	2290 22	764	4596.35	981	7620 14	120%	11404 . 20	1424	15948 - 52
541	2332.83	77	4656.63	99	7697-70	121	11499 . 04	143	16060 64
55	2375.83	778	4717:30	994	7775 65	1214	11594 - 28	1481	16173 15
554	2419 22	78	4778 37	100	7854 00	122	11689 - 89	144	16286 - 05
56	2463.01	781	4839 83	100%	7932 - 73	1224	11785 . 90	1443	16399 - 34
56%	2507 - 19	79	4901.68	101	8011.86	123	11882.31	145	16513.03
57	2551 76	794	4963 92	1014	8091 . 38	1231	11979-11	1451	16627 - 11
574	2596 - 72	80	5026 . 56	102	8171 . 30	124	12076:31	146	16741 . 58
58	2642.08	804	5089.58	1023	8251.60	1244	12173 - 89	1461	16856 - 45
581	2687-83	81	5158:00	103	8332 - 30	125	12271-87	147	16971 - 70
59	2733 - 97	814	5216.82	1031	8413.40	1251	12870 - 24	1474	17087 - 35
594	2780.51	82	5281.02	104	8494.88	126	12469.01	148	17203 - 40
60	2827 44	824	5845 62	1044	8576 . 76	1264	12568 16	1484	17319 83
601	2874-76	83	5410.62	105	8659.03	127	12667.71	149	17436 - 66
61	2922 47	831	5476.00	105#	8741 . 69	1274	12767 65	1494	17553 88
614	2970.57	84	5541.78	106	8824 . 75	128	12867 . 99	150	17671 50
62	3019 07	03	2027 10	100	DOLL 10	100	22001 00	100	TIOLT OO

TABLE OF THE WEIGHTS OF GASHOLDERS

In pounds for every One-Tenth of an Inch Maximum Pressure, and from 20 to 200 Feet in Diameter.

Diameter of Gas- holder in Feet.	Weight in lbs. for each One-tenth of an Inch Pressure.	Diameter of Gas- holder in Feet,	Weight in lbs.for each One-tenth of an Inch Pressure.	Diameter of Gas- holder in Feet.	Weight in lbs. for each One-tenth of an Inch Pressure.	Diameter of Gas- holder in Feet.	Weight in lbs. for each One-tenth of an Inch Pressure.
20	164	58	1149	86	3026	119	5793
21	181	54	1193	87	3097	120	5891
22	198	55	1238	88	3168	121	5990
23	217	56	1283	89	3241	122	6089
24	236	57	1329	90	3314	123	6189
25	256	58	1376	91	3388	124	6290
26	277	59	1424	92	3463	125	6392
27	298	60	1478	93	3538	126	6495
28	321	61	1522	94	8695	127	6598
29	344	62	1573	95	8692	128	6703
30	368	63	1624	96	3770	129	6808
31	393	64	1676	97	3849	130	6914
32	419	65	1729	98	3929	131	7021
33	446	66	1782	99	4010	132	7128
34	473	67	1837	100	4091	133	7237
35	501	68	1892	101	4173	134	7346
36	530	69	1948	102	4256	135	7456
37	560	70	2005	103	4340	136	7567
38	591	71	2062	104	4425	137	7678
39	622	72	2121	105	4510	138	7791
40	655	73	2180	106	4597	139	7904
41	688	74	2240	107	4684	140	8018
42	722	75	2301	108	4772	141	8133
43	757	76	2363	109	4861	142	8249
44	792	77	2426	110	4950	143	8366
45	828	78	2489	111	5041	144	8483
46	866	79	2553	112	5132	145	8601
47	904	80	2618	113	5224	146	8720
48	943	81	2684	114	5317	147	8840
49	982	82	2751	115	5410	148	8961
50	1023	83	2818	116	5505	149	9083
51	1064	84	2887	117	5630	150	9205
52	1106	85	2956	118	5696	200	16,364

To Ascertain the Weight of a Gasholder by the above Table, the Diameter and Maximum Pressure being known.

RULE.—Multiply the number of lbs. standing opposite to the diameter by the pressure in tenths of an inch.

Example.—What is the weight of a Gasholder 78 feet in diameter, giving a maximum pressure of 32/10ths?

 $2489 \times 32 = 79,648$ lbs., weight of Gasholder.

To Ascertain, by the preceding Table, the Pressure which a Gasholder will give, the Diameter and Weight being known.

RULE.—Divide the weight in lbs. of the Gasholder by the weight given opposite to the diameter.

Example.—What pressure will a Gasholder give whose weight is

32,075 lbs., and diameter 56 feet ?

 $32.075 \div 1283 = 25/10$ ths, maximum pressure of Gasholder.

The figures given in the foregoing table are based on the weight of a cubic foot of water—viz., 62.5 lbs.; a column of water 1/10th of an inch high, with an area of 1 square foot, being .52083 lbs., or the 120th part.

Thus, if the area of the Holder in feet (obtained by squaring the diameter and multiplying by ·7854) be multiplied by 62·5, the weight of a cubic foot of water in lbs., and divided by 120, the number of 10ths of an inch in a foot, the product will be the weight of the Holder in lbs. for each 1/10th of an inch maximum pressure.

Or thus: The area of a circle is to the square of its diameter as '7854 is to 1; hence the weight of a Gasholder in lbs., to give 1/10th of an inch pressure, is to the square of its diameter in feet as '52083 × '7854 is to unity; or, which is the same thing, as '4091 is to unity. So to ascertain the weight of a Holder, say, 100 feet diameter, giving a maximum pressure of 35/10ths—

 $100^{2} \times 35 \times 4091 = 143,185$ lbs., weight of Gasholder.

DIMENSIONS OF THE PRINCIPAL MATERIALS IN GASHOLDERS IN ACTUAL WORKING.

Single Gasholder.

Diameter, 30 ft. Depth, 15 ft.

Roof sheets, No. 17 B. wire gauge. Side sheets, No. 18 B, wire gauge. Inlet and outlet pipes, 6 in. diam.

Single Gasholder.

Diameter, 35 ft. Depth, 12 ft.

Roof sheets, No. 15 B. wire gauge. Side sheets, No. 16 B. wire gauge. Crown plate, 3 ft. 6 in. diam., \(\frac{3}{8} \) thick. 4 main and 4 secondary bars, of 3 in. T-iron.

Top and bottom curbs, of 3 in. angle-iron.

4 columns, 13 ft. 6 in. long; diam. at base, 6 in.; at top, $5\frac{1}{2}$ in. 4 holding-down bolts to each column, 4 ft. long, 1 in. round iron.

Single Gasholder.

Diameter, 36 ft. Depth, 12 ft.

Roof sheets, No. 17 B. wire gauge. Side sheets, No. 18 B. wire gauge.

Single Gasholder.

Diameter, 40 ft. Depth, 15 ft.

Crown plate, 3 ft. 5 in. diam., 3 in. thick.

Roof sheets, No. 14 B. wire gauge.

Side sheets, top and bottom tiers, No. 14 B. wire gauge; all the rest, No. 15 B. wire gauge.

Rivets for sheets, $\frac{1}{4}$ in. diam., 1 in. apart, centre to centre. Rivets for top curb, $\frac{1}{2}$ in. diam., $1\frac{1}{2}$ in. apart, centre to centre. Rivets for bottom curb, $\frac{1}{4}$ in. diam., 6 in. apart, centre to centre.

Centre-pipe of cast-iron, 6 ft. long, 4 in. diam.

Truss cup, cast-iron, 2 ft. 6 in. diam.

12 main bars, T-iron, $2\frac{1}{2} \times 2\frac{1}{2} \times 2\frac{1}{2} \times \frac{3}{8}$ in.

4 vertical stays, T-iron, $3 \times 2\frac{1}{2} \times \frac{5}{8}$ in.

Top curb, angle-iron, $3 \times 3 \times \frac{3}{8}$ in. Bottom curb, angle-iron, $3 \times 3 \times \frac{3}{8}$ in.

4 columns, 17 ft. long; diam. at base, 9 in.; diam. at top, 7 in. 3 holding-down bolts to each column, 7 ft. long each, 1½ in. diam.

Girders of T-iron, $3 \times 4 \times \frac{1}{2}$ in., trussed. Balance-weights, 40 cwt.; $\frac{1}{2}$ in. chains.

Single Gasholder.

Diameter, 44 ft. 6 in. Depth, 20 ft.

Rise of crown, 1 ft. 9 in.

Crown plate, 3 ft. 6 in. diam., 3 in. thick.

Roof sheets, inner and outer circles, No. 12 B. wire gauge; all the rest, No. 14.

Side sheets, top and bottom tiers, No. 12 B. wire gauge; the rest, No. 17.

Rivets for Nos. 12 and 14 sheets, 5-16ths in diam.; for No. 16 sheets, ½ in. diam.

5 main and 5 secondary bearing bars, of T-iron, $3 \times 3 \times \frac{3}{8}$ in. 5 columns, 22 ft. long, 7 in. diam. at base, $5\frac{3}{4}$ in. diam. at top; metal 11-16ths thick.

4 holding-down bolts, 16 ft. long, 11 in. square-iron

Single Gasholder.

Diameter, 50 ft. Depth, 20 ft.

Rise of crown, 12 in.
Roof sheets, No. 14 B, wire gauge.
Side sheets, No. 15 B, wire gauge.
Rivets, 1 in. apart, centres.
Top and bottom curbs, 3 in. angle-iron.
8 vertical bars.

8 columns, 26 ft. long, cast in two lengths each; 12 in. diam. at base, 6 in. diam. at top.
Inlet-pipe, 9 in. diam.
Outlet-pipe, 10 in. diam.

Single Gasholder.

Diameter, 50 ft. Depth, 16 ft.

Rise of crown, 2 ft. 6 in.

Crown plate, 3 ft. diam., 1 in. thick.

Roof sheets, inner and outer circles, No. 12 B. wire gauge; all the others, No. 14.

Side sheets, top and bottom tiers, No. 14 B. wire gauge; the others, No. 16.

Rivets, 1 in. diam., 1 in. apart, centres.

Rivets for joining sheets to angle-iron, $\frac{3}{8}$ in. diam., $1\frac{1}{2}$ in. apart, centres.

Rivets for bottom curb, $\frac{1}{2}$ in. diam., 9 in. apart, centres. 10 main and 10 secondary rafters, of T-iron, $3 \times 3 \times \frac{3}{8}$ in.

Top curb, of angle-iron, $3 \times 3 \times \frac{3}{8}$ in.

Bottom curb, two rings of angle-iron, $3 \times 3 \times \frac{3}{8}$ in., 6 in. apart, with flat bar of iron, 6 in. wide and $\frac{1}{2}$ in. thick, between them.

Centre strut, cast-iron pipe, 9 ft. long, 6 in. external diam., 3 in. thick; bearing flanges, 13 in. diam., 11 in. thick; outer rim of cup strengthened by a ring of S C and crown-iron, 2 × 1in., shrunk on hot.

10 vertical ribs, T-iron, $3 \times 3 \times \frac{3}{8}$ in., secured to top and bottom curbs and to side sheets.

5 columns, 18 ft. long; diam. at base, 7 in.; diam. at top, 5 in.; metal, 3 in. thick.

Suspension chains, & in. short link, tested to 5 tons.

Single Gasholder.

Diameter, 50 ft. Depth, 18 ft.

Roof sheets, No. 14 B. wire gauge. Side sheets, No. 15 B. wire gauge. Inlet and outlet pipes, 9 in. diam.

Single Gasholder.

Diameter, 60 ft. Depth, 17 ft.

Rise of crown, 3 ft.

Crown plate, 4 ft. diam., 1 in. thick.

Roof sheets, inner and outer circles, No. 18 B. wire gauge; the rest, No. 14.

Side sheets, top and bottom tiers, No. 14 B. wire gauge; the rest No. 15.

Top curb, $4 \times 4 \times 7$ -16ths in. angle-iron.

Bottom curb, two bars of $3 \times 3 \times \frac{3}{8}$ in. angle-iron, placed back to back, and bar of flat-iron riveted to the bottom with $\frac{3}{8}$ in.

16 vertical bars, $2\frac{1}{2} \times 2\frac{1}{2} \times \frac{3}{2}$ in. T-iron, riveted to top and bottom curbs and to side sheets.

8 columns, 18 ft. long; diam. at base, 63 in.; at top, 5½ in.; metal, 3 in. thick.

Single Gasholder.

Diameter, 60 ft. Depth, 18 ft.

Roof sheets, inner and outer circles, No. 13 B. wire gauge; the others, No. 14.

Side sheets, top and bottom tiers, No. 14 B. wire gauge; the others, No. 15.

Top curb, $4 \times 4 \times \frac{1}{8}$ in. angle-iron.

Bottom curb, formed of two bars of angle-iron, $4 \times 4 \times \frac{1}{2}$ in., riveted back to back with $\frac{1}{2}$ in. rivets 12 in. apart, centres.

14 vertical bars, $4 \times 3 \times \frac{1}{2}$ in. T-iron.

7 columns, 19 ft. 6 in. long each.

Single Gasholder.

Diameter, 81 ft. 8 in. Depth, 20 ft. 6 in.

Rise of crown, 3 ft.

Crown plate, 4 ft. diam., 1 in. thick.

Roof sheets, inner and outer circles, No. 10; all the rest, No. 14 B. wire gauge.

Side sheets, top and bottom tiers, No. 14; all the rest, No. 16 B. wire gauge.

Rivets, $\frac{1}{4}$ in. diam., 1 in. apart, centres. 16 main rafters, $5 \times 8 \times \frac{1}{2}$ in. T-iron. 16 secondary rafters, $4 \times \frac{1}{2}$ in. flat-iron, placed on edge.

Centre strut, cast-iron pipe, 9 ft. long, 7 in. external diam., 1 in. thick; flanges, 13 in. diam., 11 in. thick; cup strengthened by a hoop 2 × 1 in. S C iron, shrunk on hot.

Tension rods, long Queen bolts, short Queen bolts, long suspenders, short suspenders, 16 in number each, of 11 in., 11 in., 11 in., 1 in., and 7 in. round-iron respectively.

Top curb, of angle-iron, $4 \times 4 \times \frac{1}{2}$ in.

Bottom curb, of angle-iron, $4 \times 4 \times \frac{1}{2}$ in., with bar of flat-iron, 6 x 1 in. between, and riveted with 5 in. rivets, 12 in. apart. 12 vertical bars, 4 × 3 × ½ in. T-iron.

Single Gasholder.

Diameter, 87 ft. Depth, 20 ft.

Rise of crown, 4 ft.

2 crown plates, 4 ft. diam., ½ in. thick.

Roof sheets, inner and outer circles, No. 12; the rest, No. 14 B. wire gauge, except 9 sheets upon which the sliding carriages are fixed, No. 7 B. wire gauge.

Side sheets, top and bottom tiers, No. 12; all the remainder, No.

14 B. wire gauge.

Rivets, 5-16ths in. diam., 1 in. apart, centres.

Centre-pipe of wrought-iron, 12 ft. long, 12 in. diam.

Truss cup, wrought-iron, 3 ft. diam., 3 in. thick.

18 main bars, T-iron, $4 \times 3 \times \frac{1}{2}$ in. 18 secondary bars, T-iron, $3 \times 3 \times \frac{1}{2}$ in.

9 rings or purlins of bracket bars, the middle purlin of angle-iron $3\frac{1}{2} \times 3\frac{1}{2} \times \frac{1}{2}$ in., the remainder of flat-iron $2 \times \frac{1}{2}$ in., secured to main and secondary bars with § in. bolts.

18 principal tension rods, 11 in. diam. 36 diagonal tension rods, 7 in. diam.

36 truss bars; 18 of $1\frac{1}{2}$ in. diam., 18 of $1\frac{1}{4}$ in. diam. Top curb, 2 rings of angle-iron, $3\frac{1}{2} \times 3\frac{1}{2} \times \frac{3}{8}$ in. Bottom curb, 2 rings of angle-iron, $3\frac{1}{2} \times 3\frac{1}{2} \times \frac{3}{8}$ in. 18 vertical truss bars, T-iron, $3\frac{1}{2} \times 3\frac{1}{2} \times \frac{1}{2}$ in. 9 columns, 22 ft. long each, 14 in. diam. at base, 11 in. at top. 4 holding-down bolts, 8 ft. long, $1\frac{1}{7}$ in. diam.

Single Gasholder.

Diameter, 100 ft. Depth, 20 ft.

Rise of crown, 5 ft.

2 crown plates, 5 ft. diam., 5 in. thick.

Roof sheets, inner and outer circles, No. 10; the remainder, No.

12 B. wire gauge, except carriage sheets, ½ in. thick. Side sheets, top and bottom tiers, No. 9; the remainder, No. 12 B. wire gauge.

Rivets, 5-16ths in. diam., 1 in. apart, centres.

Centre-pipe of wrought-iron, 14 ft. long, 24 in. diam., 5-16ths in. thick.

18 main and 18 secondary bars.

Top curb, 2 rings of angle-iron, $4 \times 4 \times 7$ -16ths in.

Bottom curb, 2 rings of angle-iron, $4 \times 4 \times 7$ -16ths in., and a flat bar of wrought-iron, $6 \times \frac{3}{2}$ in.

18 vertical bars, T-iron, 4 × 4 × 3 in.

9 columns, 24 ft. long, 24 in. diam. at base, 18 in. diam. at top, 11 to 1 in. metals.

4 holding-down bolts, 8 feet long, 11 in. diam.

Single Gasholder.

Diameter, 110 ft. Depth, 26 ft.

Rise of crown, 5 ft. 6 in.

Crown plates, 4 ft. diam.; 3 in. thick.

Roof sheets, row next centre and outer row next curb, ‡ in. thick; second row from centre, ‡ in. thick; and second row next curb, 3-16ths in. thick; the remainder, No. 12 B. wire gauge.

Side sheets, top and bottom rows, ½ in. thick; next row to each, 3-16ths in. thick; the remainder, No. 12 B. wire gauge.

Rivets, $\frac{1}{4}$ in. and 3-16ths in. plates, $\frac{3}{8}$ in. rivets, 2 in. centres; the $\frac{1}{8}$ in. and No. 12 B. wire gauge sheets 5-16ths in. rivets, $1\frac{1}{2}$ in. centres; $\frac{1}{4}$ in. plates and curb $\frac{5}{8}$ in. rivets, 2 in. centres.

Top curb of 2 angle-irons $5 \times 4 \times \frac{1}{2}$ in. Bottom curb of 2 angle-irons $4 \times 4 \times \frac{1}{2}$ in. Vertical stays, 14, of 2 angle-irons $3 \times 3 \times \frac{1}{2}$ in., and a piece of timber 12 in. \times 4 in. bolted between.

Centre pipe of $\frac{1}{4}$ in. plate, 2 ft. diam. Main rafters, 28, of T-iron $5 \times 3 \times \frac{1}{2}$ in.

Purlins, of T-iron $3 \times 4 \times \frac{1}{2}$ in., and remainder of angle-iron $3 \times 3 \times \frac{3}{2}$ in.

Struts, 3, on main rafters 11 and 11 in. diam.

Tie rod, principal 15 in. diam., second 11 in. diam., and third 1 in. diam.

Columns, 14, of cast-iron 1 ft. 6 in. in diam. at bottom, 1 ft. 2 in. at top; metal $\frac{1}{8}$ in. at bottom, diminishing to $\frac{5}{8}$ in. thick at top.

Holding-down bolts, 4, 11 in. diam., 20 ft. long.

Lattice girders, 14, 1 ft. 6 in. deep, of two frames of angle-iron, $3 \times 3 \times \frac{1}{2}$ in., and braces $2\frac{1}{2} \times \frac{1}{4}$ inch riveted between, top and bottom of girder covered with a plate 10 in. wide by $\frac{3}{8}$ in. thick.

Single Gasholder.

Diameter, 142 ft. Depth, 55 ft.

Roof, without trussing or framework.

Roof sheets, first, or outside circle, 3 ft. long, $\frac{3}{8}$ in. thick; rivets $\frac{5}{8}$ in. diam., $2\frac{1}{2}$ in. apart, centres. Second circle, 3 ft. long, $\frac{1}{4}$ in. thick; rivets, 9-16ths in. diam., $2\frac{1}{4}$ in. apart, centres; centre sheets, forming a circle, 30 ft. diam., $\frac{1}{4}$ inch thick, butted and riveted to each other by lapping pieces, $3\frac{1}{2}$ in. wide; rivets, 9-16ths in. diam.; remainder of roof sheets, 5 ft. long, 3-16ths in. (No. 7 B. wire gauge) thick; rivets, $\frac{3}{8}$ in. diam., $1\frac{1}{4}$ in. apart, centres.

Side sheets, top and bottom tiers, $\frac{1}{4}$ in. thick; rivets, $\frac{1}{2}$ in. diam., $1\frac{1}{2}$ in. apart, centres. Intervening side sheets, No. 10 B. wire

gauge; rivets, & in. diam., 11 in. apart, centres.

Top curb, a circular chamber or girder, in section nearly rectangular, outer depth, 18 in.; inner depth, $19\frac{1}{4}$ in.; width, 2ft., 6 in.; constructed of $4 \times 4 \times \frac{1}{2}$ in. angle-iron.

Bottom curb, formed of two circles of $\frac{3}{8}$ in. boiler-plates, 12 in. wide, each riveted to a circle of angle-iron, $4 \times 4 \times \frac{1}{2}$ in.

32 vertical stays, three sides of a rectangular figure, 12 in. wide, 10 in. deep; formed of 4 angle-irons $3 \times 3 \times \frac{3}{8}$ in. and $\frac{1}{4}$ in. boiler-plate.

16 columns, diam. at base, 3 ft.; at top, 2 ft. 3 in.; metal, $\frac{7}{8}$ in. to $\frac{3}{4}$ in. thick.

4 holding-down bolts, 10 ft. long, 21 in. round-iron.

Two-lift Telescopic Gasholder.

Diameter of outer lift, 441 ft. Depth, 16 ft. Diameter of inner lift, 43 ft. Depth, 16 ft.

Rise of crown, 1 ft. 9 in.

Crown plate, 3 ft. 6 in. diam., 3 in. thick.

Roof sheets, inner and outer circles, No. 12; all the rest, No. 14 B. wire gauge.

Side sheets in both lifts, top and bottom tiers, No. 12; all the rest, No. 16 B. wire gauge.

Rivets for Nos. 12 and 14 sheets, 5-16ths in. diam.; for No. 16 sheets, 1 in. diam.

Cup, inner lift, formed by 2 rings of 21 × 21 × 5-16ths in. angleiron, connected together with No. 8 plates, with side of No. 10 plate, and a ring $1\frac{1}{4} \times \frac{1}{2}$ in. half-round iron, riveted round.

Dip, outer lift, the counterpart of the cup inverted.

Main-bearing bars, T-iron, $3 \times 3 \times \frac{1}{2}$ in.

Secondary bearing bars, T-iron, 3 × 3 × \$ in. 6 vertical bars, inner lift, T-iron, 21 × 21 × 3 in.

6 vertical bars, outer lift, T-iron, $2\frac{1}{2} \times 1\frac{1}{2} \times \frac{3}{8}$ in. Bottom curb, angle-iron, double, 3 × 3 × \$ in.

6 columns, 12 in. diam. at base, 10 in. at top; metal, 1 in. to 3 in. thick.

Two-lift Telescopic Gasholder.

Diameter, outer lift, 87 ft. Depth, 20 ft.

Diameter, inner lift, 85 ft. Depth, 201 ft.

Rise of crown, 4 ft.

2 crown plates, 4 ft. diam., 1 in. thick.

Roof sheets, inner and outer circles, No. 12; the rest, No. 14 B. wire gauge, except 9 sheets upon which the carriages are fixed. No. 7 B. wire gauge.

Side sheets, top and bottom tiers, both lifts, No. 12; all the rest.

No. 14 B. wire gauge.

Rivets, 5-16ths in. diam., 1 in. apart, centres. Hydraulic cup and dip, 7 in. wide, 16 in. deep. Centre-pipe of wrought-iron, 12 ft. long, 12 in. diam. Truss cup, wrought-iron, 3 ft. diam., 3 in. thick. 18 main bars, T-iron, $4 \times 3 \times \frac{1}{2}$ in.

18 secondary bars, T-iron, $3 \times 3 \times \frac{1}{2}$ in.

9 rings or purlins of bracket bars, the middle purlin of angle-iron, $3\frac{1}{2} \times 3\frac{1}{2} \times \frac{1}{2}$ in., the remainder of flat-iron, $2 \times \frac{1}{2}$ in., secured to main and secondary bars with $\frac{5}{8}$ in. bolts.

18 principal tension rods, $1\frac{1}{4}$ in. diam. 36 diagonal tension rods, $\frac{7}{8}$ in. diam.

36 truss bars; 18 of $1\frac{1}{2}$ in. diam., 18 of $1\frac{1}{4}$ in. diam. Bottom curb, 2 rings of angle-iron, $3\frac{1}{2} \times 3\frac{1}{2} \times \frac{3}{8}$ in.

18 vertical truss bars, T-iron, 31 × 31 × 1 in.

9 columns, 41 ft. long, 30 in. diam. at base, 20 in. at top, $1\frac{1}{8}$ to $\frac{7}{8}$ in. metal, cast in 4 lengths.

4 holding-down bolts, 8 ft. long, 11 in. diam.

Two-lift Telescopic Gasholder.

Diameter, outer lift, 100 ft. Depth, 22 ft.

Diameter, inner lift, 98 ft. Depth, 22 ft.

Roof sheets, No. 11 B. wire gauge.

Side sheets, top tier, No. 11; all the others, No. 12 B. wire gauge.

Rivets, 1 in. diam., 1 in. apart, centres.

Hydraulic joint, 8 in. wide, 15 in. deep, No. 10 B. wire gauge; top edge of cup and bottom each of dip bound by half-round iron 2×1 in. thick.

Bottom curb, angle-iron, 4×1 in. at the root, and ring of bar-iron 4×1 in.

12 columns, 24 in. diam. at base, 16 in. at top; metal 1 to 1 in. thick.

4 holding-down bolts, 10 ft. long, 2 in. square-iron.

Two-lift Telescopic Gasholder.

Diameter, outer lift, 102 ft. Depth, 22 ft.

Diameter, inner lift, 100 ft. Depth, 221 ft.

Rise of crown, 4 ft.

Crown plate, 5 ft. diam., 5 in. thick.

Roof sheets, first ring next centre, No. 9; next and outer rings, No. 11; all the rest, No. 12 B. wire gauge.

Side sheets, outer lift, top and bottom tiers, No. 11; all the rest, No. 13 B. wire gauge. Inner lift, top and bottom tiers, No. 13; all the rest, No. 17 B. wire gauge.

Cup and dip, 8 in. wide, 15 in. deep, of angle-iron 3 × 3 × 3 in.; plate, No. 7 B. wire gauge; edges stiffened with $1\frac{1}{2} \times \frac{3}{4}$ in. half-round-iron; $\frac{1}{4}$ in. rivets, 6 in. apart.

10 columns, 18 in. diam. at base, 14 in. at top; metal, $1\frac{1}{4}$ to $\frac{3}{4}$ in.

thick, cast in 4 lengths.

4 holding-down bolts, 8 ft. long, 2 in. square wrought-iron.

Two-lift Telescopic Gasholder.

Diameter, outer lift, 103 ft. Depth, 251 ft.

Diameter, inner lift, 101 ft. Depth, 24 ft.

2 crown plates, 4 ft. diam., 1 in. thick.

Roof sheets, inner and outer rings, 1 in. thick; all the rest, 1-10th in. thick.

Side sheets, top and bottom tiers, & in. thick; the remainder, 1-10th in. thick.

Two-lift Telescopic Gasholder.

Diameter, outer lift, 112 ft. Depth, 26 ft.

Diameter, inner lift, 110 ft. Depth, 26 ft.

Rise of crown, 6 ft.

Roof, trussed. Roof sheets, centre plate & in. thick, next row & in.; next. 3-16ths in.; outer row, $\frac{1}{4}$ in.; next, 3-16ths in.; and the intermediate 7 rows, $\frac{1}{8}$ in. thick.

Side sheets, 3-16ths in. thick top and bottom rows; remainder, No. 12 B. wire gauge; the cup, 8 in. x 18 in., is formed of 2 rings of $3 \times 3 \times \frac{3}{8}$ in, angle-iron, the bottom and sides being of 1 in. plate, having 2 x 1 in. half-round bead at edge of plate.

Top curb, of two rings of angle-iron $5 \times 3\frac{1}{2} \times \frac{1}{2}$ in.

Bottom curb, of 2 rings of angle-iron 5 x 3 x 1/2 in. placed 9 in. apart, between which the bottom roller carriages are secured.

Vertical stays, inner lift, 28, 14 of which are of 2 angle-irons $3 \times 3 \times \frac{1}{2}$ in. riveted on each side to a web plate 9 in. wide and $\frac{1}{4}$ in. thick; the remaining 14 being of T-iron $5 \times 3 \frac{1}{2}$ in. trussed with three struts and a tie rod. Outer lift has 28 vertical stays of 3 in. guard-iron 5 in. wide, against which the guide pieces on the cup slide.

Centre column, 17 ft. 6 in. long and 2 ft. diam. of wrought-iron plates $\frac{3}{8}$ in. thick, $\frac{3}{4}$ in. rivets, $2\frac{1}{2}$ in. pitch; this is secured to the under crown plate, which is 4 ft. in diam., by a ring of angle-iron $5 \times 4 \times \frac{1}{2}$ in. and $\frac{3}{4}$ in. rivets; at the lower end of the column are 2 rings of angle-iron, $5 \times 4 \times \frac{3}{4}$ in., placed $3\frac{1}{4}$ in. apart to form a jaw to receive ends of tension rods.

Main rafters, 14, of T-iron, $4 \times 5 \times \frac{1}{2}$ in., trussed with six wrought-iron struts $1\frac{1}{4}$, $1\frac{1}{2}$, and $1\frac{3}{4}$ in. diam., and a $1\frac{1}{2}$ in. diam. tension rod. Fourteen main tie rods of $1\frac{3}{4}$ in. round-iron, extending from curb to bottom of centre column, and suspended in two places from the main rafters with $\frac{1}{2}$ in. round rods; the main tie rods and the tension rods have each a wrought-iron coupling box with right and left hand threads.

Secondary rafters, 14, T-iron, $3 \times 5 \times \frac{1}{2}$ in., trussed as above with four struts $1\frac{1}{4}$ and $1\frac{1}{2}$ in. diam., tension rod $1\frac{1}{4}$ in diam., with coupling box; these rafters extend from curb to within 21 ft. of the centre of holder, the inner ends being secured to a

main brace bar or purlin.

Purlins, 7 rows between side and centre. The main purlin mentioned above is $4\frac{1}{2} \times 4\frac{1}{2} \times 9$ -16ths in.; the one next curb, $4 \times 3 \times \frac{1}{2}$ in.; and the remainder, $3 \times 3 \times \frac{3}{8}$ in., all of T-iron.

Columns, 14, of cast-iron, 2 ft. 6 in. diameter at bottom, 2 ft. at top, and 55 ft. 8 in. high, surmounted with a large ball 30 in.

diam., with spiked finial.

Girders, 2 rows, each 2 ft. deep, and 10 in wide, of 4 angle-irons $3 \times 3 \times \frac{3}{8}$ in., with plate $10 \times \frac{3}{8}$ in., top and bottom diagonal braces $3 \times \frac{3}{8}$ in., at the intersection of which is a cast-iron spiked ball in two halves, 17 in. diam. across spikes.

Holding-down bolts, 4, 2 in. diam., 11 ft. 6 in. long.

Two-lift Telescopic Gasholder.

Diameter, outer lift, 120 ft. Depth, 24 ft.

Diameter, inner lift, 118 ft. Depth, 24 ft.

Rise of crown, 6 ft.

Roof, untrussed, resting when down on timber framing in tank. Roof sheets, first or outside row, \(\frac{3}{4}\) in. thick; second row, \(\frac{1}{4}\) in.; third row, 3-16ths in.; fourth row, No. 8 B. wire gauge; crown plates, \(\frac{1}{4}\) in. thick and 6 ft. in diam.; inside row, next crown plate, 3-16ths in.; next, No. 8 B. wire gauge; and the remaining 10 rows of intermediate sheets, No. 11 B. wire gauge.

Side sheets, inner lift, 12 courses high; top and bottom course, in. thick; second course at top, 8-16ths in.; and the re-

mainder, No. 12 B. wire gauge.

Side sheets, outer lift, 12 courses high; top and bottom course, \(\frac{1}{4}\) in. thick; second course at bottom, 3-16ths in.; and the remainder, No. 12 B. wire gauge. The thicker sheets in both inner and outer lift, riveted together with \(\frac{3}{6}\) in. rivets, \(\frac{1}{4}\) in. apart, centres, and the others with 5-16ths in. rivets, \(\frac{1}{6}\) in. apart, centres.

Top curb, of 2 angle-irons, one at junction of roof with side sheets, $5 \times 5 \times \frac{5}{8}$ in., and the other at the inner edge of outer row of sheets, $4 \times 4 \times \frac{1}{2}$ in.; the two stiffened by gusset-

pieces springing from the vertical stays.

Bottom curb, of two $5 \times 4 \times \frac{5}{8}$ in. angle-irons, riveted to the outside of the lower row of sheets, with $\frac{3}{8}$ in. rivets, 6 in. apart. Between these two curbs, which are placed 2 in. apart, are fixed the 28 guide carriages and rollers.

Cups, formed of rolled channel-iron $8 \times 3\frac{1}{2} \times \frac{1}{2}$ in., riveted to the side sheets and rising plates, with $\frac{1}{2}$ in. rivets 4 in. apart. A half-round bead $2 \times \frac{5}{2}$ in. being riveted to edge of rising

plates, which are \$ in. thick and 18 in. deep.

Vertical stays, 28, formed of two $4 \times 4 \times \frac{1}{2}$ in. angle-irons and a web-plate between, $\frac{3}{8}$ in. thick and 9 in. wide, secured with $\frac{3}{8}$ in. rivets, 6 in. apart; at the upper end of these is attached a gusset-plate with angle-iron edges $3 \times 3 \times \frac{3}{8}$ in., extending to the inner angle-iron curb of roof, to which and the outer curb it is riveted.

Standards 14, in the form of the letter T, 4 ft. 2 in. × 3 ft. at bottom, tapering to 1 ft. 9 in. each way at the top; each standard 51 ft. high. Between the angle-iron framework of the standards is cast-iron trellis work, 1 in. thick, on one of its sides, and wrought-iron lattice work on the other; the standards are secured to cast-iron hollow base plates 6 in. deep; 4 holding-down bolts to each standard, 11 ft. 6 in. long, 2½ in. diam.

Lattice girders, 2 rows in the height; first or lower row, 27 in. deep; top row, 30 in. deep; formed of 4 angle-irons, 3 × 3 × ½ in. wrought-iron tension bars, 3 × ½ in., and cast-iron struts.

Two-lift Telescopic Gasholder.

Diameter, outer lift, 151 ft. 6 in. Depth, 40 ft. Diameter, inner lift, 149 ft. Depth, 40 ft. 3 in.

Crown trussed, rise 8 ft.

Roof sheets, outer row, 5-16ths in.; next row, 3-16ths in.; and the

remainder No. 10 B. wire gauge, two centre plates 3 in. thick and 4 ft. 6 in. diam.

Side sheets, top and bottom rows in both lifts ½ in. thick, the remainder No. 11 B. wire gauge, ½ in. rivets, 1 in. centre; cup and grip10 in. wide and 20 in. deep, Piggot's form; plates ¾ in. thick, strengthened at edges with bead-iron.

Top curb, of 2 rings of angle-iron $5 \times 5 \times \frac{1}{2}$ in., placed one above the other; the lower one is secured to a flat bar 10 in. wide and $\frac{1}{2}$ in. thick, which is again connected by straps 4 in.

wide and 1 in. thick to the top row of sheets.

Bottom curb, of 2 rings of angle-iron $5 \times 4 \times \frac{5}{8}$ in. riveted to the outside of the bottom of row of sheets with $\frac{5}{8}$ in. rivets. Between these two rings are fixed the bottom guide roller carriages.

Vertical stays, 32 in top lift of H-iron 12 in. deep, and 32 in bottom lift, of channel-iron $8 \times 2\frac{1}{2} \times \frac{1}{2}$ in., attached to sheets, cups, and curbs with $\frac{5}{8}$ in. bolts in upper lift, and $\frac{5}{8}$ in. screwed pins in lower lift.

Centre column, 3 ft. 6 in. diam., 22 ft. long, of plates 7-16ths in.

thick.

Roof framing, 24 main radial T-iron bars 6 × 4 × 1 in. curved to roof, each with a main tension rod 2 in. in diameter at curb. and reduced to 11 in. at the foot of centre column, and having a coupling box with right and left hand thread, 4 struts and 4 tension rods form the bracing to each main bar, the former of cross-iron $4 \times 4\frac{1}{2} \times \frac{3}{4}$ in. placed vertically, and the latter of 1, 11, 11, and 18 in. round-iron placed diagonally, the strongest section being nearest the centre column; 48 secondary radial bars of 4 x 1 in. flat-iron, that is, 2 equidistant between the main radial bars, and extending from top curb towards centre a distance of 26 ft., and then for a further distance of 16 ft., in direction of the centre, another bar of the same dimensions is fixed. 17 rings or rows of purlins, divided equally from curb to centre, are fixed between main and secondary bars; the first row from centre being of 6 x 1 in. flat-iron; next 4 rows of angle-iron, $1\frac{1}{2} \times 1\frac{1}{2} \times \frac{1}{4}$ in.; next row of angle-iron $2 \times 2 \times \frac{1}{4}$ in.; next row of T-iron $3 \times 6 \times \frac{1}{2}$ in.; next 2 rows, which are subdivided in length by the secondary radial bars above mentioned, are of angle-iron $1\frac{1}{2} \times 1\frac{1}{2} \times \frac{1}{4}$ in.; next row extending from main bar to main bar is of I-iron 3 x 6 x 1 in.; next two rows are divided in 3 lengths between main bars by the two secondary bars, and are of $1\frac{1}{2} \times 1\frac{1}{2} \times \frac{1}{4}$ in. angle-iron; next row extending from main to main is of T-iron 4 x 6 x ½ in.; next row divided in 3 lengths as before of

 $1\frac{1}{2} \times 1\frac{1}{2} \times \frac{1}{4}$ in. angle-iron, and the remaining 2 rows divided in 3 as before of $2 \times 2 \times \frac{1}{4}$ in. angle-iron; 3 bars of flat-iron $2\frac{1}{2} \times \frac{3}{8}$ in. cross diagonally in each bay formed by the two main bars.

Columns, 16, of cast-iron, 83 ft. high, 3 ft. in diam. at base, and 2 ft. 8 in. at top, metal 1 in. thick; cast-iron channel guide up the column, 5 × 3 in. inside measure, weighing 56 lbs. per

foot.

Girders, 16, at top 4 ft. deep, 7 in. wide, of 4 angle-irons $3 \times 3 \times \frac{3}{8}$ in. and a top and bottom plate 7 in. wide by $\frac{3}{8}$ in. thick; diagonal brace bars $4 \times \frac{3}{8}$ in.; 16 intermediate girders 3 ft. 6 in. deep, 6 in. wide, of 4 angle-irons $2\frac{1}{2} \times 2\frac{1}{2} \times \frac{3}{8}$ in., and top and bottom plates 6 in. wide by $\frac{3}{8}$ in. thick, diagonal brace bars $3 \times \frac{3}{8}$ in.; at the intersection of the brace bars a cast-iron star 12 in. in diam. is riveted.

Holding-down bolts, 4, 2 in. square and 14 ft. long.

Capacity, 1,400,000 cubic feet.

Two-lift Telescopic Gasholder.

Diameter, outer lift, 197 ft. 6 in. Depth, 36 ft.

Diameter, inner lift, 195 ft. Depth, 36 ft.

Crown, untrussed, rise 10 ft.

Roof sheets, centre plate \(\frac{1}{4}\) in. thick, 6 ft. diameter; row next centre of No. 7 B. wire gauge; row next curb, \(\frac{1}{2}\) in. thick; next row, 5-16ths in. thick; third row, No. 7 B. wire gauge.

and the remaining rows of No. 11 B. wire gauge.

Side sheets, of inner lift in 18 rows; top row, ½ in.; bottom row forming cup, ¾ in.; second row from top and bottom, ¼ in.; third row from top and bottom of No. 7 B. wire gauge; and the 12 intermediate rows of sheets of No. 11 B. wire gauge in thickness. Those of outer lift in 18 rows; top row forming cup, ¼ in.; bottom row, 5-10ths in.; second from top, No. 9 B. wire gauge; second from bottom, 3-16ths in.; third from bottom, No. 9 B. wire gauge, and the 13 intermediate rows of No. 11 B. wire gauge in thickness.

Cups, 10 in. wide, 18 in. deep, of channel-iron, $10 \times 3\frac{1}{2} \times \frac{1}{2}$ in. rising side plates, $\frac{3}{2}$ in. thick, with $2\frac{1}{2} \times \frac{3}{2}$ in. bead riveted to

edges.

Top curb, of 2 angle-iron rings, outer one $6 \times 6 \times \frac{3}{4}$ in.; inner one, $5 \times 5 \times \frac{5}{8}$ in., both double riveted to top and side sheets, with $\frac{3}{4}$ in. rivets, 2 in. apart centre to centre.

Bottom curb, of 2 angle-iron rings, 6 × 5 × 5 in., riveted to

side sheets, with & in. rivets, 6 in. apart.

Vertical stays, 44, in upper lift of H-iron, $8 \times 5 \times 5 \times 7$ -16ths insecured to top and bottom rows of sheets and the outer angle-iron curb, but not to the intermediate sheets, except just at the centre, where there are two clips, 6 in. wide \times 5-16ths in. thick, to which the sheet is riveted. Gusset pieces, 44, of 2 angle-iron frames, $2\frac{1}{2} \times 2\frac{1}{2} \times \frac{3}{8}$ in., riveted to a 7-16ths inweb-plate placed between them and riveted together, and to the vertical stays, outer row of top sheets, and inner angle-iron curb with $\frac{5}{8}$ in. rivets, 4 in. pitch. Vertical stays in lower or outer lift, 44, of channel-iron, $8 \times 2\frac{1}{2} \times \frac{1}{2}$ in., riveted to bottom curb, and to the sheets half way up, with four $\frac{3}{4}$ in rivets, countersunk heads in the channel, and bolted to the channel-iron of grip with two $\frac{7}{8}$ in. bolts.

Guide wheels, 22, at top lift of malleable cast-iron, 24 in. diameter, with steel axles or pins, mounted on wrought-iron carriages, 44 fixed under cup of upper lift, 22 on grip, and 44 on bottom curb of outer lift, all of malleable cast-iron, having

steel pins and wrought-iron carriages.

Columns, 22, of cast-iron, 3 ft. diameter at bottom, and 2 ft. 6 in. at top, mounted on ornamental base 4 ft. square and 9 ft. 9 in. high, two entablatures and ornamental cap; 4 holding-down

bolts to each column, 21 in. diameter.

Girders, upper tier, 3 ft. 6 in. deep; lower tier, 3 ft. deep, of two frames of angle-iron, $4 \times 4 \times 7.16$ ths in., with lattice bars, $4 \times \frac{5}{8}$ in. riveted between them; the top, bottom, and ends of girders covered with a $\frac{3}{8}$ in. plate 9 in. wide; rivets, $\frac{3}{4}$ in., 4 in. apart centres; at the intersection of the diagonal braces with each other are fixed plates, 12 in. diameter and $\frac{3}{8}$ in. thick.

Quality of iron, plate, angle, and T-iron of best South Staffordshire brands, the channel and H-iron of the best Belgian; the sheets of the very best South Staffordshire, equal to B. B. H. best. Rivets, all sizes, of the best soft charcoal-iron. Those for the

Rivets, all sizes, of the best soft charcoal-iron. Those for the No. 11 B. wire gauge sheets, of No. 3 B. wire gauge in diameter and 1 in. pitch; and those for No. 7 B. wire gauge sheets, with \(\frac{3}{3} \) in. rivets 1\(\frac{1}{4} \) in. apart centres.

Capacity, 2 million cubic feet.

Two-lift Telescopic Gasholder.

Diameter, outer lift, 200 ft. Depth, 25 ft. 3 in. Diameter, inner lift, 198 ft. Depth, 25 ft. 9 in. Roof untrussed, and flat. Roof sheets, centre plate 3 in., row next centre plate 1 in.; next row 1 in.; outer row next curb 1 in.; second row 1 in.; and

the whole of the remaining rows 1 in. thick.

Side sheets, outer lift, bottom row 1 in.; next 3-16ths in.; top row 3-16ths in.; intermediate rows all 1 in. thick; inner lift, bottom and top rows 3-16ths in. thick; remainder 1 in. thick.

Top curb is a box girder 3 ft. x 2 ft. of 3 in. plates and 41 × 41 × 1 in. angle-irons in the inside corners, riveted

together.

Bottom curb, of 2 angle-irons, 4½ × 4½ × ½ in. riveted to a 3 in. plate 8 in. wide; the whole riveted to the lower sheet of holder.

Cup formed of channel-iron $8 \times 3 \times 3 \times \frac{5}{8}$ in. thick; rising plate $\frac{3}{8}$ in. thick and 15 in. deep; a $1\frac{1}{2}$ in. half-round iron

bead is riveted to edge of rising plate.

Columns, 28, 50 ft. long, 3 ft. diameter at bottom, and 2 ft. 4 in. diameter at top; metal 11 in. thick at bottom and 1 in. at top. Capacity, 11 million cubic feet.

Three-lift Telescopic Gasholder.

Diameter, outer lift, 214 ft. Depth, 53 ft.

Diameter, middle lift, 211 ft. Depth, 53 ft. 3 in.

Diameter, inner lift, 208 ft. Depth, 53 ft. 6 in.

Rise of crown, 14 ft. Roof, untrussed.

Roof sheets, outer row forming part of curb, 3 in. thick, of steel plates 3 ft. wide; next row No. 7 B. wire gauge; then another row of No. 9 B. wire gauge; the remainder being all of No. 10 B. wire gauge; these latter riveted with 5-16ths in. rivets 1 in. pitch; the No. 7 B. wire gauge sheets riveted to the 3 in.

steel curb plate by $\frac{3}{4}$ in. rivets, $2\frac{1}{2}$ in. pitch.

Side sheets of No. 11 B. wire gauge, secured to each other with 5-16ths in. rivets, 1 in. pitch, lap of sheets 1½ in.; the bottom and top rows of sheets in outer lift are ½ and 3-16ths in. thick respectively; in the middle lift 3-16ths in., and in the top lift 3-16ths and ½ in. respectively, being riveted to the other sheeting with § in. rivets, 1½ in. pitch, 1¾ in. lap. Piggot's cup and dip, the former of 7-16ths in. plate, and the latter of \$\frac{3}{8}\$ in. plate, secured to adjoining sheets with \$\frac{5}{8}\$ in. rivets, 13 in. pitch, 2 in. lap; cup and dip 12 in. wide and 21 in. deep; edge of cup and dip stiffened by a 21 x 1 in. flat-iron.

Top curb, formed by two $\frac{\pi}{4}$ in. steel plates, one forming the outer row of sheets on the crown being 36 in. wide, the other forming top row of sheets on the side 12 in. wide; these are joined together at the angle with a $5 \times 5 \times \frac{\pi}{4}$ in. angle-steel curb, and further stiffened at the inner edge of the crown plate with a $6 \times 3 \times \frac{1}{2}$ in. angle-steel, all riveted together with $\frac{\pi}{8}$ in. and 1 in. steel rivets, 4 in. pitch. Bottom curb, formed by a plate $\frac{\pi}{8}$ in. thick, and 15 in. wide,

Bottom curb, formed by a plate $\frac{5}{8}$ in. thick, and 15 in. wide, secured at right angles to the lower rows of sheets to a $6 \times 3 \times \frac{1}{2}$ in. angle-iron with $\frac{3}{4}$ in. rivets, $5\frac{1}{2}$ in. pitch; another angle-iron of the same dimensions being placed 1 ft. 5 in. higher, forming a space in which are fixed the bottom roller

carriages.

Vertical stays, 48, on lower and middle lifts are made of No. 10 B. wire gauge sheets bent in the form thus_ $\Omega_8 \times 4\frac{1}{2}$ in., riveted to the outside of the sheets, and on the inside opposite these are $8 \times 3\frac{1}{4} \times \frac{1}{2}$ in. channel-irons, placed between two $4 \times 3 \times \frac{1}{4}$ in. angle-irons, which are riveted through the sheets to the outside stays. The top or inner lift is stiffened by No. 8 B. wire gauge sheets of the same form as above, but are $12 \times$

9 in., placed inside only.

Standards, 24, in the form of the letter H, 20×16 in. and 158 ft. 6 in. high above coping of tank, of wrought-iron formed of four $3 \times 3 \times \frac{3}{8}$ in. angle-irons $\frac{3}{8}$ in. web plate, and $\frac{1}{2}$ in. inside and outside plates, having 5 tiers of struts from standard to standard, and 10 sets of diagonal braces. Two channel-irons $8 \times 3 \times \frac{1}{2}$ in. riveted to each other back to back and to the standards, form the guides upon which the radial and tangential rollers work; the bottoms of standards are fastened to triangular shaped cast-iron base-plates, each secured to the tank with three $2\frac{1}{2}$ in. bolts.

Capacity, 51 million cubic feet.

THE STATION GOVERNOR.

An unnecessarily high pressure of gas in the mains and service-pipes

is synonymous with a heavy leakage account.

Ordinary valves are powerless to effect the desired pressure regulation, however well they may be attended to. No gas-works, therefore, whatever its size, should be without a Station Governor to control the initial pressure.

When properly constructed it accomplishes this important object perfectly, however much the consumption on the one side and the

density of the gas on the other may vary.

The construction of the Governor is of the most simple character, consisting of a small cast-iron water-tank, through the bottom of which the gas from the regular holder enters, and makes its exit by means of a stand-pipe rising above the water level. This pipe may be either annular or rectangular in form. In the former case the gas enters by way of the central opening, and makes its exit by the annular space. In the latter arrangement the pipe is divided in two by a midfeather, one division being the inlet and the other the outlet for the gas; the inlet division of the pipe occupying the central position in the tank. Within the tank is a floating bell or gasholder made of tinned sheet-iron, from the crown of which a conical or parabolic shaped valve is suspended by an eye-bolt. It is the raising and lowering of this valve within the inlet gas aperture, by reason of the gas exerting a pressure of greater or less force, (according as the consumption varies), on the inner surface of the floating bell, that accomplishes the necessary regulation.

The holder may be balanced or buoyed up either by means of an air chamber within itself, placed round its lower curb (Fig. 80), and consequently immersed in the water of the tank, or by a chain secured to its crown outside (Fig. 79), passing over one or two pulleys and terminating in a rod carrying the required balance weights, the needed pressure being obtained by placing cast-iron or lead weights on the crown of the holder; or it may be weighted with water allowed to flow from a feed pipe into a tank formed by continuing the sides of the holder a few inches above the crown. The method of weighting by water is preferable to the other, as the pressure can be applied or removed in a more gradual manner, the opening in the supply and

discharge taps being regulated as desired.

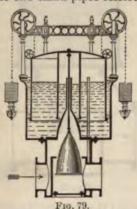
The conical valve for increasing or diminishing the area of the gas aperture has generally given place to that in the form of a parabola; the latter requiring a shorter range to produce the necessary effect, and being more delicate and certain in its action. The parabola should be made twice its diameter in length, and of weight sufficient to resist,

without oscillation or blinking, whatever pressure may be exerted against it by the inflowing gas. With the like object it was formerly necessary to make the floating bell with an area 20 times greater than the area of the base of the valve; but with the improvements effected in Governors this is not now required, and much less space is now occupied by the apparatus.

Serious accidents have arisen from the escape of gas by the tilting of the floating bell; and, to obviate this danger, improvements have been

introduced in the construction of Governors.

The Governor of Messrs. J. and J. Braddock (Fig. 79 in section) will show what has been done in this direction. The gas enters from above the valve chamber. Over the valve, and of the same area as its base, is a compensating chamber within the bell, which is supplied with gas through a small pipe enclosing the valve rod, so placing the bell and valve in equilibrium. The bell is actuated by the outlet pressure, through a small pipe attached to the outlet branch. It will thus be seen that if by accident the bell were tilted or rent, the quantity of gas escaping would be limited to that which would be discharged through the two small pipes referred to.



Mr. F. W. Hartley introduced a safety and regulating plate over the valve to effect the same object, and obtained compensation by means of a small tank and holder placed alongside the Governor, the holder being suspended from the chain carrying the counterpoise weights.

Mr. D. Bruce Peebles employs the pressure of the inlet gas, supplied through a small pipe having a dry regulator fixed upon it, to load the bell of the Governor, which is enclosed in a gas-tight case; and the only adjustment required is by means of small weights to the

regulator.

Mr. W. Cowan has introduced various improvements in Governors, by which the adjusted pressure is maintained under all variations of draught or changes at the inlet. (See Fig. 80.) He has also invented an "Automatic Pressure Changer," a most ingenious instrument for raising and reducing the pressure automatically at any given time, thus dispensing with the attendant, except on extraordinary occasions.

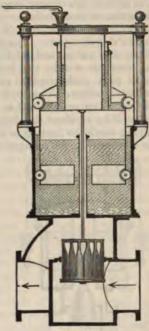


Fig. 80.

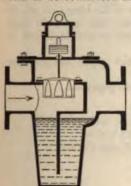
Mr. C. Hunt has adapted the ordinary throttle-valve to the purpose of a Governor. By this plan a holder scarcely larger in diameter than the main only is required. Within the supply-main leading from the works to the street, the disc or throttle is accurately balanced on two small steel centres; the lever or radius arm by which it is actuated, being also inside the main, is attached to the centre of the disc. A small vertical pipe, communicating the holder with the main, serves to enclose the connecting-pipe attached to the radius arm and to the crown of the holder, and also conveys the gas into the latter.

By means of this arrangement, a holder only $12\frac{1}{2}$ inches in diameter, will actuate an 8-inch valve; and one only 17 inches diameter, an 18-inch valve.

In winter time the water in a Governor tank is liable to freeze, particularly if the house containing it is in an exposed situation. A very efficient and simple remedy for this is provided by the steam stove. This is merely a cast-iron cylinder or pipe in the form of a pedestal, 2 ft. 6 in. to 3 ft. in height, and 10 or 12 in. in diameter, having a base, and an ornamental top or covering brightened by being ground and polished. The stove is placed on end on the floor of the Governor room, in any convenient part, and a steam-pipe about \(\frac{3}{4} \) in. in diameter, with stop-cock, is inserted through the bottom, in which is another stop-cock for letting off the water of condensation. In time of frost, by means of this stove, the atmosphere of the room can be maintained at an equable temperature, at a minimum expense. A piece of ordinary cast-iron pipe can be adapted to the purpose; on the other hand the stove is susceptible of any amount of ornamentation.

DISTRICT OR DIFFERENTIAL GOVERNORS.

Gas pressure varies according to the elevation, increasing and decreasing at the rate of about one-tenth of an inch for each 10 feet of rise and fall respectively. It is thus obvious that if the pressure in the lower mains is sufficient, that in the higher mains (assuming them to be connected throughout) must be in excess.



Frg. 81.

For the supply of gas to varying levels, therefore, separate leading mains, with a Station Governor upon each, are highly advantageous, and should be employed wherever practicable.

District or Differential Governors, for the automatic regulation of the pressure in the mains at high altitudes considerably removed from the gas-works, are also of the utmost utility. These are produced both in the wet and dry form by most makers of gas apparatus. Fig. 81 shows the District Governor made by Messrs. D. Bruce Peebles and Co.

By doubling the amount of pressure, the consumption of gas is increased by about one-

half. Leakage from a pipe is, of course, increased in the same ratio—
i.e., in the proportion of the square root of the pressure.

MAIN PIPES.

The leakage which arises in the distribution of gas is largely

due to defective and badly jointed Main pipes.

Hence it is of the first importance to ensure that the pipes employed for that purpose are made of a good quality of metal, close in texture, free from defects of every kind, and as equal as possible in their sectional thickness.

To secure these three latter conditions, all cast-iron pipes 5 inches internal diameter and upwards should be cast vertically in dry sand moulds. Smaller sizes are usually cast in green sand and in inclined

monlds.

The pipes should be tested by hydrostatic pressure equal to at least 75 lbs. on the square inch (150 feet head of water), either at the place of manufacture or on the gas-works; and whilst under pressure they should be smartly rapped with a 3 lb. hammer from end to end. This will often reveal faults, such as sandy, porous, and blown places, not otherwise discernible.

Rapping the pipes whilst on the ground will also indicate their character. If the sound emitted is clear and bell-like, the pipe may be considered free from defects. On the other hand, if dull and

leaden, it is cracked or otherwise imperfect.

All pipes that do not stand the tests should be rejected.

The metal of pipes, whilst compact and close, should not be excessively brittle and splintery, but such as may be readily chipped and drilled.

Cast-iron pipes below 3 in. diameter are 6 ft. long; 3 in. to 11 in. diameter, 9 ft. long; when 12 in. diameter and upwards they may be either 9 ft. or 12 ft. long. The socket is not included in these lengths.

It is usual to pay for any overweight in the pipes beyond the

weight specified, not exceeding 4 per cent.

Formula for calculating the weight of cast-iron pipes:—

 $W = 2 \cdot 45 (D^2 - d^2).$ Where D = outside diameter of pipe in inches. d = inside diameter of pipe in inches. W = weight of a lineal foot of pipe in lbs.

TABLE.

CAST-IRON GAS PIPES, WITH OPEN JOINTS.

The weight of the socket, and bead on spigot, is equal to 9-10ths of a lineal foot of the pipe, and this is included in the weights given.

Internal Diameter of Pipe.	Thickness of Metal in Body of Pipe.	Lengh of Socket, inside measure.	Length of Pipe not including Socket.	Weight per Pipe inclusive of Socket and Bead.			
Inches.	Inches.	Inches.	Feet.	Cwts. qrs. lbs.			
1	5-16ths	21	6	0 1 0			
13	5-16ths	21	6	0 1 10			
2	5-16ths	8 8 8	6	0 1 242			
$2\frac{1}{2}$	8-8ths	8	6	0 2 17			
8	8-8ths	8	9	1 0 11			
4	8-8ths	4	9	1 1 19			
5	7-16ths	4	9	2 0 7			
6	7.16ths	4	9	2 1 21			
5 6 7 8	5.10ths	4	9 9 9 9 9 9	3 0 2 7			
8	5 10ths	4	9	8 2 19			
9	5-10ths	44	9	4 0 11			
10	9-16ths	41	9	5 0 16			
11	9-16ths	43		1 1 19 2 0 7 2 1 21 3 0 27 8 2 19 4 0 11 5 0 16 5 2 14 8 8 16 9 2 12			
12	5-8ths	43	12	8 8 16			
18	5-8ths	44	12				
14	5-8ths	44	12	10 1 8			
15	5-8ths	41	12	11 0 4			
16	11-16ths	44	12	12 8 24			
17	11-16ths	41	12	18 2 24			
18	11-16ths	44	12	14 2 0			
19	3-4ths	41	12	16 2 24			
20	3-4ths	44 4 4 4 4 4 4 4 4 4 5 5 5 5 5 6 6 6	12	17 2 8			
21	8-4ths	5	12	18 1 20			
22	18-16ths	5	12	20 8 20			
28	18-16ths	5	12	21 8 8 24 2 8			
24	7-8ths	5	12	24 2 8			
80	1	5	12	85 0 0			
36	1 ith	6	· 12	47 0 16			
42	laths	6	12	57 8 16			
48	1½th	6	· 12	69 2 0			

For the smaller sizes of pipes up to 8 in. diameter, the open jointing space is § in., and for larger diameters § in. wide all round. The following are the usual depths of the socket, inside measure, for the various sizes of open-jointed gas-pipes, plugged with yarn and lead:—

	D	am	eter.												D	epti	of Bocket.
Up	to	3	inches	٠.												3	inches.
			**														
			,,													43	1)
21	to	80		•			•_				•		•			5	,,
		82	"	and	uj	owa	rds	•	•	•	•	•				6	,,

TABLE.

· Cast-Iron Gas Pipes, with Turned and Bored Joints, having a Recess in Front for Lead.

The weight of the socket and thickened spigot is equal to $1\frac{1}{10}$ lineal foot of the pipe, and this is included in the weights given.

Internal Diameter of Pipe.	Thickness of Metal in Body of Pipe.	Length of Socket, inside measure.	Length of Pipe, not including Socket.	Weight per Pipe, inclusive of Socket and thickened Spigot		
Inches.	Inches.	Inches.	Feet.	Cwt, qrs. lbs.		
1	5-16ths	21/2	6	0 1 1		
13	5-16ths	24	6	0 1 12		
2	5-16ths	8	6	0 1 24		
24	8-8ths	8	6	0 2 19 1 0 14		
8	3-8ths	82	9			
4	3-8ths	4	9	1 1 22		
5	7-16ths	4	9	2 0 18		
6	7-16ths	43	9	2 1 27		
3 4 5 6 7 8 9	5-10ths	44	699999999999	1 1 22 2 0 18 2 1 27 8 1 8 8 3 0 4 0 28 5 1 0 5 8 1 9 0 4		
8	5-10ths	44	9	8 8 0		
9	5-10ths	44	9	4 0 28		
10	9-16ths	41	9	5 1 0		
11	9-16ths	41	9	5 8 1		
12	5-8ths	44	12	9 0 4		
18	5-8ths	41	12	980		
14	5-8ths	43	12	10 1 24		
15	5-8ths	5	12	11 0 24		
16	11-16ths	5 5	12	13 0 16		
17	11-16ths	51	12	18 8 20		
18	11-16ths	51	12	14 2 24		
19	3-4ths	51	12	16 8 24		
20	8-4ths	51	12	17 8 12		
21	8-4ths	51	12	18 2 24		
22	13-16ths	51	12	21 1 0		
28	13-16ths	51	12	22 0 20		
24	7-8ths	51	12	24 8 24		
80	i	51	12	85 2 4		
86	lith	6	12	47 8 16		
42	1 ths	6 6 6	12	58 3 4		
48	lith	Ř	12	70 2 8		

When the turned and bored joint, on being tested, is found gastight, it is not necessary to fill the recess with lead. The usual filling material adopted under such circumstances is Portland or Roman cement. These cements, if kneaded with warm water, set quickly; with cold water not so soon.

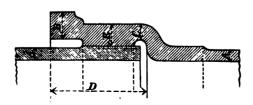


Fig. 82.

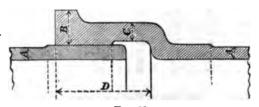
TABLE.

TABLE.

Dimensions of the Sockets of Turned and Bored Cast-Iron Gas Pipes, with a Recess in Front (Fig. 82.)

Dimensions of the Sockets of Turned and Bored Cast-Iron Gas Pipes, without a Recess in Front. (Fig. 88.)

					the control of the co					
Diameter of Pipe.	A	В	c	D	E	Diam. of Pipe.	A	В	O	D
Inches.	Inches.	In.	In.	In.	In.	Inches.	Inches.	Inches.	Inches.	Inches
2	5-16ths	11	1	8	3	2	5-16ths	7	2	3
21	3-8ths	1	10	31	13	21	8-8ths	1.5	16	34
3	3-8ths	18	8	34	1	3	3-8ths	1	4	84
81	3-8ths	1	8	34	7	31	3-8ths	11	1	8
4	3-8ths	11	11	4	14	4	3-8ths	11	11	4
5	7-16ths	11	11	4	14	5	7-16ths	18	11	4
6	7-16ths	14	4	41	1	5	7-16ths	13	1	44
7	5-10ths	1,5	3	44	1	7	5-10ths	1,0	2	44
8	5-10ths	12	18	41	1,10	8	5-10ths	15	12	44
9	5-10ths	18	3	44	1,4	9	5-10ths	111	Z	41
10	9-16ths	170	8	41	1,0	10	9-16ths	19	7	44
11	9-16ths	11	14	41	11	11	9-16ths	114	14	44
12	5-8ths	14	10	41	11	12	5-8ths	114	14	44
13	5-8ths	1 2	10	44	11	13	5-8ths	17	14	43
14	5-8ths	170	i a	41	11	14	5-8ths	17	1.5	41
16	5-8ths	18	1 0	5	14	15	5-8ths	2)	i	5
16	11-16ths	114	1	5	1,4	16	11-16ths	2	1	5
17	11-16ths	12	1,1	51	18	17	11-16ths	21	1,1	51
18	11-16ths	118	110	51	18	18	11-16ths	21	110	51
20	3-4ths	118	11	51	1,7	20	3-4ths	21	11	51



F16. 83.

TABLE.

CAST-IRON GAS PIPES, WITH FLANGE JOINTS.

The weight of the flanges is equal to 1 lineal fact of the pipe, and this is included in the weights given.

				Plangue.	•			
Internal Diameter of Pips.	n Bedy or Pipe.	Dia- meter across Planges.	Thick- ness of Metal.	Number of Bolt Holes.	Dia- meter, centre to centre, of Bolt Holes.	Dia- meter of Bolts.	outside	Weight per Pipe inclusive of the Flanges.
1 1 2 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21 22 23 24 24 25 26 27 27 28 28 29 20 20 20 20 20 20 20 20 20 20 20 20 20	Inches. 5-16ths 5-16ths 5-16ths 5-16ths 3-8ths 7-16ths 7-16ths 5-10ths 5-10ths 9-16ths 9-16ths 5-8ths 5-8ths 11-16ths	Inches. 4 44-1 64-7-1 7-5 9 101-1 13 14-5 16 17-1 18-1 18-1 19-1 20-5 21-2 24 25 26 27 28 29 30 31 32 38	Inches. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1.	3 3 4 4 4 4 4 4 4 4 4 4 4 6 6 6 6 6 6 6	10ches. 21 88 45 52 52 78 82 13 14 12 13 14 16 17 18 19 12 22 23 24 24 24 25 26 12 26 14 16 16 16 16 16 16 16 16 16 16 16 16 16	1 m ches.	Feet. 6 6 6 6 9 9 9 9 9 9 9 9 9 9 12 12 12 12 12 12 12 12 12 12 12 12 12	Cwis. qrz. lbs. 0 1 0 0 1 11 0 1 22 0 2 18 1 0 11 1 1 22 0 10 2 1 24 3 1 5 3 2 5 4 0 17 5 0 22 5 2 20 10 1 16 11 0 12 13 0 8 13 3 8 14 2 12 16 3 12 17 2 24 18 2 8 21 0 8 22 0 0 24 3 0 24 3
36 42 48	liths laths lith	45 51 57	18 18 12	18 20 24	41½ 47½ 53½	1 1 1	12 12 12 12	35 1 0 47 2 0 58 1 8 70 0 4

Cast-iron in cooling from the molten condition shrinks one-eighth of an inch per foot.

Main Pipe Joints.

A host of joints for Main pipes have been invented from time to time, which, though theoretically good, have not all proved very satis-

factory in practice.

The classes of joint generally in use are the turned and bored, and the open joint. The ball and socket joint is employed under exceptional circumstances, as when the Main has to be laid in the bed of a river or harbour, or across a narrow arm of the sea.

A difference of opinion exists among engineers as to which form of joint is best—the turned and bored, or the open joint filled with

lead, rust cement, or other substance, metallic or otherwise.

We, who have had large experience in both, and under most circumstances, prefer the turned and bored, both for ease in adjustment, economy, and efficiency.

In districts where the ground is extensively undermined and liable to subsidence, the vulcanized india-rubber joint (which is virtually an open joint) is the most suitable.

Special pipes, such as bends, tees, and junctions are, for convenience

sake, made with open joints.

The turned and bored joint is shown in Fig. 84.



Fro. 84.

There is no difficulty in swinging round ordinary curves with a line of Mains jointed in this manner; but when the radius of the curve is short, an occasional yarn and lead joint is required.

In specifying for pipes with these joints, care should be taken that the bored and turned surfaces are not made with too much taper; indeed, the nearer the surfaces approach to parallel lines, the better

they will fit.

When laying the pipes, the spigot and socket ends, after being cleaned with cotton waste, are coated with thick paint composed of one part each white and red lead mixed with boiled linseed oil; the end is then inserted and driven home with a mallet, or, should the pipe be large, with a swing block.

In driving the pipes they will sometimes be found to spring back at every stroke. This may be due either to the surfaces being made too

conical, in which case it is difficult to ensure a good joint; or there is a slight ridge or roughness on the inner edge of the bored

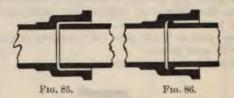
part of the socket. Chip this off with a sharp chisel.

Red lead sets sooner and harder than white; and the following reason is given for preferring the white to the red for joints:—When an expansion or contraction takes place in the pipes, the red lead is liable to crack, and so cause a leakage; whereas the white lead is more tractable, and better adapts itself to the varying circumstances. An equal mixture of the two is preferable.

The socket may either be bored flush up to the face, as in Fig. 83, or it may have a recess in front, as in Figs. 82 and 84. The latter is to be preferred, as it can be supplemented with lead or other filling

should the turned joint prove defective.

Two examples of the open joint are given in Figs. 85 and 86.



In placing the pipes, twined gasket is caulked in all round so as to fill nearly half the length of the open space. A roll of tough plastic clay is then passed round and pressed against the socket face, and through a lip on the upper side molten lead is poured till the remaining space is filled. On the lead being set up with a blunt caulking tool and hammer the joint is complete.

The ladle should contain sufficient molten lead to fill the joint at one pouring, otherwise the adhesion of the metal throughout will not

be perfect.

Molten lead, when heated to redness, will fly when poured upon a wet or damp surface.

TABLE

Giving the Weight of Lead in Pounds required for Jointing Cast-Iron

Mains.

Diameter of Pipe in Inches.	Depth of Lead in Inches.	Weight of Lead in Pounds.	Diameter of Pipe in Inches.	Depth of Lead in Inches.	Weight of Lead in Pounds.
14	18	11	11	21	161
2 24	19 19	21	. 12 . 18	22 22	18 <u>i</u> 21
3	18	22	14	2	231
4	13	4.	15	24	26
5	14	51	16 17	21	281
9	2	82	18	2 <u>i</u> 2 <u>i</u>	81 824
Ŕ	24	101	19	2	84
ğ	$ar{2}_{4}^{8}$	121	20	28	354
10	21	141	24	3	48

For pipes $1\frac{1}{2}$ to 8 inches in diameter the lead is assumed to be about $\frac{3}{2}$ -inch thick; and in pipes 9 inches in diameter and upwards, $\frac{1}{2}$ -inch thick.

In place of lead, rust cement and a mixture of beeswax and tallow are used for jointing mains. "Spence's metal" also is an efficient substitute, and its cost is considerably less.

Iron or Rust Cements for Flange and Open Socket Joints.

- (1) 1 lb. of clean iron borings, pounded fine in a mortar.
 - 2 oz. sal ammoniac (muriate of ammonia) in powder.
 - 1 oz flowers of sulphur.

Mix the whole together by pounding and keep dry. For use, mix one part with twenty of iron borings pounded, adding water to the consistency of mortar.

- (2) 98 parts fine iron borings.
 - 1 part flowers of sulphur.
 - 1 part sal ammoniac.

Mix, and when required for use, dissolve in boiling water. This cement sets quickly.

If required to set slowly, which makes the better joint-

- (8) 197 parts iron borings.
 - 1 part flowers of sulphur.
 - 2 parts sal ammoniac.

When required for use, mix with boiling water.

The iron borings used for making joints should be perfectly free from grease and oil.

The cubical content of the joint in inches, divided by 5, gives the

weight in pounds of iron cement required.

The india-rubber joint (Fig. 87) is formed by passing a vulcanized ring of that material round the spigot end of the pipe, which is specially cast with a groove and bead to suit this description of joint. When the pipe end is pushed forward into the socket, the ring is



Fig. 87.

compressed or flattened, and butts against the raised bead. No other packing is necessary, so that it is an expeditious method of jointing, whilst the vulcanized india-rubber, unaffected by the presence of gas or moisture, is practically indestructible.

The other advantages of this joint are referred to above.

The ball and socket joint is shown in Fig. 88. This particular form is the invention of Mr. J. Z. Kay, and has been successfully employed for Main pipes crossing through rivers and harbours where the



Fig. 88.

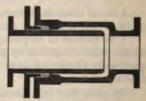


Fig. 89.

ordinary rigid joint is inapplicable. The lead is first run in and caulked; and the connected pipes, being like a chain, can be paid out of a lighter, or other vessel, when they will find their own bed in the river bottom.

The expansion joint (Fig. 89) is useful in all cases where a line of Main is exposed to varying temperatures, as in pipes placed against a wall or alongside a bridge, or in an open trench or channel.

Mill-board or engine-board coated with red or white lead, makes

a good and durable joint for flanges.

A combination of asbestos and india-rubber woven sheeting, makes a superior flange joint, especially for steam purposes, as these substances resist the action of both heat and moisture. To prevent adhesion to the iron (in the case of blank flange and manhole joints that require to be frequently broken), the flange should be rubbed over

with powdered black lead before placing the cover.

Metallic rings are commonly used for flange joints. These are best made with \(\frac{1}{4}\)-inch or \(\frac{3}{8}\)-inch lead pipe, with the ends soldered evenly together; the ring is then covered with flax, and well smeared with red lead or paint. The pipe must not be beaten flat, but left round, so that when the joint is screwed up it may bed into any irregularities in the surfaces. The remaining space between the flanges is filled with rust or other cement.

Flange pipes can be jointed without the interposition of any packing material, by having the flanges faced in a lathe. In such case the surfaces are merely coated with white lead paint, and the joint

tightened up.

Bolts used for jointing flanges, &c., should have a gummet of flax or tow, smeared with red or white lead, placed round their neck to bed under the head when screwed up.

Red and white lead should always be mixed with boiled linseed oil.

Other oil can be made to answer, but not nearly so well.

Wrought-Iron Main Pipes.

Of recent years a considerable trade has sprung up in the manufacture of wrought-iron and steel Main pipes of large diameter for foreign countries. Although the first cost of these is much greater than that of the same sizes in cast-iron, yet owing to their being lighter and less liable to fracture, the reduced expense of freight and haulage to their destination makes their ultimate cost, length for length, materially less.

The wrought-iron pipes are lap-welded, and those of the steel are riveted in the seam. They are generally in 15-feet lengths. The first table on p. 228 gives the usual thickness and weight of wrought-

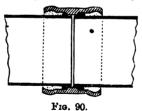
iron pipes.

TABLE.

Thickness and Weight of Wrought-iron Main Pipes.

Diameter Inside. Inches.	Thickness. Inches.	Weight per Foot. Pounds.
3	5-32 full,	6
81	5-32 full.	7
4	3-16	, 9
5	8-16	101
6	8-16	18
7	1-4 bare.	. 18
8	1-4 b a re.	20
9	1-4 bare.	244
10	1-4	28
12	1-4	93
14	5-16	48
16	5-16	5 D

The smaller sizes, 8 in., 8½ in., and 4 in. diameter have screwed ends and sockets. The larger diameters may be either screwed or



plain. In the latter case the "Kimberley" Collar (Fig. 90) is employed for connecting them; this is also made of wrought-iron.

TABLE.

Weight of Lead required for Jointing Wrought-iron Main Pipes with the "Kimberley" Collar.

Internal	Depth of Lead	Weight	Internal	Depth of Lead	Weight
Diameter	on each side	of	Diameter	on each side	of
of Pipe.	of Collar.	Lead.	of Pipe.	of Collar.	Lead.
Inches.	Inches.	Pounds.	Inches.	Inches.	Pounds,
5 6 7 8 9	12 12 12 12 12	82 10 112 132 15	10 11 12 14 16	13 13 13 14 2 2	16½ 18 20 26

The Laying of Main Pipes.

Special care is needed in the laying of Main pipes. As a general rule the covering of soil over them should be at least 21 inches deep, to protect them from the influences of heavy traffic and low and varying temperatures.

The excavation to receive the pipes should not be unnecessarily wide, as the less filling up that is required the better, not to mention the

saving in cost.

The bottom of the trench on which the pipes rest should be even and firm, and if not so, then thoroughly consolidated by punning. The soil should be scooped out at the various points in the trench bottom, where the sockets come, so that the body of the pipe may lie solid throughout its length. In cases where this cannot well be done resort may be had to underpinning.

Each pipe should be laid with the proper inclination or fall, and securely jointed; all joints being proved either with gas or air under

high pressure while the trench is open.

In refilling the trench, the soil should be shovelled in in layers, and rammed firmly and equally all round and above the pipes.

Gas pipes should be free from excrescences, and moderately smooth

on their inner surface.

They are better not coated internally with any kind of substance soluble in naphtha or other hydrocarbon liquid. Such coating is soon dissolved by the gas, and drains partially away into the drip wells; the residue collecting into viscid masses at different points, principally near to the joints. The coating can only be intended to reduce friction by rendering the surface smooth for the passage of the gas, because as a preservative to the iron, internally, it is not required. Its effect is to impede the flow. The slight deposit which takes place from the gas alone soon gives the metal a smooth coating. These objections do not, of course, apply to the internal coating of water-pipes.

It is only for appearance sake, as a rule, that a covering of this description can be recommended for the outside of cast-iron pipes. It

often serves only to hide defects in the casting.

The reddish-brown oxide covering which cast-iron pipes acquire in a short time, when laid in ordinary soil, is one of the best preservatives of the metal. This covering is impervious to moisture, its effect being to arrest further corrosive action.

There are, however, circumstances where it is desirable and necessary to coat pipes externally, as, for example, when they are of wrought-iron, and when, though of cast-iron, they are to be laid in soils intermixed with engine ashes, furnace slag, vitrified cinders, clinker, dross, scoriæ, or chemical refuse of any kind.

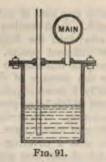
Furthermore, the pipes in such cases should be carefully embedded in good common soil obtained for that purpose, or puddled round with clay—especially protecting the upper side with a thick covering.

It is worse than useless to place clay only underneath the pipe. When so placed, it serves to receive and retain the water, which, percolating through the material forming the ground, is charged with acid bisulphides and other deleterious compounds. The metal of the pipe thus lying, as it were, in a bath of acidulous liquid, is destroyed sooner than it would be if no clay were present. The protection afforded by the clay should therefore be complete, all round the pipe, and particularly over its upper surface.

Gas pipes laid through arable land do it no harm, but rather good, inasmuch as they help to drain the land. The joints should be perfect,

however, as the escape of gas is fatal to vegetable life.

Mains in level ground should be laid with a slight inclination, say 1 foot in 400 yards, and at each lowest point a syphon or drip-well (Fig. 91), of cast-iron, should be placed underneath, and connected by a tube to the pipe to receive the liquid arising from condensation. Another form of syphon, with sockets to receive the Main pipes, is shown in Fig. 92. In all cases where a Main dips, a syphon is required at the place where the dip is reversed.





The liquor from these receptacles is pumped out periodically into a cask on wheels, and deposited in the tar-well on the gas-works.

In laying down Mains in lieu of others of a smaller size, the difference in value between the two sizes of pipes only should be charged to capital account.

Appliances used in Mainlaying.

In beginning to lay an extensive length of Main pipes, considerable delay, and consequent loss, is often experienced at first, owing to a

want of foresight in providing beforehand the necessary men, tools, and other appliances required. The following is an enumeration of what is necessary to be provided, varying according to the peculiarities of the district and the extent of the work to be done :-

One or two skilled main-layers.

A number of labourers according to the extent of the work.

A paviour and his labourer. A night watchman. A pick and spade (and a tool, if clay) for each labourer.

A supply of picks, pick-handles, and wedges should be kept in stock to replace broken ones.

A screen for separating stones and soil.

Shear-legs or tripod; or, what is better, if the Mains are of large diameter, a moveable pipe-layer, supported on wheels, running on rails laid alongside of the trench.

Blocks, tackle, and ropes or chain. A chain or clip to encircle the pipes.

Eight hand-spikes of wood, for moving the pipes about.

Two pieces of 2 or 3-inch wrought-iron tube (according to the size of main), on which to roll the pipe previous to lowering it to its place in the trench.

Two or four long iron bars, and two short ones.

Two planks for long and strong leverage.

Red and white lead, mixed with boiled oil, if turned and bored joints. Some cotton waste and old cards to clean the joints, if turned and bored. A supply of spun yarn and lead, if open joints.

A wooden mallet for driving small bored and turned pipes.

Two or four oak blocks, strengthened with bolts or hoops, to lay

against the pipe-sockets when driving.

A 3 or 4-inch cast-iron pipe, to swing with a rope or chain from centre of shear-legs when driving, or a wooden swing block if preferred.

Wood plugs for the various sizes of pipes and branches.

India-rubber cloth bags for plugging the mains. (See Fig. 23.)

A lead pot and two ladles. Chisels and caulking tools.

Tarred rope for trying the joints and pipes.

A coke fire-grate for melting the lead and for use by the night watchman.

Three setts, with handles, for cutting any pipes required.

Two large hammers, 7 lbs. weight, and several smaller ones, $1\frac{1}{2}$, 2, and 3 lbs. each.

Screwing tackle. Some fine flax for indifferent joints.

A few casks of cement.

A bogie or hand-drag, and two or three hand-barrows.

Portable bench, with vice attached. Covered hand-cart, under lock and key.

A supply of good soil for bedding the pipes, and to prevent the contact of ashes, if such should be present in the cutting.

A spirit-level and a straight-edge 10 or 12 feet long.

A supply of planking to cover up any part of the trench temporarily.

A box for the night watchman.

Two red signal lamps to warn passengers of the open trench during the dark hours.

Two stand-pipes for the signal lights.

Apparatus for proving the Mains for leakage before filling up the trench.

Look up beforehand what bends, tees, thimbles, flanges, drip-wells, and other special castings will be required in the course of the work, and have them in readiness when needed.

In enlarging or replacing pipes, many services require to be coupled up and renewed, and in that case service-layers and tools should be got ready.

Explosions in Main Pipes.

In the laying of large Main pipes, due care and diligence should be exercised by the skilled and responsible officials in charge of such Calamitous explosions have occurred owing to neglect in work. these particulars.

Such an explosion took place in London in 1862, and again in 1880; and one in Manchester, in 1873, when a large cast-iron syphon-well

was being attached to a Main.

Coal gas when unmixed with air or oxygen, as is well known, is perfectly inexplosive, and is even incombustible. It is only when the gas comes in contact with the oxygen of the air, as at the burner for example, that it can be ignited; combustion being in fact the union in the presence of heat of the hydrogen and carbon of the gas with atmospheric oxygen.

Explosions of the kind referred to are produced by a mixture of gas and air in certain proportions. The explosive force of a compound of this character is greatest when gas is mixed with eight times its bulk

of air.

Under ordinary circumstances it is impossible for air to become mixed with the gas in the street Mains. This can only occur when a Main is in course of being laid, or when a fresh junction is being made with an existing Main.

In the case of the London explosions referred to, a new Main was

being laid. In order to allow of this being done, the gas was either wholly or partially shut off at the junction with the live Main. Probably the gas was only partially excluded; and the limited quantity entering would, by the operation of the law of the diffusion of gases, gradually mix with the air existing in the new length of Main, till it became charged throughout its course with a dangerously explosive compound. On the application of a light, either accidentally or from intention, the mixture was ignited, with disastrous consequences to life and property.

It is not necessary that there should be the presence of actual flame to cause ignition. Dr. Frankland and other authorities have demonstrated the fact, well known to most gas engineers, that explosive mixtures of coal gas and air may be inflamed by a spark struck from stone or metal; that ignition may be caused by a spark produced from the hammer and chisel of a workman, or even from the tramp of a

horse upon the pavement.

There is no absolute necessity that the gas should be excluded from such an extent of Main pipes in course of being laid as to incur the risk of accident; because the Main for a short space from the point where the junction is being made can readily be closed by the ordinary india-rubber valves. When the Main is of such large diameter as to preclude the possibility of a valve of this kind being used, the utmost precaution is necessary to ensure the expulsion of the air before a light is applied to test the soundness of the joints.

Under any circumstances the application of a light is objectionable and unnecessary, as the joints can be proved when the Main is under pressure by brushing them over with a solution of soap in

water.

The Testing of Gas-Mains in the Ground.

The reduction of the loss of gas by leakage during recent years is remarkable. It is safe to estimate that twenty to twenty-five years ago, the unaccounted-for gas averaged sixteen per cent. of the gas produced. At the present time the average is only one-half that figure, or eight per cent. This reduction is largely due to the closer attention that is given to the pressures by day and night; to the use of governors in street lighting; and to the better supervision that is exercised in the laying of Mains and service-pipes.

It may be stated as a salutary rule, that the maximum initial pressure in a district during the hours of the heaviest consumption, should not exceed 20-tenths. When there is found to be a necessity for more, the trunk Mains, or some of the most contracted Mains branching

therefrom, should be replaced by larger ones.

Considerable expense must be incurred in any systematic attempt to reduce leakage; but wherever in a district the unaccounted-for gas

exceeds 10 per cent. of the make, the expenditure is not only justifiable on sanitary and other grounds, but is eventually found to be a good

and profitable investment.

Various appliances have been devised for testing gas Mains in the ground. Brothers' apparatus consists simply of two 30-light meters, one of which registers the passage of gas in the usual way; and the other is made to act as an exhauster, either by continuing the spindle of the drum through the casing and attaching a handle to it, or by means of a small wheel geared into a larger one on the periphery of the drum—the former being actuated by a handle from the outside. The Main having been severed, and the two ends carefully plugged, the exhauster inlet is connected to the live Main, and the meter outlet to the dead section of Main; the exhauster and meter also being joined. On the exhauster being gently turned, gas is drawn from the live Main, and forced through the meter into the length of Main under test, and thus the amount of loss in a certain time and under a given pressure is indicated.

The great cost is in cutting the pipes, reinstating them, and finding the exact locality of the escape. To obviate the necessity of severing the pipes, a suggestion was made at the meeting of the Manchester District Institution of Gas Engineers in November 1879, that watervalves or traps which would also answer the purpose of drip wells, might be permanently placed at intervals in the line of Mains. These traps, having a diaphragm extending to within a regulated distance of the

bottom, on being charged with water, would form a hydraulic valve, shutting off the gas from any section of Main as desired, and enabling a test to be made without difficulty and at reduced expense.

difficulty and at reduced expense.

Acting on this suggestion, Mr. J. H. Lyon has introduced an improved syphon box or hydraulic valve, for attaching to Mains, and by means of a leakage indicator affixed to stand pipes on each side of the box or valve, the quantity of gas escaping is readily ascertained. (See Fig. 94.)

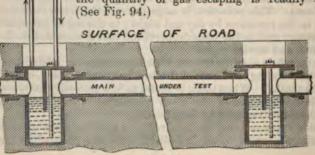


Fig. 94.

Showing the Average Cost per Yard of Laying Mains, 9 feet long each, with Turned and Bored Joints, and with Lead Joints, including the Total Expenses of Material (the Pipes excepted), Excavating, Reinstating, TABLES

Diameter in Inches.	13.		14.	4	15.	10	1	16.	17.		1	18,
Description of Joint.	Turned and Bored.	Lead.	Turned and Bored.	Lead.	Turned and Bored.	Lead.	Turned and Bored.	Lead.	Turned and Bored.	Lead.	Turned and Bored.	Lend.
In ordinary ballast In roads macadamized with Welsh or limestone In ordinary paved streets In bituminized streets In footpaths made with sand or ashes. In footpaths flagged In footpaths flagged	*** ** *** ** *** *** *** *** *** ***	8. 4 4 9 10 20 4 4 9 9 10 10 20 10 10 20 10 10 10 10 10 10 10 10 10 10 10 10 10	8 8 8 8 8 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9	s. d. 5 2 5 10 10 8 5 0 5 0 6 9	** 00 4 40 00 00 00 10 10 10 10 10 10 10 10 10 10	8. d. 6 0 111 4 11 4 7 7	%4 4 70 20 44 470 4.4 20 00 00 40 1	8. d. 6 10 7 1 12 3 6 3 6 5 7 11	7.4 10 10 0 4 40 5.0 01 40 0 00	8. d. 7 6 7 6 12 10 6 10 7 0 8 6	8. d. 5 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6	8. d. 7 111 113 6 11 113 6 11 113 6 11 113 6 17 11 113 6 17 113 113 113 113 113 113 113 113 113
Diameter in Inches.	19.		20.	0.	21.		22.	5	23,	*	63	24.
Description of Joint.	Turned and Bored.	Lead.	Turned and Bored.	Lead.	Turned and Bored.	Lead.	Turned and Bored.	Lead.	Turned and Bored.	Lead.	Turned and Bored.	Lead.
In ordinary ballast in roads macadamized with I nosds no limestone. In ordinary paved streets. In footpaths made with sand or ashes. In footpaths fagged In footpaths fagged In footpaths asphalted.	20 9 10 20 20 20 20 20 20 20 20 20 20 20 20 20	98 8 8 10 8 8 8 10 10 10 10 10 10 10 10 10 10 10 10 10	76 6 6 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9	8. d. 8 10 9 4 16 0 8 7 8 10 10 4	86 6 0 5 2 8 8.	9. 4. 9. 10. 10. 10. 10. 10. 10. 10. 10. 10. 10	8, d. 7 7 7 7 7 7 7 7 7 10 13 6 6 10 7 1 7 8 7 1 8 7 1 8 7 1 8 7 1 1 8 7 1 1 1 1	9, 9, 9, 9, 9, 9, 9, 9, 9, 9, 9, 9, 9, 9	8, d. 7 10 13 8 10 8 10 8 10	3. d. d. d. d. d. d. d. d. d. d. d. d. d.	3,7 7 7 7 7 6 9 7 7 7 6 9 7 7 7 1 8 9 7 7 1 9 7 7 1	2, d. 111 8 112 0 112 0 111 0 111 113 8 113 8

TABLE

Giving Weight and Cost per Yard of Cast-Iron Main Gas Pipes, 2, 3, and 4 inches diameter, at Rates from £4 to £10 per Ton. (Calculated to the nearest Penny.)

Diameter in Inches.		2.			8.			4.	
Class of Joint.	Open.	T. & B.	Finge.	Open.	T. & B.	Finge.	Open.	T. & B.	Flnge.
Weight per yard in lbs.	25	26	25	41	42	41	58	54	54
Cost per yard at 2 6 9 9 4 7 6 9 4 10 0 9 4 12 6 9 4 15 0 9 4 15 0 9 4 15 0 9 15 10 0 9 12 6 9 7 6 9 10 0 9 12 6 9 17 6 9 10 0 0 9 12 6 9 17 6 9 10 0 0 9 12 6 9 17 6 9 10 0 0 9 12 6 9 17 6 9 10 0 0 9 12 6 9 17 6 9 10 0 0 9 12 6 9 17 6 9 10 0 0 9 12 6 9 17 6 9 10 0 0 9 12 6 9 17 6 9 10 0 0 9 12 6 9 17 6 9 10 0 0 9 12 6 9 17 6 9 10 0 0 9 12 6 9 17 6 9 10 0 0 9 12 6 9 17 6 9 10 0 0 9 12 6 9 17 6 9 10 0 0 9 12 6 9 17 6 9 10 0 0 9 12 6 9 17 6 9 17 6 9 10 0 0 9 12 6 9 17 6	s.d. 0111 0 11 1 1 1 1 1 2 1 2 3 1 1 3 4 1 1 4 5 5 1 1 6 6 6 6 7 7 1 1 8 8 8 1 9 9 1 100 11 11 11 11 11 2 2 2 2 2 2 2 2 2	s.d. 111001111111111111111111111111111111	s.d. 1111	s.d. 667778899910111100011111000111111111111111	s.d. 677888991001111100011122223344555666778889910011111001112222222222222222222222	8. d. 666778889990111110001112222222222222222222222	8.11110112223445667789910111101122234456677899101100112233455677899	d. 1101122334456667899901111012233455667788990010110012333333333333333333444444444444	8.11101112211122222233455667777910111101112222222222222222222222222

Giving Weight and Cost per Yard of Cast-Iron Main Gas Pipes 5, 6, and 7 inches diameter, at Rates from £4 to £10 per Ton. (Calculated to the nearest Penny.)

Diameter in Inches.		5.		-	6.			7.	
Class of Joint.	Open.	T. & B.	Flnge.	Open.	T. & B.	Finge.	Open.	T. & B.	Finge
Weight per yard in lbs.	77	79	79	91	98	92	121	124	123
Cost per yard at et 0 0 per ton. 4 2 6	8. 4 9 9 10 1 0 1 2 3 4 4 5 6 7 8 9 10 11 0 1 2 3 4 4 5 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6	s. d. 221101233333344566789900111012334456678990111012334566666666666666666666666666666666666	s. 0.90 0.12234566789101101233456678991011012334566789910110123345667899101101233456678991011012334566789910101233456678991010101233456678991010101233456678991010101233456678991010101010101010101010101010101010101	s. 33 4 5 6 6 8 9 9 10 0 1 2 3 4 4 4 4 4 4 4 4 4 4 4 5 5 5 5 5 5 5 5	8. 4 5 6 6 7 9 10 11 1 2 2 3 5 6 6 7 9 10 11 1 2 2 3 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	7 8 7 10 7 11 8 0 8 1	10 5 10 6 10 8	10 3 10 5 10 6 10 8 10 10 10 11	8. 4 4 6 8 4 4 10 1 1 3 4 4 6 8 4 4 10 1 1 1 3 4 4 6 8 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6

Giving Weight and Cost per Yard of Cast-Iron Main Gas Pipes 8, 9, and 10 inches diameter, at Rates from £4 to £10 per Ton. (Calculated to the nearest Penny.)

Diameter in Inches,		8.			9.			10.	
Class of Joint.	Open.	T. & B.	Finge.	Open.	T. & B.	Flnge.	Open.	T. & B.	Flnge.
Weight per yard in lbs.	137	140	139	158	157	155	192	196	194
Cost per yard at #4 0 0 per ton. 4 2 6	s. d. 411 5 12 5 6 6 5 8 6 6 7 9 6 6 11 7 7 2 4 7 7 6 8 7 10 7 7 11 8 1 3 8 5 7 7 10 7 7 11 8 1 3 8 5 7 8 8 10 9 9 9 9 11 1 10 3 10 5 1 10 8 10 10 10 11 10 11 11 11 11 11 11 11 11	5. d. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0. 0.	s. d. 0 1 1 3 5 5 5 5 5 5 1 1 1 2 4 6 6 6 6 6 6 7 7 7 7 7 7 7 7 7 7 7 7 7	s. d. 6 5 8 5 10 0 6 6 2 4 6 6 6 6 10 0 7 7 7 7 7 7 7 7 7 7 7 7 7 8 8 2 4 4 6 8 8 8 8 10 1 3 5 7 9 9 11 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	s. d. 7 5 9 6 0 2 6 6 4 6 6 6 8 6 10 7 7 2 7 7 6 9 7 7 11 8 8 5 5 8 8 7 9 9 10 10 2 10 4 10 10 11 3 11 5 11 11 12 3 12 5 12 7 13 9 13 0 13 0 14 1 15 1 16 1 17 1 18	s. d. 6 6 9 1 1 1 6 6 6 5 7 7 7 7 7 7 1 1 2 4 6 6 8 8 8 8 9 9 9 9 4 6 8 8 8 8 8 9 9 9 9 9 9 10 0 0 10 0 5 7 11 11 11 11 11 11 11 11 11 11 11 11 1	8. d. 6 10 1 7 7 3 7 7 6 9 7 7 11 8 8 8 7 9 9 9 3 5 8 8 9 9 9 9 10 1 1 10 0 6 6 10 0 9 10 1 12 11 1 4 7 9 10 10 10 10 10 10 10 10 10 10 10 10 10	s. d. 7 0 7 3 7 7 5 8 7 11 8 1 4 8 6 8 9 9 9 9 2 9 9 5 9 9 10 10 1 10 6 10 9 10 11 10 12 0 12 3 6 12 8 12 11 13 7 11 13 7 14 13 14 5 14 8 14 11 15 6 6 16 5 16 6 0 16 2 16 5 8 16 8	s.d. 612 4 7 7 7 7 7 7 7 7 7 7 7 8 8 8 8 8 8 8 11 1 1 1

Giving Weight and Cost per yard of Cast-Iron Main Gas Pipes, 11, 12, and 13 inches diameter, at Rates from £4 to £10 per Ton. (Calculated to the nearest Penny.)

Diameter in Inches.		11.			12.			13.	
Class of Joint.	Open.	T. & B.	Finge.	Open.	T. & B.	Finge.	Open.	T. & B.	Finge
Weight per yard in lbs.	210	215	212	249	258	251	269	278	271
Cost per yard at #4 0 0 per ton. #4 2 6	s. d. 7 6 7 9 8 0 8 2 8 5 8 8 8 9 4 9 7 10 10 1 10 7 10 10 1 11 0 7 10 10 1 11 10 3 11 6 11 1 9 11 11 12 3 12 5 13 12 5 13 12 1 14 4 4 14 6 15 0 16 16 5 16 10 1 17 7 17 17 17 17 17 17 17 17 17 17 17 18 18 3 18 6 18 9 18 9	s. d. 7 8 7 11 8 2 5 8 8 8 8 11 9 4 9 77 10 10 10 11 1 1 11 1 6 11 1 9 12 0 3 12 6 12 8 13 10 14 2 5 14 15 1 1 15 1 1 16 16 7 7 15 10 17 7 6 16 17 7 9 18 0 3 18 6 18 9 9 2 19 2	12 1 12 4 12 6 12 9 13 0 13 3 13 6 13 9 14 0	s. d. 8 11 9 2 9 5 9 10 0 10 3 6 10 10 10 11 1 1 11 12 12 5 12 9 13 1 1 14 2 14 5 14 9 15 3 15 7 13 11 14 2 14 5 16 6 8 16 11 17 8 6 16 11 17 8 16 17 10 18 1 18 8 8 18 11 19 2 19 20 0 10 10 10 10 10 10 10 10 10 10 10 10	s. d. 9 0 9 4 9 7 9 11 10 2 10 5 11 0 11 10 12 2 12 12 8 13 0 13 3 13 10 14 1 14 5 14 8 15 10 16 8 15 10 16 8 17 6 18 11 19 2 18 13 17 6 18 11 19 2 19 6 19 2 10 4 10 9 11 10 9 1	14	16 3 16 6 116 10 17 1 17 5 17 9 18 0 18 4 18 7 18 11 19 3 19 6 19 10 20 1 20 5 20 9 21 0 21 4 21 7 1 122 3 22 6 22 10 23 1	s. d. 9 9 10 1 10 8 11 0 8 11 10 8 11 10 8 11 11 11 12 2 6 12 10 13 15 13 15 6 14 0 14 8 14 11 15 3 15 6 16 2 16 5 16 9 17 1 1 17 8 18 0 3 18 7 18 11 19 2 6 19 10 10 20 1 5 20 9 21 0 1 20 5 20 9 21 0 2 22 10 2 23 6 23 9 24 1 5	8. d 9 6 10 (6 11 11 12 11 11 12 11 11 12 11 11 12 11 11

Giving Weight and Cost per Yard of Cast-Iron Main Gas Pipes, 14, 15, and 16 inches diameter, at Rates from £4 to £10 per Ton. (Calculated to the nearest Penny.)

Diameter in inch	88.	14,			15.	- 1		16.	
Class of Joint.	Open.	T. & B.	Finge.	Open.	T. & B.	Finge	Open.	T. & B.	Flnge.
Weight per yard in	1bs. 289	298	291	809	814	811	363	368	366
Weight per yard in Cost per yard s 4 0 0 per to 4 2 6 4 5 0 " 4 7 6 " 4 10 0 " 4 12 6 " 4 17 6 " 5 0 0 " 5 2 6 " 5 16 0 " 5 12 6 " 5 16 0 " 6 12 6 " 6 10 0 " 6 12 6 " 6 10 0 " 7 2 6 " 7 7 6 " 7 10 0 " 7 15 0 " 7 15 0 " 7 16 0 " 7 17 6 " 7 10 0 " 7 15 0 " 7 17 6 " 7 10 0 " 7 15 0 " 7 16 0 " 7 17 6 " 8 0 0 0 " 8 2 6 " 8 5 0 " 8 7 6 " 8 10 0 " 8 12 6 " 8 15 0 " 8 16 0 " 8 17 6 " 9 10 0 " 9 2 6 " 9 10 0 " 9 12 6 " 9 10 0 " 9 12 6 " 9 10 0 " 9 12 6 " 9 10 0 " 9 12 6 " 9 10 0 " 9 11 6 " 9 11 0 0 " 9 12 6 " 9 10 0 " 9 11 6 " 9 11 0 0 " 9 11 6 " 9 11 0 0 " 9 11 6 " 9 11 0 0 " 9 11 6 " 9 11 0 0 " 9 11 6 " 9 11 0 0 " 9 11 6 " 9 11 0 0 " 9 11 6 " 9 11 0 0 " 9 11 6 " 9 11 0 0 " 9 11 6 " 9 11 0 0 " 9 11 6 " 9 11 0 0 " 9 11 6 " 9 11 0 0 " 9 11 6 " 9 11 0 0 " 9 11 6 " 9 11 0 0 " 9 11	t s. d.	s. d. 10 6 10 9 11 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	s. d. 10 5 10 9 11 1 1 11 4 11 8 12 0 12 4 12 8 13 0 13 4 13 8 14 0 14 3 14 7 14 11 15 3 15 7 15 11 16 3 16 7 16 11 17 3	s. d. 11 00 11 5 11 9 12 1 12 5 12 9 13 1 13 5 13 10 14 2 14 6 14 10 15 2 15 6 15 10 16 3 16 7 16 11 17 7 17 11 18 3 18 7 17 7 17 11 18 3 18 7 19 0 19 4 20 4 20 4	S14 S. d 11 3 3 11 7 7 13 0 14 4 9 15 5 5 16 6 6 10 17 20 16 6 7 10 16 3 18 7 7 18 11 19 3 3 19 7 7 20 20 8 21 22 23 6 23 10 22 24 6 24 10 25 3 25 7 25 11 26 7 27 0 27 4 4 6 7 7 7 7 7 7 7 7 7	\$11	S68 S. d. 13 9 14 2 14 7 15 0 16 2 16 7 17 10 18 3 18 8 19 0 17 16 17 10 18 3 18 8 19 0 19 5 19 10 20 3 20 8 21 1 10 22 3 23 1 1 22 3 23 1 24 4 9 25 16 25 11 26 4 24 9 27 6 25 11 28 4 24 9 27 6 27 11 28 4 28 9 27 28 4 28 9 27 28 4 29 2 29 7 30 5 30 9 31 2 31 7 31 31	8.68 8. d. 13 22 13 7 14 0 14 5 14 9 15 2 15 7 16 0 16 5 16 10 17 8 18 16 18 11 19 8 20 2 20 6 18 11 21 4 21 2 22 7 23 0 23 5 23 10 24 8 25 5 23 10 24 8 25 1 25 6 27 11 27 6 27 11 28 4 28 9 29 7 30 0 30 5 30 10 31 2 31 8 8	\$\frac{1}{3}\$, \$\frac{1}{6}\$, \$\frac{1}{3}\$, \$\frac{1}{1}\$, \$\frac{1}{3}\$, \$\frac{1}{1}\$, \$\frac{1}{3}\$, \$\frac{1}{1}\$, \$\frac{1}{4}\$, \$\frac{1}{4}\$, \$\frac{1}{4}\$, \$\frac{1}{1}\$, \$\frac{1}{6}\$, \$\frac{1}{1}\$, \$\frac{1}{6}\$, \$\frac{1}{1}\$, \$\frac{1}{6}\$, \$\frac{1}{1}\$, \$\frac{1}{6}\$, \$\frac{1}{1}\$, \$\frac{1}{6}\$, \$\frac{1}{1}\$, \$\frac{1}{6}\$, \$\frac{1}{2}\$, \$\frac{1}{3}\$, \$\frac

Giving Weight and Cost per Yard of Cast-Iron Main Gas Pipes, 17, 18, and 19 inches diameter, at Rates from £4 to £10 per Ton. (Calculated to the nearest Penny.)

Diar	nete	r in Inches.		1	7.				18	8.	1				1	9.		
C	lass	of Joint.	Open.	T. 6	ŁB.	Flnge.	Op	en.	T. d	B.	Fh	nge.	Op	en.	T.	& B.	FI	nge.
Weigh	t pe	r yard in lbs.	384	35	90	387	40	06	41	2	46	09	4	68	4	75	4	72
£4 0 4 2	t pe 0 6	r yard at per ton.	s. d. 13 8 14 2	s. 13 14	d. 11 4	s. d. 13 10 14 3		d. 6 11	8. 14 15	d. 8	s. 14 15	d. 7	s. 16 17	d. 8	s. 16 17	d. 11 6	8. 16 17	d. 10 5
4 5 4 7	6	31	14 7 15 0	14 15	9	14 8 15 1	15 15	5 10	15 16	7	15 16	6	17 18	9 3	18 18	0 7	17 18	11 5
4 10 4 12	6	"	15 5 15 10	15 16	8	15 6 15 11	16 16	9	16 17	7	16 16	5 11	18 19	10	19	7	18 19	11 6
4 15 4 17	6	0 11	16 3 16 9	16	6	16 5 16 9	17 17	2 8	17 17	6	17	10	19	10	20	2 8	20	0 7
5 0 5 2	0	22	17 2 17 7	17 17	5	17 3 17 9	18	7	18	5 10	18	3 9	20 21	11 5	21	2 9	21	1 7
5 5	0	"	18 0	18	8	18 2	19	0	19	4	19	2	21	11	22	3	22	1
5 7 5 10	6	29	18 5 18 10	18	9	18 7 19 0	19 19	6	19 20	9	19 20	8	22 23	6	22 23	10	22 23	8 2
5 12 5 15	6	**	19 3 19 8	19 20	7	19 5 19 10	20 20	5	20	8 2	20 21	6	23 24	6	23 24	10 5	23 24	8
5 17	6	"	20 2 20 7	20 20	5 11	20 4	21	9	21 22	7	21	5	24 25	7	24 25	11 5	24 25	9 3
6 2	6	21	21 0 21 5	21	4 9	21 2 21 7	22	8	22 23	6	22	10	25 26	7	26 26	0	25 26	10
6 7	6	**	21 10	22 22	2 7	22 0 22 5	23 23	7	23	5	23	8	26	8	27	0	26	10
6 10 6 12	6	11	22 9	23	1	22 11	24	0	24	11 4	24	9	27 27	8	27 28	7	27	5 11
6 15 6 17	6	33	23 2 23 7	23 23	6	23 4 23 9	24 24	11	25	10	24 25	8	28 28	7	28 29	7 2	28 29	5
7 0 7 2	6	1)	24 0 24 5	24 24	10	24 2 24 7	25 25	10	25 26	9 3	25 26	7 0	29 29	3 9	29 30	8	29 30	6
7 5 7	6	"	24 10 25 3	25 25	8	25 0 25 6	26 26	3 9	26 27	8 2	26 26	6	30	3 10	30	9 3	30	7
7 10 7 12	0	**	25 8 26 2	26 26	7	25 11 -26 4	27 27	2 8	27 28	7	27 27	5	31	4 10	31	10 4	31	8 2
7 15	0	"	26 7 27 0	27 27	0 5	26 9 27 2	28 28	1 7	28	6	28	3 9	32	4	32	10	32	8 2
8 0	0	22	27 5	27	10	27 8	29	0	29	5	29	2	33	5	33	11	33	8
8 2 8 5	6	11	27 10 28 3	28	9	28 1 28 6	29 29	5 11	30	11 4	29	8	33 34	6	34	6	34	9
8 7 8 10	6	"	28 8 29 2	29 29	2 7	28 11 29 4	30 30	10	30	10	30	70	35	6	35 36	6	35 35	10
8 12 8 15	6	"	29 7 30 0	30	0	29 10 30 3	31	8	31	8 2	31 31	6	36 36	7	36	7	36 36	10
8 17 9 0	6	**	30 5 30 10	30	11	30 8 31 1	32 32	2 7	32	8	32 32	5	87 87	1 7	37 38	8	87	5
9 2 9 5	6	"	31 3 31 8	31	9	31 6 31 11	33	1 6	33	7	83	4 9	38	2 8	38	8	38	5
9 7	6	"	32 1	32	8	32 5	34	0	34	6	84	8	39	2	39	9	39	6
9 10 9 12	6	"	32 7 33 0	83	6	32 10 33 3		11	35	5	34	8 2	39 40			10	40 40	7
9 15 9 17	6	"	33 5 33 10	33	11 5	33 8 34 1	35 35	10	35 3 36		35 36	7	40		41		41 41	7
10 0	0	23	34 3	34	10	34 7	36	3	36	9	36	6	41	9	42	5	42	2

Giving Weight and Cost per Yard of Cast-Iron Main Gas Pipes, 20, 21, and 22 inches diameter, at Rates from £4 to £10 per Ton. (Calculated to the nearest Penny.)

Diameter	in Inches.	-	20.					21	l.					2	2.		
Class	f Joint.	Open.	T. & F	. F1	nge.	Ope	en.	T. &	В.	Fli	ge.	Op	en.	T. 8	В.	Fh	nge
Weight per	yard in lbs.	492	500	4	96	51	6	52	14	52	0	58	9	59	15	56	90
Cost per	yard at	s. d.	s. d			s.	d.	8.	d.	в.	d.	8.	d.	В.			d.
E4 0 0	per ton.	17 7	17 1			18	5	18	8	18	7	20	11	21	3	21	R
4 2 6	11	18 1	10000	18	100	19	0	19	4	13	2	21	7	21	11	21	16
4 5 0	31	18 8	19			19	7	19	11	19	9	22	8	22	7	22	1
4 7 6	55	19 3	19			20	2	20	6	20	4	22	11	23	8	23	0
4 10 0	25	19 9		19	200	20	9	21	1	20	11	23	6	23	11	23	1
4 12 6	33	20 4	20		100	21	4	21	8	21	6	24	2	24	7	24	1
4 15 0	15	20 10		2 21		21	10	22	3	22	1	24	10	25	3	25	
4 17 6	**	21 5		21		22	6	22	10	22	8	25	6	25	11	25	2
5 0 0	11	21 11		1 22		28	0	28	5	23	2	26	2	26	7	26	-
5 2 6	19	22 6	22 1			23	7	24	0	23	9	26	10	27	3	27	-
5 5 0	35	23 1 23 7		$ \begin{array}{c c} 5 & 23 \\ \hline 23 & 23 \\ \end{array} $		24	2	24	7	24	4	27	5	27	11	27	
5 7 6	51			7 24		24	9	25	2	25	0	28	1	28	7	28	
5 10 0	39	24 2				25	4	25	9	25	6	28	9	29	3	29	9
5 12 6	33	24 9		1 24		25	11	26	4	26	1	29	5	29	11	29	
5 15 0	21	25 3				26	6	26	11	26	8	30	1	30	6	30	
5 17 6	. 22	25 10				27	1	27	6	27	3	30	9	31	3	30	
6 0 0	31	26 4		9 26		27	8	28	1	27	10	31	5	31	10	31	
6 2 6	39	26 11	-			28	8	28	8	28	5	32	0	32	6	82	
6 5 0	21	27 5				28	0	29	3	29	0	32	8	33	2	32	_
6 7 6	93	28 0 28 7		5 28		23	4	29	10	29	7	38	4	33	10	33	
6 10 0 6 12 6	32			7 29	7	29	11	30	5	30	2		0	34	6 2	34	
-	93	29 1 29 8		29		30 31	6	31	0	30	9	34 35	8	35		34 35	1
6 15 0 6 17 6	311	30 2		8 30		31	8	31	7 2	31	11	36	0	36	10	36	3
7 0 0	33	30 9	100	3 31		32	3	32	9	32	6	36	7	37	6 2	36	1
7 2 6	31	31 4	31 1			32	10	33	4	33	1	37	3	37	10	87	-
7 5 0	23	31 10		4 32		33	5	33	11	33	8	37	11	38	6	38	
7 7 6	33*	32 5	32 1			34	0	34	6	34	3	38	7	39	2	38	1
7 10 0	11	32 11	-	6 33		34	7	35	1	34	10	39	8	39	10	39	1
7 12 6	11	33 6		33		35	2	35	8	35	5	39	11	40	6	40	
7 15 0	19	34 0		7 34		35	8	36	3	36	0	40	6	41	2	40	1
7 17 6	**	34 7		2 34		36	3	36	10	36	7	41	2	41	10	41	1
8 0 0	11	35 2		8 35		36	10	37	5	37	2	41	10	42	6	42	
8 2 6	11	85 8		3 36		37	5	38	0	87	9	42	6	43	2	42	1
8 5 0	**	36 3	36 1			38	0	38	7	38	4	43	2	43	10	43	
8 7 6		36 9		5 37		38	7	39	2	38	11	43	10	44	6	44	
8 10 0	"	37 4	37 1			89	2	39	9	39	5	44	6	45	2	44	
8 12 6	**	37 11	2.00	6 28	2	39	9	40	4	40	0	45	2	45	10	45	
8 15 0	"	38 5		1 38	9	40	4	40	11	40	7	45	9	46	6	46	
8 17 6	"	39 0		7 39		40	11	41	6	41	2	46	5	47	2	46	
9 0 0	***	39 6		2 39		41	5	42	ĭ	41	9	47	1	47	10	47	1
9 2 6	"	40 1		9 40		42	0	42	8	42	4	47	9	48	6	48	
9 5 0	"	40 7		3 40		42	7	43	3	42	11	48	5	49	2	48	-
9 7 6	31	41 2	41 1			43	2	43	10	43	6	49	1	49	10	49	
9 10 0	11	41 9	42	5 42	1	43	9	44	5	44	1	49	8	50	5	50	
9 12 6	"	42 3		0 42			4	45	0	44	8	50	4	51	1	50	
9 15 0	"	42 10		6 48		44	11	45	7	45	3	51	0	51	9	51	
9 17 6	**	43 5	44	1 48	3 9	45	6	46	2	45	10	51	8	52	5	52	U
10 0 0	11	43 11	44	8 44	1 3		1	46	9	46	5		4		1	52	

Giving Weight and Cost per Yard of Cast-Iron Main Gas Pipes, 23, 24, and 30 inches diameter, at Rates from £4 to £10 per Ton. (Calculated to the nearest Penny.)

Diar	neter	in Inches.		5	23,					5	34.			1		-	30.		
C	Class	of Joint.	Open	T.	&B.	Fli	nge.	OI	en.	T,	& B	F	nge	0	pen.	T.	& B	FI	nge
Weigh	nt per	yard in lbs.	611	6	21	61	16	6	88	6	99	6	93	9	980	9	95	9	87
£4 0	st pe	r yard at per ton.	s. d 21 10			s. 22	d. 0	s. 24	d. 7	B. 24		8 24	d.	и. 35		8.		s. 35	d. 3
4 2	6	n	22 6	22	10	22	8	25	4	25	9	25	6	36	1	36	8	36	4
4 5	0	***	23 10		7 3	23	4	26 26	11	26	-	26		37		37	9	37	5
4 7 4 10	6	"	24 6			24	9	27	8	27 28	4	27	10	38		40	10	38	7 8
4 12	6	"	25 8		8	25	5	28	5	28	10	28	7	40		41	1	40	9
4 15	0	**	25 11		4	26	1	29	2	29	8	29	5	41	7	42	2	41	10
4 17	6	23	26 7		0	26	10	29	11	30	5	30	2	42		43	4	43	0
5 0 5 2	6	"	27 8 28 0		9 5	27 28	6 2	30	8	31 32	20	30	11 9	43	10	44 45	5	44 45	1 2
5 5	0	"	28 8		1	28	10	32	3	32	9	32	6		11	46	8	46	3
5 7	6	"	29 4		10	29	7	33	0	33	7	33	3		0	47	9	47	4
5 10	0	***	30 0		6	30	3	33	9	34	4	34	0	48	1	48	10	48	5
5 12	6	53	30 8	31	2	80	11	34	7	35	1	34	10	49	3	50	0	49	7
5 15 5 17	6	11	31 4 32 1	31 32	10	31	7 4	35	4	35	11 8	35 36	7 4	50	4 5	51 52	1 2	50 51	8 9
6 0	0	33	32 9	33	3	33	0	36	10	37	5	37	1	52	6	58	4	52	10
6 2	6	"	33 5	34	0	33	8	37	8	38	3	37	11	53	7	54	5	54	0
6 5	0	15	34 1	34	8	34	4	38	5	39	0	38	8	54	8	55	6	55	1
6 7	6	**	34 9	35	4	35	1	39	2	39	9	39	5	55	9	56	8	56	2
6 10	6	35	35 5 36 2	36 36	9	35	9	39	11 8	40 41	7 4	40	20	56 58	10	57	10	57 58	3 5
6 12	0	.11	36 10	37	5	37	1	41	5	42	1	41	9	59	1	59	11	59	6
6 17	6	"	37 6	38	1			42	3	42	11	42	6	60	2	61	0	60	7
7 0	0	**	38 2	38	10	38	6	48	0	43	8	43	4	61	3	62	2	61	8
7 2	6	***	38 10	39	6	39		43	9	44	6	44	1	62	4	63	3	62	9
7 5	0	33	39 6 40 3	40	2 11	89		44 45	6	45 46	3 0	44 45	10 7	63	6	64	5 6	63	11 0
7 7 7 7 10	6	21	40 11	41	7	41	3	46	1	46	10	46	5	65	7	66	7	66	1
7 12	6	33	41 7	42	3			46	10	47	7	47	2	66	9	67	8	67	2
7 15	0	25	42 3	42	11	42		47	7	48	4	47	11	67	10	68	10	68	3
7 17	6	21	42 11	43	8	43	-	48	5	49	2	48	9	68	11	69	11	69	5
8 0	6	33	43 8	44 45	4	44		49	11	49 50	11 9	49 50	6 3	70 71	0	71 72	0	70 71	6 7
8 2 8 5	0	93	45 0	45	9	45		50	8	51	6	51	0	72	2	73	3	72	8
8 7	6	93	45 8	46	5	46		51	5	52	3	51	10	73	3	74	4		10
8 10	0	17	46 4	47		46		52	2	58	0	52	7	74	4	75	6	74	11
8 12	6	17	47 0	47		47		58	0	53	10	53	4	75	6	76	8	76	0
8 15 8 17	0	37	47 9 48 5	48 49	6 3	48		53 54	9	54	7 5	54	2 11	76 77	7 8	77 78	9 10	77 78	1 3
8 17 9 0	6	11	49 1	49		49		55	3	56	2	55	8	78	9	79	11	79	4
9 2	6	11	49 9	50	70	50		56	1	56	11	56	6	79	10	81	1	80	5
9 5	0	33	50 5	51				52	10	57	9	57	3	80	11	82		81	6
9 7	6	12	51 2	52		51		57	7	58	6	58	0	82	0	88		82	7
9 10	0	19	51 10 52 6	52		52 52 1		58 59	4 2	59 60	3	58 59	9 7	83		84	100	83	8
9 12 9 15	6	11	53 2	54		53	_		11	-	10	60	4	85		86			10
9 17	6	"	53 10	54		54		60	8	61	8	61	i	86	-	87	-	87	0
10 0	Õ	**	54 7	55		55		61	5	62			10					88	1

Giving Weight and Cost per Yard of Cast-Iron Main Gas Pipes 36, 42, and 48 inches diameter, at Rates from £4 to £10 per Ton. (Calculated to the nearest Penny.)

Diam	eter i	in Inches.		8	6.					45	2.					48,			
Cl	ass of	Joint.	Open.	T. 6	ŧВ.	File	ige.	Op	en.	T. &	B.	Fin	ige.	Ope	n.	r. &	B.	Fln	ge,
Weight	per	yard in lbs.	1320	1	141	18	30	169	21	16	46	16	88	194	6	197	6	19	51
Cost £4 0		yard at per ton.	s. d.	8.	d.	s. 47	d.	s. 57	d. 11	s. 58	d.	s. 58	d.	8. 6		s. 6	d. 7	8. 70	d. 0
4 2	6	11	48					59	8	60	7	60	2	71		72	9	72	3
4 5	0	13	50 1		11	50	5	61	6	62	5	61	11	73	10	75	0	74	5
4 7	6	11	51				11	63	4	64	4	63	9			77	2	76	7
4 10	0	33		58			5	65	1	66	2	65	7	78		79	5	78	9
4 12 4 15	6	22	56 (54	11 5	66 68	11 9	68	10	67 69	5	80 82		81	7	81	0 2
4 17	6	22	57 8			57	11	70	7	71	8	71	1	84		83 1 86	10	83 85	4
	ŏ	**	58 11				4	72	4	78	6	72	11			88	2	87	6
	6	25	60 4		4	60	10	74	2	75	4	74	9	89		90	5	89	9
5 5	0	22	61 10	62	10	62	4	76	0	77	2	76	6	91		92	7	91	11
	6	**	63 4		4	63	10	77	10	79	0	78	4	93			10	94	1
	0	11	64 10		10	65	4	79	7	80	10	80	2	95		97	0	96	3
	6	11	66 4		4	66	10	81	5	82	8	82	0	97		99		98	6
	6	11	67 9		10	68	3 9	83	3	84	6	83	10			01	5 1		8
	0	**	69 3 70 8		10	69 71	3	85	10	86	2	85		102 104	1131		81		10
	6	33	72 2	78	4	72		88	8	90	0	89		106	51		01		3
	0	57	78 8		10	74	2	90	5	91	10	91		108	71		31		5
	6	11	75 2		4	75	8	92	3	98	8	92		110	81		61		7
6 10	0	11	76 7		10	77	2	94	1	95	6	94	9	112 1	11	14	81		10
	6	**	78 1		8	78	9989898	95	11	97	4	96	8	115	11		11 1	16	0
	0	- 27	79 7	80	10	80	2	97	8	99	2	98		117	31		11		2
	6	25	81 0 82 6		10	81		99	7.0	101		100		119	5 15		41		4
	6	33	84 0		10	83		101		102	10 1		ıí	121	7 15		6181		7 9
	0	"	85 5	86	10	86		104	11			05			0 1		111		11
	6	**	86 11	88	4	87		106		108		07		128	2 13		11		2
7 10 (0	27	88 5	89	9	89		108		110		09		130	4 13		41		4
	6	15	89 10		4	90	6	110		112	11			132	6 13	34	61		6
	0	**	91 4	92	9	92		112			11 1				8 18		91		8
	5	31	92 10		3	93		114		115			10		0 13		111		11
	6		94 3 95 9	95 97	9	95 96		115		117	5 1	16			014		21		1
	Ö	31	97 3		9	97	11			21		20		43	2 14		71		5
	6	"		100	3	99		121		23	ili				614	-	91	25	8
	0	10		101		100	11				11 1		11		8 14		ili		10
	B	**	101 8	103	3	102	5	124	10 1	126	91	25	9		0 18		11		0
	0	**	10 mg/s	104			11	7.5.5	100	128	7 1				0 1	54	4 1	53	2
	5	33		106	2.10	105		128	- 10	130	5 1				2 1		6 1		5
	6	,		107			10			132	31			156	4 15		91		7
	0	,		109		108	10	132	10	34	11 1	33			7 16		11		9
	6	"		112		111		135		137		36	10		8 16		21		11
	Ö	"		113		112	10			139		38		165	1116		71		4
	6	17		115		114		139		141		40			3 16		91		6
	0	**		116		115		141		143		42		169	5 17		01		8
	6	"		118		117	3	142	11	145	11	44	0	171	7 17		21		10
10 0	0	20	117 10	119	9	118	9	144	91	146	11 1	45	10	173	9 17	76	51	75	1

TABLE showing the Discharges of Gas in Cubic Feet per Hour. Specific Gravity 420. Pressure, 1 inch. (Clegg, 4th Ed., p. 304.)

I L								DIAMETE	R OF PIP	DIAMETER OF PIPES IN INCHES.	HES.				
in fin Yards,	ci	22	4	.5	.9	7.	ø	.6	10.	12.	14.	16.	18.	20.	22.
1			1						-	-					
000	2,291	7,258	19160			:	:	:	:		*	**	:	:	:
40	1,859	5,127	11,340	18,192	28,965	: :	: :	: :	: :	: :	: :	: :	: :	: :	: :
20	1,666	4,580	9,417	_		38,168	53,308	***	-	:	**	:		:	:
100	1,177	3,244	6,652	_		56,989	37,670	50,519	65,475			:		:	:
150	961	2,653	6,421	_		19,027	30,758	95,757	46 575	84,758	124,362	150.681		:	:
250	745	2,204	4.212	_		17,066	28,846	32,367	42,580	65,708	96,579	134,774		_	_
300	629	1,871	3,844	_		15,479	21,686	29,196	37,985	59,875	88,111	123,033			_
400	589	1,615	3,326	_		13,594	18,576	25,259	32,845	51,904	76,204	106,464	_	_	_
200	529	1,433	2,980	_		12,089	16,848	22,526	29,430	46,461	68,266	95,785	_	_	_
900	480	1,824	2,721	_		10,970	15,292	20,557	26,865	43,379	62,181	87,145	_	_	_
002	442	1,227	2,505			10,187	19,169	12,026	24,840	39,288	59 078	80,924	108,037	140,400	177,071
900	: :	1.081	9,903			8,996	12,268	16,839	21.870	84.599	50,803	71.248	_	_	_
000		1,020	2,095	_		8,533	11,836	15,965	20,790	32,853	48,157	67,382	_	_	_
094			1,576	_		6,416	8,985	12,137	17,010	24,688	36,250	50,803		_	_
640	**		1,296			5,225	7,257	9,841	12,690	20,217	29,682	41,512	_	_	_
620	**	:	1,123	_		4,498	6,307	8,529	11,070	17,526	25,686	85,942	_	_	_
280	**		:			8,704	5,184	6,889	9,040	14,191	20,905	28,030	_	_	_
040	**	**				3,175	4,496	6,014	7,836	13,247	17,992	25,228	_	_	_
900			:		:			5,358	7,020	10,886	16,140	22,464	_	_	_
000					100	100				7080	15 ORI	01 000	-	-	-

Of the Discharge of Gas, in Cubic Feet per Hour, through Pipes of various Diameters and Lengths, at different Pressures.

By Thomas G. Barlow. Extended by Thomas Newbigging.

(The specific gravity of the gas is taken at 0.4, air being 1.)

The tables are calculated according to the formula given by Professor Pole in his valuable article * "On the Motion of Fluids in Pipes," viz.:—

Q = quantity of gas in cubic feet per hour.

l = length of pipe in yards.

d =diameter of pipe in inches.

h =pressure in inches of water.

s = specific gravity of gas, air being 1.

$$Q = 1850 \ d^3 \sqrt{\frac{h \ d}{s \ l}}$$

—i.e., multiply the pressure in inches of water by the diameter of the pipe, also in inches. Divide the product by the specific gravity of the gas multiplied by the length of the pipe in yards. Extract the square root of the quotient, which root, multiplied by the constant quantity 1850, and the square of the diameter of the pipe in inches, gives the number of cubic feet discharged in one hour.

EXAMPLE.—It is required to find the number of cubic feet of gas of the specific gravity of '400, which will be discharged in one hour from a pipe 8 inches in diameter, and 1250 yards in length, under a pressure of 15-10ths, or 1½ inches head of water.

Thus—
$$(h d) = 8 \times 1.5 = 12$$
.

$$\left(\sqrt{\frac{h\ d}{s\ l}} = \frac{12}{\cdot 4\ \times\ 1250}\right) = \cdot 024$$
, the square root being = ·1549.

$$\left(1850 \, d^3 \sqrt{\frac{h \, d}{s}}\right) = 1850 \times 64 \times 1549 = 18,888 \, \text{cubic feet} = Q.$$

^{*} See "King's Treatise," Vol. II., p. 374, et seq.

Diameter of Pipe, 0.5 Inch.

Length in yards.	10.	20.	30.	50.	75.	100.	150.
Quantity delivered	1.12.00						1
with 0.1 in. pressure.	37.7	26.7	21-7	16.8	13.8	11.9	9.7
0.2 ,,	53.4	37.7	30.6	23.8	19.5	16.8	13.8
0.3	65.2	46.3	37.7	29.1	23.8	20.7	16.8
0.4 ,,	75.2	53.3	43.2	33.7	27.5	23.8	19.5
0.5 ,,	84.3	59.4	48.6	37.4	30.7	26.7	21.7
0.0	92.1	65.1	58.8	41.1	33.7	29.0	23.8
0.0	106.7	75.4	61.4	47.5	38.8	33.7	27.4
1.0	119.1	84.3	68.8	53.3	43.2	37.7	80.8
1.0	130.6	92.1	75.2	58.3	47.5	41.1	33.7
1.5	146.1	103.2	84.3	65.1	53.3	45.9	37-8
1.0	159.9	113.0	92.1	71.5	58.3	50.6	41.1
0.0	168.7	119.1	97.2	75-2	61.4	58.8	43.5
2.5 "	188-6	133.3	108-6	84.3	68.8	59.4	48.6

Diameter of Pipe, 0.75 Inch.

Length in yards.	10.	20.	80.	50.	75.	100.	150.
Quantity delivered							
with 0.1 in. pressure.	104.3	73.8	60.0	46.6	37.9	32.9	26.9
0.2	147.5	104.3	84.9	65'8	58-7	46.6	37-9
0.8 ",	179.9	126.8	104.3	80.9	65.8	57.0	46.6
0.4 ,,	207.3	146.5	119.9	93.2	75.9	65.8	53.8
0.5 ,,	282.3	164.0	133-6	103.2	84-2	73.8	60.0
0.6 "	254.3	179-9	146.5	113.9	92.6	79.7	65-3
0.8	293.8	207.3	169.3	131.3	107.0	92.6	75.9
1.0 "	328-8	232.3	189.8	146.5	119.9	103.2	84.2
1.2 ,,	359.9	254.3	207:3	160.9	131.3	113.9	92-6
1:5	402.4	284.0	232.3	179.9	146.5	126-8	103-2
1/0	441.1	311.3	254.3	192-2	160-9	138-9	113.9
0:0	464.7	328.8	268.0	207.3	169.3	146.5	119.9
2.5 ,,	519.4	367.5	299.9	232.2	189-8	164.0	183.6

Diameter of Pipe, 1 Inch.

1	Length in yo	ards.	10.	20.	30.	50.	75.	100,	150,
Qu	antity deli	vered							
	0.1 in. pr		214.0	151.0	124.0	95.0	78.0	67.0	55.0
	0.2	**	302.0	214.0	175.0	135.0	110.0	95.0	78.0
	0.3	1)	368 - 5	260.5	214.0	165.0	185.0	117.0	95.0
	0.4	11	426.6	301.0	245.7	190.0	156.0	135.0	110.0
	O.F	13	476.5	337.5	274.0	213.3	172.8	151.0	123.0
	0.0	11	522.4	368.5	301.0	233.5	190.3	164.7	135.0
	0.0		603.4	426.6	348.3	270.0	220.0	190.3	155.2
4	1.0	"	675.0	476.5	388.8	301.0	245.7	213.3	172.8
	1.0	,,	738 4	522.4	426.6	329.4	270.0	233 - 5	190.3
	1.5	19	826-2	584.5	476.5	368.5	301.0	260.5	213.3
	1.0	,,	904:5	639.9	522.4	405.0	329.4	286 - 2	233.5
	0.0	,,	954.4	675.0	550.8	426.6	348.3	301.0	245.7
	D.E		1,066.5	754 6	615.6	476.5	388 8	337-5	274.0

Diameter of Pipe, 1.25 Inches.

Length in	yards.	25.	50.	75.	100.	150.	200.	800.
Quantity d						Time		
with 0.1 in.	pressure.	236.0	167:0	137.0	118.0	96.0	84.0	68.0
0.2	11	333.0	236.0	192.0	167-0	137.0	118.0	96.0
0.8	"	407.1	289.0	236.0	205.0	167.0	144.0	118.0
0.4		470-3	333-2	272-1	236.0	192.0	167.0	137.0
0.2	11	527.3	371.2	303 - 7	263.6	215.1	187-0	152.0
0.6	**	575.8	407.1	333 - 2	286.8	235.8	203 - 9	166.6
0.8	"	666.5	470-8	383.9	888-2	272.1	235.8	192.3
1.0	11	744.6	527.3	430.3	371.2	803.7	263.6	215.1
1.2		816.3	575.8	470.8	407-1	333.2	286 · 8	235.8
1.5	"	913.3	645 4	527.3	455.6	371.2	322-7	263 . 6
1.8	.,	999.8	706.4	575.8	499.9	407.1	352-2	286 . 8
2.0	**	1.054.6	744.6	607.5	527.3	430.3	371.2	303 - 7
2.5	"	1.179 1	833.2	679.2	588.5	480-9	415.5	339.6

Diameter of Pipe, 1.5 Inches.

Length in yards.	25.	50.	75.	100.	150.	200.	800.
Quantity delivered			200		1.2		
with 0.1 in. pressure.	374.0	264.0	215.0	187-0	152.0	132.0	107.0
0.2	528.0	374.0	304.0	264.0	215-0	187.0	152.0
0.3 ,,	643.9	458.0	874.0	322.0	264.0	229.0	187-0
0.4	741-1	525 4	428.2	374.0	304.0	264.0	215.0
0.5	829.2	586 . 2	479.9	413.1	339.5	295.0	239.0
0.6 ,,	911-2	643.9	525.4	455.6	370.5	321.9	261-2
0.8 ,,	1.050 9	741-1	607.5	525.4	428.2	370.5	303 . 7
1.0 ,,	1.175-5	829 - 2	677.3	586.2	479.9	413.1	339.5
1.2 ,,	1,287 - 9	911.2	741-1	643.9	525.4	455.6	370.5
1.5 ,,	1,439.7	1.017.5	829 2	719.8	586.2	507.2	413.1
1.8	1,576.4	1.114.7	911.2	789 - 1	643.9	555.8	455 6
2.0 ,,	1.661 . 5	1.175.5	59.8	829 - 2	677-3	586.2	479.9
2.5 "	1,858.9	1,315.2	1.072-2	929 4	759.3	656.1	534 6

Diameter of Pipe, 2 Inches.

Length in yards.	50.	75.	100.	150.	200.	300.	500.
Quantity delivered		7.0					
with 0.1 in. pressure	. 540	441	381	311	270	220	170
0.2	763	623	540	441	381	311	241
0.8 "	934	763	665	540	468	381	296
0.4	1.080	880	761	623	540	441	341
0.5 ,,	1,204	983	853	697	604	492	381
0.6	1.318	1,080	934	761	659	540	416
0.8	1,523	1,242	1,080	880	761	621	481
1.0 ,,	1,706	1,393	1,204	983	853	697	540
1.2 ,,	1,868	1,523	1,318	1,080	934	761	589
1.5 ,,	2,090.	1,706	1,474	1,204	1,042	853	659
1.8 "	2,290	1,868	1,620	1,318	1,145	934	724
2.0 "	2,414	1,971	1,706	1,393	1,204	983	761
2.5 "	2,700	2 203	1,906	1,555	1,350	1,102	853

Diameter of Pipe, 2.5 Inches.

Length in yards.	50.	75.	100.	150.	200.	800.	500.
Quantity delivered			1			0.00	1
with 0.1 in. pressure.	943	770	667	545	471	335	298
0.2 ,,	1,335	1,090	943	770	667	545	421
0.3	1,628	1,335	1.172	943	819	667	516
0.4	1.882	1,540	1,333	1.090	943	770	596
0.5 ,,	2,109	1,721	1,485	1,215	1,055	861	667
0.6 "	2,303	1,882	1,628	1,383	1,148	943	731
0.8 ",	2,666	2,177	1,882	1,540	1,333	1,088	844
1.0 "	2,978	2,430	2,109	1,721	1,485	1,215	943
1.2 ,,	3,265	2,666	2,303	1,882	1,628	1,333	1,029
1.5 "	3,653	2,978	2,582	2,109	1,823	1,485	1,148
1.8 "	3,999	3,265	2,827	2,303	2,000	1,628	1,266
2.0 ,,	4,219	3,443	2,978	2,430	2,109	1,721	1,333
2.5 "	4,717	3,848	3,333	2,717	2,354	1,924	1,485

Diameter of Pipe, 3 Inches.

Length in yards.	100.	150.	250.	500.	750.	1000.	1250.
Quantity delivered	10.01					-	
with 0.1 in pressure.	1,054	859	666	471	384	333	298
0.2	1,440	1,214	942	666	543	471	875
0.3	1,823	1,487	1.153	815	666	576	529
0.4	2,102	1.713	1,332	942	768	666	596
0.5	2,345	1,920	1,482	1.054	859	744	666
0.6	2,576	2,102	1,628	1,152	942	815	739
0.8	2,965	2,430	1,882	1.324	1,081	942	845
1.0 "	3,317	2,709	2,102	1,482	1,215	1,052	942
1.0	3,645	2,965	2,296	1,628	1,324	1.152	1,030
1.5	4.070	8,317	2,576	1,823	1.482	1,288	1,152
1.9	4.459	3,645	2,819	1,993	1,628	1,409	1,262
9.0	4.702	3,839	2,965	2,102	1,713	1,482	1.324
2.5 "	5,261	4,289	3,317	2,345	1,920	1,652	1,482

Diameter of Pipe, 4 Inches.

Length in yards.	100.	250.	500.	700.	1000.	1250.	1500.
Quantity delivered	1	To be a second				-	None Land
with 0.1 in pressur	e. 2.160	1,366	966	788	683	611	557
0.2	3.054	1,932	1.366	1,114	966	864	788
0.8 "	3,737	2,366	1.673	1,366	1,183	1,058	966
0.4 ,,	4,320	2,722	1,932	1,576	1,366	1,222	1,114
0.5 "	4.817	3.046	2,160	1,761	1,526	1,366	1.245
0.6	5,270	3,346	2,354	1,932	1,672	1,496	1,366
0.8 ,,	6,091	3,845	2,722	2,225	1,932	1.728	1,576
1:0	6,826	4,320	3,046	2,484	2,160	1,932	1,761
1.0	7,474	4,730	3,346	2,722	2,354	2,115	1,922
1.5	8,859	5,270	3,737	3,046	2,635	2,354	2,160
1.0	9,158	5,789	4.082	3,346	2,894	2,592	2,354
0:0	9,655	6.091	4,320	3,521	3.046	2,722	2,484
2.5 "	10,800	6,826	4,817	3,931	3,413	3,046	2,786

Diameter of Pipe, 5 Inches.

Length in yards.	100.	250.	500.	750.	1000.	1250.	1500.
Quantity delivered							
with 0.1 in. pressure.	3,540	2,245	1,587	1,296	1,122	1,000	910
0.2 ,,	5,005	3,174	2,245	1,832	1,587	1,414	1,296
0.3 ,,	6,514	3,888	2,748	2,245	1,943	1,732	1,575
0.4 ,,	7,526	4,759	3,174	2,592	2,245	2,000	1,820
0.5 ,,	8,438	5,333	3,778	2,888	2,508	2,236	1,934
0.6	9,214	5,839	4,118	3,174	2,748	2,449	2,245
0.8 ,,	10,665	6,750	4,759	3,881	3,174	2,828	2,596
1.0 "	11,914	7,526	5,333	4,354	3,778	3,174	2,877
1.2 ,,	13,061	8,285	5,839	4,759	4,118	3,679	3,375
1.5 "	14,614	9,214	6,514	5,333	4,590	4,118	3,540
1.8	15,998	10,125	7,156	5,889	5,063	4,523	4,118
2.0 ,,	16,875	10,665	7,526	6,143	5,333	4,759	4,354
2.5 "	18,866	11,914	8,438	6,885	5,940	5,333	4,860

Diameter of Pipe, 6 Inches.

Length in yards.	250.	500.	750.	1000.	1250.	1500,	1750.
Quantity delivered					-	bearing.	1000
with 0.1 in. pressure.	3,770	2,660	2,170	1,880	1,680	1,530	1,420
0.2	5,320	3,770	3,130	2,660	2,370	2,170	2,010
0.3 ,,	6,530	4,620	8,770	3,270	2,920	2,660	2,460
0.4 "	7,540	5,320	4,340	3,770	3,360	3,060	2,840
0.5	8,408	5,970	4,860	4,210	3,770	3,430	3,180
0.6 "	9,185	6,512	5,820	4,620	4,180	3,770	3,460
0.8 "	10,643	7,528	6,124	5,320	4,740	4,340	4,020
1.0 "	11,858	8,408	6,853	5,929	5,320	4,860	4,500
1.2 "	13,025	9,185	7,528	6,512	5,832	5,297	4,929
1.5 ,,	14,580	10,303	8,408	7,290	6,512	5,970	5,500
1.8 ,,	15,941	11,275	9,185	7,970	7,139	6,512	6,026
2.0 "	16,816	11,858	9,720	8,408	7,528	6,853	6,360
2.5	18,808	13,268	10,838	9,380	8,408	7,679	7,096

Diameter of Pipe, 7 Inches.

Length in yards.	250.	500.	750.	1000.	1250.	1500.	1750.
Quantity delivered					1.00		
with 0.1 in. pressure.	5,560	3,920	3,200	2,780	2,470	2,270	2,100
0.2 ,,	7,840	5,560	4,510	3,920	8,500	3,200	2,960
0.3 ,,	9,600	6,800	5,560	4,800	4,300	3,920	3,640
0.4	11,120	7,840	6,400	5,560	4,940	4,540	4,200
0.5	12,370	8,750	7,180	6,200	5,560	5,060	4,680
0.6	13,554	9,585	7,840	6,800	6,080	5,560	5,130
0.8	15,611	11,047	8,996	7;840	7,020	6,400	5,930
1.0 "	17,463	12,370	10,054	8,732	7,840	7,180	6,610
1.2	19,170	13,554	11,047	9,585	8,533	7,805	7,210
1.5 ,,	21,433	15,148	12,370	10,716	9,585	8,750	8,120
1.8 "	23,477	16,597	13,554	11,709	10,452	9,855	8,864
2.0 ,,	24,740	17,463	14,288	12,370	11,047	10,054	9,360
2.5 ,,	27,651	19,567	15,942	13,825	12,370	11,292	10,452

Diameter of Pipe, 8 Inches.

Length in yards.	250.	500.	750.	1000.	1250.	1500.	1750.
Quantity delivered	-	-					
with 0.1 in. pressure.	7,760	5,470	4,470	3,880	3,460	3,160	2,920
0.2 ,,	10,940	7,760	6,310	5,470	4,880	4,470	4,130
0.3 "	13,400	9,450	7,760	6,700	5,980	5,470	5,050
0.4	15,520	10,940	8,940	7,760	6,920	6,320	5,840
0.5 ,,	17,280	12,200	9,900	8,640	7,760	7,020	6,520
0.6	18,922	13,383	10,940	9,450	8,480	7,760	7,150
0.0	21,851	15,379	12,614	10,940	9,780	8,940	8,260
1.0 "	24,365	17,280	14,083	12,182	10,940	9,900	9,237
1.0	26,767	18,922	15,379	13,383	11,923	10,886	10,109
1.5	29,894	21,082	17,280	14,947	13,383	12,200	11,300
1.0	32.746	23,155	18,922	16,330	14,602	13,383	12,355
0.0	34,560	24,365	19,872	17,280	15,379	14,083	18.040
2.5 "	38,621	27,302	22,291	19,267	17,280	15,725	14,609

Diameter of Pipe, 9 Inches.

Length in yards.	250.	500.	750.	1000.	1250.	1500.	1750.
Quantity delivered				The same			
with 0.1 in. pressure.	10,400	7,380	6,350	5,200	4,650	4,250	8,950
0.2 ,,	14,760	10,400	8,500	7,380	6,480	6,000	5,620
0.8 ,,	18,000	12,780	10,400	9,000	8,300	7,380	6,800
0.4 ,,	20,800	14,760	12,700	10,400	9,300	8,500	7,900
0.5	23,182	16,500	13,420	11,900	10,400	9,680	8,800
0.6 ,,	25,369	17,933	14,760	12,780	11,400	10,400	9,650
0.8 "	29,306	20,667	16,938	14,760	13,100	12,000	11,050
1.0 ,,	32,805	23,182	18,918	16,403	14,760	13,420	12,380
1.2 "	35,867	25,369	20,667	17,933	16,064	14,653	13,559
1.5 "	40,131	28,409	23,182	20,011	17,933	16,500	15,200
1.8 ,,	43,959	31,055	25,369	21,979	19,683	17,933	16,621
2.0 ,,	46,864	32,805	26,681	23,182	20,667	18,918	17,600
2.5 ,,	51,332	36,632	29,853	25,916	23,182	21,105	19,574

Diameter of Pipe, 10 Inches.

Length in yards.	500.	750.	1000.	1250.	1500.	1750.	2000.
Quantity delivered						7	
with 0.1 in. pressure.	9,560	7,800	6,750	6,050	5,520	5,100	4,780
0.2 ,,	13,500	11,040	9,560	8,520	7,800	7,300	6,750
0.3 ,,	16,500	13,500	11,700	10,520	9,560	8,850	8,259
0.4 ,,	19,120	15,600	18,500	12,100	11,040	10,200	9,560
0.5	21,300	17,400	15,050	13,500	12,380	11,400	10,650
0.6	23,355	19,120	16,500	14,800	13,500	12,500	11,650
0.8 "	27,000	22,005	19,120	17,050	15,600	14,400	13,500
1.0	30,105	24,570	21,330	19,120	17,400	16,150	15,050
1.2 ,,	32,940	27,000	23,355	20,911	19,035	17,550	16,578
1.5	36,855	30,105	26,055	23,355	21,300	19,600	18,500
1.8 ,,	40,500	32,940	28,620	25,515	23,355	21,600	20,250
2.0 ,,	42,660	34,830	30,105	27,000	24,570	22,800	21,300
2.5	47,655	38,880	33,750	30,105	27,540	25,501	23,760

Diameter of Pipe, 12 Inches.

Length in yards.	500.	750.	1000.	1250.	1500.	1750.	2000.
Quantity delivered	100						
with 0.1 in. pressure.	15,100	12,300	10,700	9,550	8,700	8,050	7,550
0-2	21,400	17,400	15,100	13,450	12,300	11,350	10,700
0.3	26,100	21,400	19,500	16,500	15,100	13,880	13,050
0.4	30,200	24,600	21,400	19,100	17,400	16,100	15,100
0.5	33,600	27,500	23,800	21,400	19,440	18,050	16,800
0.6 "	36,741	30,200	26,100	23,300	21,400	19,800	19,500
0.8 "	42,578	34,603	30,200	26,900	24,600	22,700	21,400
1.0 "	47,433	38,880	33,631	30,200	27,500	25,450	23,800
1.2	52,099	42,573	36,741	32,853	30,112	27,799	26,049
1.5 ,,	58,320	47,433	41,212	36,741	33,600	31,250	29,250
1.8 ,,	63,763	52,099	45,100	40,896	36,741	34,020	31,881
0.0	67,262	54,820	47,433	42,578	38,880	36,100	33,600
2.5 ,,	75,232	61,430	53,071	47,433	43,351	40,240	37,519

Diameter of Pipe, 14 Inches.

Length in yards.	500.	750.	1000.	1250.	1500.	1750.	2000.
Quantity delivered.	Time			Lond	1. O. C.		I.C.
with 0.1 in. pressure.	22,100	18,100	15,600	13,950	12,750	11,800	11,050
0.2	31,200	25,500	22,100	19,800	18,100	16,700	15,600
0.3	38,400	31,200	27,100	24,250	22,100	20,500	19,200
0.4	44,200	36,200	31,200	27,900	25,500	23,600	22,100
0.5	49,400	40,400	35,000	31,200	28,500	26,460	24,700
0.6	54,216	44,200	38,400	34,300	31,200	28,900	27,100
0.8	62,445	51,067	44,200	39,600	36,200	33,400	31,200
1.0 "	69,854	57,153	49,480	44,200	40,400	37,300	35,000
1.2 "	76,681	62,445	54,216	48,421	44,188	40,986	38,340
1.5	85,730	69,854	60,593	54,216	49,400	45,700	42,600
1.8	93,906	76,681	66,414	59,270	54,216	50,009	46,834
2.0 ,,	98,960	80,703	69,854	62,445	57,153	52,920	49,400
2.5	110,602	90,228	78,268	69,854	63,768	59,005	55,301

Diameter of Pipe, 15 Inches.

Length in yards.	500.	750.	1000.	1250.	1500.	1750.	2000.
Quantity delivered.							
with 0·1 in. pressure.	26,300	21,400	18,600	16,600	15,200	14,000	13,150
0.2 ,,	37,200	30,400	26,300	23,500	21,400	19,900	18,600
0.8 ,,	45,500	37,200	32,250	28,750	26,300	24,300	22,750
0.4 ,,	52,600	42,800	37,200	33,200	30,400	28,000	26,300
0.5 ,,	58,700	48,000	41,600	37,200	34,000	31,400	29,350
0.6 ,,	64,395	52,600	45,500	40,700	37,200	34,450	32,250
0.8 ,,	74.115	60,750	52,600	47,000	42,800	39,800	37;200
1.0 ,,	82,923	67,736	58,623	52,600	48,000	44,400	41,600
1.2 "	91,125	74,115	64,395	57,408	52,548	48,600	45,562
1.5 ,,	101,756	82,923	71,983	64,395	58,700	54,300	50,800
1.8 ,,	111,476	91,125	78,914	70,470	64,395	59,535	55,586
9.0	117,551	95,985	82,923	74,115	67,736	62,800	58,700
2.5 ,,	131,523	107,223	92,947	82,923	75,937	70,166	65,610

Diameter of Pipe, 16 Inches.

Length in yards.	500.	750.	1000.	1250.	1500.	1750.	2000.
Quantity delivered.		Francisco					la Land
with 0.1 in. pressure.	31,000	25,250	21,850	19,550	17,850	16,550	15,500
0.2 ,,	43,700	35,700	31,000	27,700	25,250	23,400	21,850
0.8 ,,	58,600	43,700	38,100	34,000	31,000	28,700	26,800
0.4	62,000	50,500	43,700	39,100	35,700	33,100	31,000
0.5 ,,	69,120	56,600	49,000	43,700	39,900	37,150	34,560
06 "	75,686	62,000	53,600	47,900	43,700	38,100	40,700
0.8 "	87,402	71,193	62,000	55,400	50,500	46,800	43,700
1.0	97,459	79,488	69,120	62,000	56,600	52,400	49,000
1.2 ,,	107,066	87,402	75,686	67,703	61,516	57,024	53,533
1.5 "	119,577	97,459	84,326	75,686	69,120	63,900	60,100
1.8 "	130,982	107,066	92,620	82,944	75,686	70,087	65,318
20 ,,	138,240	112,665	97,459	87,402	79,488	74,300	69,120
2.5 ,,	154,483	126,144	109,209	97,459	89,164	82,598	77,068

Diameter of Pipe, 18 Inches.

Length in yards.	500.	750.	1000.	1500.	2000.	2500.	3000.
Quantity delivered							
with 0.1 in. pressure.	41,400	33,800	29,400	23,900	20,700	18,400	16,900
0.2	58,800	47,800	41,400	33,800	29,400	26,200	23,900
0.8 "	71,800	58,800	50,800	41,400	85,900	32,100	29,400
0.4 ,,	82,800	67,600	58,800	47,800	41,400	36,800	33,800
0.5	92,600	75,700	65,600	53,500	46,300	41,400	37,850
0.6 "	101,476	82,800	71,800	58,800	50,800	45,400	41,400
0.8	117,223	95,790	82,800	67,600	58,800	52,300	47,800
1.0	131,220	106,725	92,728	75,700	65,600	58,800	53,500
1.2	143,467	117,223	101,476	82,668	71,733	64,254	58,61
1.5 "	161,400	131,220	113,636	92,728	80,000	71,800	65,600
1.8 "	175,834	148,467	124,221	101,476	87,917	78,732	71,73
2.0 "	185,457	151,340	131,220	106,725	92,728	82,800	75,70
2.5 ,,	207,827	169,273	146,529	119,410	103,663	92,728	84,50

Diameter of Pipe, 20 Inches.

Length in yards.	500.	750.	1000.	1500.	2000.	2500.	3000.
Quantity delivered		1000					
with 0.1 in, pressure.	54,000	44,000	38,250	31,200	27,000	24,200	22,000
0.2	76,500	62,400	54,000	44,000	38,250	34,200	81,200
0.8	93,500	76,500	66,100	54,000	46,750	41,800	38,250
0.4 "	108,000	88,000	76,500	62,400	54,000	48,400	44,000
0.5 "	120,500	98,800	85,800	69,800	62,250	54,000	49,400
0.6 ,,	131,760	108,000	93,500	76,500	66,100	59,100	54,000
0.8	152,280	124,200	108,000	88,000	76,500	68,400	62,400
10 "	170,640	139,320	120,420	98,800	85,300	76,500	69,80
1.2 "	186,840	152,280	131,760	108,000	98,420	83,646	76,140
1.5 "	208,980	170,640	147,420	120,420	102,300	93,500	85,800
1.8 "	228,960	186,840	162,000	131,760	114,480	102,060	93,420
2.0 "	241,380	197,100	170,640	139,320	120,420	108,000	98,800
2.5	270,000	220,320	190,620	155,520	135,000	120,420	110,200

GAS ENGINEERS AND MANAGERS.

Diameter of Pipe, 22 Inches.

Length in yards.	500.	750.	1000.	1500.	2000.	2500.	8000.
Quantity delivered with 0·1 in. pressure 0·2 ,, 0·8 ,, 0·4 ,, 0·5 ,, 0·6 ,, 0·8 ,, 1·0	. 68,600	56,000	48,400	39,600	34,300	30,700	28,000
	96,800	79,200	68,600	56,000	48,000	43,400	39,600
	118,800	96,800	84,000	68,600	59,400	53,800	48,400
	137,200	112,000	96,800	79,200	68,600	61,400	56,000
	153,500	122,500	108,200	88,600	76,800	68,400	61,200
	168,577	137,200	118,800	96,800	84,000	75,000	68,600
	193,406	158,122	137,200	112,000	96,800	86,500	79,200
	216,275	176,418	152,895	122,500	108,200	96,800	88,600
1·2 ,,	237,184	193,406	168,577	136,560	118,265	105,850	96,703
1·5 ,,	265,280	216,275	187,525	152,895	132,000	118,800	108,200
1·8 ,,	290,697	237,184	203,860	168,577	145,054	130,026	118,265
2·0 ,,	306,444	249,598	216,275	176,418	152,895	137,200	122,500
2·5 ,,	342,381	279,655	242,280	197,326	171,190	152,895	140,000

Diameter of Pipe, 24 Inches.

Length in yards.	500.	750.	1000.	1500.	2000.	2500.	8000.
Quantity delivere	ed	7500		7.5		100	7
with 0.1 in. pressu	re. 84,000	68,600	59,500	48,500	42,000	37,500	34,300
0.2 "	119,000	97,000	84,000	68,600	59,500	53,400	48,500
0.3 ,,	145,500	119,000	103,000	84 000	72,700	65,200	59,500
0.4	168,000	137,200	119,000	97,000	84,000	75,000	68,600
0.5	187,500	155,000	135,600	108,600	93,800	84,000	77,500
0.6	208,396	168,000	145,000	119,000	103,000	92,000	84,000
0.8	240,900	196,655	168,000	137,200	119,000	106,000	97,000
1.0 ,,	269,049	219,283	189,734	155,000	135,600	119,000	108,600
1.2 ,,	294,710	240,900	208,396	170,294	146,966	131,414	120,450
1.5 "	329,702	269,049	233,280	189,734	163,000	145,500	135,600
1.8 ,,	360,806	294,710	255,052	208,396	180,403	161,585	146,966
2.0 ,,	380,946	311,040	269,049	219,283	189,784	168,000	155,000
2.5 ,,	425,347	347,587	300,931	245,721	212,284	189,734	172,000

Diameter of Pipe, 26 Inches.

Length in yards.	750.	1000.	1500.	2000.	2500.	8000. ·	4000.
Quantity delivered		ı ———	i i				
with 0.1 in. pressure.	85,000	73,500	60,000	52,000	46,500	42,500	36,750
0.2 ,	120,000	104.000	85,000	73,500	65,800	60,000	52,000
08 "	147,000	127,000	104,000	90,000	80,600	73,500	63,500
0.4 ,,	170,000	147,000	120,000	104,000	93,000	85,000	78,500
0.5 ,,	189,000	165,000	134,000	116,000	104,000	94,500	82,500
0.6 ,,	208,000	180,000	147,000	127,000	114,000	104,000	90,000
0.8 ,,	240,013	208,000	170,000	147.000	132,000	120,000	104,000
1.0 ,,	268,304	232,621	189,000	165,000	147,000	134,000	116,000
1.2 ,,	293,857	254,615	208.072	179,782	160,617	146,928	126,851
1.5 ,,	328,536	284,731	232,621	201,000	180,000	165,000	142,000
1.9	360,385	312,109	254,615	220,666	197,121	179,782	156,054
0.0	379.641	328,536	268,304	232,621	208,000	189,000	165,000
0.5	424,359	367,777	300,245	260,091	232,621	213,000	184,000
3.0 ,,	465,334	402,456	32 8,536	284,731	254,615	232,621	201,000

Diameter of Pipe, 28 Inches.

Length in yards.	1000.	1500.	2000.	2500.	8000.	4000.	5000.
Quantity delivered		Director.				1	10000
with 0.5 in. pressure.	198,000	161,000	140,000	125,000	114,500	99,000	88,600
0.6 "	216,866	176,752	153,362	136,533	124,891	107,956	96,314
0.8 "	249,782	204,271	176,752	157,701	143,942	124,891	111,978
1.0 "	280,000	229,000	198,000	177,000	161,000	140,000	125,000
1.2 ,,	306,724	249,782	216,866	193,687	176,752	153,362	136,533
1.5	342,921	280,000	241,000	216,000	198,000	171,000	158,500
1.8 "	375,626	306,724	265,658	237,081	216,866	187,336	167,227
2.0 ,,	395,841	322,812	280,000	250,000	229,000	198,000	177,200
2.5	442,411	360,914	313,074	280,000	255,000	222,000	198,000
8.0 "	484,747	395,841	342,921	306,724	280,000	241,000	216,000

Diameter of Pipe, 30 Inches.

Length in yards.	1000.	2000.	3000.	4000.	5000.	7500.	10000.
Quantity delivered							
with 0.5 in. pressure.	234,000	166,000	135,000	117,000	105,000	86,000	74,500
0.6	257,580	182,250	148,230	128,790	115,182	94,041	81,405
0.8	296,460	210,195	171,315	148,230	132,435	108,135	94,041
1.0 ,,	332,000	234,000	192,000	166,000	149,000	121,500	105,000
1.2 "	364,500	257,580	210,195	182,250	162,810	132,435	115,182
1.5 ,,	407,025	287,000	234,000	203,000	182,000	149,000	128,500
1.8 "	445,905	315,657	257,580	222,345	199,260	162,810	140,940
2.0 "	470,205	331,695	270,000	234,000	210,000	172,000	149,000
2.5 "	526,095	371,790	303,750	263,000	234,000	192,000	166,000
3.0 ",	575,910	407,025	331,695	287,955	257,000	210,000	182,000
4.0 ,,	664,605	470,205	383,940	331,695	298,000	243,000	210,000

Diameter of Pipe, 36 Inches.

Length in yards.	1000.	2000.	8000.	4000.	5000.	7500.	10000.
Quantity delivered						Contract of the last of the la	
with 0.5 in. pressure.	370,915	262,440	213,451	185,457	165,862	135,419	117,223
0.6	405,907	286,934	234,446	202,953	181,783	148,366	127,720
0.8 ,,	468,892	330,674	271,013	234,446	209,952	171,285	148,366
1.0 ,,	530,000	370,000	303,000	265,000	234,000	192,000	166,000
1.2 ,,	573,868	405,907	330,674	286,934	257,016	209,952	181,783
1.5 "	642,103	456,000	372,000	322,000	288,000	234,900	204,000
1.8 ,,	703,339	496,886	405,907	351,669	314,928	257,016	222,199
2.0 ,,	741,830	524,880	428,000	372,000	332,000	271,000	234,000
2.5	829,310	586,116	477,640	416,000	372,000	303,000	265,000
3.0 ,,	908,042	642,103	524,880	454,546	407,000	332,000	288,000
4.0 "	1,049,760	742,180	605,361	524,880	468,892	384,000	332,000

The foregoing tables are calculated upon the basis of the specific gravity of the gas being ·400. The quantity of gas of any other specific gravity discharged may be ascertained by multiplying the quantity indicated in the table by ·6325 (the square root of ·400), and dividing by the square root of the specific gravity of the other gas.

Example.—If a 12-inch pipe, 1000 yards long, discharges 28,800 cubic feet of gas per hour, specific gravity ·400 at ·5 in. pressure, how much gas will the same pipe discharge, at the same pressure, when the specific gravity is ·560?

$$\frac{28,800 \times 6325}{.7488} = 20,116$$
 cubic feet.—Answer.

The quantity of gas discharged at any other pressure may be ascertained by multiplying the quantity indicated in the table by the square root of the new pressure, and dividing by the square root of the original pressure.

EXAMPLE.—If a quantity of gas equal to 28,855 cubic feet is discharged in one hour at a pressure of 1.2 inches, what quantity will be discharged through the same pipe at 2.2 inches pressure?

$$\frac{28,855 \times 1.4882}{1.0954} = 81,628 \text{ cubic feet.} -Answer.$$

To facilitate these calculations, tables are annexed of the square roots of specific gravities from .850 to .700, rising .005 at a time; and of the square roots of pressures from 1-10th of an inch to 4 inches, rising 1-10th at a time.

TABLE.

Square Root of the Specific Gravity of Gas from .850 to .700.

Specific Gravity.	Square Root.	Specific Gravity.	Square Root.	Specific Gravity.	Square Root.	Specific Gravity.	Square Root.	Specific Gravity.	Square Root.
•350	-5916	•425	·6519	•495	·7085	.565	•7517	.635	•7969
*855	.5958	•430	.6557	.500	·7071	•570	.7549	640	·8000
· 360	·6000	·435	·6595	• 505	·7106	.575	·7583	•645	·8031
·365	·6041	•440	6633	·510	.7141	•580	·7616	.650	*8062
•870	•6083	•445	.6671	•515	.7176	. 585	·7648	•655	·8093
.875	·6124	•450	6708	•520	.7212	-590	· 7681	.660	·8124
.380	·6164	455	·6745	•525	7246	-595	•7718	.665	·8155
-385	6205	•460	6782	-580	·7280	.600	.7746	.670	·8185
.890	6245	• 465	6819	.535	•7814	-605	7778	·675	8216
.395	-6285	•470	6856	•540	·7848	·610	7810	.680	· 8246
·400	6825	•475	6892	.545	·7382	-615	·7842	•685	·8276
405	6364	·480	6928	.550	.7416	.620	·7874	.690	-8306
·410	6408	· 485	-6964	. 555	·7449	.625	7905	.695	·8837
·415	6442	· 490	7000	.560	·7488	.630	7987	.700	-8367
·420	·6481	250	1,000	500	1 200	1 300		, .00	0007
120	0401	1			l i		· 1		

Square Root of Pressures, rising by Tenths of an Inch, from One-Tenth to Four Inches.

Inches and	Square	Inches and	Square	Inches and	Square
Tenths.	Root.	Tenths.	Root.	Tenths.	Root.
1-10th. 2-10ths. 3 " 4 " 5 " 6 " 7 " 8 " 9 " 1 inch. 1 '1-10th. 1 '2-10ths. 1 '3 "	*3162 *4472 *5477 *6824 *7071 *7745 *8366 *8944 *9487 1 0000 1 0488 1 0954 1 1401 1 14892	1·5·10ths. 1·6 " 1·7 " 1·8 " 1·9 " 2 inches. 2·1·10th. 2·2·10ths. 2·3 " 2·4 " 2·5 " 2·6 "	1·2251 1·2649 1·3038 1·3416 1·3784 1·4142 1·4491 1·4832 1·5165 1·5811 1·6123 1·6431	2·8-10ths. 2·9 " 3 inches. 3·1-10th. 3·2-10ths. 3·3 " 3·4 " 3·5 " 3·6 " 3·7 " 3·8 " 3·9 " 4 inches.	1·6733 1·7029 1·7320 1·7606 1·7888 1·8165 1·8439 1·8708 1·8973 1·9235 1·9493 1·9748 2·0000

Should it be required to find the pressure in inches of water to discharge a certain quantity of gas of given specific gravity in an hour, through a pipe the dimensions of which are known, the formula is—

$$h = \frac{Q^2 s l}{(1350)^2 d^5}$$

i.e., multiply the square of the number of cubic feet of gas to be discharged in one hour by the specific gravity of the gas, and by the length of the pipe in yards; divide the product by the square of the constant number 1350, multiplied by the diameter in inches raised to the fifth power, and the quotient is the pressure.

EXAMPLE.—It is required to find the pressure in inches of water to discharge in an hour 12,000 cubic feet of gas, specific gravity 5, through a pipe 8 inches in diameter and 1900 yards long. Then—

$$\frac{Q^2 \times s \times l}{1350^2 \times d^5} = \frac{144,000,000 \times .5 \times 1900}{1,822,500 \times 32,768} \times \frac{136,800,000,000}{59,719,680,000} = \left\{ \begin{array}{c} 2.3 \text{ ins.} \\ \text{nearly.} \end{array} \right.$$

If the diameter of a pipe is required which will discharge a given quantity of gas under a given pressure, we have the formula—

$$d = \sqrt[8]{\frac{Q^2 s l}{(1350)^2 h}}$$

1

This can easily be calculated by a table of logarithms—thus $\log_{10} d = \frac{1}{4} (2 \log_{10} Q_1 + \log_{10} s_2 + \log_{10} l_1 - 2 \log_{10} 1850 + \log_{10} h_1)$

Example.—It is required to find the diameter of a pipe 1240 yards long, to discharge 48,000 cubic feet of gas, of the specific gravity 4, in one hour, with a pressure of 2 inches. Then—

2 log. Q = 2 log. 48,000 . . . = 9.8624824 log.
$$s = log. \cdot 4$$
 = 1.6020600 log. l . = log. 1240 . . . = 8.0984217 $\hline 12.0579641$ 2 log. 1850 = 6.2606676 log. $h = log. \cdot 2 = 0.8010300$ } . = 6.5616976 log. d = 1.0992588 Therefore $d = 18$ inches, nearly.

The following axioms are worth remembering:-

- 1. The discharge of gas will be doubled when the length of the pipe is only one-fourth of any of the lengths given in the tables.
- 2. The discharge of gas will be only one-half when the length of the pipe is four times greater than the lengths given in the tables.
- 8. The discharge of gas will be doubled by the application of four times the pressure.

Handy Rule for finding (approximately) the Content of a Pipe in Gallons and Cubic Feet.

RULE.—Multiply the square of the diameter of the pipe in inches by the length in yards, and divide by 10 for gallons, and by 60 for cubic feet.

Example.—A pipe is 6 in. diameter and 400 yards long, what is the content? then—

$$6^{2} \times 400 \div 10 = 1440$$
 gallons.
 $\div 60 = 240$ cubic feet.

SERVICE-PIPES AND FITTINGS.

In the term Service-pipes are included all pipes branching out of the mains to the consumers' meters, and for the supply of public and

private lamps, &c.

Leakage or unaccounted-for gas is due more to defects in Servicepipes than to all the other causes combined. The leaks are chiefly caused in the pipe by corrosion, or at its junction with the main. Such being the case, it is clear that the utmost care should be devoted to the habilitation and maintenance of this portion of the dis-

tributory plant.

Service-pipes are of cast-iron, wrought-iron, and lead. The use of cast-iron pipes for this purpose is, as a general rule, confined to the supply of gas to large establishments, where the diameter of the pipe exceeds 2 inches. The smaller sizes are too fragile to bear the overhead traffic, and the number of joints is objectionable. Such Services as are of less bore than 3 inches are usually of wrought-iron, or lead.

Wrought-iron pipes or tubes are chiefly employed for Services. They can be obtained of any convenient length, and are easily and

expeditiously fixed.

Wrought-iron tubes and fittings, such as tees, bends, elbows, ferrules, sockets, &c., should be perfectly cylindrical, with no ribs or flat places, and internally as smooth as possible. The welding should be scarcely discernible from the other parts, and the screw should be equally deep throughout the thread.

In laying wrought-iron pipes, the coupling or socket at the end, and which is supplied along with the pipe, should always be removed, the thread painted with red or white lead paint, and then replaced.

Lead pipes have their advantages, though they require more care in laying; and to prevent their sagging in the ground, wood lags

have to be placed underneath them throughout their length.

On the other hand, they can be laid with fewer joints; the only jointing places being the connections with the main and the meter, unless the premises to be supplied are beyond the ordinary distance from the main. When taken up, also, to be renewed, the old metal is of more value than old iron.

All Service-pipes, whether of wrought-iron or lead, when laid in the ground, should be protected from the oxidizing influences of the soil, moisture, and air, by being encased in a \(\sigma\) -shaped or V-shaped channel of wood or other material, filled, after the pipe has been laid therein, with a mixture of hot pitch and tar. This prolongs their life indefinitely, and prevents leakage, and consequently is well worth the trifling extra cost and trouble entailed.

The tinning or galvanizing of the surface of wrought-iron pipes adds greatly to their durability when laid in sandy soil impregnated with saline matter.

The Barff-Bower process of covering iron with a thin layer of oxide to protect it from corrosion, either in the soil or when exposed to the atmosphere, is peculiarly valuable as applied to wrought-iron tubes and fittings, and deserves to be universally adopted.

Mains should be drilled, not cut with a chisel, for the insertion of Service pipes. The full sectional thickness of the metal is thus pre-

served, and the hole is a true circle in form.

Mr. Upward's drilling apparatus secures immunity from leakage in attaching the Service-pipe to the main; and it is easily applied and

All Service-pipes should, if possible, be laid with a slight fall to the main to admit of the condensed moisture draining away thereto. When the pipe is of great length, and a continuous inclination to the main is impracticable, a small drip-well, commonly called a bottle-syphon (Fig. 96 on page 268) should be attached at the lowest point.



Fig. 95.

The Service-cleanser of Messrs. D. Hulett and Co. (Fig. 95) is exceedingly useful for removing water and other obstructions from

Service-pipes.

It is not possible always to see whether a wrought-iron Service-pipe is worn out or not, unless it is taken up out of the ground. The under part of the pipe will often be found completely oxidized, when

the upper surface is sound and good. The rust forms a shell, which crumbles on being disturbed, but when untouched is sufficient to

prevent the immediate escape of gas.

All abrupt angles, such as square elbows, whether in mains, Services, or internal fittings, owing to the resistance they offer to the regular and even flow of the gas, act as condensers, and diminish the available pressure. Their use should, therefore, be discarded wherever practicable; bends or round elbows being much more preferable. For the same reason the internal surface of pipes should be as smooth as

possible. No pipe should be put in use without careful examination. and the removal of all existing roughnesses.

2-inch cast-iron pipes as mains, ‡-inch wrought-iron pipes as Services, and

4-inch lead or composition pipes for internal supply, should be

utterly abandoned.

The first are a grievous source of direct leakage, owing to breakages at their junction with the Service-pipes; the whole three, if used to any great extent, entail high initial pressure, which is synonymous with a heavy leakage account.

If the distance from the main to the meter does not exceed 30 yards, the following sizes of Service-pipes will supply the number of lights named:—

		10		(consuming	say 4 c. ft. p	er hour es	ich)	W	Tu	ht-iron be. inch.
11		30		,,	"	,,			1	22
31	,,			**	**	**			11	"
61				33	"	**			11/2	77
121	"	200	,,	***	11	33			2	"

The above sizes allow for partial contraction of the area of the pipe by corrosion or deposition.

TABLE.

Weight per Foot of Wrought-Iron Tubing For Gas, Water, and Steam.

G	AS.	W	ATER.	STEAM.				
Internal Diameter.	Weight per Foot.	Internal Diameter.	Weight per Foot.	Internal Diameter.	Weight per Foot.			
Inches.	Lbs. Ozs. 0 14½ 1 5½ 1 15 2 10 8 2½ 4 6½ 5 10½	Inches. 1 1 1 1 1 2 2 2 1	Lbs. Ozs. 0 15 1 7½ 2 1 2 14 3 9 4 14 6 4	Inches.	Lbs. Ozs. 0 15½ 1 8 2 3½ 3 4 4 0 5 8 7 0			

TABLE.

Weight of Wrought-Iron Gas Tubes and Fittings.

	i			Tubes	•			ll .		Fitt	ings.		
Size.		eight p 00 feet			Weig 1000	ht per feet.			th of		ht of	Weight of 10 Crosses	
1	Cwts.	100 feet. rts. Qrs. Lbs. 0 1 0			Cwts.	Qrs.	Lbs.	Lbs.	Ozs.	Lbs.	Ozs.	Lbs.	Oss.
i	١ŏ	ĩ	14	0		8	ŏ	ll ī	7	lî	8	i	14
Ĭ	0	2	6	0	ង 5 8	2	4	1	18	2	4	2	8
i	0	8	63	0		0	8 1	2	15	8	0	8	4
2	1	0	221	0	12	0	1	4	6	5	4	5	11
1	1	2	26	0	17	1	8	6	4	7	10	9	2
11 11 12 2 21 21 22	2	1	11	1	3	1	26	10	10	12	15	14	11
11	2 8	8	7	1	8	0	14	15	8	16	7	18	10
12	8	Ō	12	1	11	0	8	15	12	20	0	21	4
2	8	8	21	1	19	1	14	22	6	27	0	81	4
21	4	0	26	2	2	1	8	80	2	82	8	41	4
23	5	0	5	2	10	1	22	46	2	50	15	51	4
27	5	1	19	2	14	Ō	22	55	10	68	8	80	10
8	6	0	20	8	1	8	4	78	8	85	5	88	12
84	7	1	14	8	18	3	0	101	0	121	0	129	0
4	8	2	0	4	5	0	0	126	0	144	0	158	0

TABLE.

Pitch of the Whitworth Taps and Dies for Gas Tubing.

Internal Diameter of Pipe.	External Diameter of Pipe.	Number of Threads per Inch.	Internal Diameter of Pipe.	External Diameter of Pipe.	Number of Threads per Inch.
1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	· 385 · 520 · 665 · 882 1 · 034 1 · 802 1 · 492	28 19 19 14 14 11	2 21 21 21 21 22 22	2·347 2·467 2·587 2·794 8·001 8·124 8·247	11 11 11 11 11 11
12 12 12 16 12 13	1.650 1.745 1.882 2.021 2.047 2.245	11 11 11 11 11 11	21 8 8 81 81 81 4	3·367 3·485 3·698 3·912 4·125 4·339	11 11 11 11 11 11

Uniformity in the screws or threads of Service-pipes and fittings is greatly to be desired, a large proportion of the leakage being due to the want of this. The screwed joint may be too slack, in which

case leakage often follows; on the other hand, when a socket is too small to receive the screwed end of a pipe, instead of running the tap into the one, or the dies over the other, careless workmen are often content to let the joint pass, provided they succeed in getting a single thread to bite. The natural settlement of the ground, the traffic over the surface, or the first keen frost, disjoints the connection and an escape follows.

To Calculate the Required Size of Service-Pipes.

The following table gives the theoretical diameter required for pipes which have to supply a certain number of burners at distances from the street main. The table is calculated by the formula

 $d = \sqrt[3]{\frac{Q^2 s l}{(1850)^2 h}}$ being the same as that used in the determination

of the quantities of gas delivered by large pipes.

As, however, the actual discharge from small pipes is less than the calculated quantity, the tabular number must be increased by one-third if the Service-pipe is of lead, and by one-half if of wrought-iron. When of the latter material, it is not advisable to put in the ground a pipe of less than 3-inch in diameter.

Example of the Manner of Using the Table.—Supposing there are 40 lights to be supplied, at the distance of 70 feet from the main, the tabular number opposite 70 and under 40 is .73540. To this add one-third if a lead service, making .98053, and one-half if a wroughtiron service, making 1.10310. The sizes of pipes next above the numbers are 1 inch and 1½ inch respectively, and these are the sizes required.

Originally Chap's

TABLE

Showing the Diameter of Pipes, in Decimals of an Inch, to Supply Lights at Certain Distances from the Main.

L		s fr	OTE	e of Ma		1	Num	ber of Lig	hts, each a Press	Burni sure o	ng F f One	Five Feet per Hour, with one Inch.			
			'eet	•			8.	5.	10.	15	•	20.	25.	80.	
-5						•	·15457	·18882	·24912	•294	124	- 32876	85946	·88894	
10	•	•	:	•	•	:	17682	·21691	28617	836		87765	41291	•44415	
15	•	•	•	•	•	:	19176	28524	·81084	-866		40956	•44779	·48167	
20	•	•	•	•	•	:	·20311	·24916	·82872	-386		43381	47429	-51019	
8 0	•	•	•	•	•	:	22027	·27020	.85649	•419		•47045	51488	•55329	
40	•	•	•	•	•	:	23331	28620	.87760	•444		49830	-54488	-58605	
50	•	•	•	•	•	:	•24896	29927	39483	•464		·52105	56970	61280	
60	•	•	•	•	:	:	·25802	81024	•40950	•481		·54041	-59086	-68556	
70	•	•	•	•	•	:	·26094	·82010	42281	496		•55788	60986	-65546	
80	•	•	:	•	•	:	26802	·32876	•48875	-519		.57241	62585	67011	
90	•	•	•	•	•	:	27489	·83660	•44408	•529		58606	64077	68925	
100	•	•	:	•	•	:	28028	·84877	45354	-538		-59854	65442	.70898	
150	•	•	•	•	•	:	· 90891	87281	·49185	.570		64909	70970	.76339	
200	•	•	•	•	•	:	·32191	89489	-52098	-619		68758	•75178	-80860	
	•	•	•	•	•	:	88660	•41201	-54476	-640		·71891	78604	84550	
QAA				•	•	•						.74561	81528	·87691	
950 900 ===	:	•	•	_	•	·. —	*84901	42825	•56507	•664					
900				e of		=				Burni	ing F	ive Feet	per Hour,		
900		s fr		Ma		=	Num	nber of Lig	this, each a Press	Burni sure o	ing F	ive Feet	per Hour,	with	
900		s fr	om	Ma		=			hts, each	Burni sure o	ing F	ive Feet			
900		s fr	om	Ma		=	Num	nber of Lig	this, each a Press	Burni sure o	ing F	ive Feet	per Hour, 200.	with 300.	
100 L		s fr	om	Ma		n	Num	aber of Lig	this, each a Press	Burnisure of	ing F f One	live Feet e Inch.	per Hour, 20082581 -94862	with 300.	
5 10 15		s fr	om	Ma			40. -48381 -49882 -54041	50. -47430 -54484 -59086	100 - 625 - 718	Burnisure of	ing F f One	Tive Feet e Inch. 50. 3911 3775 1693	per Hour, 200. -82581 -94862 1.0288	with 300. -97525 1.1157 1.2099	
5 10 15 20		s fr	om	Ma		n .	4048881 -49882 -54041 -57241	50. -47430 -54484 -59086 -62585	this, each a Press	Burnisure of 1	ing F one	Tive Feet e Inch. 50. 3911 3775 1693 7123	200. -82581 -94862 1.0288 1.0897	97528 1 · 1157 1 · 2099 1 · 2815	
5 10 15 20 80		s fr	om	Ma			40. -48881 -49882 -54041 -57241 -62076	50. -47430 -54484 -59086 -62585 -67872	100 - 625 - 718 - 779 - 825 - 896	Burnisure o	ing F f One	Tve Feet e Inch. 50. 9911 9775 1698 7128 533	20082581 -94862 1 0288 1 0897 1 1817	97525 1·1157 1·2099 1·2815 1·3898	
5 10 15 20 80 40		s fr	om	Ma			4048881 -49882 -54041 -57241	50. -47430 -54484 -59086 -62585	this, each a Press	Burnisure o	ing F one	Tve Feet e Inch. 50. 9911 9775 1698 7128 533	20082581 -94862 1-0288 1-0897 1-1817	97525 1 1157 1 2099 1 2815 1 3898 1 4721	
5 10 15 20 80 40 50		s fr	om	Ma			40. -48881 -49882 -54041 -57941 -62076 -65758 -68753	50. -47430 -54484 -59086 -62585 -67872 -71891	100 - 625 - 718 - 779 - 825 - 8948 - 991	Burnisure of the state of the s	1 .73 .83 .99 .1 .00 1 .11 1 .10	71ve Feet e Inch. 50. 3911 3775 1693 7123 553 156 665	200. -82581 -94862 1-0288 1-0897 1-1817 1-2517 1-3089	with 800. -975225 1-1157 1-2099 1-2815 1-3836 1-4721 1-5398	
5 10 15 20 80 40 50 60		s fr	om 'eet	Ma			40. -48881 -49882 -54041 -62076 -65758 -68753 -71907	50. -47430 -54484 -59086 -62585 -67872 -71891 -75173 -77928	100 - 625 - 7718 - 779 - 935 - 948 - 941 1 028	Burnisure o	1 .7899. 1.1.1.1.1.1.1.1.1.1.1.1.1.1.1.	3911 3775 1698 7123 533 156 665 099	20082581 -94862 1-0288 1-0897 1-1817 1-2517 1-3089 1-3674	with 300. -97525 1-1157 1-2096 1-2815 1-3898 1-4721 1-5393 1-5965	
5 10 15 20 80 40 50 60 70		s fr	om 'eet	Ma		- · · · · · · · · · · · · · · · · · · ·	40. -43391 -49882 -54041 -57241 -62076 -65758 -68753 -71307 -73540	50. -47490 -54494 -59086 -62885 -67872 -71891 -75172 -77928	100 - 625 - 718 - 779 - 935 - 948 - 991 1 028	Burnisure o	1 .788 .99 .90 1:10 1:12 1:12 1:12	Tive Feete Inch. 50. 3911 9775 1698 77123 533 156 665 0099 478	200. -82581 -94862 1-0288 1-0897 1-1817 1-2517 1-3069 1-3574 1-3999	900. 97525 1:1157 1:2099 1:2815 1:8998 1:4721 1:5393 1:5965	
5 10 15 20 80 40 50 60 70 80		s fr	om 'eet	Ma			40. -43381 -49832 -54041 -57241 -6276 -65753 -68753 -71307 -78540 -75580	50. 47490 547494 59086 62565 67872 71891 75172 77928 80406 82582	100 - 625 - 718 - 779 - 885 - 991 1 038 1 1 069	Burnisure of the state of the s	1	Tive Feet e Inch. 50. 3911 8775 1693 7123 533 156 665 999 478 874	200. -82581 -94862 1-0288 1-0897 1-1817 1-2517 1-3089 1-3874 1-3999 1-4878	with 800. -97525 1-1157 1-2099 1-2815 1-3898 1-5965 1-6464 1-6910	
5 10 15 20 80 40 50 60 70 80 90		s fr	om 'eet	Ma		· · · · · · · · · · · · · · · · · · ·	40. -49381 -49882 -54041 -62076 -65753 -68753 -71907 -73540 -75580	50. -47490 -54484 -59066 -62565 -67872 -71891 -75172 -77928 -80405 -82582 -84582	100 - 625 - 718 - 779 - 935 - 948 - 991 1 028 1 060 1 089	Burnisure of the state of the s	77. 88. 99. 11. 11. 11. 11. 11. 11. 11. 11. 11	Tive Feet e Inch. 50. 3911 9775 1693 7123 533 156 665 099 478 874	200. -82581 -94862 1-0288 1-0897 1-1817 1-2517 1-3089 1-3574 1-3999 1-4378 1-4721	97522 1·1157 1·2095 1·2815 1·3898 1·4721 1·5985 1·5965 1·6464 1·6910	
5 10 15 20 80 40 50 60 70 80 90		s fr	om 'eet	Ma			40. -43891 -49892 -54041 -57241 -62076 -65753 -68753 -71307 -73540 -75830 -77881 -78978	50. -47490 -54494 -59066 -62585 -67872 -71991 -75172 -77998 -90405 -82582 -84550 -86381	100	Burnisure of the state of the s	1	Tive Feet e Inch. 50. 3911	200. -82581 -94862 1-0288 1-0897 1-1817 1-2517 1-3069 1-3574 1-3999 1-4878 1-4721 1-5035	with 900. 97525 1:1157 1:2099 1:2815 1:5936 1:4721 1:5936 1:6464 1:6910 1:7881	
5 10 15 20 80 40 50 60 70 80 90 100 1150		s fr	om 'eet	Ma			40. -48381 -49882 -54041 -57241 -62076 -65768 -68753 -71307 -73540 -75580 -778976 -78976 -885649	50. 47490 547494 59086 62585 67872 77998 80405 82582 84550 86351 98888	100 - 625 - 718 - 779 - 935 - 948 - 991 1 028 1 1089 1 115 1 139 1 225	Burnisure o	1 · 77 · 88 · 99 · 99 · 1 · 10 · 11 · 11 · 12 · 11 · 12 · 11 · 12 · 11 · 13 · 11 · 14 · 14 · 14 · 14 · 14	Tive Feet e Inch. 50. 3911 9775 1698 7123 533 156 665 974 121 121 400 582	200. -82581 -94862 1.0288 1.0897 1.1817 1.2517 1.3089 1.3574 1.8999 1.4878 1.4721 1.5085 1.6305	with 97525 1 1157 1 2099 1 2815 1 3898 1 5965 1 6464 1 6910 1 7313 1 7681	
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PRICE LIST OF WROUGHT-

			_					
No.	INTERNAL DIAMETER, INCHES.	1 8	1 4	3 8	1/2	34	1	
		s. d.	s. d.	s. d.	s. d.	s. d.	s. d.	
1	Tubes, 2 to 14 feet long, per foot .	0 2	0 24	0 3	0 41	0 6	0 84	
2	Pieces, 12 to 231 inches long, each.	0 4	0 5	0 7	0 9	1 0	1 4	
3	Do. 3 to 111 " " "	0 2	0 8	0 4	0 6	0 8	0 11	1
4	Longscrews, 12 to 231 ,, " .	0 5	0 7	0 9	0 11	1 2	1 6	
5	" 3 to 11½ ", " .	0 4	0 5	0 6	0 8	0 10	1 0	П
6	Bends	0 54	0 61	0 6	0 8	0 11	1 8	
7 8 9	Springs, not Socketed , .	0 1	0 0	0 0	101	0 9	0 11	
10 11	Socket Union (10), Pipe Do. (11) .		2 0	2 6	3 0	4 0	5 6	
12	Elbows, Wrought-Iron	0 6	0 61	0 7	0 8	0 10	1 2	
13	Tees " · · · ·		0 61	0 7	0 9	1 0	1 8	
14	Crosses ,,	0 10	1 0	1 0 0	1 5 0 8	1 9 0 31	2 3	
15	Plain Sockets	0 19	0 19	0 2	0 0	0 02	0 4	
16	Diminished Sockets		0 3	0 4	0 5	0 6	0 7	
17	Flanges	0 8	0 9	0 10	1 0	1 2	1 4	
18 19	Caps (18), Plugs (19)		0 8	0 3	0 4	0 5	0 6	
20 21	Backnuts (20, Nipples (21)	0 1	0 2	0 2	0 3	0 31	0 4	
22	Union Bends	0.2	2 6	3 0 8	3 9	5 0	6 3	
23	Round Elbows, Wrought-Iron	0 7	0 7	0 8	0 8	1 0	1 4	
24	Iron Main Cocks	2 8	2 3	2 9	3 6	4 6	6 6	
25	Do. with Brass Plugs .		44	4 6	5 6		10 6	
26	Round Way Iron Cocks		4.	3 6	4 0	5 6	7 6	
27	Do. with Brass Plugs .	**	**	5 0	6 6		13 0	
28	Cock Spanners, Wrought-Iron		**	1 0	1 4 0 8	1 8 0 10	2 0	
29	Do. Malleable Cast-Iron.	1.5	**	0 7	0 8	0 10	1 2	
30	Syphon Boxes, 1 Quart				11 0	12 0	13 0	
31	Do. 2 ,			- 11			17 0	
32	Do. 3 "						22 0	
33	Do. 4 "						23 0	
34	Malleable Cast Round Elbows	0 6	0 61	0 7	0 8	0 10	1 2	
1		-						

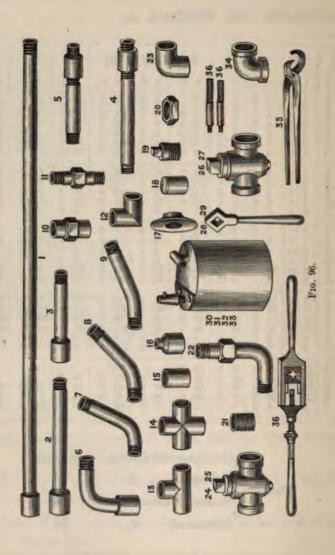
- (35) Tongs or Nippers, (36) Stocks, Dies, and Taps, at prices as quoted by the manufacturer.
- If Tubes are required to be of longer length than 14 feet, they are charged at the next higher rate.
- Tubes of intermediate diameters charged at the price of the next larger size.
- Springs; if socketed, sockets added at list prices.

IRON TUBING AND FITTINGS, &c.

1	ł	1	1	1	2	!	2	2	1	2	1	2	3	;	8	8	1		4
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8	0	8 2 2 8 0	6	4	6	5	3	10	6	16	Ó	21	0	80	0	42	Ō	50	C
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8	6 11	10	0 6	11 3	6 4	18	6 10	16	0 6	19 10	0	22 13	0	25 16	0	30 25	0	. 32	0
	-							- -		-	_	1				1		!	_
8	6 0	11 19	0	14 25	0	18 32	0	27 47	Ŏ	86 60	0	90	0	50 110	0	75 140	0	90 190	0
15 10	ŏ	18	6	17	6	22	ŏ	38	0	54	Ö	62	ŏ	70	0	100	ŏ	160	0
19	0	28	0	36	0	42	0	60	0	85	Ó	105	Ó	120	0	180	0	280	
2	8	8	0	3 2	6 9	4 8	0 8	4	9	6	0	7	6 6	9	0	12 12	0	14	0
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14 18 24	0	15 19	Ŏ	15	6	16 23	0	18 25	0	٠.	٠,		٠,	۱.,٠	٠,		•		
24	ŏ	25	0	21 26	6	28	0	82	0	80 85	0	85 40	0	40 45	0	50	0	56	·o
25	0	25 27	0	29 8	0	31	0	84	0	38	0	42	0	47	0	54	0	60	Ö
1	9	2	8	8	0	3	6	5	6	9	0	12	0	15	0	30	0	40	0

Diggount	Gas tubes and fittings,		per cent.
	Galvanized	do.	do.
	Steam and water	do.	do.
	Galvanized	do.	do.

Iron Cocks over 2 inches at special discounts.



PUBLIC LIGHTING.

The height of a lamp pillar or column (Fig. 98), measured from the surface of the ground to the centre of the flame, should not exceed 10 feet.

A 3-inch or even a 1-inch lead pipe is not suitable for placing in the interior of a lamp column. In cold districts, in winter, the condensed moisture in a pipe of this small bore becomes frozen, filling up the entire length with solid ice in a very short space of time. This is probably due to the wavy irregularities in the pipe preventing the water from draining rapidly away.

Galvanized wrought-iron pipe is best for lamp columns, and for placing against a wall for the supply of a bracket lamp; and ½-inch is the smallest size that should be used. In situations exposed to cutting winds, and where the frost is keen, ¾-inch wrought-iron pipes

are best.

If the service-pipe at the entrance to the base of a lamp column has not very ample fall to the main, the water of condensation, unable to drain quickly away, will inevitably be frozen at that point during frost, and, by accretion, will eventually interrupt the passage of the gas.

It is not unusual to find one-half the public lights in some districts extinguished at night when a severe frost prevails. This is simply due to mismanagement, as it would not occur if attention were paid

to the matters indicated above.

Seventy yards is the maximum distance apart at which public

lamps should be placed.

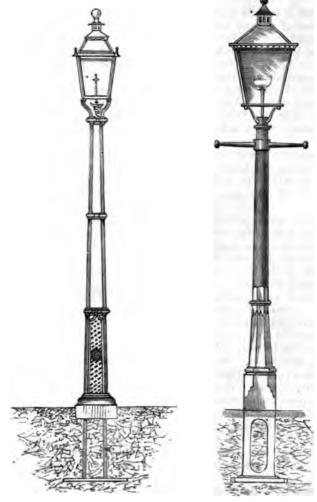
A new and entirely novel form of Lamp Post (Fig. 97), has been introduced by J. and J. Braddock. It consists of four 1-inch wrought-iron tubes, held together at three points, in addition to the base, by cast-iron binders, one of the tubes being used as the service-pipe for conveying the gas to the burner. Panels may be fixed at the foot, or it can be left open, as desired. No ladder-arm is required, as the tubes, on any side, form a square support for a ladder to rest against. The tubes are continued down through the visible base, and are screwed into a cast-iron plate underground. Altogether, the post has a neat appearance, and, owing to its lightness—under 2 cwt.—and the ease with which it can be taken to pieces and set up again, it is specially adapted for export.

The ordinary four-sided lamp is the most serviceable for general use. It is 14 inches square at the widest part, and made of tinned

copper.

The street lamps designed by Mr. Sugg (Fig. 99) and Mr. Bray (Figs. 100 and 101), with clusters of flat-flame burners, and the lamp

and regenerative burner of Herr F. Siemens (Fig. 102) have much improved the lighting of streets and squares wherever they have been introduced; and have proved, at the same time, that efficient



F10. 97.

F16. 98.

street illumination by means of gas is perfectly attainable where there is a willingness on the part of towns' authorities to incur the expense.

The earlier street lamps were constructed with opaque reflecting tops, and the glazed tops were afterwards introduced as an improve-



Fig. 99.



Fig. 100.

ment. When the whole of the light is reflected downwards, the fronts of the houses, except for a short space above the height of the lamp column, are placed in a state of utter darkness, and to passengers



Fig. 101.



Fig. 102.

walking along the streets the gloomy canopy overhead, rendered all the more sombre and distressing from the concentrated light underneath, has an unearthly and depressing effect. On the other hand, where the main thoroughfares of a large town are lighted with the capacious lamps recently introduced, with semi-transparent crowns, admitting of the radiation of a portion of the light on the house fronts, the perfection of street lighting is attained as near

as possible.

The square at the bottom of a lamp is generally in two or three parts, one of them being hinged on the outer edge, for raising when the lamp is being lighted by the pole. It is a common occurrence to find a portion of the bottom missing altogether, and the flame, thus exposed to the action of the wind, is in a state of constant oscillation, whereby much of the illuminating power of the gas is sacrificed.

The supply of gas to public lamps is usually fixed at 5 cubic feet per hour for common gas up to 17 candles value; for cannel gas up to 30 candles value, the supply per hour varies from 3 to 4 cubic

feet.

Satisfactory public lighting, as between gas companies and local authorities, is best secured by the adoption of a good average meter system, and the application of a regulator to every lamp.

Weight and Thickness of Glass for Public Lamps, &c.

No. of the or Weight in (Dur	ices	De	Thickness in ccimals of an Inch.	No. of the or Weight in o	Oun	ces	Thickness in Decimals of an Inch		
12				.059	21				·100	
13				.063	24				1111	
15				.071	26				·125	
16				.077	32				154	
17				.083	36				·167	
19				· 0 91	42		-		.200	

Rule to find the Length of Day and Night.

Day.—The hour of sunset, doubled, is the length of the day. Night.—The hour of sunrise, doubled, is the length of the night.

The Moon's Rising and Setting.

At	4	days	old,	the	Moon	sets	about	10	o'clock	at	night.
At		11	99		**		**	11	**		11
At		**	**		11		22	12))
At		. "	11		11		"	1			the morning.
At			99	the	Moon	rises	11	6		in	the evening.
At			27		- 11		22	7			11
At			11		22		23	8	, ,,	7	9.
At			**		91		11	10	2)	at	night.
At			71		25		22	11	31		11
At	2) ,,	**		33		71	12	11		**

TABLE

Showing the Consumption of Gas by One Burner per Month, and for the Twelve Months, during the Average

Hours of Burning from Sunset throughout the Year.

	.tesung 1	amoH lo	Hours of	Con	sumption Lamps	of Gas by	Consumption of Gas by One Burner per Month, and for the whole Year. Lamps assumed to be Lighted from Sunset to Surrise, and Private from Sunset until Nine o'Clock.	er per Mo sed from S tunset unt	Burner per Month, and for the Lighted from Sunset to Sunri from Sunset until Nine o'Clock	or the who sunrise, an	d Private	Public Street Lamps	reet
Month.	emiT ez	Duration of Burni		3 Cub	8 Cubic Feet per Hour.	St Cubic Fe per Hour.	St Cubic Feet per Hour.	4 Cubi	Cubic Feet per Hour.	44 Cubic Feet per Hour.	four.	5 Cubi	5 Cubic Feet per Hour.
	Avere	Мевп	dmnN giN	Public Lamps.	Private Lamps.	Public Lamps.	Private Lamps.	Public Lamps.	Private Lamps.	Public Lamps.	Private Lamps.	Public Lamps.	Private Lamps.
	Б. т.	р, ш.	p.	c. ft.	c. ft.	c. ft.	c. ft.	o. ft.	o. ft.	o. ft.	o. ft.	c. ft.	c. ft.
January.	4 13	16 31	512	1536	445	1792	619	2048	594	2304	899	2560	742
February	2 9	14 41	411	1233	326	1438	380	1644	436	1850	490	2055	544
March .	9 9	12 19	385	1146	270	1337	315	1528	360	1719	405	1910	450
April .	9		295	885	185	1032	216	1180	246	1327	277	1475	308
Mav .	7		242	726	115	847	134	896	154	1089	173	1210	191
June .	8 16	6 30	195	585		683	:	780		878	:	975	:
July .	20		217	651	:	260	.,	898	:	976	:	1085	:
Angust .	1		307	921	162	1074	190	1228	216	1382	242	1535	268
September	9		345	1035	240	1207	280	1380	320	1662	360	1425	400
October .	1.7		421	1263	840	1474	396	1684	453	1895	609	2105	566
November	4 25	15 46	473	1419	413	1655	481	1892	220	9128	619	2665	688
December	3 49		527	1581	483	1845	564	2108	644	2372	725	2635	803
Total for	:	:	4327	18,981	2379	15,144	8475	17,308	8973	19,472	4468	21,635	4960

LABLE

Showing the Number of Hours during which Gas is usually Burned in each Month, Quarter, and Year, according to the Times of Lighting and Extinguishing.

	•1	Total of Year	27 49 76 107 1144 1180 217 432	5489
		Ohristmas.	173 265 857 449 641 633 725 1421	327 235 143 64
		Michaelmas.	869 850 850 869 869	18 ::
1		Midsummer.	32 95 277 368 732	8e ::
		Lady-Day.	102 188 278 368 458 548 638 1305	306 216 126 58
	9.	December.	80 1111 142 173 204 235 266 527	187 106 75 44
	Christmas Quarter.	Мочетьет.	62 92 152 162 182 242 473	9888
	0	October,	81 62 93 124 155 186 217 421	80 49 18:
	ins .	September.	22 52 52 82 111 142 172 845	88 ::
	Michaelmas Quarter.	August.	14 40 71 102 1133 1164 307	9:::
	M	July.	::: 133 44 75 106 217	::::
	er	Jane.	:::8 88 88 88 88 195	1111
	Midsummer Quarter.	May.	:: 4 29 60 60 60 842 842 842 842 842 842 842 842 842 842	64 : : :
	M	April.	28 88 88 1148 148 295 295 295 295 295 295 295 295 295 295	88 ::
	b.	Maroh.	4 31 62 93 124 165 186 382	104 :
	Lady-Day Quarter.	February,	88 61 89 117 145 173 201 411	98 14 14 14 14 14
	Н	January.	65 96 127 158 189 220 220 251 512	137 106 75 44
-		Times of Ligning and Extinguishing.	If lighted at dusk and extinguished at— 6 p.m. 7 " 8 " 10 " 11 " 12 " All night	4a.m.tilld'ylight

* A deduction of one-sixth may be made for moonlight nights; and in the case of private lamps not being lighted on Sundays, deduct one-seventh.

CONSUMERS' GAS METERS.

Gas Meters are either "Wet" or "Dry."

The wet Meter has a measuring wheel or drum enclosed in an iron case charged with water up to a certain level, called the "waterline." The drum is divided into compartments similar to the station Meter; and the measurement and indication, or registration, of the gas

passing through it are performed in the same manner.

The dry Meter has usually a case of tinned iron. This is divided into compartments by a central partition and two or more movable diaphragms with prepared flexible leather sides. The gas enters and leaves these compartments alternately through valves whose passages are made to open and close at the proper moment. The alternate expansion and contraction of the inner and outer spaces (after the manner of the ordinary bellows), by the pressure of the gas exerted on the surfaces of the diaphragms, are communicated by levers and cranks to the wheelwork of the indicators, which are alike in both classes of Meter.

Meters, as tested under the provisions of the "Sales of Gas Act, 1859," are stamped as correct by the Inspector when their registration does not vary from the true standard measure of gas more than 2 per cent. in favour of the seller, and 3 per cent. in favour of the consumer.

Added together, the range is 5 per cent.

"Compensating" Meters were introduced to overcome the difficulty caused by the limitation in the range of the water level of wet Meters.

Most of these have a reservoir of water within the case distinct from the water in which the measuring wheel revolves; and various automatic expedients are adopted for transferring this water, as long as it lasts, to the body of the Meter, to compensate for the diminution of

water therein by evaporation or otherwise.

The action of the Warner and Cowan measuring wheel is independent of the water-line; the compensation in this instance being effected by a second and smaller wheel contained within, and revolving with, the larger one, but having its partitions arranged in the opposite direction. When a depression occurs in the water-line of a Meter from any cause, a volume of gas in excess of the true quantity is passed; but in this instance the excess in volume of the gas is returned by the small wheel to the Meter inlet to be remeasured.

The Sanders and Donovan Meter is provided with a compensating hollow float of metal plate, accurately balanced on pivots within the front portion of the case, and independent of the Meter's action. As the water is added to or withdrawn, the float rises or sinks in propor-

tion, and thus the correct level is maintained.

When the drum or measuring wheel of a Meter is driven at a speed exceeding 120 revolutions per hour (except 2 and 3 lights, when it may have a speed of 144), it absorbs an undue amount of the available gas pressure, and its registration is falsified. It is important, therefore, to see that all Meters fixed are adequate to the supply of the greatest number of lights in use at one time on the premises of the consumer.

Mr. Urquhart's "Reliance" Meter and Mr. Hunt's Meter, both of which are on the compensating principle, though different in character, are exceptions to the rule above stated, as they measure correctly even when the measuring wheel is caused to revolve at speeds in excess of the normal rate. This result is obtained by a reverse action, by which the gas enters through passages in the valve chamber in the body of the Meter, and thence into the drum, from which it makes its escape through the bent tube to the outlet. The inlet pressure thus bears upon nearly the whole surface of the contained water, and the measuring chambers are practically unaltered in capacity.

It need scarcely be pointed out, however, that anything like a general resort to the practice of allowing the use of Meters too small for the consumption except at extraordinary pressures, is a serious evil in various ways—loss by leakage is increased; the illuminating power of the gas is practically reduced; and consumers, whose Meters and

fittings are adequate, suffer by the prevailing high pressure.

One-light Meters, which formerly were extensively employed, are now altogether inadmissible; and even two-light Meters should only be sparingly used. The low price at which gas is sold encourages its extended consumption; and the houses are becoming fewer in number every day where this small size is sufficient to afford an adequate supply at reasonable pressures, to the quantity of lights in regular use.

The regular periodical inspection of Meters is a point of the utmost importance, and ought never to be neglected. The indices of Meters in dwelling-houses, &c., should be noted, and water supplied to the proper level wherever deficient, at least once every six weeks. The Meters in mills, manufactories, and large establishments of every kind where the consumption of gas is heavy, should be inspected for the like purpose once every 14 days.

The Inspector should always be provided with a supply of leather washers for the different screws and plugs, to replace any that are

worn out.

Meters in cold and exposed positions should be protected by a suitable covering during frost, to prevent interruption to the supply of gas by the water becoming frozen. Woollen rags or wrappings of any kind will answer the purpose.

The Motive Power Meter is but rarely required; but it is exceedingly



Fig. 103. weight aforementioned. in Fig. 103.

useful in certain positions, where the pressure, from some unavoidable cause, is insufficient to afford an adequate supply of gas. In construction it is like an ordinary Meter, but instead of the gas pressure being the motive power, the gas is exhausted from the main by the measuring wheel. This is set in motion by a descending weight, attached to which is a cord wound on a drum revolving in bearings on the top of the Meter case, the drum being geared to the shaft of measuring wheel, which through the back of the case. The speed of the Meter, and consequently the pressure of gas obtained, are regulated by the Parkinson's Motive Power Meter is shown

The "Prepayment Gas-Meter" recently introduced, and of which there are already several different forms, is an ingenious device for extending the sale of gas amongst small consumers. By the addition of a simple mechanism contained in a small box attached to the ordinary wet or dry meter, and on dropping a penny through a slot therein, a quantity of gas of the value of the penny is allowed to pass to the burner. When the gas thus paid for is consumed, the supply ceases until another prepayment is made.

By another arrangement, on prepayment of a given sum—say 4d. for 100 cubic feet—an extra dial on the meter is set to pass the quantity of gas; and when this is consumed, a valve shuts off the supply, unless, in the meantime, a further payment has been made, and the dial is reset.

Testing Meters.

For the verification of gas Meters by a public Inspector under the "Sales of Gas Act," a somewhat elaborate set of apparatus is required.

For ordinary use in testing Meters in a gas works, the following may be provided (see Fig. 104):—A standard gasholder of 10 cubic feet capacity. A proving bench. An overhead water cistern. A float of lights, and thermometers for taking the temperature of the air and water.

In testing, it is important to secure uniformity in the temperature of the air or gas in the test holder, the water in the tank, and the air in the room—viz., 60° Fahr.; otherwise corrections for varying temperature have to be made.

Place the Meter to be tested on the proving bench, charge it with water to the proper water-line (if a wet Meter), and connect it with the holder and to the float of lights (if gas is being used).

See that the pointer of the small metal drum above the index in the wet Meter, or of the small circle on the index plate of the dry Meter, coincides with one of the figures marked thereon. If it does not, pass a small quantity of gas through till the necessary adjustment is effected.

Next, fill up the test holder till the 0 line of the scale upon it is

exactly opposite its pointer.

This being done, turn the gas or air on to the Meter, and allow the Meter to work till the small metal drum has made one or more revolu-

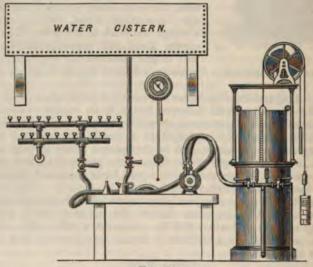


Fig. 104.

tions, taking care to close the stop-cock when the pointer of the drum

is exactly over the figure from which the start was made.

The Meter registration is then compared with that of the holder scale. If they correspond, the Meter is exactly correct; but if the scale on the holder indicates less or more than the small drum on the Meter, the percentage of error is calculated; or it can be ascertained on reference to the Table.

The percentage Tables on the following pages are taken from those issued by the Metropolitan Board of Works for the use of their Meter

Inspectors.

TABLES

Showing the Percentage of Error in Meters according as their Registration differs from the Indications of the Test Gasholders.

The sign + is used to indicate fast, and - to indicate slow.

Meters not exceeding 2 per cent. fast, or 3 per cent. slow, are correct within the meaning of the "Sales of Gas Act."

	egistering oot.	Meter R	egistering eet.	Meter R	egistering Feet.		egistering Feet.
Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder,	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.
Foot. 0'90 '91 '92 '93 '94 '95 '96 '97 '98 '99 1'00 '01 '02 '03 '04 '05 '06 '07 '08 '09 1'10 '11 '12	Per Cent. + 11 · 11 + 9 · 89 + 8 · 70 + 7 · 25 + 6 · 36 + 5 · 26 + 4 · 17 + 3 · 09 + 2 · 04 + 1 · 01 Nil. - 1 · 97 - 2 · 92 - 4 · 74 - 5 · 66 - 6 · 54 - 7 · 40 - 8 · 26 - 9 · 10 - 9 · 91 - 10 · 07	Feet. 1 '80 '81 '82 '83 '84 '85 '86 '87 '88 '89 1 '90 '91 '92 '93 '94 '95 '96 '97 '98 '99 2 '00 '01 '02 '03 '04 '05 '06 '07 '08 '09 2 '10 '11 '12 '13 '14 '15 '16 '17	Per Cent. + 11·11 + 10·50 + 9·89 + 8·11 + 7·53 + 6·95 + 6·95 + 5·82 + 5·82 + 5·26 + 2·04 + 1·52 + 1·	Feet. 2:70 -71 -72 -73 -74 -75 -76 -77 -78 -79 2:80 -81 -82 -83 -84 -85 -86 -87 -88 -89 2:90 -91 -92 -93 -94 -95 -96 -97 -98 -90 -91 -92 -93 -94 -95 -96 -97 -98 -90 -91 -92 -93 -94 -95 -96 -97 -98 -99 -90 -91 -92 -93 -94 -95 -96 -97 -98 -99 -90 -91 -92 -93 -94 -95 -96 -97 -98 -99 -90 -90 -90 -90 -90 -90 -90 -90 -90	Per Cent. + 11·11 + 10·70 + 9·89 + 9·49·90 + 8·70 + 8·70 + 7·53 + 7·14 + 6·76 + 6·38 + 6·76 + 6·38 + 6·16 + 4·53 + 4·17 + 3·81 + 3·81 + 2·74 + 1·69 + 2·39 + 1·69 - 0·38 - 0·38 - 0·38 - 0·39 - 1·32 - 1·64 - 2·28 - 2·91	Feet. 3:10 -11 -12 -13 -14 -15 -16 -17 -18 -19 3:20 -21 -22 -23 -24 -25 -26 -27 -28 -29 3:30 -31 -32 -33 -34	Per Cent. - 3 * 22 - 3 * 54 - 4 * 16 - 4 * 16 - 5 * 06 - 5 * 66 - 5 * 85 - 6 * 25 - 6 * 24 - 7 * 12 - 7 * 70 - 7 * 79 - 8 * 82 - 8 * 84 - 8 * 82 - 9 * 94 - 9 * 91 - 10 * 18

Meter R	egistering eet.	Meter R 5 F	egistering eet.		egistering eet.	Meter R	egistering Feet.
Reading of Scale of Gas- holder,	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.
Feet.	Per Cent.	Feet.	Per Cent.	Feet.	Per Cent.	Feet.	Per Cent
4.20	+ 11.11	5.02	- 0.40	5.24	- 9.75	9.00	+ 11.1
'51	+ 10.86	-03	- 0.60	*55	- 9.91	.01	+ 10-95
*52	+ 10.62	.04	- 0.79	*56	- 10.07	.02	+ 10.86
*58	+ 10.38	.05	- 0.99	*57	- 10.23	-03	+ 10.7
*54	+ 10.13	.06	- 1.19	-58	- 10.39	-04	+ 10.6
.55	+ 9.89	-07	- 1.33	.20	- 10.55	.05	
*56	+ 9.65	-08	- 1.57	5.60	- 10.71		+ 10.5
•57	+ 9.41	-09	- 1.77			*06	+ 10.3
-58	+ 9.17	5.10	- 1.96	:61	- 10.87	-07	+ 10.2
*59		-11		*62	- 11.03	-08	+ 10-1
4.60			- 2.15	.63	- 11.19	-09	+ 10.0
		•12	- 2.34			9.10	+ 9.8
'61	+ 8.46	.13	- 2.53			-11	+ 9.7
.62	+ 8.23	14	- 2.72			-12	+ 9.6
.68	+ 7.99	-15	- 2.91		1 1	•13	+ 9.5
*64	+ 7.76	.16	- 3.10			.14	+ 9-4
*65	+ 7.53	.17	- 8.29	D 1		-15	+ 9.2
*66	+ 7.30	-18	- 3.47		i	-16	+ 9-1
*67	+ 7.07	*19	- 3.66	U		-17	+ 9.0
.68	+ 6.84	5.20	- 3.85	KI D		-18	+ 8.9
•69	+ 6.61	-21	- 4.03	V		-19	+ 8.8
4.70	+ 6.38	.22	- 4.21	II - X		9.20	+ 8.7
.71	+ 6.16	•23	- 4.40			.21	+ 8-5
.72	+ 5.93	-24	- 4.58	1		-22	+ 8-4
.78	+ 5.71	.25	- 4.76			.23	+ 8.3
.74	+ 5.49	•26	- 4.94			-24	+ 8.2
.75	+ 5.26	.27	- 5.12			+25	+ 8-1
.76	+ 5.04	.28	- 5.30			.26	+ 7.9
.77	+ 4.82	•29	- 5.48			-27	+ 7.8
-78	+ 4.60	5.30	- 5.66			-28	+ 7.7
•79	+ 4.38	-31	- 5.84			-29	+ 7.6
4.80	+ 4.17	-32	- 6.02		1	9.30	+ 7.5
-81	+ 3.95	.33	- 6.19			.31	+ 7.4
*82	+ 8.78	.34	- 6.37	1		-82	+ 7.9
.83	+ 3.52	*35	- 6.54			-33	+ 7.1
*84	+ 3.31	•36	- 6.72			-34	+ 7.0
185	+ 8.09	-37	- 6.89			•35	+ 6.9
-86	+ 2.88	•38	- 7.06			-36	
*87	+ 2.67	-39	- 7.24			-37	
*88	+ 2.46	5.40	- 7.41			-88	
*89	+ 2.25	.41	- 7.58			.39	
4.90	+ 2.04	.42	- 7.75			9.40	
.91	+ 1.83	.43	- 7.92		V /	•41	+ 6.8
.92	+ 1.63	.44	- 8.09			.42	
-93	+ 1.42	.45	- 8.26		V 1	•43	
•94	+ 1.21	.46	- 8.42			-44	+ 6.0
•95	+ 1.01	-47	- 8.59				+ 5.9
.96	+ 0.81	48	- 8.76			45	+ 5.8
-97	+ 0.60	.49	- 8.93			*46	+ 5.7
-98	+ 0.40	5.20	- 8.09			:47	+ 5.6
-99	+ 0.50	5.50	- 9.09			.48	+ 5.4
5.00	Nil.					-49	+ 5.8
.01	- 0:20	·52 -53	- 9.42			9.50	+ 5.2
W.A.	0.20	00	- 9.59			.51	+ 5.1

	egistering Feet.		egistering Feet.	Meter R	egistering Feet.		egisterin Feet.
Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amoun of Error.
Feet.	Per Cent.	Feet.	Per Cent.	Feet.	Per Cent.	Feet.	Per Cen
9·52 ·53	+ 5.04	10·04 ·05	- 0·40 - 0·50	10·56 •57	- 5·39	11.08	- 9·7 - 9·8
•54	+ 4.82	-06	- 0.60	.58	- 5·48	11.10	- 9·9
.55	+ 4.71	.07	- 0.70	.59	- 5.57	-11	- 9·9
.26	+ 4.60	.08	- 0.79	10.60	- 5.66	.12	- 10.0
·57 ·58	+ 4·49 + 4·88	10·10	- 0.89 - 0.89	:61	- 5·75 - 5·84	·13 ·14	- 10·1
. 59	+ 4·38 + 4·28	10 10	- 1·09	·62 ·63	- 5.93	15	- 10·2 - 10·8
9.60	+ 4.17	.12	- 1.19	·64	- 6.02	.16	- 10.8
•61	+ 4.08	·13	- 1.28	·65	- 6.10	•17	- 10.4
.62	+ 3.95	14	- 1.88	.66	- 6.19	.18	- 10·E
·63 ·64	+ 8·84 + 8·78	·15 ·16	- 1·48 - 1·57	·67 ·68	- 6·28 - 6·37	·19 11·20	- 10·6
-65	+ 3 63	.17	- 1.67	.69	- 6.45	11.20	- 10.7
•66	+ 8.2	•18	- 1.77	10.70	- 6.24	.22	- 10.8
•67	+ 8.41	.19	- 1.86	.71	- 6.63	.23	- 10.5
· 6 8	+ 8·81 + 8·20	10.20	- 1.96	.72	- 6.72	.24	- 11:0
•69 9·70	+ 8.09	·21 ·22	- 2·06 - 2·15	·73	- 6.89 - 6.89	•25	- 11.1
.71	+ 2.99	.23	- 2.25	•75	- 6.98	i	
.72	+ 2.88	.24	- 2.34	.76	- 7.06		
•78	+ 2.77	•25	- 2.44	.77	- 7.15		l
·74 ·75	+ 2·67 + 2·56	·26 ·27	- 2·53 - 2·63	·78 ·79	- 7·24 - 7·32		
•76	+ 2.56 + 2.46	-28	- 2.72	10.80	-7.41		
.77	+ 2.35	.29	- 2.82	-81	- 7.49		
•78	+ 2.25	10.30	- 2.91	' .82	- 7.58		
.79	+ 2.15	·31 ·32	- 3·01 - 8·10	.83	- 7.66		
9·80 ·81	$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	•33	- 3·10 - 3·19	·84 ·85	- 7·75 - 7·83		İ
-82	+ 1.88	•34	- 3.29	.86	- 7·92	ł	
.83	+ 1.78	•35	- 3.38	·87	- 8.00		
·84	+ 1.63	.36	- 8.47	.88	- 8.09	ļ	
·85 ·86	+ 1.42	·37 ·38	- 3·57 - 3·66	·89	- 8·17 - 8·26		
·87	+ 1.82	.39	- 3.75	.91	- 8·34		
.88	+ 1.21	10.40	- 3.85	.92	- 8.42	ĺ	
.89	+ 1.11	•41	- 8.94	.93	- 8.51		l
9.90	+ 1.01	•42	- 4.03	.94	- 8:59		i
·91 ·92	+ 0.81 + 0.81	·43 ·44	- 4·12 - 4·21	·96	- 8·68 - 8·76		1
.98	+ 0·70	•45	- 4·31	.97	- 8.84		!
•94	+ 0.60	•46	- 4.40	•98	- 8.93		
.95	+ 0.50	:47	- 4.49	.99	- 9.01		1
•96 •97	+ 0·40 + 0·30	·48 •49	- 4·58 - 4·67	11·00 ·01	- 9·09 - 9·18		1
-98	+ 0.30	10.20	- 4·76	.02	- 9·16 - 9·26	<u> </u>	
.99	+ 0.10	.51	- 4·85	.03	- 9.34	li	1
10:00	Nil.	.52	- 4.94	.04	- 9.42		
•01	- 0.10	:53	- 5:03	:05	- 9.51		1
·02 ·08	- 0·20 - 0·80	·54 ·55	- 5·12 - 5·21	·06 ·07	- 9·59 - 9·67	ll	

	egistering Feet.		egistering Feet.		egistering Feet.		egistering Feet.
Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.
Feet.	Per Cent.	Feet.	Per Cent.	Feet.	Per Cent.	Feet.	Per Cent
18.00	+ 11.11	18.52	+ 7.99	19.04	+ 5.04	19.56	+ 2.2
.01	+ 11.05	.28	+ 7.93	•05	+ 4.98	.57	+ 2.20
.02	+ 10.99	*54	+ 7.87	*06	+ 4.93	-58	+ 2.1
-03	+ 10.92	155	+ 7.82	107	+ 4.87	.69	+ 2.0
.04	+ 10.86	·56 ·57	+ 7.70	*08	+ 4.82	19.60	+ 2.0
.05	+ 10.80	*58		19.10	+ 4.76	61	+ 1.9
·06	+ 10.4	.59	+ 7.64	19 10	+ 4.65	63	+ 1.9
.08	+ 10.62	18.60	+ 7.53	.12	+ 4.65	-64	+ 1.8
•09	+ 10.2	.61	+ 7.47	•13	+ 4.54	.65	+ 1.8
18.10	+ 10.50	-62	+ 7.41	•14	+ 4.49	.66	+ 1.7
•11	+ 10.44	-63	+ 7.36	15	+ 4.43	-67	+ 1.6
.12	+ 10.38	*64	+ 7.80	•16	+ 4.88	. 68	+ 1.6
•13	+ 10.31	.65	+ 7.24	17	+ 4.33	*69	+ 1.5
-14	+ 10.25	-66	+ 7.18	•18	+ 4.28	19.70	+ 1.5
.15	+ 10.19	-67	+ 7.13	.19	+ 4.22	.71	+ 1.4
.16	+ 10.13	•68	+ 7.07	19.20	+ 4.17	.72	+ 1.4
-17	+ 10.07	-69	+ 7.01	.21	+ 4.11	.78	+ 1.8
-18	+ 10.01	18.70	+ 6.95	*22	+ 4.06	.74	+ 1.8
19	+ 9.95	'71	+ 6.90	.23	+ 4.00	.75	+ 1.5
18.20	+ 9.83	·72 ·73	+ 6.84	24	+ 8.95	176	+ 1.2
-22	+ 9.83	.74	+ 6.72	-26	+ 3.89	77	+ 1.1
-23	+ 9.71	.75	+ 6.66	27	+ 3.78	-79	+ 1.0
.24	+ 9.65	.76	+ 6.61	-28	+ 3.73	19.80	+ 1.0
.25	+ 9.59	.77	+ 6.55	-29	+ 3.68	.81	+ 0.8
.26	+ 9.53	-78	+ 6.50	19.80	+ 3.63	-82	+ 0.8
.27	+ 9.47	.79	+ 6.44	.31	+ 3.57	.83	+ 0.8
.28	+ 9.41	18.80	+ 6.38	-32	+ 3.52	*84	+ 0.8
• 29	+ 9.35	.81	+ 6.32	'83	+ 3.46	85	+ 0.2
18:30	+ 9.29	*82	+ 6.27	*34	+ 3.41	.86	+ 0.3
·31	+ 9.23	*83	+ 6.16	·35 ·36	+ 3.36	.87	+ 0.6
-33	+ 9.11	85	+ 6.10	-87	+ 3.31	. *88	
- 34	+ 9.05	186	+ 6.04	+38	+ 3.25	19.90	+ 0.6
*35	+ 8.99	-87	+ 5.98	.39	+ 3.14	-91	+ 0.4
-86	+ 8.93	*88	+ 5.98	19.40	+ 3.09	-92	+ 0
*37	+ 8.87	.89	+ 5.87	•41	+ 3.04	-93	+ 0.8
98	+ 8.81	18.90	+ 5.82	•42	+ 2.99	-94	+ 0.1
29	+ 8.76	.91	+ 5.76	*43	+ 2.93	-95	+ 0.5
18.40	+ 8.70	•92	+ 5.71	*44	+ 2.88	-96	+ 0.8
*41	+ 8.64	.93	+ 5.65	45	+ 2.82	.97	+ 0.
·42 ·43	+ 8.58	94	+ 5.60	'46 '47	+ 2.77	-98	+ 0.
444	+ 8.46	96	+ 5.49	48	+ 2.72	20.00	+ O·
.45	+ 8.40	+97	+ 5.43	-49	+ 2.61	02	- O.
•46	+ 8.34	-98	+ 5.87	19.50	+ 2.56	*04	- 0.
•47	+ 8-29	-99	+ 5.31	.51	+ 2.51	•06	- 0.
*48	+ 8.23	19.00	+ 5.26	.62	+ 2.46	.08	- 0.
•49	+ 8.17	.01	+ 5.20	.58	+ 2.40	20.10	- 0.
18.50	+ 8.11	.02	+ 5.15	*54	+ 2.35	•12	- 0.
.51	+ 8.05	.03	+ 5.09	*55	+ 2.30	-14	- 0.

	egistering Feet.		egistering Feet.		egistering Feet.		egistering Feet.
Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder,	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.
Feet. 20·16 18 20·20 22 24 26 28 20·30 32 34 46 46 46 46 46 46 46 46 66 62 64 66 62 64 66 68 20·70 72 74 76 78 20·80 82 84 88 20·90 92 94 96 98 21·00 02 04 06 08 21·10 12 14 16 18	Per Cent. — 0 · 79	Feet. 21 · 20 · 22 · 24 · 26 · 28 21 · 80 · 32 · 34 · 36 · 38 21 · 40 · 44 · 46 · 56 · 58 21 · 60 · 52 · 54 · 56 · 68 21 · 70 · 72 · 74 · 76 · 78 21 · 80 · 82 · 84 · 86 · 88 21 · 90 · 92 · 94 · 96 · 98 22 · 00 · 02 · 14 · 16 · 18 22 · 20 · 12 · 14 · 16 · 18 22 · 20	Per Cent. - 5 *66 - 5 *75 - 5 *84 - 5 *98 - 6 *02 - 6 *10 - 6 *19 - 6 *28 - 6 *63 - 6 *63 - 6 *63 - 6 *63 - 6 *72 - 6 *89 - 7 *06 - 7 *15 - 7 *24 - 7 *32 - 7 *41 - 7 *32 - 7 *49 - 7 *56 - 7 *75 - 7 *83 - 8 *00 - 8 *09 - 8 *17 - 8 *26 - 8 *34 - 8 *42 - 8 *42 - 8 *42 - 8 *48 - 8 *69 - 8 *68 - 8 *68 - 8 *68 - 8 *68 - 8 *68 - 8 *69 - 9 *69 -	Feet. 22:24	Per Cent 10·07 - 10·15 - 10·23 - 10·81 - 10·89 - 10·47 - 10·55 - 10·63 - 10·71 - 10·95 - 11·03 - 11·11	Feet. 27 · 00 · 02 · 04 · 06 · 08 · 27 · 10 · 12 · 14 · 16 · 18 · 27 · 20 · 24 · 26 · 38 · 27 · 40 · 42 · 44 · 46 · 48 · 27 · 50 · 52 · 54 · 56 · 68 · 27 · 70 · 72 · 74 · 76 · 66 · 68 · 27 · 70 · 72 · 74 · 76 · 78 · 27 · 80 · 92 · 94 · 94 · 96 · 98 · 28 · 00 · 02	Per Cent. + 11·11 + 11·095 + 10·95 + 10·96 + 10·70 + 10·62 + 10·36 + 10·36 + 10·36 + 10·36 + 10·36 + 10·36 + 10·36 + 10·36 + 10·36 + 9·97 + 9·86 + 9·97 + 9·66 + 9·41 + 9·37 + 8·66 + 8·77 + 8·66 + 8·84 + 8·87 + 8·84 + 8·

	egistering Feet.		egistering Feet.		egistering Feet.		egisterin; Feet.
Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.
Feet.	Per Cent.	Feet.	Per Cent.	Feet.	Per Cent.	Feet.	Per Cent
28.04	+ 6.99	29.08	+ 3.16	30.12	- 0.40	31.16	- 3.7
.06	+ 6.92	29:10	+ 3.09	•14	- 0.47	•18	- 3.7
.08	+ 6.84	•12	+ 8.02	•16	- 0.53	31.20	- 3.8
28.10	+ 6.76	14	+ 2.95	•18	- 0.60	.22	- 3.9
·12	+ 6.69	.16	+ 2.88	30.50	- 0.66	.24	- 3.9
•14	+ 6.61	•18	+ 2.81	*22	- 0.73	•26	- 4.0
•16	+ 6.53	29.20	+ 2.74	*24	- 0.79	.28	- 4.0
•18	+ 6.46	-22	+ 2.67	.26	- 0.86	31.30	- 4.1
28.20	+ 6.38	24	+ 2.60	.28	- 0.92	-32	- 4.2
.22	+ 6.31	.56	+ 2.28	80.30	- 0.99	*84	- 4.2
.24	+ 6.23	28	+ 2.46	:32	- 1.06	.36	- 4.8
26	+ 6.16	29 '30	+ 2.39	*34	- 1.12	38	- 4.4
28 30	+ 6.01	·32 ·34	+ 2.32	·36 ·38	- 1.19	31.40	- 4.4
*32	W 00	36	1	30-40		·42 ·44	- 4.5
-34	+ 5.86	-38		•42	- 1·32 - 1·38	-46	- 4.6
*36	+ 5:78	29.40	+ 2.11	•44	- 1.44	48	- 4.7
-38	Table again	•42		-46	- 1:51	31.50	- 4-7
28.40	+ 5.41	.44	+ 1.97	•48	- 1.57	-52	- 4.8
.42	+ 5.56	•46	+ 1.83	30.50	- 1.64	154	- 4.8
•44	+ 5.49	•48	+ 1.76	.52	- 1.71	-56	- 4.9
46	+ 5'41	29.50	+ 1.69	•54	- 1.77	.58	- 5.0
.48	+ 5.34	.52	+ 1.63	.56	- 1.83	31.60	- 5.0
28.50	+ 5.26	.54	+ 1.56	*58	- 1.89	- 62	- 5.1
'52	+ 5.19	*56	+ 1.49	30.60	- 1.96	-64	- 5.1
•54	+ 5.11	•58	+ 1.42	-62	- 2.02	-66	- 5.5
'56	+ 5.04	29.60	+ 1.85	*64	- 2.09	.68	- 5.8
•58	+ 4.96	-62	+ 1.28	•66	- 2.15	31.70	- 5-8
28.60	+ 4.89	.64	+ 1.51	.68	- 2.22	.72	- 5.4
-62	+ 4.82	-66	+ 1.14	30.70	- 2.28	.74	- 5
'64	+ 4.75	.68	+ 1.08	•72	- 2.34	.76	- 5.
•66	+ 4.67	29.70	+ 1.01	.74	- 2.40	.78	- 5.6
28.70	+ 4.60	.72	+ 0.94	.76	- 2.47	31.80	- 5.0
•72	+ 4.45	74	+ 0.81	30.80	- 2·58 - 2·60	·82 ·84	- 5.7
-74	+ 4.38	-78	200	-82	- 2.66	186	- 5.8
.76	+ 4.81	29.80	+ 0.4	-84	- 2.72	*88	- 5
.78	+ 4.24	-82	+ 0.60	*86	- 2.78	81.90	- 5.9
28.80	+ 4.17	•84	+ 0.53	.88	- 2.85	-92	- 6.0
-82	+ 4.10	-86	+ 0.47	30.90	- 2.91	.94	- 6.0
.84	+ 4.02	*88	+ 0.40	.92	- 2.97	•96	- 6
.86	+ 8.95	29.90	+ 0.83	.94	- 3.04	-98	- 6.
.88	+ 3.88	-92	+ 0.26	.96	- 3.10	32.00	- 6
28.90	+ 3.81	.94	+ 0.20	.98	- 3.16	.02	- 6.
.92	+ 3.78	-96	+ 0.13	31.00	- 8.22	•04	- 6.8
.94	+ 8.66	•98	+ 0.07	.02	- 3.29	.06	- 6.4
•96	+ 3.59	30.00	Nil.	.04	- 3.35	.08	- 6.
-98	+ 3.52	.02	- 0.07	.06	- 8.42	32-10	- 6.
29.00	+ 8.45	.04	- 0.13	.08	- 3.48	.12	- 6.
*02	+ 3.38	.06	- 0.20	31.10	- 3.54	.14	- 8.6
*04	+ 3.31	.08	- 0.27	12	- 3.60	16	- 6.7
*06	+ 8.24	30.10	- 0.33	14	- 3.66	*18	- 6.1

	egistering Feet.		egistering Feet.		egistering Feet.		egistering Feet.
Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.
Feet. 32:20 -22 -24 -26 -28 -28 -28 -28 -28 -29 -34 -36 -36 -38 -32 -44 -46 -48 -32:50 -52 -54 -56 -62 -64 -66 -68 -82:70 -72 -74 -76 -78 -82:80 -82 -84 -86 -88 -82:90 -92 -94 -96 -98 -98 -98 -98 -98 -98 -98 -98 -98 -98	Per Cent. - 6.83 - 6.85 - 7.01 - 7.12 - 7.12 - 7.13 - 7.24 - 7.30 - 7.36 - 7.41 - 7.47 - 7.59 - 7.64 - 7.76 - 7.82 - 7.82 - 7.83 - 8.04 - 8.15 - 8.32 - 8.37 - 8.43 - 8.60 - 8.71 - 8.54 - 8.60 - 8.71 - 8.82 - 8.87 - 8.98 - 8.98 - 8.98 - 8.99 - 9.04 - 9.09 - 9.15 - 9.20 - 9.31 - 9.36 - 9.47 - 9.53 - 9.54 - 9.53 - 9.54	Feet. 33-24 - 26 - 28 33-30 - 32 - 34 - 36 - 38 - 38 - 40 - 44 - 46 - 46 - 56 - 58 - 58 - 56 - 58 - 33-60 - 62 - 64 - 72 - 74 - 76 - 78	Per Cent 9.75 - 9.81 - 9.86 - 9.91 - 9.96 - 10.01 - 10.02 - 10.18 - 10.28 - 10.34 - 10.39 - 10.45 - 10.61 - 10.66 - 10.71 - 10.76 - 10.93 - 10.98 - 11.98 - 11.98 - 11.98 - 11.98 - 11.98	Feet. 36 00 02 04 06 08 36 10 12 14 16 18 36 20 22 24 24 26 28 36 30 32 34 36 36 36 36 36 36 36 37 30 38 36 36 36 36 36 36 36 36 36 36 36 36 36	Per Cent. + 11·11 + 11·05 + 10·99 + 10·86 + 10·86 + 10·68 + 10·68 + 10·68 + 10·68 + 10·68 + 10·56 + 10·56 + 10·50 + 10·19 + 10·19 + 10·19 + 10·19 + 10·19 + 10·19 + 10·19 + 9·83 + 9·83 + 9·41 + 8·99 + 8·83 + 8·64 + 8·64 + 8·46 + 8 + 8 + 8 + 8 + 8 + 8 + 8 + 8 + 8 + 8	Feet. 37 04	Per Cent. + 7 · 99 + 7 · 82 + 7 · 87 + 7 · 82 + 7 · 764 + 6 · 764 + 7 · 764

	egistering Feet.		egistering Feet.		egistering Feet.		egisterin Feet.
Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder,	Amount of Error.
Feet.	Per Cent.	Feet.	Per Cent.	Feet.	Per Cent.	Feet.	Per Cent
38.08	+ 5.04 + 4.98	39:12	+ 2.25	40.16	- 0·40 - 0·45	41.20	- 2.9
38.10	+ 4.98	14	+ 2.15	40.20	- 0.49	•24	- 3.0
.14	+ 4.87	•18	+ 2.09	-22	- 0.55	•28	- 3.0
•16	+ 4.82	89.20	+ 2.04	.24	- 0.60	*28	- 3.10
•18	+ 4.76	.22	+ 1.99	-26	- 0.65	41.80	- 3.16
38.20	+ 4.71	•24	+ 1.94	.28	- 0.70	*82	- 3.19
•22	+ 4.65	•26	+ 1.88	40.30	- 0.75	.34	- 3.24
.24	+ 4.60	.28	+ 1.83	-82	- 0.79	*36	- 3.29
*26	+ 4.54	39.30	+ 1.78	.34	- 0.84	.38	- 3.34
•28	+ 4.49	*32	+ 1.73	*36	- 0.89	41.40	- 3.38
38·30 ·32	+ 4.44	·34 ·36	+ 1.68	40.40	- 0.94	.42	- 3.48
-34	+ 4.33	-38	+ 1.63 + 1.57	•42	- 1.04	·44 ·46	- 3·47 - 3·59
-36	+ 4.28	39.40	+ 1.52	.44	- 1.09	.48	- 8.57
*38	+ 4.73	.42	+ 1.47	-46	- 1.14	41.50	- 3.61
39.40	+ 4.17	•44	+ 1.42	•48	- 1.19	.52	- 8.66
•42	+ 4'11	*46	+ 1.37	40.50	- 1.24	.54	- 8.71
.44	+ 4.06	.48	+ 1.32	.52	- 1.28	.56	- 8-75
*46	+ 4.00	39.50	+ 1.26	*54	- 1.33	*58	- 3.80
•48	+ 8.95	.25	+ 1.21	•56	- 1.38	41.60	- 3.85
38.50	+ 3.90	.54	+ 1.16	*58	- 1.43	*62	- 3.90
-52	+ 3.84	*56	+ 1.11	40.60	- 1.48	*64	- 3.94
·54 ·56	+ 3.78	39.60	+ 1.01	·62 ·64	- 1.58	·66 ·68	- 8.99
•58	+ 3.73	62	+ 0.96	-66	- 1·57 - 1·62	41.70	- 4·08
38-60	+ 3.63	.64	+ 0.91	-68	- 1.67	.72	- 4.12
-62	+ 3.57	.66	+ 0.86	40.70	- 1.72	.74	- 4.17
*64	+ 3.52	.68	+ 0.81	.72	- 1.77	.76	- 4:21
•66	+ 3.46	39.70	+ 0.75	.74	- 1.82	.78	- 4.26
*68	+ 3.41	.72	+ 0.70	.76	- 1.86	41.80	- 4.31
88.70	+ 8.36	.74	+ 0.65	.78	- 1.91	-82	- 4.36
•72	+ 3.31	•76	+ 0.60	40.80	- 1.96	*84	- 4:40
.74	+ 3.25	•78	+ 0.55	.82	- 2.01	*86	- 4.45
·76	+ 3.20 + 3.14	39.80	+ 0.50	*84	- 2·06 - 2·10	41.90	- 4:49
8.80	+ 3.14 + 3.09	-84	+ 0.40	-88	- 2.10	92	- 4.54 - 4.58
.82	+ 3.04	*86	+ 0.35	40.90	- 2.20	94	- 4:63
*84	+ 2.99	*88	+ 0.30	-92	- 2.25	-96	- 4.67
*86	+ 2.93	39.90	+ 0.25	-94	- 2.30	-98	- 4.72
*88	+ 2.88	.92	+ 0.20	.96	- 2.34	42.00	- 4.76
8.90	+ 2.82	-94	+ 0.15	.98	- 2.39	-02	- 4.81
-92	+ 2.77	-96	+ 0.10	41.0C	- 2.44	-04	- 4.85
94	+ 2.72	-98	+ 0.05	+02	- 2.49	.06	- 4.90
*96	+ 2.67	40.00	Nil.	.04	- 2.53	.08	- 4.94
98	+ 2.61	.02	- 0.02	·06	- 2.58	42.10	- 4.99
-02	+ 2.56	·04 ·06	- 0.10	41.10	- 2·63 - 2·68	14	- 5 03 - 5 08
-04	+ 2.46	-08	- 0.50	12	- 2.72	-16	- 5.12
.06	+ 2.40	40.10	- 0.25	•14	- 2.78	18	- 5.17
	+ 2.85	12	- 0.30	•16	- 2.82	42.20	- 5.21
9.10	+ 2.30	.14	- 0.85	-18	- 2.87	-22	- 5.26

	egistering Feet.		egistering Feet.		legistering Feet.	Meter Registering 50 Feet.				
Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.			
Feet.	Per Cent.	Feet.	Per Cent.	Feet.	Per Cent.	Feet.	Per Cent			
42.24	- 5.30	43.28	- 7.58	44.82	- 9.75	45.00	+ 11.11			
26	- 5.35	43.30	- 7:62	*84	- 9.79	.02	+ 11.06			
·28 42·80	- 5·39 - 5·44	-32	- 7·66 - 7·71	·36	- 9·83 - 9·87	·04 ·06	+ 11.0			
-32	- 5.48	.86	- 7.75	44.40	- 9.91	-08	+ 10.90			
*34	- 5.53	•38	- 7.79	-42	- 9.95	45.10	+ 10.86			
-36	- 5.57	43.40	- 7.83	•44	- 9.99	12	+ 10.81			
-38	- 5.62	-42	- 7.88	•46	- 10.03	.14	+ 10.76			
42.40	- 5.66	•44	- 7.92	•48	- 10.07	.16	+ 10.72			
.42	- 6.71	'46	- 7.96	44.50	- 10.11	-18	+ 10.67			
*44	- 5.75	.48	- 8.00	-52	- 10.15	45.20	+ 10.62			
*46	- 5.80	43.20	- 8*05	*54	- 10.19	.22	+ 10.57			
•48	- 5.84	-52	- 8.09	*56	- 10.23	•24	+ 10.52			
42.50	- 5.88	*54	- 8.13	*58	- 10.27	*26	+ 10.48			
.52	- 5.93	.56	- 8.17	44.60	- 10.31	28	+ 10.48			
-64	- 5-98	10.00	- 8.22	:62	- 10.35	45.80	+ 10.38			
-56	- 6·02 - 6·06	43.60	- 8·30	·64 ·66	- 10.39	·32 ·34	+ 10.33			
42.60	- 6.10	64	- 8.84	- 68	- 10·43 - 10·47	-36	+ 10.28			
62	- 6.15	.66	- 8.38	44.70	- 10.51	.38	+ 10.18			
-64	- 6.19	*68	- 8:42	.72	- 10.55	45.40	+ 10.13			
-66	- 6.24	43.70	- 8.47	-74	- 10.59	-42	+ 10.08			
-68	- 6.28	.72	- 8.51	•76	- 10.63	•44	+ 10.03			
42.70	- 6.33	.74	- 8.55	•78	- 10.67	*46	+ 9.99			
-72	- 6.37	•76	- 8.59	44.80	- 10.71	•48	+ 9.94			
-74	- 6.41	-78	- 8.64	-82	- 10.75	45.50	+ 9.89			
•76	- 6.45	43.80	- 8.68	*84	- 10.79	.52	+ 9.84			
-78	- 6.50	182	- 8.72	*86	- 10.84	54	+ 9.79			
42.80	- 6.54	184	- 8.76	*88	- 10.87	*56	+ 9.75			
*82	- 6·63 - 6·63	*86	- 8·80 - 8·84	44.90	- 10·91 - 10·95	45.60	+ 9.70			
-86	- 6.68	43.90	- 8.89	+94	- 10.99	62	+ 9.65			
-88	- 6.72	.92	- 8.83	•96	- 11.03	-64	+ 9.55			
42.90	- 6.76	.94	- 8.97	-98	- 11.07	•66	+ 9.50			
-92	- 6.80	.96	- 9.01	45.00	- 11.11	-68	+ 9.46			
.94	- 6.85	.98	- 9.05	1		45.70	+ 9.41			
.96	- 6.89	44.00	- 9.09			.72	+ 9.36			
-98	- 6.94	.02	- 9.14			*74	+ 9.31			
43.00	- 6.98	.04	- 9.18			•76	+ 9.27			
.02	- 7.02	•06	- 9.22			.78	+ 9.22			
*04	- 7.06	.08	- 9.26			45.80	+ 9.17			
·06 ·08	- 7·11 - 7·15	44.10	- 9.30			·82 ·84	+ 9.12			
43.10	- 7.16	-12 -14	- 9.34	3		-86	+ 9.03			
+12	- 7.24	*16	- 9.42			*88	+ 8.98			
.14	- 7.28	'18	- 9.47			45.90	+ 8.93			
*16	- 7.32	44.20	- 9.51			-92	+ 8.88			
•18	- 7.87	-22	- 9.55			•94	+ 8.84			
43.20	- 7.41	'24	- 9.59			.96	+ 8.79			
-22	- 7.45	*26	- 9.68			.98	+ 8.75			
*24	- 7.49	.28	- 9.67			46.00	+ 8.70			
• 26	- 7'54	44.30	- 9.71			*02	+ 8.65			

	egistering Feet.		egistering Feet.		egistering Feet.	Meter Registering 50 Feet.					
Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder,	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.				
Feet.	Per Cent.	Feet.	Per Cent.	Feet.	Per Cent.	Feet.	Per Cent				
46.04	+ 8.60	47.08	+ 6.20	48.12	+ 3.91	49.16	+ 1.7				
.06	+ 8.56	47.10	+ 6.16	14	+ 3.86	.18	+ 1.6				
.08	+ 8.51	•12	+ 6.11	.16	+ 3.82	49.20	+ 1.6				
46.10	+ 8.46	'14	+ 6.07	•18	+ 8.77	•22	+ 1.5				
·12	+ 8.41	.16	+ 6.02	48.20	+ 3.73	*24	+ 1.5				
.14	+ 8.37	•18	+ 5.98	•22	+ 3.69	.26	+ 1.5				
•16	+ 8.32	47.20	+ 5.98	•24	+ 3.65	*28	+ 1.4				
.18	+ 8.58	-22	+ 5.89	.26	+ 3.60	49.30	+ 1.45				
46.20	+ 8.23	.24	+ 5.84	.28	+ 3.56	-32	+ 1.38				
-22	+ 8.18	.26	+ 5.80	48.30	+ 3.52	.34	+ 1.3				
.24	+ 8.13	.28	+ 5.75	. 32	+ 3.48	-36	+ 1.29				
.26	+ 8.09	47.30	+ 5.71	*34	+ 3.44	*38	+ 1.2				
46.30	+ 8.04	*82	+ 5.67	·36 ·38	+ 3.39	49.40	+ 1.21				
.32	+ 7·99 + 7·94	·34 ·36	+ 5.62	48-40	+ 3.35	•42	+ 1.17				
•34	2000	*38	+ 5.53	40 40	+ 3.31	•44	+ 1.18				
•36	+ 7.90 + 7.85	47.40	+ 5.49	•44	+ 3.22	48	+ 1.09				
*38	+ 7.81	•42	+ 5.44	*46	+ 3.18	49.50	+ 1.05				
46.40	+ 7.76	•44	+ 5.40	-48	+ 3.13	52	+ 1.01				
•42	+ 7.71	•46	+ 5.35	48.50	+ 3.09	54	+ 0.98				
•44	+ 7.67	+48	+ 5.31	152	+ 3.05	.56	+ 0.89				
*46	+ 7.62	47.50	+ 5.26	-54	+ 3.01	*58	+ 0.85				
•48	+ 7.58	-52	+ 5.22	-56	+ 2.96	49.60	+ 0.81				
46.50	+ 7.58	.54	+ 5.17	158	+ 2.92	.62	+ 0.77				
•52	+ 7.48	-56	+ 5.13	48.60	+ 2.88	.64	+ 0.73				
*54	+ 7.44	.58	+ 5.08	.62	+ 2.84	-66	+ 0.68				
*56	+ 7.39	47.60	+ 5.04	-64	+ 2.80	*68	+ 0.64				
.58	+ 7.35	.62	+ 5.00	*66	+ 2.75	49.70	+ 0.60				
45.60	+ 7.30	*64	+ 4.95	.68	+ 2.71	.72	+ 0.56				
:62	+ 7.25	.66	+ 4.91	48.70	+ 2.67	.74	+ 0.52				
*64	+ 7.21	.68	+ 4.86	•72	+ 2.63	•76	+ 0.48				
·66 ·68	+ 7.16 + 7.12	47.70	+ 4.82	·74 •76	+ 2.59	•78	+ 0.44				
46.70	+ 7.07	.74	+ 4.78	-78	+ 2.50	49-80	+ 0.40				
.72	+ 7.02	.76		48.80	+ 2.46	-84	+ 0.36				
-74	+ 6.98	178	+ 4.64	.82	+ 2.42	186	+ 0.32				
•76	+ 6.93	47.80	+ 4.60	*84	+ 2.38	-88	+ 0.24				
.78	+ 6.89	-82	+ 4.56	*86	+ 2.33	49.90	+ 0.20				
46.80	+ 6.84	.84	+ 4.51	*88	+ 2.29	-92	+ 0.16				
*82	+ 6.79	*86	+ 4.47	48.90	+ 2.25	-94	+ 0.12				
*84	+ 6.75	.88	+ 4.42	-92	+ 2.21	-96	+ 0.08				
*86	+ 6.70	47.90	+ 4.38	-94	+ 2.17	.98	+ 0.04				
'88	+ 6.66	•92	+ 4.34	-96	+ 2.12	60.00	Nil.				
46.90	+ 6.61	•94	+ 4.30	-98	+ 2.08	.02	- 0.04				
.92	+ 6.56	.96	+ 4.25	49.00	+ 2.04	*04	- 0.08				
*94	+ 6.52	.98	+ 4.21	•02	+ 2.00	.06	- 0.15				
*96	+ 6.47	48'00	+ 4.17	.04	+ 1.96	.08	- 0.16				
'98	+ 6.43	.02	+ 4.13	.06	+ 1.91	50.10	- 0.20				
47.00	+ 6.38	*04	+ 4.08	*08	+ 1.87	12	- 0.24				
02	+ 6.34	*06	+ 4.04	49.10	+ 1.83	:14	- 0.28				
-06		48.10	+ 3.99	12		16	- 0.32				
00	+ 6.25	40.10	+ 3.95	*14	+ 1.75	•18	- 0.36				

	egistering Feet.		egistering Feet.		egistering Feet.	Meter Registering 50 Feet.				
Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder,	Amount of Error.	Reading of Scale of Gas- holder,	Amoun of Error.			
Feet.	Per Cent.	Feet.	Per Cent.	Feet.	Per Cent.	Feet.	Per Cen			
50.20	- 0.40	51.24	- 2.42	52:70	- 5.12	55.30	- 9.5			
.22	- 0.44	.26	- 2.45	.75	- 5:21	*35	- 9.6			
*24	- 0.48	.28	- 2.49	*80	- 5.80	*40	- 9.7			
26	- 0.52	51.30	- 2.53	185	- 5.39	45	- 9.8			
28	- 0.26 - 0.60	32	- 2·57 - 2·61	.90	- 5·48 - 5·57	55:50	- 9.8			
50.30	- 0.64	36	- 2.65	53.00	- 5.66	60	- 9.9			
-34	- 0.68	-38	- 2.69	.05	- 5.75	65	- 10.1			
.36	- 0.71	51.40	- 2.72	.10	- 5.84	.70	- 10.5			
.38	- 0.75	.42	- 2.76	15	- 5.93	•75	- 10.8			
50.40	- 0.79	.44	- 2.80	-20	- 6.02	*80	- 10.8			
.42	- 0.83	+46	- 2.83	*25	- 6.10	*85	- 10.4			
.44	- 0.87	.48	- 2.87	•30	- 6.19	.90	- 10-6			
'46	- 0.91	51.50	- 2.91	*85	- 6.28	-95	- 10.6			
*48	- 0.95	.52	- 2.95	.40	- 6.37	56.00	- 10.7			
50.50	- 0.99	*54	- 2.99	*45	- 6.45	*05	- 10.7			
'52	- 1.03	'56	- 3.03	53.50	- 6.24	10	- 10.8			
54	- 1.07	.58	- 3.06	.55	- 6.63	15	- 10.8			
*56	- 1.11	51.60	- 8:10	.60	- 6.72	20	- 11'(
158	- 1.15	62	- 3·14 - 3·18	65	- 6.80	'25	- 11.1			
50.60	- 1·19 - 1·23	-66	- 3.51	·70 ·75	- 6.89 - 6.89	10.34	1 2 10			
64	- 1.23	-68	- 3.25	-80	- 7.06					
*66	- 1.30	51.70	- 8.29	.85	- 7.15					
.68	- 1.34	.72	- 3.33	•90	- 7.24		1900			
50.70	- 1.38	•74	- 3.36	95	- 7.82		17 22			
.72	- 1.42	-76	- 3.40	54.00	- 7.41		17 10			
.74	- 1.46	.78	- 3.43	*05	- 7.49		11			
.76	- 1.49	51.80	- 3.47	'10	- 7.58		15			
*78	- 1.53	*82	- 8.51	15	- 7.66					
.50.80	- 1.57	'84	- 8.55	20	- 7.75		1			
*82	- 1.61	'86	- 8.58	125	- 7.83		1			
'84 '86	- 1.65 - 1.69	51.90	- 3.62	*30	- 7·92 - 8·00					
*88	- 1.73	.92	- 3.70	40	- 8.09					
50.90	- 1.77	.94	- 3.74	45	- 8.17					
92	- 1.81	.96	- 3.77	54.50	- 8.26					
-94	- 1.85	•98	- 3.81	.55	- 8.34					
.96	- 1.88	52.00	- 3.85	.60	- 8.42					
.98	- 1.92	.05	- 3.94	.65	- 8.51					
51.00	- 1.96	10	- 4.03	.70	- 8.59					
.02	- 2.00	15	- 4.12	.75	- 8.68	1000				
.04	- 2.04	•20	- 4.21	.80	- 8.76	200	1			
,06	- 2.07	25	- 4.81	*85	- 8.84	1 7 7 1	1			
.08	- 2.11	180	- 4.40	.90	- 8.93		1			
51.10	- 2·15 - 2·19	35	- 4·49 - 4·58	55.00	- 9.00		1			
12	- 2.19	•45	- 4.67	05	- 9·09 - 9·18		1			
16	- 2.26	52.50	- 4.76	10	- 9.18		1			
-18	- 2.30	55	- 4.85	15	- 9.34					
51.20	- 2.34	•60	- 4.94	-20	- 9.42					
-22	- 2.38	-65	- 5.03	-25	- 9.51					

	egistering Feet.		egistering Feet.		egistering Feet.	Meter Registering 100 Feet.				
of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.			
Feet.	Per Cent.	Feet.	Per Cent.	Feet.	Per Cent.	Feet.	Per Cent			
90.00	+ 11.11	92.65	+ 7.93	95.30	+ 4.93	97:95	+ 2.08			
.05	+ 11.05	.70	+ 7.87	.35	+ 4.87	58.00	+ 2.04			
•10	+ 10.99	.75	+ 7.82	•40	+ 4.82	.05	+ 1.99			
15	+ 10.92	.80	+ 7.76	45	+ 4.76	10	+ 1.94			
.20	+ 10.86	*85 *90	+ 7.70	95.50	+ 4.71	15	+ 1.88			
.30	+ 10.80	-95		·55 ·60	+ 4.65	20				
*85	+ 10.68	93.00		65	+ 4.60	-30	+ 1.78			
.40	+ 10.62	05	+ 7.53	•70	+ 4.49	-85	T 1.68			
45	+ 10.56	-10	+ 7.41	•75	+ 4.43	•40	+ 1.68			
90.50	+ 10.50	•15	+ 7.36	-80	+ 4.38	•45	+ 1.57			
.55	+ 10.44	.20	+ 7.30	.85	+ 4.33	98.50	+ 1.59			
60	+ 10.38	.25	+ 7.24	-90	+ 4.28	.55	+ 1.47			
-65	+ 10.31	•30	+ 7.18	195	+ 4.22	.60	+ 1.42			
-70	+ 10.25	•35	+ 7.13	96.00	+ 4.17	•65	+ 1.37			
.75	+ 10.19	•40	+ 7.07	.05	+ 4.11	.70	+ 1.35			
-80	+ 10.13	.45	+ 7.01	-10	+ 4.06	.75	+ 1.26			
*85	+ 10.07	93.50	+ 6.95	*15	+ 4.00	.80	+ 1.2			
90	+ 10.01	. 55	+ 6.90	•20	+ 8.95	.85	+ 1.16			
95	+ 9.95	-60	+ 6.84	•25	+ 3.89	.90	+ 1.11			
91.00	+ 9.89	:65	+ 6.78	•30	+ 3.84	95	+ 1.06			
.05	+ 9.83	·70 ·75	+ 6.66	·35 ·40	+ 3.78	99.00	+ 1.01			
-10 -15	+ 9.77	-80	+ 6.61	45	+ 3.48	·05	+ 0.91			
20	+ 9.65	-85	+ 6.55	96.50	+ 3.68	15	+ 0.86			
25	+ 9.59	.90	+ 6.50	*55	+ 3.57	-20	+ 0.81			
-30	+ 9.58	•95	+ 6.44	.60	+ 8.52	25	+ 0.78			
*35	+ 9.47	94.00	+ 6.38	-65	+ 3.46	*80	+ 0.70			
*40	+ 9.41	•05	+ 6.32	•70	+ 3.41	.35	+ 0.6			
45	+ 9.35	.10	+ 6.27	.75	+ 3.36	.40	+ 0.60			
91.50	+ 9.29	.15	+ 6.21	.80	+ 3.31	'45	+ 0.2			
*55	+ 9.23	.20	+ 6.16	:85	+ 3.25	99.50	+ 0.50			
.60	+ 9.17	•25	+ 6.10	.90	+ 3.20	'55	+ 0.4			
65	+ 9.11	.30	+ 6.04	95	+ 3.14	'60	+ 0.40			
·70 ·75	+ 8.99	'35	+ 5.98	97.00	+ 3.09	*65	+ 0.30			
-80	+ 8.83	·40 ·45	+ 5.93	:05	+ 3.04	·70 ·75	+ 0.5			
*85	+ 8.87	94.50	+ 5.87	*10 *15	+ 2.93	-80	0.0			
-90	+ 8.81	55	+ 5.82	.20	+ 2.88	.85	+ 0.12			
.95	+ 8.76	-60	+ 5.71	25	+ 2.82	-90	+ 0.10			
92.00	+ 8.70	.65	+ 5.65	•30	+ 2.77	.95	+ 0.00			
.05	+ 8.64	.70	+ 5.60	*35	+ 2.72	100.00	Nil.			
-10	+ 8.58	.75	+ 5.54	.40	+ 2.67	.05	- 0.05			
-15	+ 8.52	.80	+ 5.49	.45	+ 2.61	.10	- 0.10			
.20	+ 8.46	*85	+ 5.48	97.50	+ 2.56	:15	- 0.15			
.25	+ 8.40	.90	+ 5.37	.55	+ 2.51	.20	- 0.50			
'30	+ 8.34	.95	+ 5.31	.60	+ 2.46	.25	- 0.25			
.35	+ 8.29	95.00	+ 5.26	.65	+ 2.40	*80	- 0.80			
40	+ 8.23	*05	+ 5.20	.70	+ 2.35	*85	- 0.85			
92.50	8.17	10	+ 5.15	.75	+ 2.30	:40	- 0.40			
55	+ 8.05	*15	+ 5.09	*80	+ 2.25	100.50	- 0.48			
-60	+ 8.05	20	+ 5.04	·85 ·90	+ 2.20	100.50	- 0.50			

	egistering Feet.		egistering Feet.		egistering Feet.	Meter Registering 100 Feet.					
Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error.	Reading of Scale of Gas- holder.	Amount of Error,	Reading of Scale of Gas- holder.	Amount of Error,				
Feet.	Per Cent.	Feet.	Per Cent.	Feet.	Per Cent.	Feet.	Per Cent.				
100.60	- 0.65 - 0.65	103.25	- 3·15 - 3·19	105.90	- 5:57	108.55	- 7·88 - 7·92				
·65	- 0.40	-85	- 3.19	106.00	- 5·62 - 5·66	·60 ·65	- 7.96				
-75	- 0.75	•40	- 8.29	05	- 5.71	•70	- 8.00				
•80	- 0.79	*45	- 3.34	•10	- 5.75	•75	- 8:05				
*85	- 0.84	103-50	- 3.38	•15	- 5.80	-80	- 8.09				
.90	- 0.89	•55	- 8.43	•20	- 5.84	*85	- 8.13				
.95	- 0.94	.60	- 3.47	•25	- 5.88	.90	- 8:17				
101.00	- 0.99	·65 ·70	- 3·52 - 3·57	*30	- 5·93 - 5·98	109:00	- 8·22 - 8·26				
.10	- 1.09	.75	- 3.61	-40	- 6.02	.05	- 8.30				
.15	- 1.14	-80	- 3.66	•45	- 6.06	.10	- 8.34				
-20	- 1.19	-85	- 3.71	106.50	- 6.10	.15	- 8.38				
.25	- 1.24	.90	- 8.75	•55	- 6.15	.20	- 8.42				
.80	- 1.28	.95	- 3.80	-60	- 6.19	*25	- 8.47				
*85	- 1.83	104.00	- 3.85	-65	- 6.24	.30	- 8.51				
•40	- 1.38	.05	- 8.90	-70	- 6.28	*85	- 8.55				
101.50	- 1.43	10	- 8.94	.75	- 6.33	'40	- 8.59				
101.50	- 1·48 - 1·53	15	- 3·99 - 4·03	*80 *85	- 6·37 - 6·41	109.50	- 8·64 - 8·68				
-60	- 1.57	-25	- 4.08	.90	- 6.45	.55	- 8.72				
.65	- 1.62	-30	- 4.12	.95	- 6.50	.60	- 8.76				
.70	- 1.67	•35	- 4.17	107.00	- 6.54	•65	- 8.80				
•75	- 1.72	•40	- 4.21	.05	- 6.59	-70	- 8.84				
.80	- 1.77	•45	- 4.26	•10	- 6.63	•75	- 8.89				
*85	- 1.82	104.50	- 4.31	15	- 6.68	-80	- 8.93				
·90 ·95	- 1·87 - 1·91	•55	- 4·36 - 4·40	·20 ·25	- 6·72 - 6·76	·85 ·90	- 8·97 - 9·01				
102.00	- 1.96	•65	- 4.45	30	- 6.80	95	- 9.05				
.05	- 2.01	.70	- 4.49	*35	- 6.85	110.00	- 9.09				
.10	- 2.06	.75	- 4.54	•40	- 6.89	·10	- 9.18				
•15	- 2.10	-80	- 4.58	•45	- 6.94	-20	- 9.26				
•20	- 2.15	.85	- 4.63	107:50	- 6.98	-30	- 9.34				
.25	- 2.20	.90	- 4.67	•55	- 7.02	-40	- 9.42				
*80	- 2·25 - 2·80	.95	- 4·72 - 4·76	.60	- 7.06	*50	- 9.51				
-40	- 2.34	105.00	- 4.76 - 4.81	·65 ·70	- 7·11 - 7·15	·60 ·70	- 9·59 - 9·67				
45	- 2.39	10	- 4.85	-75	- 7.20	-80	- 9.75				
102.50	- 2.44	•15	- 4.90	*80	- 7.24	-90	- 9.83				
.55	- 2.49	-20	- 4.94	*85	- 7.28	111.00	- 9.91				
-60	- 2.58	.25	- 4.99	-90	- 7.32	•10	- 9.99				
*65	- 2.58	-80	- 5.03	-95	- 7.37	.20	- 10.07				
.70	- 2.63	*35	- 5.08	108.00	- 7.41	*30	- 10.15				
·75 ·80	- 2·68 - 2·72	40	- 5·12 - 5·17	.05	- 7:45	:40	- 10.23				
-85	- 2.72	105.50	- 5.21	·10	- 7·49 - 7·54	·50 ·60	- 10.31				
-90	- 2.82	55	- 5.26	.20	- 7.58	•70	- 10.47				
.95	- 2.87	.60	- 5.30	.25	- 7.62	.80	- 10.55				
103.00	- 2.91	.65	- 5.85	.80	- 7.66	.90	- 10.63				
.05	- 2.96	•70	- 5.39	+35	- 7.71	112.00	- 10.71				
.10	- 3.01	•75	- 5.44	'40	- 7.75	.10	- 10.79				
15	- 8.06	.80	- 5.48	100.50	- 7.79	20	- 10.87				
.20	- 3.10	185	- 5.58	108.50	1 - 7.83	.30	- 10.95				

Note.—Any other quantity may be calculated by the rule of proportion, thus:—

Meter registering '		100·00 89·95	feet
Difference	fa	10·05	,,
And Meter registering		100.00	feet
Difference		-	"
112.55:100::12.55:11.15	sle	ow.	

TABLE

Showing the Dilatation of Gas in Contact with Water and Saturated with Aqueous Vapour, for given Temperature. (Professor Airey.)

(Used in making Corrections for Temperature in the Testing of Gas Meters.)

Temperature in Fahrenheit's Scale.	Percentage of Dilatation.	Temperature in Fahrenheit's Scale.	Percentage of Dilatation.	Temperature in Fahrenheit's Scale.	Percentage of Dilatation.
31.40	0	54.33	51	74:30	11
33.54	4	56.24	6	75.94	113
35.70	1	58.12	61	77.23	12
37.84	13	60.02	7	78'81	124
39.91	2	62.00	71	80.40	13
42.05	21	63.77	8	81.94	131
44.17	8	65.63	81	88.44	14
46.22	81	67.43	9	84.88	144
48.25	4	69.18	91	86.39	15
50.32	41	70.90	10	87.83	151
52'36	5	72.60	101	89.20	16

Note.—The table shows the percentage of increase of the volume of gas above its volume at the temperature of 31.4° Fahr.

INTERNAL FITTINGS.

The advantages of an ample supply of good and pure gas are frequently neutralized by the defective manner in which premises are fitted internally.

Bad gas-fittings are generally the result of cupidity or ignorance. They are a common cause of complaint from consumers who are often ready to attribute the inefficient light which they afford to a want of pressure or purity, or a low illuminating power in the gas.

The following regulations (with such additions and modifications as may be found necessary) may be adopted with advantage by gas authorities.

Regulations as to Internal Fittings.

- 1. The company's (or local authority's) servants will in all cases lay on the service-pipe, conveying the same through the outer wall of the premises to be supplied with gas.
- 2. The main-cock must be attached to the end of the service-pipe within the building, and close to the outer wall.
- 3. The gas meter must be placed perfectly level, either on the floor or on a substantial support, and within 2 ft. 6 in. of the main-cock.
- 4. The piping attached to the meter, whether inlet or outlet, must not be smaller in internal diameter than that of the meter unions.
- 5. The following are the sizes of the meters, and their measuring capacity, from which the number of lights which they supply can be readily calculated:—

Size						Inl	et an utlet	id .				Car	easuring pacity evolution bio Fe	per				Ca	feasuring pacity per Hour.
2-	light						ł				4		75						12
8	**						4						1						18
5	**	1			12		4						1						30
10	11						1						- 6						60
15	11						1						4						90
20	,,	1					11						1						120
30	11		10			4	18						18				14		180
50	"					3	14						24						300
60	13		-			-	14	-					3						360
80	17		19				19	63)		101	0		4			0	10	130	480
100	**	1					2						5			-			600
150	17	-	10		0	134	3	3	181			10	74	10		0	1		900
200	27		10	6	00	20	3	60	i a		0	-	10	0	101	13			1200
250	100						4						124						1500
300	**						4					3	15			3			1800
400	11	-				*	4	-				-	20					100	2400
500	**		-				5					*	25		-			-	3000
600	33		*	1		-	5						30		100	-	10	-	3600
900	33			-			0					*	00						0000

To ascertain the number of lights which any size of meter will supply, divide the measuring capacity per hour by the quantity of gas per hour which each jet is estimated to consume. Example: What number of lights, consuming 4 cubic feet of gas per hour, will a 20-light

meter supply? Then,
$$\frac{120}{4} = 30$$
 lights, answer.

6. The following are the sizes and lengths of iron, lead, or composition tubes to be used according to the number of ordinary lights:—

Internal Dir of Tubin Inches	g.	er		Greatest Length allowed. Feet.										reatest l	rs	
4						20									3	
1						80									6	
9		*				40								4	12	
4						50									20	
1						70									85	
11		1				100					1				60	
15						150									100	
2						200									200	

- Tubing of ‡ inch bore is not allowed to be used.
- 7. The tubes or pipes must be laid with proper fall, and in such a manner that they are easily accessible, and protected from liability to damage. Attention is to be given to leaving a space round them at such places as wall crossings, &c., where fracture or crushing of the pipes might be caused by the subsidence of the building. The joinings of the tubes and pipes are to be made in the most solid and substantial manner; and carefully rounded bends (not elbows) are to be used wherever the direction of a pipe is changed.
- 8. Floor boards covering pipes must be secured with screws, so that they may be easily removed to afford access to the pipes, especially at the points of connection.
- 9. On the completion of the work of fitting, and before the piping is covered up, notice thereof must be given in writing to the gas manager (the requisite form for that purpose being obtained at the gas office), who will cause an inspection to be made of the work, and if found in accordance with the regulations herein contained, it will be passed by the company (or local authority), and the gas turned on.
- 10. If the regulations are not conformed to in every respect, the company (or local authority) reserve the right to refuse a supply of gas until the necessary alterations are made.
- 11. Gas-fitters complying with these regulations have their names registered on the company's (or local authority's) list of approved

fitters, and they are at liberty to designate themselves "Authorized Gas-Fitters." Repeated negligence will cause the license to be withdrawn.

A handy and useful apparatus for testing the soundness of gasfittings, has been devised by Harrison and Sheard. It consists of a small force pump and a King's pressure-gauge, in which mercury is employed instead of water; the two being connected together on one base board, and provided with a coupling for ready attachment to the Fittings to be tested.

To use the apparatus, air is forced, by means of the pump, into the Fittings until the pressure therein is equivalent to, say, 12 inches of water, as indicated on the dial of the gauge. The pump is then shut off by means of a stopcock, and it is noted whether the pressure is maintained or falls away. If the pointer remains stationary, the Fittings are sound; while if it goes back, there is a leakage.

To facilitate the discovery of leakages, gas may be forced into the

Fittings, by connecting an inlet pipe on the pump, by means of indiarubber tubing, with any convenient gas supply; when the gas escaping through the defective Fittings at a high pressure, enables the locality of the leakages to be readily discovered.

Ordinary sitting rooms are best lighted by means of a central chandelier. When the room is of large dimensions, wall brackets may be added. A bracket at each side of the mantelpiece has a tasteful appearance, and lights are handy in that position.

The jets of chandeliers and brackets should be not less than 36 inches

from the ceiling.

A tea-spoonful of salad oil added on the top of the water in the tube of a water-slide pendant, tends, in a great measure, to prevent or retard

evaporation of the water.

Burners arranged in the horizontal position are not usually effective, and are not to be recommended except on the conditions noted hereafter. The flames of such have an unpleasant pulsatory or tremulous motion, very disagreeable when fixed on a level with or but slightly above the eye of the spectator, due to the upward current of air striking the underside.

The arrangement is bad for another reason-viz., the flame is prevented from receiving its due supply of oxygen on all sides, and as a consequence, the combustion is imperfect; bad illumination, and a deposit of unconsumed carbon on the ceiling being the result.

It is not, however, to be assumed that lights placed in the horizontal or the inclined position are never effective. They can be rendered so by causing the tails of the flames to impinge one upon the other, and by making provision in the construction of the pendant for the air current to play upon the upper surface of the flame.

The question of the efficient ventilation of rooms where gas is being consumed is one of importance both to the gas producer and the user. The subject has been a comparatively neglected one, although it pro-

mises in the future to occupy greater prominence.

Ventilating globe and other lights of various designs have been intro-

duced by Messrs. Sugg, Cowan, Bray, Strode, and other makers, with highly satisfactory results, and their more general adoption is only a question of time. Fig. 105 shows Mr. Cowan's ventilating globe light; and Fig. 106, the ventilating sunlight as made by Mr. Strode.

In the matter of internal Fittings, the gas manager, by judgment and tact, can exercise a useful supervision even without the aid of statutory powers; and his advice in regard to the sizes of pipes and the kind of burners and lamps

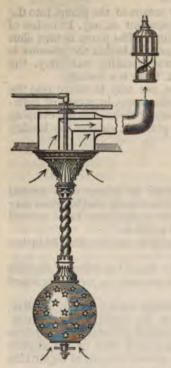


Fig. 105.



Fig. 106.

to be used in different situations will generally be accepted and acted upon.

To obtain the maximum of light from a burner, it is necessary that the pressure, when that is in excess in the mains, as it must necessarily be, should be controlled and regulated in the passage of the gas to the point of ignition.

This cannot be accomplished satisfactorily by checking either the taps on the Fittings, or the stop-cock at the meter, because there is a continual variation of pressure according to the consumption that is in

progress.

The house governor or regulator was invented to achieve that end. It may be fixed on the pipe leading from the meter outlet, or what is better, on the principal pipe supplying each floor level of the premises.

The regulator is automatic in its action; and when weighted to afford the required pressure for all the burners in use, it will continue to give a practically uniform supply, however much the pressure in the mains may vary, or whether the whole or only a portion of the burners being supplied through it may be alight at one time. The "Needle" governor burner of Mr. Peebles, and the "Acme" regulating burner of Wright, are examples of regulation applied close to the point of consumption.

It is a clearly established fact that the lower the pressure (provided there is just sufficient) at which gas can be burned, the better the light. If, instead of being advantageously consumed, the gas is forced through the burners into the atmosphere, the carbon is rapidly oxidized by the excess of air drawn into the flame by the heavy pressure, with the

usual unsatisfactory results as regards illumination.

Dr. Letheby found that a vulcanized india-rubber tube of about 30 feet in length, reduced the power of a weak gas to the extent of nearly 25 per cent., by absorbing the illuminating hydrocarbons.

Varnish to Prevent the Escape of Gas through India-rubber Tubing.

1½ parts treacle.

2 ,, gum arabic. 7 .. white wine.

7 ,, white wine. $3\frac{1}{2}$,, strong alcohol.

First dissolve the treacle and gum in the white wine, and afterwards add the alcohol very slowly, constantly stirring the mixture to prevent the gum from being thrown down.

HANDY RULE

For Estimating (Approximately) the Number of Burners required to Light Churches, Public Halls, and other Large Buildings.

Rule.—The floor area in feet divided by 50 for common gas, and by 70 for cannel gas, will give the number of flat-flame burners required for effective lighting.

Example.—A room is 80 feet long and 56 feet wide. What number of burners is required? Then—

 $80 \times 56 = 4480$ sq. ft. area $\frac{4480}{50} =$ say 90 burners with common gas, consuming 5 c. ft. per hour each.

 $\frac{4480}{70}$ = say 60 burners with cannel gas, consuming 4 c. ft. per hour each.

TABLE

Showing the Loss of Light per cent. through Shades or Globes.

TABLE

Showing the Amount of Light Obstructed by the Use of Globes or Moons.

(Mr. A. H. Wood.)

Light	obstructed	by a clear glass globe about 12 percent	
11	9	a clear globe with slightly ground flowers	
33	"	globes of about the usual pattern . " 35 "	
**	**	globes ground all over , 40 ,,	
77	**	opal globes , 60 ,,	
99	11	painted opal globes ,, 64 ,,	
21	"	common window glass , 9 ,,	

TABLE

Showing the Loss of Light through flat Sheets of Glass of different Qualities and Colours. (Mr. F. H. Storer, U.S. America.)

Description of Glass. T	hicknes	s of Glass.							ss of Light er Cent.
Thick English plate	+ of	an inch.	-	4				100	6.15
Crystal plate	1	**					-		8.61
English crown	į.				1			100	13.08
Double English window glass	1 -	11	16		2		-	-	9.39
Double German*	1			7				-	13.00
Single German	de	,,						TO	4.27
Double German, ground	1	**	16	100	-			1	62-34
Single German	J.	"							65.75
Berkshire (Mass.)	1	**							62.74
Berkshire enamelled - i.e.,									2000
ground only upon portions									
of its surface—small figure .	To of	an inch.							51.23
Orange coloured window glass	18	11			As	use	d		34.48
Purple	1	"			f	or	81		85.11
Ruby ,	1.	"			chi	ure	h		89.62
Green ,	7	"		wi	inde	ows	. 0	ta.	81.97
A porcelain transparency	10	"						10	97.68

The results of the experiments with globes given in the foregoing tables were obtained with the light in a direct line with the photometer disc, and with the defective moons or globes formerly in use, having narrow openings at the bottom. With the improved globes of the present day, the bottom openings of which are 4 to 5 inches diameter, the results more recently obtained by Mr. F. W. Hartley differ from those detailed.

In 1880, Mr. Hartley carried out a series of experiments with ground and plain glass of various kinds, both flat and rounded on their surface, and with the lighting horizontal and overhead.† These experiments are interesting and valuable; but the details are too lengthy to be given, even in outline, here. The general conclusion, however, at which Mr. Hartley arrived is as follows :-

HORIZONTAL LIGHTING.

Sheet Glass.

1. That ordinary sheet glass, apart from thickness, varies in its obstructive power to the passage of light. That the percentage loss increases with the distance of the glass from the flame, and increases also as the light grows stronger.

^{*} Among the Boston dealers, the term "German" is applied to glass of Belgian

manufacture.
† "Observations on Glass as an Obstructor and Reflector of Artificial Light," by
F. W. Hartley, Assoc. Inst. C.E., Journal of Gas Lighting, January, 1881.

- 2. That ground sheet glass, apart from thickness, also varies in obstructive power. That the percentage loss increases with the distance of the glass from the flame, and decreases as the light grows stronger. That the percentage loss depends on which side—clear or ground—is presented to the flame.
- That with flashed opal the losses follow the same law as ground glass for distance from and for power of light.
- 4. That with clear glass as an obstructor of light in front of the flame and clear glass behind as a reflector of light, the reflected light reduces the loss to a degree dependent on the distance of each glass from the flame.

Globes.

- That a clear glass globe obstructs light from an Argand flame, but increases the sensible light from a flat flame.
- 6. That globes of ground glass obstruct less light than sheets of ground glass. That the percentage loss diminishes as the light grows stronger; and is, for an average light, from 18 to 20 per cent.
- That opal globes obstruct an amount of light equal to 33 to 65 per cent.

OVERHEAD LIGHTING.

- That the amount of light yielded by a flame in an angular direction is much less than it yields in a horizontal direction.
- That glass globes with elevated or overhead Argand flames, reduce the power of the light—clear globes, about 3 per cent.; ground globes, about 21 per cent.; and albatrine globes, about 28 per cent.
- 10. That glass globes with flat-flame burners, at a certain elevation and within a certain radius, increase the power of the light clear globes, about 6 per cent.; ground globes, about 9 per cent.; albatrine globes, about 23 per cent.; and German opal globes, about 21 per cent.
- 11. That reflectors greatly increase the power of the light, within a radius dependent on the shape and size of the reflector; the range in the experiments being from 52 to 92 per cent.
- That screens at the base of an Argand flame cause a reduction in the power of the light, whatever be the size and form of the reflector.

LEAD AND COMPOSITION PIPES FOR GAS.

Weights per Yard, and Lengths usually Manufactured.

				L	GHT	•				1				H	eavy	•			
	Diameter Inside.		-	P	ight er ard. oz.			Bund			meter nside.	Weight per Yard. lbs. oz.				Lengths of Bundles usually Manufactured.			
ł	inch.			0	113			80	yards.	1	inch.			0	15			67	yards.
1	,,	•	:	1 2	2 0	•	•	60 32	"	1	"	•	•	1	61 10	٠	•	46 16	"
į	91 99	:	•	2	4			25	"	1	"	:	÷	3	0	:	:	20	"
1	"	:	:	3 4	8 8	:	:	25 26	"	1	"	:	:	8 6	12	:	:	19 20	"
13	,,		•	8 12	0	-		16 10	,,	11	"		•	10	0	•		12	"
1; 2	"	:	:	18	ŏ	:	:	5	"	2	"	:	:	14 21	0	:	:	9 5	"

BRASS TUBE, PLAIN-WEIGHT PER FOOT.

Diameter. Inches. 1-4th			Weights.	ozs.	Diamete Inches. 7-8ths						lbs.	eight. ozs. or 8.00
5-16ths .			.15	2.40	1 inch						.59	9.44
3-8ths .			·19	3.04	11,,						·81	12.96
7-16ths .			·21	8.86	11,						1.00	16.00
1 half .			.25	4.00	12 ,,					:	1.13	17.92
9-16ths .			·31	4.96	2 ,,			-			1.25	20.00
5-8ths .			.37	5.92	01 "	:		:	-	·	1.20	24.00
8-4ths .			.43	6.88	8 ,,	:			:		1.87	29.92

The size of brass and copper tube is measured by the outside diameter.

BRASS TUBE, SPIRAL AND FLUTED-WEIGHT PER FOOT.

Diameter. Inches. 8-8ths					piral eigh oz.				W	uted, eight. oz. 23	Diameter. Inches. 8-4ths					Spira Veigh oz.				Flut Weig	ht.
	•	•	•	•		•	•	•	•	-		•	•	•	•	71	•	•	•		
7-16ths	٠	•	٠	•	34	•	•	•	•	8 1	7-ths .	٠	•	•	•	72	•	•	•	. 1	
1 half					31					34	1 inch					9				. 8	}
9-16ths					44					4	11 ,,					12				. 11	1
5-8ths					5					5	11 ",					15				. 14	į

SOLDERS.

Fine Solder is an alloy of 2 parts of block tin and 1 of lead (melts at 860° Fahr.). This is used for fine work—such as soldering the drums of meters, for pewter, &c.

GLAZING SOLDER.—Equal parts of block tin and lead. Used for

Plumbing Solder.—1 part block tin, 2 lead. For all kinds of plumbers' joints and for tin and zinc.

SOLDER FOR COPPER.-Hard: 3 parts brass, 1 zinc. Soft: 8 brass.

1 zinc.

Brazing Solder or Spelter.—Hard: 1 part copper, 1 zinc. Soft: 4 parts copper, 3 zinc, 1 block tin. For fine brass work: 1 part silver, 8 copper, 8 zinc.

SOLDER FOR STEEL .- 19 parts silver, 3 copper, 1 zinc.

Pewterers' Soft Solder.—2 parts bismuth, 4 lead, 3 tin. Common: 1 part bismuth, 1 lead, 2 tin.

FLUXES FOR SOLDERING.

Iron and steel	Borax or sal ammoniac.
Tinned iron	Resin or chloride of zinc.
Copper and brass	Sal ammoniac or chloride of zinc.
Lead and composition pipes	Resin and sweet oil.
Zine	Chloride of zinc.

FOR TINNING BRASS OR IRON.

doz. muriatic acid.

1 oz. mercury.

½ oz. ground block tin.

Mix together, and dilute the whole with a small quantity of cold water. Apply with the finger or a cork.

BRAZING.

The edges of the articles, either iron or brass, to be brazed are scraped thoroughly clean, covered with the brazing solder or spelter in the form of borings or turnings sprinkled over with powdered borax, and exposed to the heat of a clear fire till the solder flows. A smokeless coke or gas fire is best for the purpose. In brazing iron, a covering of loam is sometimes placed over the solder, to exclude the air, till it melts.

BRONZE.

1 quart common vinegar.
2 ozs. sal ammoniac.
1 oz. blue stone (sulphate of copper).

The sal ammoniac and blue stone are well pounded, and then allowed to dissolve in the vinegar. The solution, when ready, is laid on with a common brush, black-leaded whilst damp, and then polished. Lacquer is then applied as described hereafter.

Green Bronze.

To imitate the antique.

1 quart common vinegar.
2 ozs. verdigris.
1 oz. sal ammoniac.

Boil for a quarter of an hour, filter, through paper, and dilute with water. Immerse the article to be bronzed until it acquires the green tinge desired; then wash carefully, and dry in sawdust.

Bronze Powders.

These can be purchased from any dealer in artists' material. They are prepared as follows:—

Copper Bronze Powder.

Strips of copper are dissolved in nitric acid in a glass vessel, and then strips of iron are added, when the dissolved copper is precipitated in the form of a very fine powder. This powder is washed with water and dried, and is then ready for use.

Gold Bronze Powder or Aurum Mosaicum,

Is the basis of many bronze powders. Any desired colour can be produced by mixing it with the common dry pigments. Thus, a red bronze powder is obtained by grinding red lead with it; and a green by the use of verdigris. It is prepared in the following manner:—

One pound of tin is melted in a crucible, and then poured cautiously into an iron dish containing half a pound of mercury. When cold it is reduced to powder, mixed with seven ounces of flowers of sulphur, and eight ounces of sal ammoniac, and triturated in a mortar. The mixture is then calcined in a flask, which expels the sulphur, mercury, and ammonia, and leaves a residuum in the form and colour of a bright flaky gold powder.

Size for Bronze Powders.

The size is made by boiling four ounces of gum animi to every pound of pure linseed oil in a flask, until the mixture is of the consistency of cream; after which it is diluted with turpentine as

required.

The article to be bronzed is coated, by means of a soft brush, with this size; and when nearly dry, a piece of soft leather is wrapped round the finger, dipped into the powder, and rubbed gently over it; or it may be laid on with a camel's-hair pencil, and then left to dry thoroughly; after which all the loose powder is brushed off.

The bronze may also be mixed with a strong solution of isinglass, and applied in the moist state, like varnish, with a brush. This latter mode, however, is not suitable for articles exposed to the weather.

For Silvering Metals.

Nitrate of silver 10 parts. Common salt 10 ,, Cream of tartar 30 ,,

Moisten with water when ready to apply, and lay the mixture on with a soft brush.

LACQUER AND VARNISH.

The solution of spirits of wine and shellac, known as "simple pale" lacquer, is the basis of most other lacquers. The two ingredients in their proper proportions, as stated below, are put into a jar or bottle, and allowed to remain for forty-eight hours, being briskly shaken three or four times during the interval. At the expiration of the time named, most of the shellac will be dissolved. The mixture is then carefully strained through filtering paper, to free it from grit and other foreign substances, and to remove any particles of undissolved shellac that may remain.

Different tints or shades, producing red, green, yellow, &c., are obtained by mixing with the pale lacquer various colouring ingredients, such as dragon's blood, arnotto, gamboge, turmeric, saffron, &c. The

proper way of adding these is to stir them in a cup with a small quantity of the pale lacquer, afterwards straining the whole through a

piece of thin cloth or gauze, and filtering if necessary.

The article to be lacquered is heated slightly by means of a steam kettle or stove; or it may be held over a hot iron plate till just as hot as to allow of its being touched by the finger without burning. The heat must not be greater than this. The lacquer is then applied with a soft camel's-hair brush.

Simple Pale Lacquer.

1 pint of spirits of wine.

4 ozs. of shellac.

Fine Pale Lacquer.

1 pint of spirits of wine.

1 oz. of pure white shellac.

1 dr. of gamboge.

2 drs. of Cape aloes.

Fine Pale Lacquer, for Silvered or Tinned Work.

1 pint of spirits of wine.

1 oz. of pure white shellac.

Gold Lacquer.

1 pint of spirits of wine.

3 ozs. of shellac.

1 oz. of turmeric.

2 drs. of arnotto.

2 drs. of saffron.

Deep Gold Lacquer.

1 pint of spirits of wine.

8 ozs. of shellac.

1 oz. of turmeric.

4 drs. of dragon's blood.

Red Lacquer.

1 pint of spirits of wine.

4 ozs. of shellac.

4 drs. of dragon's blood.

1 dr. of gamboge.

Yellow Lacquer.

1 pint of spirits of wine.

2 ozs. of shellac.

2 drs. of gamboge.

4 drs. of Cape aloes.

Green Lacquer for Bronze.

1 pint of spirits of wine.

4 ozs. of shellac.

4 drs. of turmeric.

1 dr. of gamboge.

Iron Lacquer.

1 quart of turpentine.

🛂 lb. of asphalte.

2 ozs. of shellac.

To Clean Old Brass Work for Lacquering.

Boil a strong lye of wood ashes, and strengthen with soap lees; put in the brass work, and the old lacquer will come off. Next dip it in a solution of nitric acid and water, strong enough to remove the dirt; wash it immediately in clean water; dry well, and lacquer.

Varnish for Iron Work.

Boil a quantity of gas tar for four or five hours, till it runs as thin as water; add one quart of turpentine to a gallon of the tar, and boil another half hour. Apply the varnish whilst hot.

Golden Varnish.

Pulverize 1 drachm of saffron and ½ a drachm of dragon's blood, and put them into 1 pint of spirits of wine. Add 2 ounces of gum shellac and 2 drachms of Seccotrine aloes. Dissolve the whole by gentle heat. Yellow painted work, varnished with this mixture, will appear almost equal to gold.

Varnish for Cutdoor Wood Work.

Boil together one gallon of gas tar and $2\frac{1}{2}$ lbs. of white copperas. Apply whilst hot.

Glue Cement to Resist Moisture.

1 part glue.

1 part black resin.

1 part red ochre.

Mix with the least possible quantity of water.

PUBLIC ILLUMINATIONS.

In provincial towns the Gas Manager is usually called upon to arrange and superintend the Illuminations that are given to celebrate any great national or local event. On such occasions the following particulars will be found useful:—

Mode of Supply and Price of Gas.

Illumination Devices are generally supplied with gas direct from the main, without the intervention of a meter to register the consumption. Where the Illuminations are anything like universal, the fixing of meters is altogether impracticable.

Taking the consumption of each jet * to be at the rate of one cubic foot of gas per hour, which is a fair average, including loss by leakage and trial lighting, the following will be the rate of charge according to the price per 1000 cubic feet:—

At 6s. 6d. per 1000, .078 of a penny per jet * per hour.

6 5	**	-077	**	"	,,,
6 4	**	.076	. ,,	***	,,
6 8	**	.075	100	3 99	,,
6 2	**	.074		""	,,
6 1	511	.073	= 00	11	37
6 0	***	.072	73	**	11
5 11	33	.071		111	,,
5 10	**	.070	Length	,,	11
5 9	11	.069	1000	""	**
5 8	"	.068	.,		**
5 7		.067	100	**	
5 6	"	.066	100	31	"
0 0	**	000		**	**

^{*} By the term "jet," as here used, is meant the small gas-flame at each hole drilled or punched in the pipes forming the different devices.

					
	d. per 1000,	•065 of	a penny	per jet p	er hour.
5 4		.064	"	"	99
5 8		.068	**	,,	,,
5 9	_ ,,	.062	,,	**	**
5 1	- ,,	.061	. ,,	"	**
5 (.060	**	"	**
4 11		.059	"	"	**
4 10		.058	**	,,	"
4 8		·057	**	"	"
4 8		.056	"	**	"
4 7		.055	,,	,,	"
4 6		·054	"	"	,,
4 8	• • • • • • • • • • • • • • • • • • • •	·058	,,	,,	**
4 4	• • • • • • • • • • • • • • • • • • • •	·05 2	,,	,,	**
4 8		.051	,,	"	,,
4 2		·0 5 0	. ,,	,,	**
4 1	l ,,	·049	,,	,,	**
4 () ,,	·048	,,	,,	,,
8 11	l ,,	·047	**	,,	**
8 10) ,,	·046	,,	**	,,
8 8) ,,	·045	,,	,,	,,
8 8	3 ,,	·044	,,	,,	,,
8 7	7,,	.048	,,	"	,,
8 6		·042	,,	,,	,,
8 8	5 ,,	·041	,,	,,	,,
8 4		·040	,,	"	,,
8 8		$\cdot 039$,,	,,	,,
8 9	2 ,,	.088	,,	,,	,,
8 1		·087	,,	,,	,,
3 (.086	,,	,,	,,
2 11		.085	,,	,,	••
2 10		.084	,,	,,	,,
2 2		.088	,,	,,	,,
2 8	• • • • • • • • • • • • • • • • • • • •	.082	"	"	,,
$\overline{2}$ 7		.081	,,	,,	"
2 6		.080	,,	,,	"
2 8		.029	"	,,	"
2 4		.028	,,	,,	11
2 8	- "	.027	"	••	,,
2 2	· ·	.026	,,	• • • • • • • • • • • • • • • • • • • •	,,
2 1		.025	"	"	,,
2 (`	.024	,,	"	31
\	,,,		,,	• • • • • • • • • • • • • • • • • • • •	••

When the ordinary No. 1, 2, and 8 fish-tail burners are employed,

the consumption may be reckoned at the rate of 3, 4, and 5 cubic feet per hour each respectively, and charged accordingly.

It is proper to stipulate that no Illumination should amount to less

than 50s.

SERVICE OR SUPPLY PIPES.

It is the usual rule for the Gas Authorities to convey at their own cost a service-pipe from the main, and from 8 to 12 feet up the front of the building to be illuminated, provided the whole length of pipe required does not exceed 36 feet. A charge is made for any additional length. The expense of fixing the Devices in their position is also charged. To the end of the pipe in front of the building a stop-cock is attached for shutting off or regulating the supply of gas.

Care should be taken to have the pipes of ample capacity, other-

wise the Illumination will be poor and ineffective.

When the building to be illuminated is large, it is advisable to run up a service-pipe at each end, and one in the centre, connecting them together in the front; each pipe, of course, having a distinct connection with the main in the street.

The service-pipes should be laid with a slight fall to the main; and the use of all abrupt angles—such as square elbows—should be

avoided, bends being employed instead.

The service-pipes are temporary only, being lent by the Gas Authorities, and are removed by them when the Illuminations are over.

DEVICES.

The Devices are paid for by the private inhabitants, or the Local Authorities, or by both, as the case may be.

They may consist of-

Initial and other letters, single lined—thus, A —and double-

lined—thus,

Mottoes—straight, curved, or circular.
Lanterns with coloured devices.
Laurel Scrolls.
Garlands,
Festoons.
True Lovers' Knots.
Stars of various kinds.
Mitres.

Crescents.

Crosses.

Plumes, as Prince of Wales' Feathers.

Aureoles.

Crowns.

Shields.

Anchors.

Masonic Emblems.

Heraldic Crests.

Corporation Arms.

Other Devices suitable to the particular occasion.

The Devices are made by the manufacturers of gas-fittings, wroughtiron tubing, and others, and are supplied to Gas Authorities and the Trade at about the following prices:—

Single-lined Letters, in Iron or Copper, fitted with Strong Union Couplings.

Length o	of Lett	er.			Size of l §ths inch	Inlet.			11s.	Pri 0d.	esch.
	,,				ž "				12	6	.,
30	,,				3 ,,				13	6	"
36	,,				į ,.				15	0	11
42	,,				j ,,				18	0	"
49	,,				<u> </u>				21	0	"
5.4	,,				ā ,,				25	0	"
AN.	••				ā ,,				30	0	**

Double-lined Letters, in Iron or Copper, fitted with Strong Union Couplings.

Length 18 is	of Lett	er.			Size of Inle	t. ore .			12s.	Pri 6d.	ce. each.
24	**				3 ,,				15	0	**
30	"				<u>,</u>				17	6	**
36	"				1 ,,				20	0	**
42	**				4 ,,				24	0	"
48	,,				ā ;;				28	0	"
54	11				1,				33	0	"
60	**				1				40	0	,,

Brunswick Stars and Stars with Eight Points, Made of Wrought-Iron Welded Pipe, and fitted with Strong Union Couplings.

Dia	meter.		Size o	f Inlet.		1			with ntre	81			with entr	в.	P			with entre.	
							£	8.	d.		£	8.	d.			£	8.	d.	
8	feet		1 in	ch bore			2	0	0		2	2	0			2	17	0	
4	,,		11	,,			2	12	0		2	15	0			3	10	0	
5	"		1 <u>‡</u>	,,			3	6	6		8	10	0			4	5	0	
6	"		1 1	"			4	15	0		5	0	0			5	15	0	
7	"		13	"			6	3	6		6	10	0			7	5	0	
Ŕ	,,		2	.,	_	_	7	7	Ó		7	15	0			8	10	0	

Crowns and Plumes cost about one-third more than Stars.

Scrolls, Garlands, Heraldic Crests, and other Devices, at prices varying according to the elaboration of the design.

Wrought-iron pipes, drilled, and with Star jets inserted, are sup-

plied at about the ordinary list price.

The Devices may be "home-made," and if so will be less expensive; but unless constructed by skilled and tasteful workmen, they will present a scraggy, irregular appearance when lighted up.

ILLUMINATED BORDERS.

A very pretty effect, easily managed, and one that gives a rich fulness to the central Illumination of a building, is obtained by running wrought-iron tubing along the principal angles, with holes drilled in the tube at distances about 6 inches apart, and having small jets or star burners inserted. The burners may be placed wider apart, and globes made use of. These prevent the lights from being extinguished by the wind, and also heighten the general effect. In this case a short piece of brass tube, with elbow-socket and gallery, must be inserted. Globes ground all over, or white opal globes, or white and coloured globes arranged alternately, show to the best advantage.

COLOURED FIRES.

A display of Coloured Fires, at intervals, from prominent points of elevation, adds greatly to the effect of an Illumination.

The following are some excellent recipes for their production:

Lilac Fire.

									Oz.	Drms.
Chlorate of Potash.						14	49	parts,	or 7	13
Sulphur									4	0
Chalk									3	3
Black oxide of copper									1	0

This composition weighs 1 lb., and costs 2s. 3d.

Purple Fire.

									Oz.	Drms.
Chlorate of potash			. "					43 parts,	or 6	14
Nitrate of potash (saltpetre								221 ,,		10
Sulphur									3	10
Black oxide of copper									1	9
Black sulphide of mercury	(Ethic	ор'в	mi	neral) . ×			2 ,	0	5

Weight, 11b.; cost, 2a. 3d.

		Yellow	Fire.				O- D
Nitrate of soda Sulphur Charcoal or lamp black .	::	t, 1 lb.;		 s. 6d.		75 parts, 0 19 ,, 6 ,,	
	Blue	or Be	ngal I	ire.			
Dry nitrate of potash Sulphur	: :	ght, 1lb		: : : : 1s.	: :	6 parts, 0 2 ,, 1 ,,	Oz. Drms. or 10 10½ 8 9½ 1 12
		Or	•				0. 5
Ammonic sulphate of cop Chlorate of potash	: :		: :	 s. 8d.	: :	8 parts, 6 6 ", 1 ",	Oz. Drms. or 8 8 6 7 1 1
			<i>r</i> :				
Nitrate of baryta Sulphur Chlorate of potash	· · ·	Green		 		77 parts, 18 ", 5 ", 8 ", 2 ",	Os. Drms. or 12
		Oı					
Nitrate of baryta Shellac	 Weigh			 s. 6d.	: :	9 parts, 6 8 ,, 1½ ,,	Oz. Drms. or 10 10 8 9 1 18
	(Trimson	Fire	_			
Nitrate of strontia. Sulphur Chlorate of potash. Charcoal or lamp black		it, 1 lb.;				80 parts, 6 221 ,, 20 ,, 5 ,,	Os. Drms. or 10
		Red I	Fire.				
CONTRACTOR AND AND A		: :	• • •	· · · · · · · · · · · · · · · · · · ·		40 parts, 0 13 " 5 " 8 ", 4 ",	Oz. Drms. or 10 0
	Weigh	t, 1 lb.	cost, 1	s. 6d.			

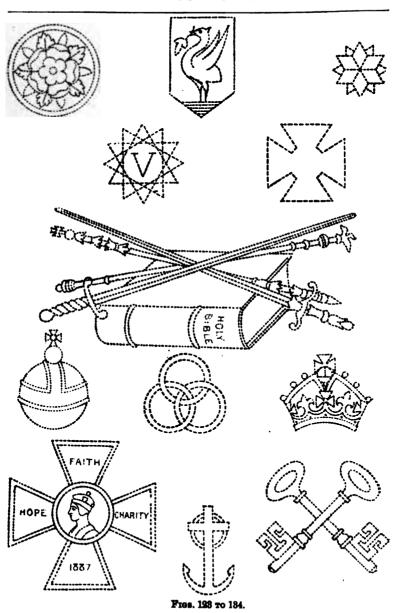
				1		1 9	Or							
Nitrate of strontia														9 parts, or 10 10
Shellac			:	:	:	:	:			1		:	:	3 " 3 9 11 " 1 13
			W	eig	ht,	1 1b	.;	cost	, 16	s. 6	d.			-00
				Wh	ite	In	ıdi	an	F_{i}	ire.				The same of
Nitrate of notash														24 parts, or 11 10
Nitrate of potash . Sulphur Sulphide of arsenic	Re	alo	ari									÷.		7 , 3 6
bulpulate of account	1200	ar M.		Wei									•	

In no case should the chlorate of potash be ground along with the sulphur, as ignition, caused by the friction, might ensue.

The ingredients should be reduced to the finest powder (excepting the shellac, which should only be beaten into small fragments) by bruising them in a mortar made of hard wood, the chlorate of potash being ground separately. They should then be intimately mixed together, by passing them three or four times through a hair sieve. When mixed, keep the material in a close-stoppered bottle, to prevent spontaneous combustion. All the ingredients must be perfectly dry to insure success.

The mixtures are best fired in hemispherical dishes, or ladles made of beaten iron, about 5 inches diameter and $2\frac{1}{2}$ inches deep in the centre. The fumes arising from the different fires should be avoided.

A pound in weight of any of the mixtures is sufficient for a fire (though any quantity may be used); and the cost varies from 1s. to 2s. 3d. each. The ingredients can be obtained from almost any chemist and druggist.

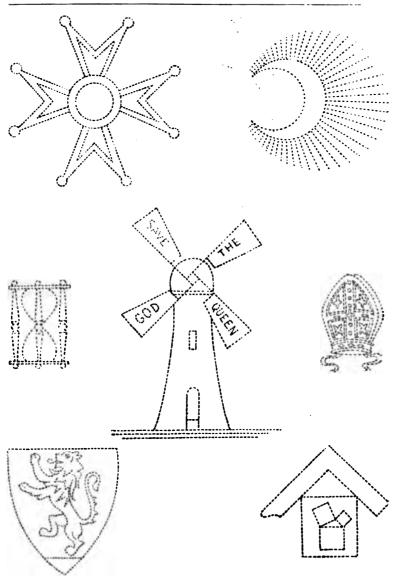




RULE BRITANNIA



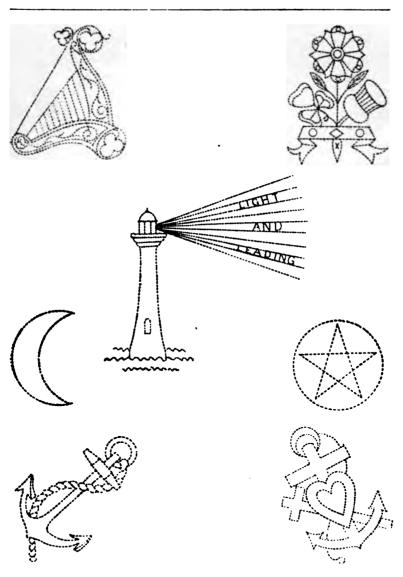
BRITANNIA RULES THE WAVES



Figs. 137 to 148.



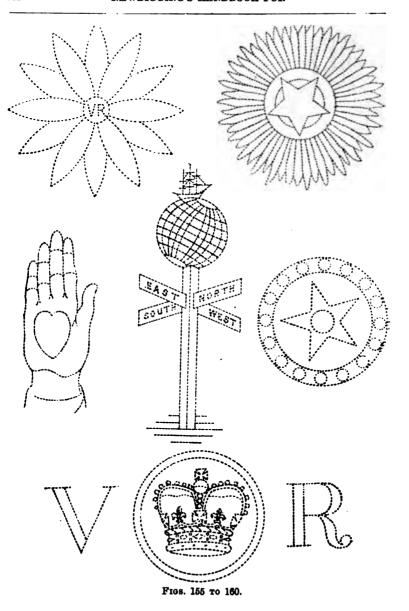
Figs. 164 and 145.

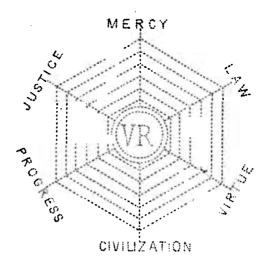


Figs. 146 to 152.





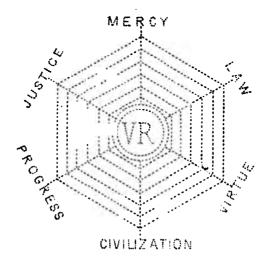




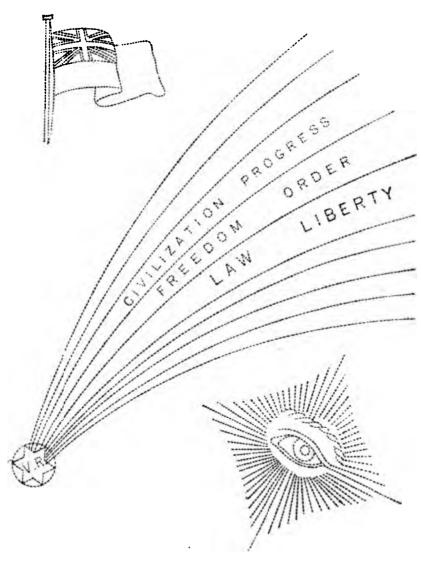


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NEWBIGGING'S HANDBOOK FOR





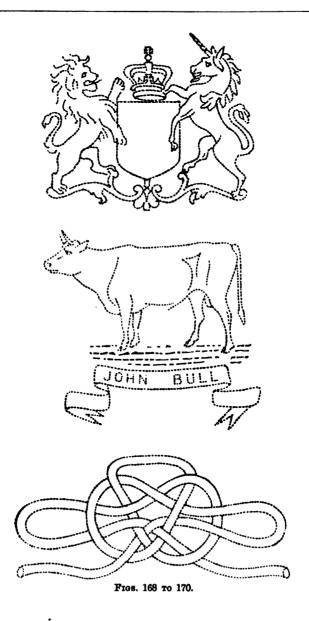


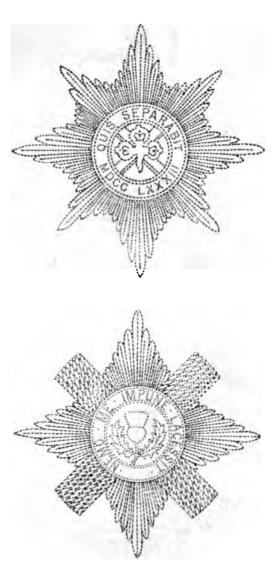
Figs. 168 To 165.

GAS ENGINEERS AND MANAGERS.



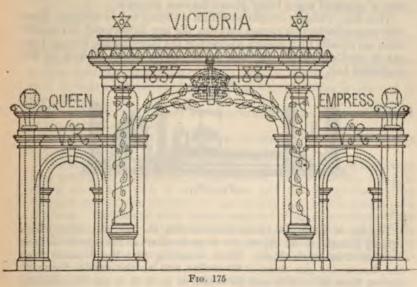
Figs. 166 and 167.





Figs. 171 and 172.





ILLUMINATING POWER.

For testing the Illuminating Power of gas in accordance with the statutory provisions, the Bunsen photometer is used; and the Letheby-Bunsen form of the apparatus (Fig. 176) is that generally adopted.

The standard candle is a sperm candle, six of which weigh 1 lb.,

and each burns 120 grains of sperm per hour.

The gas is supplied through an experimental meter, and burns at one end of a graduated bar, and the candle at the other; a movable

disc of prepared paper being placed between the two.

This disc, which is contained within a sliding box or carriage, fitted with two reflectors, is moved between the two lights until its opposite sides are equally illuminated, whereupon the Illuminating Power of the gas is read off by the operator on inspection of the figures on the graduated bar.



Fig. 176.

The bar is graduated in accordance with the law that lights which equally illuminate an object are to each other as the square of their distance, from such object. Thus, assuming that the distance from the disc to the gas flame is 80 inches, and to the candle flame 20 inches, then $80^{\circ}=6400$, and $20^{\circ}=400$, or as 16 to 1, the Illuminating value of the gas as compared with the candle.

The following apparatus are also required, viz.:—A governor to regulate the gas pressure; a clock striking every minute; a King's pressure-gauge; a candle balance and weights; a thermometer and a

barometer.

The apparatus is arranged and fixed on a substantially made table, placed in the photometer room. This room may be conveniently made about 10 or 12 feet square, and should be ventilated; but currents of air which would affect the steadiness of the gas and candle flame must be guarded against. Provision is made to exclude the daylight; and the walls are coloured a dull black.

Statutory Regulations for Testing the Illuminating Power of Gas.

The provisions in Schedule A of the Gas-Works Clauses Act, 1871, in regard to the apparatus for, and the mode of testing the Illuminating Power of gas, are as follows:—

Regulations in respect of Testing Apparatus.—The apparatus for testing the Illuminating Power of the gas shall consist of the improved form of Bunsen's photometer, known as Letheby's open 60-inch photometer, or Evans's enclosed 100-inch photometer, together with a proper meter, minute clock, governor, pressure gauge, and balance.

The burner to be used for testing the gas shall be such as shall be

prescribed.

The candles used for testing the gas shall be sperm candles of six to

the pound, and two candles shall be used together.

Mode of Testing for Illuminating Power.—The gas in the photometer is to be lighted at least fifteen minutes before the testings begin; and it is to be kept continuously burning from the beginning to the end of the tests.

Each testing shall include ten observations of the photometer, made

at intervals of a minute.

The consumption of the gas is to be carefully adjusted to 5 cubic

feet per hour.

The candles are to be lighted at least ten minutes before beginning each testing, so as to arrive at their normal rate of burning, which is shown when the wick is slightly bent, and the tip glowing. The standard rate of consumption for the candles shall be 120 grains each per hour. Before and after making each set of ten observations of the photometer, the Gas Examiner shall weigh the candles; and if the combustion shall have been more or less per candle than 120 grains per hour, he shall make and record the calculations requisite to neutralize the effects of this difference.

The average of each set of ten observations is to be taken as repre-

senting the Illuminating Power of that testing.

Instructions of the London Gas Referees as to the Times and Mode of Testing for Illuminating Power.

The testings for Illuminating Power shall be three in number daily.

The Photometers to be used in the testing places shall be the improved forms of the Bunsen Photometer, prescribed and certified by the Referees.

The burner attached to the Photometer shall be a standard burner corresponding to that which has been deposited with the Warden of

the Standards in accordance with Section 37 of The Gaslight and Coke Company's Act, 1876. A description of the standard burners to be used for testing common gas and cannel gas respectively is given. (See page 335.)

The gas in the Photometer is to be kept burning for at least fifteen

minutes before any testing is made.

The disc used in the Photometer shall be either the Leeson or the

Bunsen disc. The chimneys are to be cleaned daily.

The candles shall be such as are described in Section 25 of the Metropolis Gas Act of 1860—namely, sperm candles of six to the pound, each burning 120 grains an hour. Two of these candles shall be used together.

Each testing shall consist of ten observations of the Photometer, made at intervals of one minute. The average of each set of ten observations is to be taken as representing the Illuminating Power for

that testing.

The rate of burning of the gas in each burner shall be 5 cubic feet per hour—a rate of consumption which is shown by the long hand of the meter making exactly one revolution per minute for several minutes

consecutively.

The candles are to be lighted at least ten minutes before the beginning of each testing, so as to have attained their normal rate of burning. Before and after making each testing, the Gas Examiner shall weigh the candles; and if the rate of consumption per candle shall not have exceeded 126 grains per hour, or fallen short of 114 grains per hour, he shall make, and record in a book to be kept for the purpose, the calculations requisite to neutralize the effects of this difference. If the rate of consumption shall have varied from the prescribed rate beyond the above-named limits, the testing is to be rejected, and a fresh testing made.

Instead of weighing the candles, the Gas Examiner may observe the time in which 40 grains are burnt. This must not exceed 10.5, or fall

short of 9.5 minutes.

The Gas Examiner shall, at least once a week, compare the meter-

clock with the standard-clock in each testing-place.

At the time of each testing the Gas Examiner shall observe and record the temperature of the gas, as shown by the thermometers attached to the meters, and also the height of the barometer. The volumes of the gas operated upon during the testings may be corrected from these data (the standard of comparison being, for the barometer. 30 inches; and for the thermometer, 60 degrees) by means of the Table. (See pages 336 and 337). Suppose, for example, the thermometer stands at 54 degrees, and the barometer at 30.3 inches: multiply the quantity of gas consumed by the corresponding tabular

number—the product will be the corrected volume of the gas—i.e., the volume the gas would have occupied when measured over water at the standard temperature and pressure. Thus—

Volume of gas consumed 5 cubic feet. Tabular number for barometer and thermometer 1.025.

Then $1.025 \times 5 = 5.125$, the corrected volume.

Instead of thus correcting the volume of gas consumed, the same object may be attained by dividing the observed Illuminating Power by the tabular number, or in the manner described on page 159.

The Gas Examiner shall record his observations and calculations for determining Illuminating Power in the form prescribed on page

338.

The calculations for working out the corrections, &c., for the Illuminating Power of the gas proceed in the following manner:—Add the observations together, and divide the sum by 10, to get the average; then, as two candles are used, multiply by two, to get the Illuminating Power of the gas if tried against one candle. Then, as the standard rate of the consumption of the candles (viz., 120 grains) is to the average number of grains consumed by each per hour, so is the above-obtained number to the actual Illuminating Power. Finally, make the correction for temperature and pressure, by dividing the Illuminating Power by the tabular number. For example (taking the tabular number as 1.025):—

Observations-

```
1st minute-7.8 Consumption of the 2 candles in
 2nd ,,
              7.8
                    10 minutes,
 3rd
              8.1
                     = 41 grains.
      - 22
              8.2
 4th
                         3
       25
              8.3
 5th
      22
 6th
             8.5
                      123 = consumption of 1
      28
 7th
              8.6
                    candle per hour.
       11
 8th
              8.4
      22
              8.3
 9th
10th
              8.6
         10)82.6
```

Average, by 2 candles = 8.26

Average, by 1 candle=16.52

```
Average, by 1 candle = 16.52
      Consumption by 1
                             128 grains.
        candle per hour
                            4956
                           8804
                          1852
      Standard con-
        sumption . 120)208196
      Correction for
      • temp. & pres. 1025)16988 (16.5] = corrected Illum. Power
                                            in candles.
                           1025
                            6688
                            6150
                             5880
  The foregoing calculation can be shortened as follows, which is the
form prescribed on page 338 :-
Average, by 2 candles (arrived at as
                                      = 8·26
  shown on page 888).
Consumption by 2 candles in 10 minutes
                                          41 grains.
                                         826
                                       8804
                                    2)83866
         Tabular number
                                1025) 16988 (16.5 = corrected Illum.
                                       1025
                                                          Power in
                                                          candles.
                                        6683
                                        6150
                                         5880
```

The Standard Burner.

The burner which has been adopted as the Standard burner for testing common gas was designed by Mr. Sugg, and was called by him "Sugg's London Argand, No. 1."

A is appended, (Fig. 177), in which A represents section, half size, a supply-pipe, B the gallery, C the cone, D the steatite chamber, E the chimney.

The following are the dimensions of	those
parts of the burner upon which its	
depends:—	Inch.
Diameter of supply-pipes	0.08
External diameter of annular steatite	0 00
chamber	0.84
Internal diameter of annular steatite	
chamber	0.48
Number of holes 24	
Diameter of each hole	0.045
Internal diameter of cone—	
At the bottom	1.5
At the top	1.08
Height of upper surface of cone and	
of steatite chamber above floor of	
gallery	0.75
Height of glass chimney	6
Internal diameter of chimney	
ml - Ct - Jan Jan bear on fact to the	T

The Standard burner for testing cannel gas is a steatite batswing burner, consisting of a cylindrical stem, the top of which is divided by a slit of uniform width

by a site of dimorin widen.	Inch.
External diameter of top of stem	0.31
Internal diameter of stem	0.17
Width of slit	0.02
Depth of slit	0.15



TABLE to facilitate the Correction of the Volume of Gas at

BAR.	THER. 40°	42°	440	46°	48°	50°	520	54°	560	58°	60°
28.0	-979	-974	-970	.965	.960	•956	•951	.946	.942	-937	-932
28.1	.983	.978	•978	.969	.964	.959	1955	.951	1945	.941	-936
28.2	-986	-981	.977	.972	-967	.963	.958	.953	.949	•944	1939
28.3	.990	.985	-980	.976	•971	•966	.961	.957	.952	+947	942
28.4	.993	-988	984	.979	.974	.970	•965	•960	*955	951	*946
28.5	-997	-992	•987	•983	-978	.973	.968	.964	.959	954	-949
28.6	1.001	+995	991	.986	.981	.977	.972	1967	.962	•958	.953
28.7	1.004	+999	+994	.990	.985	.980	.975	.970	966	.961	.956
28.8	1.007	1.003	-998	-993	.988	.984	.979	.974	:969	•964	1959
28.9	1.011	1.006	1.001	•997	.992	.987	.982	.977	-973	•968	*963
29.0	1.014	1.010	1.005	1.000	.995	:990	.986	•981	-976	•971	966
29.1	1.018	1.013	1.008	1.004	.999	•994	.989	•984	.979	-975	-969
29.2	1.021	1.017	1.012	1.007	1.002	997	.992	.988	982	-978	-973
29.3	1.025	1.020	1.015	1.011	1.006	1.001	•996	•991	•986	-981	976
29.4	1.028	1.024	1.019	1.014	1,000	1.004	.999	•995	-990	•985	*980
29.5	1.032	1.027	1.022	1.018	1.013	1.008	1.003	+998	-993	.988	.983
29.6	1.036	1.031	1.026	1.021	1.016	1.011	1.006	1.001	.996	.992	.986
29.7	1.039	1.034	1.029	1.025	1.019	1.015	1.010	1.005	1.000	.995	.990
29.8	1.043	1.038	1.033	1.028	1.023	1.018	1.013	1.008	1.003	-998	.993
29.9	1.046	1.041	1.036	1.031	1.026	1.022	1.017	1.012	1.007	1.002	.997
30.0	1.050	1.045	1.040	1.035	1.030	1.025	1.020	1.015	1.010	1.005	1.000
30.1	1.053	1.048	1.043	1:038	1:033	1.029	1.024	1.019	1.014	1.009	1.003
30.2	1.057	1.052	1.047	1:042	1.037	1:032	1.027	1.022	1.017	1.012	1.007
30.3	1.060	1.055	1.050	1:045	1.040	1.036	1.030	1.025	1.020	1.012	1:010
30.4	1.064	1.059	1.054	1.049	1.044	1.039	1.034	1:029	1.024	1.019	1.014
30.5	1.067	1.062	1.057	1.052	1.047	1.042	1.037	1.032	1.027	1.022	1.017
30.6	1.071	1.066	1.061	1.056	1.051	1.046	1.041	1.086	1.031	1.026	1.020
30.7	1.074	1.069	1.064	1.059	1.054	1.049	1.044	1.039	1:034	1.029	1.024
30.8	1.078	1.073	1.068	1.063	1.058	1.053	1.048	1.043	1.037	1.032	1.027
30.9	1.081	1.076	1.071	1.066	1.061	1.056	1.051	1.046	1.041	1.036	1.031
81.0	1.085	1.080	1.075	1.070	1.065	1.060	1.055	1.049	1.044	1.039	1.034

^{**} The numbers in the above table have been re-calculated from the formula perature on the Fabrenheit scale, and a the tension of aqueous vapour at t° . at 60° and 30 inches pressure, V = v n.

different Temperatures and under different Atmospheric Pressures.

BAR.	THER 62°	640	660	680	700	720	740	760	780	80°	82°	840
28.0	•927	-922	-917	.912	•907	•902	.897	-892	-887	-881	.875	.870
28.1	.930	1926	921	-916	.911	*905	.900	*895	*890	*884	.879	'878
28.2	.934	*929	924	.919	-914	.909	.904	.898	*893	*887	'882	.876
28.3	.937	.932	.928	-922	.917	.912	.907	.902	-896	.891	*885	.880
28.4	-941	.936	.931	.926	.921	.915	*910	.905	-900	.894	*888	.883
28.5	.944	-939	.934	-929	.924	-919	914	•908	.903	-897	.892	.886
8.6	-947	943	•938	-932	1927	-922	-917	.912	.906	-901	*895	.889
8.7	.951	*946	•941	.936	.931	.925	.920	.915	.909	.904	.898	.893
8.8	.954	-949	-944	.939	.934	.929	.924	•918	•913	.907	.901	-896
8.9	-958	•953	.948	.942	.937	.932	*927	.921	.916	.910	.905	.899
9.0	-961	.956	.951	946	-941	.935	•930	.925	.919	1914	.908	.903
9-1	.964	.959	954	.949	.944	.939	.933	.928	.923	-917	.911	.906
9.2	.968	•963	.958	-952	•947	-942	1937	.931	.926	.920	•914	.909
9.8	971	-966	.961	-956	.950	.945	+940	.935	•929	-923	918	.912
9.4	.975	+969	.964	•959	.954	.949	*943	.938	.932	-927	.921	.915
9.5	.978	*973	•968	.962	.957	.952	.947	.941	•936	-930	.924	.919
9.6	.981	•976	.971	-966	.960	-955	*950	.944	.939	-933	.927	922
9.7	-985	•980	.974	.969	1964	•959	.953	*948	.942	.937	.931	-925
9.8	-988	.983	.978	.972	*967	.962	-957	-951	.946	-940	.934	.928
9.9	.991	-986	1981	-976	.970	.965	*960	*954	.949	•943	-937	.932
0.0	.995	-990	•985	.979	.974	.968	.963	.958	.952	.946	941	.935
0.1	-998	.993	-988	•983	-977	.972	1966	.961	.955	.950	-944	-938
0.2 1	-002	-996	.991	•986	•980	-975	1970	964	-959	.953	947	.941
0.3 1	.005	1.000	.995	+989	.984	-978	•973	.968	.962	.956	.950	.945
0.4 1	-008	1.003	•998	•993	.987	.982	.976	.971	*965	.959	.954	.948
0.5 1	.012	1.006	1.001	.996	.990	-985	.980	.974	969	-963	-957	.951
0.6 1	.015	1.010	1.005	-999	-994	.988	1983	.977	.972	.966	.960	954
0.7 1	.018	1.013	1.008	1.003	.997	1992	•986	.981	975	.969	•963	.957
0.8	.022	1.017	1.011	1.006	1.000	.995	•990	.984	.978	.972	.967	.961
0.9 1	-025	1.020	1.015	1.009	1.004	-998	•993	-987	.982	•976	.970	•964
1.0 1	*029	1.023	1.018	1.013	1.007	1.002	•996	•991	-985	•979	•973	1967

 $n=rac{17\cdot 64\ (h-a)}{460+t}$, where h is the height of the barometer in inches, t the tem-If v is any volume at t° and h inches pressure, and V the corresponding volume

NEWBIGGING'S HANDBOOK FOR

Barometer	Thermo	DateT	'abular Number18
Hour.	-	-	
	Consumption of sperm by two candles in ten min.	Consumption of sperm by two candles in ten min.) Observations.	Consumption of sperm by two candles in ten min. Observations.
Observations	1st min.	1st min.	1st min
taken at intervals of	2nd "	2nd ,,	2nd "
one minute.	3rd "	- 3rd "	- 3rd "
	4th ,,	- 4th "	- 4th "
	5th "	5th ,,	5th ,,
	6th ,,	- 6th "	6th ,,
	7th ,,	7th "	
	8th "	- 8th "	8th "
	9th ,,	9th "	9th ,,
	10th ,,	10th "	10th ,,
Here multiply the number obtained by the number of grains con- sumed by the two candles in ten minutes and divide by 2 Or divide by the number of minutes in which 40 grs. were consumed.		2)	2)
Illum. Power	r at	Tabular number)	(= Corrected Average Illum. Power
" "			for the
Divide the Illuminating the tabular corresponding Temperate Pressure: the will be the c Illuminating	Power by number g to Mean pre and e quotient operacted Power for	* 10/10/10	day.
Average Illi	ay.	Candles.	Gas Examiner.

The Meters used for Measuring the Gas Consumed in Making the Various Testings.

The meters used for measuring the gas consumed in making the various testings, having been certified by the Referees, shall, at periods of not less than seven days, be proved by the Gas Examiners by means of the Referees' cubic-foot measure—a description of which apparatus, with directions how to use it, is given below. Should a meter show any variation, water must be added or withdrawn until the meter is correct. Every testing place shall have the above-mentioned apparatus, so that the Gas Examiner may employ it whenever he thinks necessary.

No meter other than a wet one shall be used in testing the gas under

these instructions.

The Gas Referees' Cubic-Foot Measure.

Description of the Cubic-Foot Measure; the method of fixing it; and directions for verifying the accuracy of the Meters connected with the Photometers, and also (see page 159) with the Sulphur and Ammonia Tests.

T.

This instrument (Fig. 178) is a vessel in form like an elongated egg, made of hardened tin about one quarter of an inch thick, fitted at each end with a narrow glass tube, the joints being made sound with india-rubber packing. The instrument stands in a vertical position, firmly fixed to a strong plank.

At the top of the instrument is a three-way cock, marked on the head of the key with a T, each arm of which shows the direction of a way through the plug; and in the side of this cock there is a small hole or vent, which serves to admit the air when the measure is to be emptied of water. When the T is in its ordinary position communication is closed between the measure and the tube leading from it to the meters, but is open to the external air; with the H in this position (i.e., with the stem pointing to the opposite side of the cock to that in which the vent is drilled), the measure is open to the meters and shut to the air.

At the bottom of the instrument there are two cocks—the small one, when opened, admits water into the measure; the large one, when opened, allows the water to be run off. The former of these cocks is provided with a lever-key, in order to regulate, with greater nicety, the entrance of the water into the measure.



Fig. 178.

The cock at the top of the measure is continued by a tin pipe in the form of an arch (bending down to meet the pipe leading to the meters); and at the farther end of the arch, there is a piece of glass tube, in which a thermometer is hung to show the temperature of

the air passing from the measure into the meter.

Affixed round each of the glass tubes fitted to the upper and lower part of the measure, there is a narrow strip of paper, which indicates the exact measure of one cubic foot, as tested by the Exchequer standard cubic-foot bottle—the upper edge of both strips of paper being the true water-line of the measure.

TT

The instrument should be in communication with a tank of water

fed by a self-acting supply.

The lower water-level of the tank should be even with the top of the strip of paper marking the "full" line of the vessel; and it is advantageous that the upper water level should be below the plug of the three-way cock on the measure.

Ш.

To verify the meters employed in ascertaining the consumption of gas in the photometers, or those used in the sulphur or ammonia

tests, the mode of procedure is as follows :-

Turn the three-way cock at the top of the instrument so as to leave the vent open to the air; and shut the large cock at the bottom of the apparatus. Then open the small lever cock, and allow sufficient water to flow in to fill the lower glass tube up to the water-line. Then turn the upper cock so as to close the vent, while opening the way to the meters.

Next open the cock of the meter which is to be tested—taking care that all the other meters are closed to the cubic-foot measure. Note the exact position of the index hands—i.e., both the long hand and the 1-foot hand, if it be a photometer meter, or simply the long

hand if it be a sulphur meter.

When all is ready, open a communication between the outlet of the meter and the air—at the same time taking care that all the pressure-gauge cocks are closed. Then proceed gently to open the small lever-cock, and allow the water to flow into the measure, just fast enough to raise the pressure in the syphon pressure-gauge fixed alongside, and in communication with the measure, from half an inch to three quarters. This precaution is necessary to prevent the water being blown out of the meter by excessive pressure. A meter attached to the photometer should make twelve revolutions of the long hand, and consequently one of the cubic-foot hand, by the time the measure is full up to the strip of paper on the upper glass tube. A meter connected with the sulphur test should, in the same time, make one revolution of the long hand.

Should the meter complete the prescribed number of revolutions before the measure is full, then some water must be removed from the meter; if the contrary is the case, then water must be added to the meter. The testing is then to be repeated until the meter

is found to register correctly.

The dial of the photometer meter is divided into 50 divisions; and as each revolution indicates one-twelfth of a foot, each division consequently represents the $\frac{1}{600}$ part of a cubic foot; and therefore 6 of those divisions represent I per cent.

The dial of the sulphur meters is divided into 100 parts; and as each complete revolution indicates one foot, each division conse-

quently represents 1 per cent.

The difference of an ounce in the quantity of water in the meters

will make them register about 1 per cent. either fast or slow.

When the temperature of the cubic-foot measure is higher than the temperature at the outlet of the meter, the meter (if correct) will register a smaller quantity than has actually passed to it from the measure; when the temperature of the measure is lower than that of the meter, the quantity registered ought to be greater.

To find the volume which the meter ought to register, when such a difference of temperature exists, divide the tabular number corresponding to the barometric pressure, and the temperature of the cubic-foot measure, by the tabular number corresponding to the barometric pressure and the temperature of the meter. (See Tables,

pp. 336 and 337.)

As to the Mode of Testing the Pressure at which Gas is Supplied.

Testings of pressure shall be made by unscrewing the governor and burner of one of the ordinary public lamps, in such street or part of a street as the controlling authority may from time to time appoint, and

attaching in their stead the portable pressure gauge.

The Gas Examiners having fixed the gauge gas-tight, and as nearly as possible vertical, on the pipe of the lamp, and having opened the cocks of the lamp and gauge, shall read and at once record the pressure shown. From the observed pressure one-tenth of an inch is to be deducted to correct for the difference between the pressure of gas at the top of the lamp-column and that at which it is supplied to the basement of the neighbouring houses.

The Gas Referees' Street Lamp Pressure Gauge.

This instrument (Fig. 179) has been designed by the Gas Referees,

in accordance with Sect on 6 of The Gaslight and Coke and other Gas Companies' Acts Amendment Act, 1880, for the purpose of testing in any street at any hour the pressure at which gas is supplied. Its construction

is as follows :-

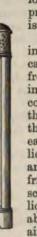


Fig. 179.

Within a lantern provided with a handle for carrying and feet for resting on the ground, is placed a candle-lamp, to give light for reading the gauge. In front of the candle-lamp is a sheet of opal glass, and in front of this a glass U-tube, partly filled with coloured water, and communicating at one end with the air, at the other with a metal pipe, which passes through the bottom of the lantern. In order to read easily and accurately the difference of level of the liquid in the two limbs, a scale divided into tenths of an inch is made to slide between them with sufficient friction to retain it in any position. The zero of the scale having been brought level with the surface of the liquid which is pressed upon by the gas, the height above this of the surface which is pressed upon by the air can be read directly. The lantern is closed in front by a glass door, at each side of which is a re-

flector for throwing light upon the scale of the gauge. Above each limb of the U-tube is a tap, which can be closed when the instrument

is not in use, to prevent the liquid being accidentally spilt.

PHOTOMETER TABLE.

Calculated for One Candle. (Sugg.)*

Con- umption			Grains p	er Hour C	onsumed l	by the Spe	rm Candle		
of Gas Feet per	1	1000	1	1 222	Jan Jan	1000	100	224	1000
Hour.	110	111	112	113	114	115	116	117	118
4.5	1.01851	1.02777	1.03703	1.04629	1.05555	1.06481	1.07407	1.08333	1.09259
4.6	-99637	1.00543	1.01449	1.02355	1.03260	1.04166	1.05072	1.05978	1.06884
4:7	-97517	*98404	+99290	1.00177	1.01063	1.01950	1.02836	1.03723	1.0460
4.8	95486	.96354	97222	98090	.98958	.99826	1.00694	1.01562	1.0243
4.9	+93537	.94387	•95238	-96088	.96938	-97789	.98639	+99489	1.0034
5'0	•91666	92500	. 93333	.94166	.95000	.95833	.96666	97499	.9833
5.1	*89869	90686	*91503	*92320	.93137	*93954	.94771	95588	9640
5.2	*88141	*88942	*89743	90544	*91346	.92147	92948	+93750	9455
5.8	*86477	87264	.88050	*88836	*89622	.90408	.91194	91981	.9276
5.4	*84876	85648	*86419	*87191	87962	*88734	.89506	+90277	.9104
5.2	*83333	-84090	*84848	*85606	*86363	*87121	*87878	*88636	-8939
Con- umption			Grains pe	r Hour Co	nsumed b	y the Sper	m Candle.		
of Gas	-	1	1	T.	f -	1	1	1	
Feet per	119	120	121	122	123	124	125	126	127
Hour.	119	120	121	122	125	124	125	120	127
4.5	1.10185	1.11111	1.12037	1.12962	1.13888	1.14814	1-15740	1.16666	1.1759
4.6	1.07789	1.08695	1.09601	1.10507	1.11413	1.12318	1.13224	1.14130	1.1503
4.7	1.05496	1.06383	1.07269	1.08156	1.09042	1.09929	1.10815	1.11.02	1.1258
4.8	1.03298	1.04166	1.05034	1.05902	1.06770	1.07638	1.08506	1.09375	1.1024
4.9	1.01190	1.02040	1.02891	1.03741	1.04591	1.05442	1.06292	1.07142	1.0799
5.0	99166	1.00000	1.00833	1.01666	1.02499	1.03333	1.04166	1.04999	1.0583
5.1	•97222	-98039	•98856	.99673	1.00490	1.01307	1.02124	1.02941	1.0375
5.2	+95352	.96153	.96955	.97756	98557	•99358	1.00160	1.00961	1.0176
5.3	.93553	.94339	95125	.95911	.96698	.97484	.98270	*99056	*9984
5.4	•91820	.92592	-93364	.94135	.94907	.95679	*96450	97222	.9799
5.5	.90151	.90909	.91666	92424	•93181	•93939	-94696	*95454	9621
Con-			Grains pe	er Hour Co	nsumed b	y the Spe	rm Candle		
of Gas	-		1 -	1	1	1	1		1
Feet per	128	129	130	131	132	183	134	135	1 22
Hour.	120	120	100	101	102	100	101	100	
4.5	1.18518	1.19444	1.20370	1.21296	1.22222	1.23148	1.24074	1.25000	
4.6	1.15942	1.16847	1.17753	1.18659	1.19565	1.20471	1.21376	1.22282	
4.7	1.13475	1.14361	1.15248	1.16134	1.17021	1.17907	1.18794	1.19680	
4.8	1.111111	1.11979	1.12847	1.13715	1.14583	1.15451	1.16319	1.17187	
4.9	1.08843	1.09693	1.10544	1.11394	1.12244	1.13095	1.13945	1.14795	100
5.0	1.06666	1.07500	1.08333	1.09166	1.10000	1.10833	1.11666	1.12500	
5.1	1.04575	1.05392	1.06209	1.07026	1.07843	1.08660	1.09477	1.10294	
5.3	1.02564	1.03365	1.04166	1.04967	1.05769	1.06570	1.07371	1.08173	
5.3	1.00628	1.01412	1.02201	1.02987	1.03773	1.04559	1.05345	1.06132	**
5.4	·98765 ·96969	99537	1.00308	1.01080	1.00000	1.02623	1.03395	1.02272	

 $^{^{\}circ}$ Mr. Sugg has also published, in a book form, series of useful photometrical tables from 9.5 to 20 candles.

RULE.—Multiply the number standing beneath the number of grains consumed by the candle, and opposite the number of feet consumed by the gas-burner, by the illuminating power as read off from the scale of the photometer; the product is the correct value of the gas reduced to the standard of 120 grains per hour and 5 cubic feet per hour.

THE AERORTHOMETER.

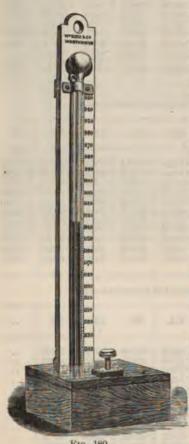


Fig. 180.

The Aerorthometer (Fig. 180) invented by Mr. A. Vernon Harcourt. is an ingenious instrument for correcting the observed volume of any portion of gas to its normal volume i.e., the volume it would have under standard conditions of temperature and pressure. A reading of this instrument furnishes a number expressing the ratio between the observed and the normal, or corrected, volumes of any gas, and serves instead of reading a barometer and thermometer and calculating or referring to a table.

It consists of a bulb and stem, like a thermometer, containing air enclosed over mercury. The mercury stands at a certain height in the stem, and rises and falls as the inclosed air contracts or expands with changes of temperature and atmospheric pressure. The volume of the air is read off by means of a scale engraved on the stem and on the wood behind it. Each degree of the scale marks a portion of the stem whose capacity is one-thousandth part of the volume of the inclosed air when under a pressure of 30 inches of mercury and at a temperature of 60° Fahr. The line at which the mercury stands under these conditions is figured accordingly 1000; and any other reading of the instrument, at a different pressure or temperature, gives the volume to which the thousand volumes have been expanded or contracted. A small drop of water having been passed into the bulb, the expansion caused by a rise of temperature includes that

due to the increased tension of aqueous vapour.

In order that the volume of air inclosed in the bulb of the Aerorthometer may be measured under the atmospheric pressure, a second tube is placed by the side of the graduated stem, which is of the same calibre and connected with the same reservoir of mercury, but open above. By the pressure of a screw upon the leathern top of the reservoir, the mercury is raised in both tubes; and when the mercury stands at the same level in both, the inclosed air is under the atmospheric pressure. By being painted white, the bulb is protected from the action of radiant heat.

Since the volume of any portion of gas contained in a holder or passing through a meter near which an Aerorthometer is placed, bears the same relation to the volume the gas would occupy under standard conditions as the volume read on the stem of the Aerorthometer bears to 1000, the figures expressing the corrected volume of the gas may be obtained by multiplying the observed volume by 1000, and dividing it by the Aerorthometer reading. Thus, if n represents the number read upon the instrument, v the observed volume or rate of passage of the gas, and V the corrected or normal value, then

 $V = v \frac{1000}{n}$

The instrument must stand or be suspended in a vertical position near the meter or holder whose registration it is to be used to correct. To make a reading, the screw is to be turned (if necessary) until the mercury stands at a lower level in the open tube than in that which is graduated. Then the screw must be turned slowly in the opposite direction until the mercury is exactly level in both tubes. The level of the mercury read upon the graduated tube gives the required number.

Various Proposed Standards of Light.

The sperm candle has long been considered an unsatisfactory Standard, owing chiefly to the shade of colour emitted by it differing somewhat from that of the gas, and the inequality of its rate of consumption.

Various Standards of light have been advocated from time to time to supersede the candle; but none of these have hitherto been adopted in

this country.



The Carcel lamp is the Standard in France : the light. equal to 9.6 sperm candles, being produced by purified colza (rape) oil, burning at the rate of 648 grains per The upper portion of this lamp is shown in section in Fig. 181; and the dimensions of its various parts are as follows :-

as lullows .—		
External diameter of burner .	.9055	inches.
Internal diameter of air-tube .	.6692	,,
External diameter of air-tube .	1.7912	"
Total length of chimney	11.4170	,,
Length from base to neck of		
chimney	2.4015	,,
External diameter of chimney		
at level of neck	1.8503	**
External diameter of chimney		
at top	1.3385	
Mean thickness of the glass .	.0787	".
1 11 11 11 1		

The wick used is that known as "light-house wick," and the plait is composed of 75 strands; a piece 4 inches long weighing 55.5 grains. When the consumption of oil is less than 586 grains, or exceeds 710 grains per hour, the trial is cancelled.

Mr. Keates invented a moderator lamp consuming . sperm oil, and yielding a light equal to 10 sperm candles,

which he advocated as a suitable Standard. The most ingenious Standard proposed is that of a portion of the gas-flame itself. The credit of the conception is shared by both Mr. Fiddes and Mr. John Methven, who, unaware of each other's investigations, conducted a

series of experiments on the same lines.

In the course of his photometrical observations, Mr. Fiddes found that if a circular hole about 1-inch diameter were made at a given height in an opaque chimney, and this placed over an argand flame in lieu of the usual glass chimney, the amount of light passing through the hole was a constant quantity, notwithstanding variations in the

illuminating power of the gas.

Mr. Methyen's researches led him to a similar conclusion; his later experiments showing that the amount of light (equal to two Standard candles), passing through a slot 1 inch long and 1 inch wide, in an opaque screen, is constant with gases ranging from 15 to 20 candles power; and that, when either common or cannel gas is carburetted with gasoline (light petroleum spirit, boiling point below 120° Fahr.), the amount of light yielded by a flame 21 inches long, is constant whatever the illuminating power of the gas employed. As the result of this latter discovery, Mr. Methyen uses a shorter and wider

Frg. 181.

slot for the carburetted gas. Fig. 182 shows the Methven Standard with the long and short slots combined on the same slide for the ordinary and carburetted gas respectively. Fig. 183, shows the carburettor fitted with bye-pass arrangement, so that when connected to the gas-pipe supplying the Methven Standard, either ordinary gas, or carburetted gas, may be used.

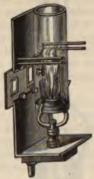
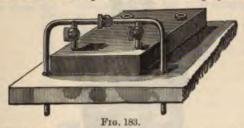


Fig. 182.

It is daily becoming more evident that the acceptance of Mr. Methven's light as a Standard would be a fairly satisfactory solution of the difficulty. Photometrical observations, also, are greatly simplified by the ease with which it can be used, the saving of time which it effects, and the avoidance of that distraction of mind on the part of the operator, which is inseparable from the employment of candles.



In the Pentane Standard of Mr. A. Vernon Harcourt, the gas employed for producing the light is "a mixture of air with that portion of American petroleum which, after repeated rectification, distils at a temperature not exceeding 122° Fahr. The liquid thus obtained consists almost entirely of pentane, the fifth member of the series of paraffines." Burning at the rate of ½ a cubic foot per hour, this gas gives a flame which yields a light equal to that of the Standard candle.

Mr. Harcourt has devised a new Pentane Standard Lamp on a different principle to that above referred to, in which, instead of a mix-



ture of pentane and air, pentane only is burned. This lamp, shown in Fig. 184, resembles an ordinary spirit lamp, with the chimney added to

keep the flame steady, and raise the temperature of combustion. A wick is employed, not, as in the ordinary lamp, at the point of ignition, but several inches from it; its use being to convey the liquid pentane by capillary action to the part of the tube where volatilization of the pentane takes place by the warmth conducted downwards from the flame. The wick is enclosed in a tube jacketed by another tube to produce a steady temperature; and this again is covered by the larger tube with the contracted upper end, as shown. The chimney is moveable for adjustment at any required height.

To put the lamp in action, first remove the lower tube, and having warmed the inner tubes, light the pentane vapour, as it rises in the smaller one. Put on the large tube with the chimney attached; and the top of the flame, on raising the wick slightly, will pass

into the chimney.

Two narrow slots are cut in the chimney on opposite sides, so that the tip of the flame is visible through either of them. When the chimney is set at a definite height above the lower tube, and the flame is adjusted so that its tip is between the upper and lower limits of the slots, the centre portion of the flame appearing between the lower tube and the chimney, gives a definite quantity of light.

TABLE

Comparing (approximately) the Specific Gravity of Gas (Air being 1.000) with the Illuminating Power in Standard Sperm Candles.

No. of Cndls.		Spec. Grav.	No. of Cndls.		Spec. Grav.	No. of Cndls.		Spec Grav
10 equal	to	about 380	20 equal	to	about '508	30 equal	to	about 678
11	11	.392	21	**	'522	31	**	'694
12	"	405	22	**	'537	32	11	.708
13	11	*416	23	33	'550	33	11	.722
14	11	430	24	11	'565	34	**	*738
15	**	*443	25	11	·585	35	11	*755
16	**	'455	26	33	'605	36	11	*775
17	**	'468	27	22	625	37	11	•790
18	,,	'482	28	25	:645			
19	**	495	29	**	662			

VARIATIONS IN THE ILLUMINATING POWER OF GAS.

Most gas managers, in the course of their experience, must have observed variations, sometimes considerable, in the illuminating power of their gas, for which they have been unable satisfactorily to account. These variations are unquestionably due, to a great extent, to changes of atmospheric pressure. When the pressure is augmented, the luminosity is increased, and vice versā. To determine this point, Dr. Frankland instituted a series of important experiments, of which the following are the results:—

Pressure of Air in Inches of Mercury.	Observed Illuminating Power.	Pressure of Air in Inches of Mercury.	Observed Illuminating Power.
30.2	100.0	18.2	37.4
28.2	91.4	16.2	29.4
26.2			19.8
24.2		12.2	
22.2		10.9	3.6
20.2			

The diminution of luminosity follows a fixed and definite law, which may be thus expressed: The decrease in illuminating power is directly proportional to the decrease of atmospheric pressure. Of 100 units of light emitted by a gas-flame burning in air, 5·1 units are extinguished by each reduction of 1 mercurial inch of atmospheric pressure. On the other hand, if a lightless flame be made to burn under augmented pressure, it becomes luminous. The chief cause of the difference is the increase in the volume, and therefore decrease of the density of those heavy hydrocarbons to which the luminosity of a gas-flame is attributed when the atmospheric pressure is reduced, and vice versã.

TABLE

Showing the Percentage of Loss of Light by Mixing Air with Coal Gas.

Per Cent.						of Light r Cent.	Per Cer Air.	nt.					I		s of Light er Cent.
1			*			6	8				4				58
2						11	9							-	64
3						18	10	-						-	67
4						26	15	-	-						80
5				0	-	33	20	0			2				93
6		-	2			44	30							0	98
7		3	1		-	53	40		-	6		-	-	-	100

JET PHOTOMETER.

The three following instruments, which are each employed to determine the illuminating value of gas, though only approximately correct in their indications, are yet sufficiently trustworthy to render them useful and valuable auxiliaries to the more absolute method of testing already described.

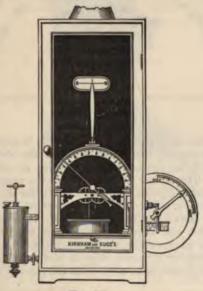
Their great recommendations are their portability, and the ease and celerity with which the illuminating power can be ascertained

by their aid.

Their action depends on the relation which the specific gravity of the gas bears to its illuminating power. The flame being kept at a given height, the pressure required, and therefore the rate of consumption, will vary according to the density of the gas and its consequent illuminating value.

The Jet Photometer.

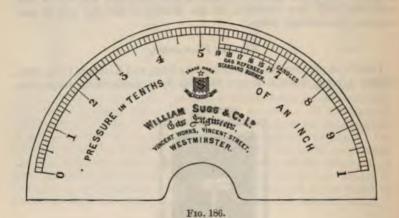
Lowe's jet photometer, as improved by Sugg and Kirkham (Fig. 185), affords a ready means of ascertaining, by a momentary inspection,



Fro. 185.

whether the gas being produced is uniform in quality. The apparatus consists of a King's gauge of delicate construction, with its semi-circular scale indicating the pressure. A steatite jet having a fine orifice is fixed at the top of this, and the gas issuing therefrom, and being lighted, gives a flame which should be constantly maintained at 7 inches.

The scale shown in Fig. 186 is for gas of 14 to 19 candles illuminating power. The same scale is used for 20, 25, or 30 candle gas, but with a different jet, and a lesser consumption per hour, the gauge pointing to the place where the figure 16 stands, but with the number changed to 20, 25, or 30 conforming to the standard quality of the gas to be supplied according to the Special Act of Parliament.



The range of the jet is necessarily short. It is correct at the gauge point, but with a slightly increasing error on the numbers above and below—the error being against the gas in going up, and in favour of it

below—the error being against the gas in going up, and in layour of it in going down. This is due to variations in the pressure—increasing or diminishing—at the point of ignition. Within the degrees marked

on the scale, however, this error is not important.

The gas-tap is shown on the right side of the instrument. The small cylinder on the left side is in communication with the water-cistern in the body of the gauge, and contains a compensator, which, on being screwed up or down as required, adjusts the water-line, so that the pointer of the gauge stands at zero when the gas-tap is closed.

Sugg's Illuminating Power Meter.

This instrument is shown in Fig. 187, and, as the name indicates, is used for ascertaining the illuminating power of gas. The mode of putting it in operation is as follows:—Having filled it up to the water line scratched on the glass in the small box on the right side, connect it to the gas supply with a piece of metal tube. The inlet is a ground union joint, fixed in the centre of the back of the instrument. Turn the lever so as to make the gas pass through the measuring-drum, and let it get rid of all the air, or other kind of gas in it. Light the burner and adjust the flame to 3 inches in height.



Fig. 187.

nen, when the large hand arrives at 16, change the position of the er, so as to make the gas pass to the burner without going ough the measuring-drum. The large hand will then stop at 16. Ind up the clock by means of the remontoir on the top of the meter in the rear of the dial ring. Start the clock by moving the slide the is on the left of the meter, close to the governor. Then, when hand of the clock is passing any one of the divisions of the minute, ge the position of the lever of the bye-pass, so as to make the gas through the meter. When the hand has made one complete ation, stop the meter by means of the lever, in the manner before

described, and read off the illuminating power. The minute clock should not be stopped either before or after the observation, unless it is desired to put the clock entirely at rest.

Thorp and Tasker's Jet Photometer.

This is an ingenious and handy instrument (Fig. 188), for enabling the illuminating value of the gas to be ascertained from inspection



Fig. 188.

at any time and place. It is well understood that the quantity of gas passed in a given time will bear a proportion to the size of

the orifice (this is the principle on which the aërorheometer is made—a useful instrument by the same inventors for indicating the quantity of gas consumed by different burners, &c.); and further that the gas-flame being maintained at a given height, the quantity of gas consumed, and the pressure, will vary as the illuminating power. A movable or floating disc inside the glass tube regulates the size of the orifice, and its position in the tube, corresponding to the graduations of the scale at the side, indicates the illuminating value.

THE SPECIFIC GRAVITY OF GAS.

Specific Gravity a Test of Quality.

If coal gas is free from carbonic acid, sulphuretted hydrogen, and air, specific gravity is a proper test of quality; the denser it is, the greater will be its illuminating power—increase in weight and light-giving property being due to the presence of a larger proportion of olefiant gas and the other richer and heavier hydrocarbons.

Ordinary Method of Determining the Specific Gravity.

The apparatus required in determining the specific gravity of gas are a thin glass globe of about 100 cubic inches capacity, with two stop-cocks on opposite sides, a good air-pump, and a very delicate balance. The experimental room should also be furnished with a barometer, showing the atmospheric pressure, and thermometers indicating the temperature both of the air and gas. The method of manipulation is as follows:—

First.—Open the two stop-cocks; the globe will then be full of air at the atmospheric pressure and temperature. Carefully weigh the

globe while in this state, and make a note of the weight.

Second.—Attach the globe by one of the stop-cocks to the airpump, close the other stop-cock, and exhaust it as perfectly as possible. Having closed the stop-cock, remove the globe and weigh it in its exhausted state. Suppose that it now weighs 31.5 grains less than before, then these 31.5 grains represent the weight of the air abstracted.

Third.—Now attach the globe either to an experimental gasholder or to a gas-pillar connected by a pipe to the main, and fill the globe with the gas. When full, remove it and weigh it a third time. Suppose that the weight is now 14.2 grains more than when in its

exhausted state, then these 14.2 grains represent the weight of the contained gas. Then, as 31.5 (the weight of the air) is to 14.2 (the weight of the gas), so is 1.000 (the specific gravity of the air) to the specific gravity of the gas. Or divide the weight of the gas by the weight of the air, and the quotient is the specific gravity of the gas; thus-

> $\frac{14.2}{31.5}$ = .450, specific gravity of the gas, compared with air as unity, or 1.000.

Dr. Letheby's Method of Determining the Specific Gravity.

With Dr. Letheby's apparatus (Fig. 189), the use of the air-pump is dispensed with. It consists of a similar glass globe, about 6 inches in diameter, furnished with two stopcocks, to one of which is attached a glass tube half an inch in diameter and 7 inches long, fitted with a jet for burning the gas, and having a thermometer inside of the tube to indicate the temperature. The other stop-cock can be attached by a suitable nozzle to a gas-pillar, and in practice the gas is kept flowing through the apparatus, being consumed from the jet at the upper end. The exact weight of the globe when full of air at mean temperature and pressure is engraved upon it; and a counterpoise weight is provided, exactly

> When it is required to determine the specific gravity of the gas, the lower or supply-cock is first closed, and the upper one immediately afterwards. This order is necessary to be observed in the shutting of the cocks, because if the upper one were first closed, the gas within the globe would be at the pressure of the gas within the

equal to the weight of the globe when exhausted.

main, instead of that of the atmosphere. The globe is then placed in the balance and a sufficient number of grains and fractional parts added to the pan containing the counterpoise weight to equalize the beam. Suppose that it takes 15 grains, then these represent the weight of the gas, and say that the globeful of air weighs 35 grains, then-

 $\frac{15}{85}$ = .429, the specific gravity of the gas.

But it is necessary in making such observations to correct the volume of gas to mean temperature and pressure, and to allow for the moisture present in all aëriform bodies in contact with water. To these points the observations which follow apply.



Corrections for Temperature, Barometric Pressure, and Moisture,

Owing to the contraction and expansion which take place in the bulk of all aëriform bodies, due to the variations in atmospheric temperature and pressure, it is necessary, when estimating and comparing their volume, to adopt one common temperature and barometric pressure as the standard. The mean temperature of 60° Fahr. and 80 inches of mercury have been adopted as the most convenient, and to this standard their volume is accordingly reduced. For example:

Corrections for Temperature.—All aëriform bodies expand 1-480th part of their volume at 32° Fahr. for every degree of increase of temperature (1-273rd of the volume of the gas at 0° Centigrade for each degree of the same scale). Now suppose it is required to ascertain what volume 1000 cubic feet of gas at 68° will occupy at 60° the mean temperature. We know by the above-mentioned law that a quantity of gas which at 32° is 480 parts, will at 60° become 508 (60-32=28+480=508), and at 68°, 516 (68-32=36+480=516), then—

$$\frac{1000 \times 508}{516} = 984$$
 cubic feet.

Or, again, if it is required to know the volume which 1000 cubic feet of gas at 56° will occupy at 60°, then—

$$\frac{1000 \times 508}{504} = 1008$$
 cubic feet.

Correction for Pressure.—The amount of decrease or increase in volume is inversely as the pressure. To ascertain what volume 1000 cubic feet of gas at 28.5 inches will occupy when the mercury stands at 30 inches, the mean barometric pressure, then—

$$\frac{1000 \times 28.5}{80} = 950 \text{ cubic feet.}$$

Or, again, if it is desired to ascertain the volume which 1000 cubic feet of gas at 30.6 inches will occupy at 30 inches, then—

$$\frac{1000 \times 30.6}{30} = 1020 \text{ cubic feet.}$$

Or,

Correcting at once for Temperature and Pressure.—Suppose it is required to ascertain what volume 1000 cubic feet of gas at 72° temperature and 29.8 inches pressure will occupy at standard temperature and pressure, then—

$$1000 \times \frac{508}{520} \times \frac{29.8}{80} = 970.5$$
 cubic feet.

Correction for Moisture.—It has been proved by experiment that one cubic inch of permanent aqueous vapour at the mean temperature of 60°, and the mean pressure of 30 inches, weighs '1929 grains; and the following table, founded on the researches of Dalton and Ure, and given by Faraday in his "Chemical Manipulations," shows the proportion by volume of aqueous vapour existing in any gas standing over or in contact with water, at the different temperatures indicated, and at a mean barometric pressure of 80 inches.

Temp. Deg. Fahr.		of	Vapour in the Volume of Gas.	Temp. Deg. Fahr.			ot	Proportion Vapour in ne Volume of Gas.	Temp Deg. Fa			Proportion of Vapour in One Volume of Gas.				
40 .			*00933	54				-01533	68				.02406			
41 .			.00973	55				.01586	69	-	-		*02483			
42 .			*01013	56		-		-01640	70			-	*02566			
43 .			-01053	57	-	-		-01693	71	-		6	.09653			
44 .			-01093	58		-		.01753	72				.09740			
45 .			-01133	59				-01810	73				-02830			
46 .			*01173	60				*01866	74			-	-02923			
47 .			*01213	61		-		.01923	75	-			*03020			
48 .			.01253	62				.01980	76				-03120			
49 .			.01293	68	3			*02060	77				-03220			
50 .			+01333	64				.02120	78		-		*03323			
<i>E</i> 1 .		6	+01380	65				-02190	79				*03423			
52 .	5.1	0	.01426	66				+02260	80				*03533			
53 .			.01480	67				.02330	1000				2.00			

To determine by means of this table the quantity of aqueous vapour present, it is necessary to multiply the volume of the gas by the tabular number corresponding to the temperature, thus—Suppose 100 cubic inches of gas weigh 16 grains at the temperature of 72°, and at mean barometric pressure, then, according to the table, the volume of aqueous vapour present is—

$$100 \times .02740 = 2.740$$
 cubic inches.

This corrected to mean temperature will be-

$$2.74 \times \frac{480 + 28}{480 + 40} = 2.677$$
 cubic inches.

Now, with respect to the volume of the gas, 100 cubic inches at 72° are equal to—

$$100 \times \frac{480 \times 28}{480 \times 40} = 97.7$$
 cubic inches at a temperature of 60°.

Hence, 97.7-2.677=95.023 cubic inches, the volume of dry gas at mean temperature and pressure.

To arrive at the weight of the volume of dry gas, the volume of aqueous vapour must be multiplied by 1929 grains, the weight of a

cubic inch of permanent aqueous vapour, as before stated, and the product deducted from the total weight of 16 grains; thus—

$$16 - (2.677 \times .1929) = 15.483$$
 grains.

Then for the weight of 100 cubic inches of dry gas, we have-

$$\frac{15.483 \times 100}{95.023} = 16.294 \text{ grains,}$$

And as 100 cubic inches of air at mean temperature and pressure weigh 31 grains, we have—

$$\frac{16.294}{31} = .525$$
, the specific gravity of the air.

If, instead of making the correction for moisture, it is preferred to dry the gas as it passes into the globe, this may be done by causing it to flow through a glass tube half an inch in diameter and about 18 to 20 inches long, containing pieces of chloride of calcium; that substance having a strong affinity for moisture. Before using, the chloride of calcium should be fused in an earthenware crucible at a low temperature, then poured on a clean stone surface, and as soon as cold, broken in pieces and put in the tube. The gas in passing through the tube to fill the globe should be made to travel slowly; about 15 minutes being the usual time allowed.

Wright's Method of Determining the Specific Gravity.

For ascertaining the specific gravity of gas, Mr. Wright used a light balloon (Fig. 190), capable of containing one cubic foot, or 1728 cubic inches.

His directions for performing the experiment are as follows:—

Expel the air from the balloon by folding it in the form in which it is first received, ascertain the weight of the balloon and car, fill the balloon with gas, insert the stopper, and put as many grains* in the car as will balance it in the air; add the number of grains which it carries to the weight of the balloon, and deduct the amount from the tabular number corresponding to the degree of temperature indicated by the thermometer, and the pressure indicated by the barometer (pp. 336-7);



Fre. 190.

divide the result by the tabular number due to the temperature and

^{*} The weights used are not troy grains, 100 of them being equal to 58.56 troy grains; they are each equal to 1.728 cubic inches of air, when the barometer is at 30 inches, and the thermometer at 60° .

pressure of the gas (to ascertain which, allow the gas to blow upon the bulb of the thermometer until the mercury is stationary), and the three first figures are the specific gravity.

EXAMPLE I.

Temperature of the air		70°) Tabular number, 924.
Barometer	100	28.9 m.)
Temperature of the gas		28.5 in. Tabular number, 959.
Barometer always the same as air		28.5 in. Tabular number, 555.

Weight of balloon and grains in car, 560.

Then-

$$\frac{924 - 560}{959} = .879$$
, the specific gravity.

EXAMPLE II.

Temperature of the air Barometer	:			40°)	Tabular number, 1067.
Temperature of the gas Barometer always the san		as a	ir	62°) 30·5 in.	Tabular number, 1012.

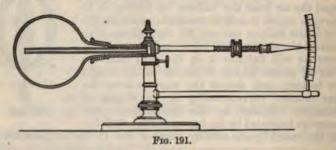
Weight of balloon and grains in car, 560.

Then-

$$\frac{1067 - 560}{1012} = .501$$
, the specific gravity.

Lux's Specific Gravity Apparatus.

The gas-balance, shown in Fig. 191, for determining the specific gravity of illuminating gas, is the invention of Mr. Frederick Lux.



It is constructed on the principle of the common lever-balance, with a curved scale attached by means of a coupling-rod to the standard.

The scale is graduated from 0 to 1; and the tongue or pointer, moving in close proximity thereto, enables the operator to take a direct reading of the specific gravity of the gas under examination.

Instead of consuming the gas through the vertical tube, a pipe can be arranged to convey the gas to the photometer for the purpose

of testing its illuminating power.

To Find the Weight in Pounds of any Quantity of Gas at 60° Fahr. and 80 in. Bar., the Specific Gravity being known.

RULE.—Multiply the quantity in feet by the specific gravity, and the product by .0767 (weight of a cubic foot of air), and the answer will be the weight of gas in lbs. avoirdupois.

Example.—What is the weight of 9400 cubic feet of gas, its specific gravity being .480?

 $9400 \times .480 \times .0767 = 346.07$ lbs. of gas.

TABLE.

Weight of 1000 Cubic Feet of Gas of Different Specific Gravities, at 60° Fahr., and 30 in. Bar.

Specific Gravity. Air 1.000.	Weight per 1000 cub. ft. lbs.	Specific Gravity. Air 1.000.	Weight per 1000 cub. ft. lbs.	Specific Gravity. Air 1 · 000.	Weight per 1000 cub. ft. lbs.
*380	29.146	•470	36.049	•560	42.952
.385	29.529	•475	36.432	*565	43 - 335
.390	29.913	•480	36.816	•570	43.719
-395	80.296	•485	87.200	-575	44.102
.400	30.680	•490	37.583	*580	44.486
-405	31.063	• 495	37:966	*585	44.870
-410	31.447	.500	38:350	*590	45 - 253
•415	31.830	.505	38.733	•595	45.636
420	32.214	.510	39.117	.600	46:020
425	82.597	.515	39.500	*605	46.403
•430	32.981	.520	39.884	•610	46.787
435	33.364	.525	40.267	•615	47:170
.440	83.748	-530	40.651	*620	47.554
.445	84.181	-535	41.034	•625	47.937
.450	34.515	-540	41.418	•630	48.321
.455	34.898	-545	41.801	.635	48:704
460	35.282	.550	42.185	.640	49.088
465	35.665	.555	42.568	•645	49-471

Handy Rule for Ascertaining (approximately) the Weight of Coal Gas in a Holder.

RULE.—Multiply the number of thousands of cubic feet contained in the holder by 37, and the product will be the weight of the gas in lbs.

Example.—A holder contains 54,000 cubic feet of gas, what is the weight of the gas?

54 × 37 = 1998 lbs., approximate weight of the gas.

THE USE OF GAS FOR COOKING, HEATING, VENTILATING, AND MOTIVE POWER.

The use of gas for cooking, heating, and motive power has made rapid strides of recent years; and the steady increase that is taking place in the consumption of gas for purposes other than illumination is a matter of interest. Fifteen to twenty years ago this consumption was only beginning to make itself felt, yet within the brief period which has elapsed, considerable industries, giving employment to much capital and many workpeople, have been called into existence to produce the machinery and appliances required. These, which are of the most numerous and varied kind, are of great excellence, whilst improvements are constantly being effected therein.

For domestic and greenhouse use there are numberless heating stoves of superior design and workmanship, and in cooking stoves and ovens there is equal variety.

The uses to which gas may be advantageously put in every branch of trade where heat is required, are only limited by the number of such trades. For example, in coffee roasting, in the manufacture of confectionery, the baking of bread, the finishing of shoes, in dentistry, in the production of jewellery, in wire welding, tempering steel, enamelling, and many others.

The gas-engine already successfully competes with the steam motor for all purposes where the power required to be exerted is intermittent and within moderate limits.

For handiness in application, and cleanliness and safety in use, gas, as a fuel, is unsurpassed. The use of gas in these ways means a saving of time and labour, and is an important step towards the solution of the smoke difficulty in towns.

Taking its advantages in these respects into account, there is economy in its employment even when, as in scattered districts, its price per 1000 cubic feet may be considered high. In towns where the price of gas is comparatively low, there is a positive economy in its adoption, beyond the special recommendations named.

The manufacture of gas-engines was at first confined to the smaller sizes, from one man power to 10-horse power, but now larger

sizes equal to as high as 100-horse power are being made.

In adopting this motor, neither boiler nor chimney are required, and hence it can be employed in buildings, and in out-of-the-way corners in establishments where a steam engine is altogether inadmissible. It is always available for work on the opening of a tap, and it goes on working continuously day and night with the least possible attention. Moreover, the percentage efficiency of the gas-engine is greatly in excess of that evolved by the steam motor.

As a ventilating agent the gas-flame is of the greatest use, and in rooms where the means of ventilation are provided it promotes their efficiency, though it has not been employed in this direction as extensively as its merits deserve. In spacious assembly rooms the gas "Sunlight," or the "Regenerative" light, with their ventilating tubes, may be recommended as superior to any other method of arti-

ficial lighting.

One of the best methods—perhaps the very best method—of reducing the proportion which capital expenditure in gas-works bears to revenue, is to cultivate a day consumption of gas, by affording facilities for and encouraging in every legitimate way the use of gas for cooking, heating, ventilating, and motive power.

cooking, heating, ventilating, and motive power.

This policy, if pursued to a successful issue, is virtually to reduce the percentage of capital in the proportion of such consumption, because the plant is brought to bear in earning profit during the day-

light as well as in the lighting hours.

The experiments on pp. 364-6, showing the advantages of cooking by means of gas, are quoted by Mr. William Carr, in his article on this subject in "King's Treatise," Vol. III., pp. 232-4:—

COOKING BY MEANS OF GAS.

(Mr. Magnus Ohren, in his work "On the Advantages of Gas for Cooking and Heating.")

Gas at 4s. 5d. per 1000 cubic feet.

Joint.	Weight. 1bs. ozs.		Tir h.	me. m.	W	eight hen oked. ozs.	Weight of Dripping. lbs. ozs.		. 343	of eight. ozs.	Gas Used. c. ft.	Cost of Gas. d.
Leg of Mutton	8	11	2	20	7	5	0	5	0	71	41	2.17
Ribs of Beef .	10	14	2	37	9	102	0	51	0	14	46	2.43
Leg of Mutton	9	7	2	30	8	6	0	73	0	91	42	2.22
Ribs of Beef .	11	0	2	45	9	13	0	41	0	141	48	2.54
	39	61			35	22	1	61	2	181	177	9-36

Coal at 22s. per ton. (OHREN.)

Joint.	Weight lbs. ozs		Weight when Cooked. lbs. ozs.	Weight of Dripping. lbs. ozs.	Loss of Weight. lbs. ozs.	Coal used.	Cost of Coal. d.	Cost of Wood. d.	Total Cost. d.	
Leg of Mutton	8, 1	2 50	7 04	0 8	0 74	281	3.36	0.50	3.86	
Ribs of Beef .	10 14	2 45	9 102	0 5	0 141	29	3.42	0.50	3.92	
Leg of Mutton	9 12	2 80	8 0	0 10	1 2	28	3.30	0.50	8-80	
Ribs of Beef .	13 2	2 50	11 13	0 6	0 15	30	3.23	0.50	4.03	
	41 13		36 84	1 13	3 7	1151	13.61	2.00	15.61	

These experiments were made twenty years ago, with the imperfect apparatus of that time. The following were made in 1879-80:—

	1			* *	*		•		•	Refle	Refle		Refie		
	Quality of Cooking.	Excellent.	Excellent.	Excellent. Well done.	very underdone.	Rather underdone	Excellent,	Good but rather underdone near bone.	Rather	Excellent.	Underdone.	Well done.	Well done.		Excellent.
	Cost of Gas at 2s. 6d. per 1000 cub. ft.	ag.	åd.	2 d.	₹d	nearly 1d.	14d.	1d.	over 2d.	nearly 2d.	over 1d.	14d. 34d.	1#d.		åd.
ALL.)	Per Ct.	8.25	:	6.00	2.00	7.30	10.80	8.80	09.9	13.00	10.25	9.50	12.50		12.33
(H. WOODALL.)	Actual Loss of Weight.	lbs. oz, 0 13 0 8	:	6.0	2 0	0 10	0 15	0 16	0 8	1 2	1 8	0 13 8 8		ROBINSON	1 0
100	Weight of Dripping.	1bs. oz. 9 2 1 13	:	1.5	1 3	0 10	1 6	2 1	0 15	1 7	1 7	1 9			1 84
bic feet.	Weight of Cooked Meat.	lbs. oz. 6 13 8 9	:	7.10	7 9	7 4	6 5	7 10	7 7	6 1	8 9	7 8 27 14	6 9	bic feet.	5 143
Gas at 2s. 6d. per 1000 cubic feet.	Other work performed (if any),		baked, total	SixChickens roasted.	:	:	W:	Bread Baked.	:		three loaves,	::	Bread Baked.	2s. 6d. per 1000 cubic	
is at 2	Gas con- sumed.	ft. 24 253	23	25 27	24	18	55	32	28	63	35	40	99	Gas at	243
G	Weight of Uncooked Leg of Mutton.	1bs. oz. 9 12 10 14	:	8 . 6	9 6	8	8 10	10 10	8 14	8 10	9 2	9 14 36 6	100	9	8
	Price.	£ s. d. 5 0 0 7 10 0	7 10 0	7 10 0 6 0 0	4 10 0	7 5 0	0 9 9	8 0 0	3 8 0	0 0 9	4 2 0	10 0 0	0:		0 9 9
	Dimensions of Oven.	in. in. < 14 × 15 < 15 × 13	× 15 × 13	× 15 × 13 × 13 × 12	< 123× 144	× 16 × 25	× 184× 18	× 17 × 60	× 15 × 14	× 22 × 18	< 15 × 124	× 18 × 24 × 28 × 24	14 ×		- 14 + 25
	No.	28. 28. 28. 28. 28. 28.	8 28 ×	5 24 ×	6 20½×	7 184×	8 26 x	8 80 ×	23	84	25 ×	17 38	505		14 + 14 +
	1 2	200	44	4. 445	-	-	30	-	10	=	12	14	16		1

Calculating Mr. Ohren's experiments with coals at the price of 16s. 6d. per ton, and gas at 8s. per 1000 cubic feet, taking the third experiment in each case, and reducing Nos. 1 and 2 in Mr. Woodall's table and Mr. Robinson's experiment to the same standard of comparison, Mr. Carr obtains the following results:

Gas at 8s. per 1000 cubic feet. Coal at 16s. 6d. per ton.

			Weig	Į į	-	Weig	1 1	1		7	Per	Cost of		Cost of		
l	Oven.	Prioe.	of U Sook Mutte	មិនដូ	Con Con Con Con Con Con Con Con Con Con	Cook Mes	D .	veugns of ripping	Los Wei	g p c	cent. on Joint.	Gas at 36. per 1000.	of Un. Con. Con. Con. Con. Con. Con. Con. Co	Coal at 16s. 6d. per ton.	Wod.	Total Cost.
	in. in. in. & s. d. lbs. oz. ft. lbs. oz. lbs. oz. lbs. oz.	£ 8. d.	ğ	8	#	lba.	38.	bs. oz.	Pg.	OZ.				đ.	ъ	ت
Obren's Experiment (Coal, 16s. 6d.)	:	:	9 12	13	:	80	•	8 0 0 10 1 2 11.58		C4	11.68	:	:	2.47	93.	2.97
Ditto (Gas, 8s.)	:	:	6	-	43	8	9	0 73 0 94 6-29	0	76	6.29	1.50	:	:	:	:
Woodall's Experiment 24×14×15 5 0 0 9 12 24	24×14×15	0 0 9	6			6 13	<u> </u>	6 1	•	18	0 18 8.25	86	Excellent.	:	:	:
Disto ditto	ditto 28×15×187 10 0 10 14 25·5	7 10 0	2	14		80	6	1 18	•	80	0 8 4.50	16.	Ditto	:	:	:
Robinson's ditto	ditto 14×14×256 6 0 8 2 4·2 5 144 1 84 1 0 12·88	0 9 9	80	C4	4. 64	9	4	1 8	-	0	12.88	.87	Ditto	:	:	:

THE RESIDUAL PRODUCTS.

It is daily becoming more imperative on the Gas Manager to do all that in his power lies to promote the interests of the undertaking under his charge, by utilizing the Residual Products of gas manufacture to the utmost extent.

It is a remarkable fact that there are no waste products in a properly conducted gas-works. The coke, breeze, tar, ammoniacal liquor, sulphur, spent lime, retort carbon, and even the clinker and ash from the furnaces are all marketable, and therefore of more or less value. The flue heat from the retort stack is even utilized for the generation of steam, and in the retort furnace where the regenerative or restorative system is applied.

Coke and Breeze.

Coke, as ordinarily produced, is not well adapted for domestic use, for kitcheners, for use in greenhouses, or stoves in general; and, in consequence, its sale is often restricted. To render it suitable for these purposes, it requires to be broken into pieces of smaller and more uniform size.

Wherever means have been adopted for this purpose, the article has been found to command a ready sale; and instead of mountains of coke in every available corner of the works, the material is cleared out almost as quickly as it is produced.

The labour and inconvenience and enormous waste attendant on stacking are thus avoided, the premises can be kept in better order, and the revenue is augmented.

For breaking the coke by hand, Mr. Bennett recommends a hammer of the form shown in Fig. 192, with a chisel edge at one end, and four prongs at the other.

A machine for breaking coke is made by Messrs. Smith, Beacock and Tannett, of Leeds. This is used by Mr. Sellers at the York Gas-Works, who gives the cost, and describes the advantages attending its rese

"The engine (a 4-horse vertical) and breaker, and fitting up of same, cost £143; being, for the engine, £108, the breaker, £28, and fitting up, £7. By placing the engine and breaker upon one frame, so that both could be moved upon one set of wheels, the cost would be materially reduced, and the working very much improved. The machine, when at full work, will break 20 tons of coke per day. We have one man to look after the engine, and two to feed the machine; but as the first named is not fully occupied with the engine, he assists the other two in helping carters to put the

broken coke into bags, &c., the net cost of all which add 9d, per ton to the price. Then in breaking a ton of coke, about 1 cwt. passes through the screen, and is sold as breeze at 1s. 6d. per ton, or, say, 1d. per cwt. The real result, therefore, of breaking coke stands thus:



Fig. 192.

We sell our unbroken coke at 10s. per ton, and broken at 10s. 8d.; the 8d. added being 9d. per ton for labour, and coke converted into breeze by breaking, less 1d. received for breeze per ton of coke broken. The cost of maintenance of engine and breaker we consider is more than recouped by, first the saving of labour that would have been employed in loading the coke if it had not been broken; secondly, the saving of the cost in labour and depreciation of stacking the coke if it were not sold; and, thirdly, the advantage gained in getting rid of the coke, so as to enable us to maintain our price of 10s. per ton, for upon our annual make of coke for sale a reduction of 1s. per ton would inflict a loss of £500 a year."

> Another excellent coke breaker is that devised by Messrs. Thomas and Somerville. This machine requires very little power to drive it, and the waste of coke by its use is

remarkably small. At a trial of the machine at the Old Kent Road works, the following results were obtained :-

	8.	d.
500 feet of gas consumed by a 2-horse power gas engine, at cost price of gas delivered in holder .	0	9
Oil and cotton waste		6
Two men supplying machine with large coke, and shovelling up broken, at 4s. 6d.	9	0
Interest and wear and tear (say)	0	8
Total per day	10	6
Charles and the second	8.	d.
For 80 tons of coke broken per day at the rate of . Add for loss by dust and waste, 1 cwt. with price of	0	11
coke at (say) 13s. 4d. per ton	0	8
Cost of breaking, per ton .	0	91/2

The coke thus manipulated finds a ready and constant market as quickly as it is produced, the result being an average net gain of 1s. 6d. per ton of coke.

Coke, immediately on being slaked with water, weighs about 15 per cent, more than when unslaked; the bulk of the moisture, however,

evaporates-about 3 per cent. only being retained.

A ton of coke is about a chaldron and a half.

A chaldron of coke varies in weight from 12th to 15 cwt.

For the quantity of coke produced by different coals, see the tables on pages 3 to 49.

Coal Tar.

The yield of tar from coal per ton in gas-works ranges up to 12 gallons, and from cannel up to about 17 gallons. The average production in gas-works throughout the country will not exceed 11 gallons per ton. The total production of coal tar in the United Kingdom is probably about 500,000 tons.

The utilization of the tar for its products is not pursued at many gas-works, though it is done at a few, and if well managed it is a

source of profit.

Considerably more skill and care are required in the distillation of tar than in the manufacture of sulphate of ammonia; nevertheless, it is safe to predict that before many years have elapsed, this branch of practical chemistry will be widely practised on those gas-works where there is space and convenience.

The manufacture on gas-works may be wisely restricted to the distillation of the tar for the light and heavy oils, and the production of

pitch.

The principal dangers to be apprehended in the process are the leaking or boiling over of the stills and the firing of vapours, causing conflagration, and the stoppage of the pipe passages with accretions of solid matter, chiefly naphthaline, resulting in explosion; but these dangers can be minimized, or altogether averted, under proper supervision, and by the use of efficient apparatus.

The specific gravity of tar produced from ordinary coal ranges from

1.120 to 1.150; that from cannel coal, from .980 to 1.060.

TABLE

Showing about the Average Proportion of the several Products obtained from the Distillation of 10,000 gallons of Coal Tar. (Dr. Letheby.)

Ammoniacal liquor 40 per cent. benzole		240 · 0 gals, 34 · 4 ,,	Solvent naphtha . Last runnings		41.8 gals. 12.0 "
90 ,, ,,	Pitch	53.1 "	Dead oil		3018.7 "

TABLE

Showing the Average Percentage of the Products Obtained from 100 Tons of Coal Tar. (Roscoe.)

								1	2	
Naphtha								3.0	2.0	per cent.
Light oils and ca	rbo	lic	aci	d			G.	1.5	0.8	19
Heavy oils, naph	tha	len	e, 1	ant	hra	cen	e.	35:0	25.0	44
Pitch								50.0	60.0	
Water and loss								10.5	12.2	- 11
								100.0	100.0	

Mr. C. Greville Williams remarks ("King's Treatise," Vol. III., p. 281) that—"The working results to be obtained from a charge of 1200 gallons vary so greatly, according to the nature of the tar and the care with which the distillation has been made, that it is exceedingly difficult to give any average which will be satisfactory to distillers in different parts of the country. The following figures are placed side by side as extreme cases":—

				incashire: tson Smith.)	appl	London: Chemistry as ied to the Arts Manufactures.")
Ammoniacal liquor			gallons	30			50
First light oils .			11	33			20
Second light oils.	3			157		-	20
Creosote oils			12	104	1		250
Anthracene oils .			17	229		4	50
Pitch			tons	3.25			4

Tar Pavement.

This is made of the breeze, ashes, and clinker of gas-works and mill furnaces, along with shingle or coarsely-ground granite, mixed with coal tar.

A coke fire is first made on the ground, and the solid ingredients cessed in a heap round and over it; layer after layer being gradually added as the heat penetrates through the mass, until sufficient bulk of the material is ready.

If preferred, or if a large quantity of material has to be dried and heated, a raised sheet-iron floor may be made, supported on bricks, with the coke fire underneath; or a permanent fire-brick floor may be constructed, ramified with flues underneath leading to a chimney, and having a fire grate at one end.

In the meantime, whilst the solid ingredients are being dried and heated, the tar is being boiled, and, when ready, the two are taken and mixed together in small heaps (say about three ordinary barrow loads) in the proportion by measure of 1 part tar to 7 parts solid.

The whole is then turned over immediately whilst hot, and thoroughly mixed, until every particle of the solid ingredients has

received a coating of tar.

The mixed material is then sorted into three separate heaps of graduated fineness, by passing it through two sieves with $\frac{3}{4}$ -inch and $\frac{3}{8}$ -inch meshes respectively. It is now ready for use, and may be laid down at once, or kept in stock for a short time until required.

It is preferred by some to sort the solid ingredients before mixing with the tar, as the latter is liable to clog the sieves. In this case an ordinary screen, \(\frac{3}{4} \) inch between the bars, and supported at an angle, is employed; and all that passes through it is afterwards riddled through a \(\frac{3}{4} \)-inch sieve.

The three different grades of material are then dried and made hot as described, and thoroughly mixed with hot tar in these proportions:

	(1 part tar 9 parts solid) or 24 gals	s. tar	to 1 to	n solid.
2. Riddlings	1 part tar 7 parts solid or 30	**	1	**
3. Fine material	1 part tar 6 parts solid or 36	10	1	

The footpath being properly kerbed, the upper edge of the stones standing 3 inches above the solid bottom of the path, the rough prepared material, No. 1, is put down 2 inches thick; then No. 2 about \$\frac{3}{8}\$ inch thick, and finally No. 3 about \$\frac{3}{8}\$ inch thick. Each layer as it is put down is rolled with a 10-cwt. roller until thoroughly consolidated. Corners which cannot be reached by the roller, must be consolidated by punning. Derbyshire spar or fine granite sprinkled over the surface improves the appearance of the pavement.

Three tons of the rough (No. 1) and 1½ tons of the fine prepared material (Nos. 2 and 3) will cover 60 square yards, or a footpath

2 yards wide and 30 yards long.

Ammoniacal Liquor.

The amount of liquor obtained up to the outlet of the scrubbers, per ton of coal carbonized, varies from 15 to 45 gallons of 10-oz. strength, depending on the class of coal used, and the efficiency of the apparatus for arresting the ammonia.

The product of ammoniacal water or liquor, when treated with sulphuric acid, is sulphate of ammonia; when treated with muriatic or hydrochloric acid, it is muriate of ammonia, or sal ammoniac.

The manufacture of sulphate of ammonia from the ammoniacal liquor is fast becoming general in gas-works, and properly so, as the process is both simple and profitable. That it must be more profitable to use the liquor at the place of production than at a distance away, is evident, taking into account the saving of the cost of transport of a bulky material.

The apparatus required is neither complicated nor costly; the process is free from danger (though fatal accidents have occurred through carelessness, or the use of imperfect appliances), and an intelligent

labourer can learn it in less than a week's time.

In actual practice (using round figures) it is found that-

The strength, and consequent value, of ammoniacal liquor, is commonly ascertained by Twaddel's hydrometer, and also by the quantity of sulphuric acid of the specific gravity 1845 required to neutralize the ammonia contained in one gallon.

Each degree of Twaddel is equal, as nearly as possible, to 2 oz. of acid per gallon of the liquor; hence arises the description of its value:—

Water of 5 degrees Twaddel is called 10-oz. liquor.

", 6 ", ", 12 ", 14 ", 14 ",

And so on, at the rate of 2 ounces for each degree, so that 10-oz., 12-oz., or 14-oz. liquor means ammoniacal liquor of such a strength that 10-oz., 12-oz., or 14-oz. of sulphuric acid, of the specific gravity of 1845, are required to neutralize the ammonia contained in a gallon of it.

To convert degrees of Twaddel's hydrometer into specific gravity, multiply the number of degrees by 5, and add 1000 to the product.

Example.—Twaddel 6×5+1000=1030 specific gravity.

To convert specific gravity into degrees of Twaddel, deduct 1000 from the specific gravity, and divide the remainder by 5.

Example.—Specific gravity 1030-1000÷5=6 degrees of Twaddel. To determine the weight of a gallon of ammoniacal liquor of any strength, find the specific gravity by the above rule. This will represent the number of ounces avoirdupois in weight per cubic foot. Divide by 16 to ascertain the number of pounds per cubic foot, and by 6·25 (gallons per cubic foot) for the weight of a gallon of the liquor.

Example.—Required weight per gallon of 10-oz. liquor (5° Twaddel), (5×5)+1000=1025, specific gravity and weight per cubic foot in ounces avoirdupois.

1025 = 64.068 lbs. per cubic foot.

64.068 = 10.25 lbs. weight per gallon of 10-oz. liquor.

Or the weight may be found more expeditiously by the rule given

immediately after the next table on page 374.

It is well known that the greater the proportion of ammoniacal gas contained in a pure solution, the less the density or specific gravity of such solution. How then, it may be asked, is the apparent contradiction to be explained, that the larger the quantity of ammonia contained in gas liquor, the greater the density?

The explanation is to be found in the circumstance that gas liquor is not a solution of ammonia pure and simple, but contains other gases in solution, and in combination with the ammonia in the form of salts, which increase its specific gravity; and the more ammonia liquor contains, the greater is its power of arresting and absorbing such other gases.

It is by reason of this latter-mentioned fact that Twaddel's hydrometer is tolerated as a gauge of the strength and value of the ammoniacal liquor of gas-works. At the best, however, its employment

for this purpose is very unsatisfactory.

The method of testing by saturating the liquor with sulphuric acid is an improvement on the hydrometer; but even that is imperfect, as has been pointed out by Mr. Greville, who ascertained by experiments on nine different samples of liquor that an average of 22.5 per cent. of the ammonia present in combination was not indicated by the acid.

The mode of testing by Mr. Thomas Wills meets the difficulty. His plan is to mix with the liquor a caustic alkali for which the acids of the salts contained in the liquor have a stronger affinity than for the ammonia with which they are combined. On the mixture being strongly heated, the salts are decomposed in presence of the caustic alkali; and the ammonia is driven off in the gaseous state, and being conveyed into a solution of sulphuric acid is secured as sulphate of ammonia. This and the other methods of testing are fully detailed by Mr. Hartley in his brochure on "Ammonia Liquor Tests."

TABLE

Showing the Specific Gravity, Weight per Cubic Foot, Weight per Gallon, and Ounce Strength of Ammoniacal or Gas Liquor of different degrees Twaddel.

Degrees. Twaddel Liquor.	Specific Gravity and Weight per Cubic Foot in Ounces Avoirdupois.	Weight per Gallon. lbs.	Ounce Strength.	Degrees Twaddel Liquor.	Specific Gravity and Weight per Cubic Foot in Ounces Avoirdupois.	Weight per Gellon lbs.	Ounce Strength
0	1000	10.0	0	124	1062.5	10.625	25
1	1002.5	10.025	0	13	1065	10.65	26
1	1005	10.05		184	1067.5	10.675	27
14	1007.5	10.075	2 3 4 5	14	1070	10.7	28
2	1010	10.1	4	144	1072-5	10.725	29
24	1012.5	10.125	5	15	1075	10.75	30
3	1015	10.15	6	154	1077.5	10.775	31
84	1017.5	10.175	6 7 8	16	1080	10.8	32
4	1020	10.2	8	164	1082.5	10.825	33
41	1022.5	10.225	9	17	1085	10.85	34
5	1025	10.25	10	174	1087.5	10.875	35
54	1027.5	10.275	11	18	1090	10.9	36
6	1030	10.3	12	184	1092.5	10.925	37
61	1032.5	10.325	13	19	1095	10.95	38
7	1035	10.35	14	194	1097.5	10.975	39
73	1037.5	10.375	15	20	1100	11.0	40
8	1040	10.4	16	201	1102.5	11.025	41
- 84	1042.5	10.425	17	21	1105	11.05	42
9	1045	10.45	18	214	1107.5	11.075	43
94	1047.5	10.475	19	22	1110	11.1	44
10	1050	10.5	20	221	1112.5	11.125	45
104	1052.5	10.525	21	23	1115	11.15	46
11	1055	10.55	22	231	1117.5	11.175	47
113	1057:5	10.575	23	24	1120	11.2	48
12	1060	10.6	24	25	1125	11.25	50

It will be seen by the above that the weight of the liquor in pounds avoirdupois per gallon is obtained by simply placing the decimal point after the first two figures of the number representing the specific gravity. Thus, liquor of 1025 specific gravity is 10·25 lbs.; and of 1037·5 specific gravity is 10·375 lbs. weight per gallon.

Each degree of Twaddel represents 350 grains above the weight of distilled water. Consequently, 5 degrees represent 1750 grains, or

1 lb.; 20 degrees, 7000 grains, or 1 lb.

In Beaume's Hydrometer, which was the first instrument of the kind, the divisions are equidistant; and it has two modes of graduation according as it is intended for liquids heavier or lighter than water. This instrument is the one principally in use on the Continent.

Beaumés' Hydrometer Compared with Specific Gravity. For Liquids Heavier than Water.

Degrees. Beaumé.	Specific Gravity.	Degrees Beaumé.	Specific Gravity.	Degrees Beaumé.	Specific Gravity.
0	1.000	26	1.206	52	1.520
1	1.007	27	1.216	53	1.535
2	1.013	28	1.225	54	1.551
3 4 5	1.020	29	1.235	55	1.567
4	1.027	30	1.245	56	1.583
5	1.034	31	1.256	57	1.600
	1:041	32	1.267	58	1.617
6 7 8	1.048	33	1.277	59	1.634
8	1.056	34	1.288	60	1.652
9	1.063	35	1:299	61	1.670
10	1.070	36	1.310	62	1.689
11	1.078	37	1.321	63	1.708
12	1.085	38	1.333	64	1.727
13	1.094	89	1.845	65	1.747
14	1.101	40	1.357	66	1.767
15	1.109	41	1.369	67	1.788
16	1.118	42	1.381	68	1.809
17	1.126	43	1.395	69	1.831
18	1.134	44	1.407	70	1.854
19	1.143	45	1.420	71	1.877
20	1.152	46	1.434	72	1.900
21	1.160	47	1.448	73	1.944
22	1.169	48	1.462	74	1.949
23	1.178	49	1.476	75	1.974
24	1.188	50	1.490	76	2.000
25	1.197	51	1.495		

Beaume's Hydrometer Compared with Specific Gravity. For Liquids Lighter than Water.

Degrees Beaumé.	Specific Gravity.	Degrees Beaumé.	Specific Gravity.	Degrees Beaumé.	Specific Gravity
10	1.000	27	0.896	44	0.811
11	0.993	28	0.890	45	0.807
12	0.986	29	0.885	46	0.802
13	0.980	30	0.880	47	0.798
14	0.973	31	0.874	48	0.794
15	0.967	82	0.869	49	0.789
16	0.960	33	0.864	50	0.785
17	0.954	84	0.859	51	0.781
18	0.948	35	0:854	52	0.777
19	0.942	36	0.849	53	0.773
20	0.936	87	0.844	54	0.768
21	0.930	38	0.839	55	0.764
22	0.924	39	0.834	56	0.760
23	0.918	40	0.830	57	0.050
24	0.913	41	0.825	58	6
25	0.907	42	0.850	59	1
26	0.901	43	0.816	60	1

Applications of Sulphate of Ammonia in Agriculture.

Mr. W. Arnold gives the following general directions for the application of sulphate of ammonia in agriculture, and a list of the crops for

which it is most suitable :-

Sulphate of ammonia is one of the most powerful fertilizers known to modern science. It is especially rich in nitrogen; and when used either by itself or in conjunction with farmyard manure, its good effects are written so plainly, in better quality and largely increased yield of corn, that no farmer who has once used it will ever give it up, but will, on the contrary, annually increase its use upon his farm.

When bought at first hand from a gas-works, sulphate of ammonia is guaranteed to contain more than twenty per cent. of nitrogen. Hence its excellent effect upon all corn crops, which is chiefly expended in increasing the yield of grain, but not the straw; and there is, therefore, much less risk of "lodging" from heavy rains. This is a very important advantage. Then, manure rich in nitrogen increases the proportion of gluten in cereals; and this increase is stated by Boussingault to be as much as 10 per cent. With an increase, therefore, of 10 per cent. in quality and of 20 per cent. in yield, the use of sulphate of ammonia ought to be increased tenfold, to the great advantage of the English farmer, for both may be done.

The most suitable dressing is one of from 2 to 3 cwt. per acre, mixed with an equal weight of fine dry earth or sand, and applied early in the spring (say March or April), in moist or showery weather. It should be thoroughly mixed in a barn or dry shed; and, if at all lumpy, beaten with a shovel, and passed through a 45-mesh riddle. It should be carefully sown by hand; or, if in large quantities, with a manure drill. If wheat is to be grown entirely with sulphate of ammonia, it is better to put it on in two dressings—one half in autumn,

and the other half in spring.

Upland or meadow grass, wheat, barley, oats, rye, colza, hemp, mangel-wurzel, cabbages, hops, garden produce generally, and beetroot (when grown for sugar), are the crops most largely benefited by this manure; simply because nitrogen, which is its dominant element, enters largely into their composition. For instance, colza, hemp, and beetroot require each of them 70 lbs. per acre of nitrogen to produce a full and healthy crop; wheat, 53 lbs.; and barley, oats, and rye, 35 lbs. per acre each.

Beans, peas, sainfoin, or clover, in which potash is the dominant element, are not benefited by an application of sulphate of ammonia; but almost all other crops that can be grown will richly repay its use.

In the case of a crop thinned out by wireworm, the ravages of birds or insects, or by a severe winter, the application of 2 cwt. of sulphate of ammonia early in the spring, and lightly harrowed in, will, in many

cases, cause a crop that looked only fit to plough up, to tiller freely, and grow away into a full yield of corn for the district.

Mr. Magnus Ohren states the exact quantity of sulphate of ammonia

which he considers is required for different crops, as follows :-

For Grass Land.—11 cwt. per acre; to be put on the land in the

month of April, before or after a shower of rain.

For Wheat, Oats, and Barley.—1 cwt. per acre for wheat, in April; 1 cwt. per acre for oats, in April; 1½ cwt. per acre for barley, in April.

For Vines.—1 bushel on the vine border, lightly forked in, in the

For Vines.—1 bushel on the vine border, lightly forked in, in the months of March, April, May, and September. This quantity (1 bushel) to be for the nourishment of four vines.

For Onion Beds .- A good sprinkling over the beds two or three

times during the growth of the onions.

For Potatoes.—11 cwt. per acre as a top dressing, before the haulms

appear above ground.

For Greenhouse Plants.—A large teacupful in a bucket of water, to water the greenhouse plants with twice a week. Not to be used, how-

ever, for heaths, rhododendrons, or orchids.

For Peach, Apricot, Plum, Currant, and Gooseberry Trees.—A similar solution to that given for greenhouse plants, in the months of March, April, and May. Rose trees and garden plants generally are benefited by the use of the solution. Celery, cabbages, and cauliflowers also grow well when watered with the solution.

For the Raising of Healthy Plants from Seeds.—Sprinkle a good quantity of the sulphate on the seed beds, and then water them a week before sowing the seeds. Melons and cucumber plants also are much

benefited by the sulphate of ammonia.

Note.—All vegetation, excepting heaths, rhododendrons, and orchids, is rendered more luxuriant, healthier, and consequently freer from the destructive attacks of insects, by the use of sulphate of ammonia. In the spring of the year vegetation requires a condensed antiseptic and nourishing food to enable it to withstand the blighting effects of the north-easterly winds, which, being the least electrical of all the winds, lower its vitality, and thus conduce to disease.

Spent Oxide of Iron.

The oxide of iron used in gas purification may be considered as "spent" when the quantity of free sulphur contained in it ranges between 45 and 55 per cent. by weight of the whole bulk of the material.

Although by continuing to use it the proportion of sulphur can be increased, it is not economical to do this beyond a certain point, as the purifiers would have to be changed more frequently, and the latequired for that purpose would be out of proportion to the derived. If, however (see ante p. 136), a small proportion

oxygen is sent through the purifiers along with the gas, revivification in situ is effected, and the oxide can be charged with 75 per cent. of free sulphur.

In addition to the sulphur, the spent oxide usually contains a small percentage of salts of ammonia, and some insoluble cyanides of iron,

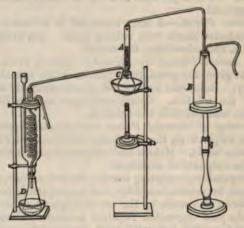
which are of value.

The spent oxide is generally sold at per unit of contained sulphur.

Mr. Andrew Stephenson has devised a handy apparatus (Fig. 193),
for estimating the amount of sulphur in the oxide, and gives the following instructions for using the same:—

Weigh 100 grains of spent oxide, dry at 212° Fahr., and weigh to ascertain moisture; put the dried material in the test-tube. A. which

is provided at the bottom with a filter of cotton wool.



Fro, 193.

Bisulphide of carbon is then blown from the holder, B, into the testtube, A, on top of the spent oxide. It percolates the mass gradually, and dissolves out the sulphur; the solution finding its way by gravitation into the flask, C, which is placed in a water-bath.

The Bunsen burner is then lighted, and the application of heat soon vaporizes the bisulphide of carbon from the flask, C. The vapour finds its way through the connecting-tube into the condenser, and is recovered in the receiver, D, under water, ready for further use.

The sulphur is left in the flask (the weight of which has been previously noted); and when all the bisulphide of carbon is driven off, the quantity of sulphur may be ascertained.

Fit the filter in the test-tube with care. If too tight, it will prevent filtration; if too loose, it will permit some of the oxide to pass through.

Three or four times the bulk of the oxide is about the proportion of

bisulphide of carbon necessary to dissolve out all the sulphur.

It must always be borne in mind that bisulphide of carbon is very inflammable, and in the gaseous state when mixed with air in certain proportions it is explosive. The bisulphide in the holder, B, should be covered with water.

It is best to melt the sulphur in the flask before weighing, to drive

off all bisulphide of carbon.

Gas Lime:

Its Composition, and Use in Agriculture.

In a valuable paper on gas lime, published in the Journal of Gas Lighting,* Professor Voelcker states that a copious supply of air is necessary to transform the injurious sulphur compounds contained in the material into fertilizing agents.

When exposed to the air (and the longer it is kept exposed the better), gas lime is in some respects superior to quick lime as a

manure.

The oxygen of the atmosphere destroys the offensive smell, and changes the sulphuret of calcium in it—first into sulphite, and finally into sulphate of lime or gypsum, well known as a valuable fertilizing substance.

In addition to its chemical virtues, gas lime exercises a beneficial mechanical effect upon land, by rendering stiff, heavy, clayey land more

porous and friable, and by consolidating light sandy soils.

The crops which are particularly benefited by gas lime are—clover, sainfoin, lucerne, peas, beans, vetches, and turnips. It is a useful fertilizer for permanent pasture, destroying the coarser grasses, and favouring the growth of a sweeter and more nutritious herbage.

It kills moss, heath, feather grass, and other plants characteristic of peaty land, its application to which cannot be too strongly recom-

mended.

As a general rule, two tons per acre is the quantity of gas lime

which ought to be put on land.

The proper time for its application is in the autumn or winter.

During the period of storage, the heap should be turned over once
or twice to ensure its complete exposure to the air.

The following is an analysis by Professor Voelcker of a sample of gas lime, kept long enough to be used with safety as a manure:—

Composition of Gas Lime (Dried at 212° Fahr.)

Water of combination as												7.24
Oxides of iron and alumi												2.49
Sulphate of lime (gypsur	n)											4.64
Sulphite of lime												15.19
Carbonate of lime						. 0		-				49.40
Caustic lime ,		3		0		0		0	-		19	18.23
Magnesia and alkalies		•			3		-		-			
Translable silicons motte		•										0.28
Insoluble siliceous matte	ar.	*								-		0.50

In fresh gas lime the proportion of water varies usually from 30 to 40 per cent.

TABLE

Showing the results Obtained by the application of certain Manures to Land. (Mr. Wilson, of Largs.)

Manure.	Produce of the Lot in lbs.	Pounds of Hay per Acre.	Increase per Acre over that Untouched.
Left untouched	420 602	3360 4816	1456
1 ton of lime from gas-works	651	5208	1848
41 cwt. of wood charcoal powder	665	5320	1960
2 bushels of bone dust	693	5544	2184
18 lbs. of nitrate of potash	742	5936	2576
20 lbs. of nitrate of soda	784	6272	2912
10 bushels of soot	819	6552	8192
28 lbs. of sulphate of ammonia	874	6776	3416
100 gals. of ammoniacal liquor from	945	7562	4202

The land was a piece of three years' old pasture, of uniform quality, divided into 10 lots of 20 perches each. All the lots were manured at the same time with the articles given in the table, and the grass cut and made into hay in July. Each application cost the same.

Ammoniacal liquor is best applied at the following strength:-

Ammon Water	iace	al 1	iqu	or	(5°	Tw	add	lel)					11	part.
Water	-6												7	parts.

The proper time for its application is in the spring, after the grass has commenced growing, and during cloudy weather. It may be sprinkled on the land as water is applied to the streets of towns to lay the dust.

COAL PRODUCTS.

Table of the Principal Substances Obtained in the Manufacture of Coal Gas, and in the Utilization of the Residual Products arising therefrom.

Remarks.	5 vols. C, 11 vols. H. A constituent (hydro-carbon) of coal gas. Belongs to the alcohol	radical series of hydrocarbons. 24 vols. C, 5 vols. H. One of the hydrocarbons in coal gas, of the oleffant gas series. It is	also a constituent of coal tar. 24 vols. C, 6 vols. H. Of the marsh gas series	of hydrocarbons. The base of all the dyes bearing this name,	hydrogen on nitro-benzole. Contained in the least volatile portion of the	der, alizarine, is derived from this substance. Derived from anthracene,	A coal tar product. Said to be the most powerful agent known for reducing tem-	A constituent of raw gas, and removed, though not entirely, by condensation.	Remarkable for its solvent power for caout- chouc, gutta-percha, resins, and fata. Used also for preparing varnishes, for removing	grease spots, and cleansing soiled white kid gloves. It is the chief constituent of naphtha, and, treated with nitrio acid, yields nitro-benzole, from which aniline is derived. 3 vols. C, 3 vols. H. One of the hydrocarbons existing in coal gas. Slightly absorbed by	water; easily condensed by cold. Like the other richer bydroarbons, it is absorbed by vulcanized india-rubber tubing.
Boiling Point. Degrees Fahrenheit.	:	As a liquid		∘098	.089		:	:	176°		11
Specific Gravity Water = 1.	4.9 (air = 1)	2.4 (air = 1)	2.49 (air = 1)	1.080	1.147		:	·622 (air = 1)	.850	2·7 (air = 1)	
Reaction.	Neutral	Neutral	Neutral	Alkaline	Neutral	Aoid	:	Neutral	Neutral	Neutral	
Formula or Symbol.	C10 H22	C ₅ H ₁₀	C ₆ H ₁₉	Ce H, N	C14 H10	C14 H8 O2	:	H20	C ₆ H ₆	C ₆ H ₆	
Name of Product.	Amyl	Amylene	Amylhydride	Aniline	Anthracene	Anthraquinone	Antipyrine	Aqueous Vapour	Benzylio Hydride, see Toluole. Benzole, Benzine, or Phene-	Benzole Vapour, or Bicar- buretted Hydrogen,	Bicarburetted Hydrogen,

-							
Remarks,	The liquid One of the impurities in coal gas; and one of the most difficult to eliminate. Not condensed by cold; not soluble in water. Removable by sulphide of calcium (foul lime) in the purifiers.	Contained in coal tar. 4 vols. C. 9 vols. H. A hydrocarbon existing in coal gas, and belonging to the alcohol	radical series. 2 vols. C, 4 vols. H. A hydrocarbon found in cone gas, and of the olefant gas series. It is also a constituent of coal tar. 2 vols. C, 5 vols. H. A hydrocarbon existing in coal gas, and belonging to the marsh gas	and is the lightest of all known liquids; its specific gravity being only '600. One of the scids of coal tar.	Contains valuable antiseptic and disinfecting properties, and is used for making dyes. It is obtained from coal tar. This element is the basis of the illuminating the parishing of the containing the parishing th	gen its particles are heated to incandescence, and emit intense light. Afterwards uniting with the oxygen of the atmosphere to form carbonic acid, one of the products of the combustion of ook gas. The solid deposit	upon the interior surface of gas-refores is almost pure carbon, and is used in the con- struction of the Bunsen galvanic battery, and for the carbon points or candles pro- ducing the Arc electric light.
Boiling Point, Degrees Fahrenbeit.	The liquid	; t:	1 11	3140	870°	ř	M
Specific Gravity Water = 1.	2.64 (air = 1)	3.94 (air = 1)	1.94 (air = 1) Gas 2. (air = 1) Liquid ·600	.973	1.065		
Reaction.	Acid	Acid	Neutral Neutral	Acid	Acid		
Formula or Symbol.	CS ₂	C. H.	C4 H ₁₀	C4 H ₆ O ₂	C ₆ H ₆ O		I.
Name of Product.	Bisulphide of Carbon	Bisulphuret of Carbon, see Bisulphide of Carbon. Brunolio Acid	Butylene, Tetryline, Dite- tryl, or Oil Gas. Butyl-hydride	Butyrio Acid	Carbon Acid, Phenic Acid or Phenol.		Towns state of

Remarks,	A sait produced by the ohemical combination of an monia with carbonic acid gas. When exposed to the atmosphere, it gradually at-	tracts more extremine and from the sir, and becomes hierbonate of ammonia, which is used by bakers, instead of yeast, in preparing light and spongy cakes. The presence of this impurity in common coal gas to the	extent of only 1 per cent. Will diminish the light about 5 per cent. Soluble in its own volume of water. Is entirely removed from gas by the use of lime. Test, lime water. a yol. O. Exists in coal gas in small proportion. 100 yols. water absorb	about 2-43. Test, an ammoniacal solution of subchloride of copper. A constituent of coal tar.	Do. do.	Do. do.	The valuable product obtained in the manufacture of coal gas. Consists mainly of carbon, a constituent of coal tar, contained in the	Includes all the hydrocarbons existing in coal	Volatile hydrocarbons existing in cost gas are liable to be condensed by extreme cold, hence the importance of preventing the gas from being subjected to a temperature below 50° Fahr. A constituent of cost tar,
Bolling Point, Degrees Fahrenheit.	:		:	2000	462°	:	854°	:	4180
Specific Gravity Water = 1.	:	1.62 (air = 1)	.967 (air = 1)		1.081	:		:	
Reaction.	+ 2 HO)	Acid	:	Alkaline	Alkaline	Neutral	 Alkaline	:	Alkaline
Formula or Symbol.	(2 NH ₃ , 3 CO ₃ + 2 HO)	600	00	C ₅ H ₁₃ N	Co H, N	C18 H19	Ce H11 N	:	C10 H1s N
Name of Product.	Carbonate of Ammonia .	Carbonic Acid, called also Black Damp.	Carbonic Oxide	Cespitine	Chinoline	Ohrysene	Coke	Condensable Hydro- carbons.	Coridine

		GA:	S BN	GIN:	EEF	RS A	ND B	ANAG	ers. 	8 8
Remarks.	Obtained in large quantities in the distillation of coal tar. Used in the preservation of timber, such as railway sleepers, &c. It is also useful as a fuel, and in combination	with causing soda and tallow, as a dip lor washing sheep. One of the coal tar acids.	The first naphtha obtained in the distillation of coal tar and which comes over at a tem-	perature from 180° to 310° Fahr. One of the coal tar alkaloids.	honstituent of coal tar, obtained from the	ignous. One of the coal tar alkaloids.	A constituent both of coal gas and tar, of the benzele series of hydrocarbons, 44 vols. C,	o vols. H. 1 vol. N, 1 vol. C. Produced during the destructive distillation of coal, but, with the exception of a very small proportion, which	passes into the gas, is condensed and carried into the tar well along with the ammoniacal liquor. Not readily absorbed by water; but by alkalies and alkaline sulphides. Combined with iron it forms Prussian blue, and is the cause of the bluish-green colour in spent lime. In union with ammonium sulpide, it forms sulphe-eyanide of ammonium, a substance used by photographers, and in the preparation of the constituent of the toys known as "Pharaoh's Serpents."	An alkaline body contained in coal tar.
Bolling Point, Degrees Fahrenheit.	:	£ 85	:	625°	881°	487°	305°	:		-48%
Specific Gravity Water = 1.	:	:	:	:	:	.952	Liquid .870 Gas 4.15 (air = 1)	1.8 (air = 1)		•
Reaction.	:	Acid	Neutral	Alkaline	· :	Alkaline	Neutral	:		Alkaline
Formula or Symbol.	:	С, н, о,	:	Cn Hn N	$C_9~H_{12}$	C ₉ H ₁₃ N	C ₉ H ₁₃	C ₈ N ₃		Clo His N
Name of Product.	Creosote, or Dead Oil	Cresylio Acid, or Cresol .	Crude Naphtha.	Cryptidine	Cumene	Cumidine	Cumole	Cyanogen		Cymidine

Name of Product,	Formula or Symbol.	Reaction.	Specific Gravity Water = 1.	Boiling Point. Degrees Fabrenheit.	Remarks.
Cymole or Cymene Dead Oil, see Creosote.	C10 H14	Neutral	Liquid ·861 Gas 4·63 (air = 1)	840°	A constituent both of coal gas and tar; of the benzole series of hydrocarbons, 5 vols. C, 7 vols. H,
Decyl. Decylene Decyl-hydride	C ₁₀ H ₂₀ C ₁₀ H ₂₀ C ₁₀ H ₂₂	Neutral Neutral Neutral	131	:::	Constituent of coal tar. Do. do.
Disulphide of Carbon, see Bisulphide of Carbon.					
Ditetryl, see Butylene.					
Elayl, see Olefiant Gas.					
Ethyl.	C, H	Neutral	2. (air = 1)	;	Aconstituent of coal gas. 2 vols. C, 5 vols. H.
Ethylamine	C_2 H_1 N	Alkaline	:	အွိ	X-16 vols. soluble in 100 vols. water. A constituent of coal tar.
Ethylene, seeOlefiunt Gas					
Ethyl-hydride	с, н _е	Neutral	1.04 (air = 1)	:	A constituent of coal gan. 1 vol. C, 8 vols. H;
Eupion	:	:	:	:	of the marsh gas series of hydrocarbons. Obtained from ooal tar, and proposed to be
Fire-damp, see Light Carburetted Hydrogen.					used as a substitute for chloroform,
Green Oil	:	:	:	:	This follows the dead oil in the distillation of coal tar, and, mived with resin and oil, is used for making railway grease. Lamp black, from which printers ink is preared.
Heptylene, see Œnanthy. lene.					is also made from ft.

Remarks.	A constituent of coal gas.	A constituent of coal tar, contained in the	ignt oil. A constituent of coal gas.				The different compounds of carbon and hydrogen, gaseous or volatile and condensable, contained in illuminating gas and in coal tar, constituting the light-giving material of the former and the rich and valuable products of the latter.
Boiling Point. Degrees Fahrenbeit.	:	160°	154°				:
Specific Gravity Water = 1.	:	:	:				:
Reaction.	Neutral	Neutral	Neutral				:
Formula or Symbol.	Ce H13	C, H14	C, H11				:
Name of Product.	Hexyl	Hexylene, or Caproylene.	Hexyl-hydride	Hydric Sulphide, see Sulphuretted Hydrogen. Hydride of Amyl, see Hydride of Butyl, see Butyl-hydride. Hydride of Decyl, see Decyl-hydride of Decyl, see Decyl-hydride. Hydride of Ethyl, see Ethyl-hydride. Hydride of Hexyl, see Hydride of Methyl, see Hydride of Methyl, see Hydride of Methyl, see Metyl-hydride. Hydride of Methyl, see Metyl-hydride, of Methyl, see Metyl-hydride, of Methyl, see Metyl-hydride of Octyl, see Octyl-hydride.	Hydride of Phenyl, see Benzole.	Hydride of Propyl, see Propyl-hydride.	Hydrocarbons

	MEW.						
Remarks.	Obtained from coal tar. The lightest known substance in nature. 100 vols, water absorb '38. Oue of the chief constituents of coal gas, in which it exists to the extent of 12 to 50 per cent. Pure hydrogen gives scarcely any light during combustion, but when solid substances are suspended in the flame, which has the high temperature of 5898° Fahr., considerable	light is emitted. Obtained from coal tar.	Obtained from coal tar.	Do. do. obtained from the	heavy ou. A constituent of coal gas to the extent of 80 to 60 per cent. 4 vol. C vapour, 2 vols. H. Not condensed by cold, and not easily decomposed by heat. 100 vols. water absorb	The oil that follows the crude naphtha, and precedes the creosote or dead oil in the destructive distillation of coal tar. It is usually redistilled along with the crude naththat for otherwine benzule. The two	are also used for making black varnish, or for burning in the common naphtha lamp. A solution of ammonia gas in water. A constituent of coal tar, contained in the light oil.
Boiling Point. Degrees Fahrenheit.	::	:	455°	°019	:	:	:008
Specific Gravity Water = 1.	·0691 (air = 1)	:	:	1.072	.56 (air = 1)	:	.946
Reaction.	Acid	Acid	Alkaline	Alkaline	Neutral	:	Alkaline Alkaline
Formula or Symbol.	H H	S (CN) H	C, H, N	C ₁₀ H ₉ N	ъ о	:	C, H, N
Name of Product.	Hydrocyanio Acid Hydroceu	Hydrosulphocysnic Acid. Hydrosulphuric Acid, see Sulphuretted Hydrogen.	Klumine, see Acetyline. Leucoline, or Quinoline	Lepidine	Light Carburetted Hydrogen, also named Marsh Gas, Pit Gas, Fire Damp, and Hydride of Methyl.	Light Oil.	Liquid Ammonia Lutidine

Nitroben-

Nitro-benzol, Nitroben-sine, or Essence of

Mirbane.

Nitrio Aoid . . .

Naphthylami .e.

GAS ENGINEERS AND MANAGERS. vol. C, 3 vols. H. 100 vols. water absorb 5.08 vols. A constituent of coal gas of the A constituent of coal gas of the cleffant gas series of hydrocarbons. s vol. C, 1 vol. H. Not soluble in water. The important salt which is produced from ammoniacal liquor when the latter is satu-5 vols. C, 4 vols. H. A constituent of coal tar. 5 vols. C, 4 vols. H. Not soluble in water, but A constituent of coal tar, obtained from the Nearly all the medicinal preparations of ammonia are obtained from this salt. Used by naphtha and coal tar. Quickly depo-A small proportion of this acid is formed rated with muriatic or hydrochloric acid. alcohol radical series of hydrocarbons. A compound produced from naphthaline. when nitrogen is burnt with coal gas. also in fixing the colours in woollen. Remarks Obtained from coal tar. sited by cold. light oil. Bolling Point. Degrees Fahrenheit, constant. 4140 3.250 Not : : : : : : Specific Gravity Water = 1. ·484 (air = 1) 1.153 4.42 (sir = 1)1.04 (wir = 1.51 : : :

Methyl-hydride, see Light Mirbane, Essence of, see Muriate of Ammonia, or

Methylene

Methylamine

Methyl . .

Mesitylene

Name of Product.

Carburetted Hydrogen.

when sublimated) Sal

Ammoniac.

Nitro-benzole.

which is used for the manufacture of aniline sembling oil of bitter almonds, to perfume The substance produced by the action of fuming nitric soid on benzole naphtha, and colours. It is also used as an odour resoaps and flavour confectionery. : Reaction. Alkaline Neutral Alkaline Neutral Neutral Neutral Neutral Acid : Formula or Symbol. C, H, NO, NH, HOI C10 H, N C, H C, H NH'C HNO

see Crude

Naphthaline Vapour .

Naphthaline.

Naphtha.

rks.	of vols. water absorb 1.48 vol. The presence of nitrogen in coal gas is sometimes due to irregularity in the working of the exhauster. by which a vacuum is created, and air drawn in through the fissures of the retoris. The nitrogen contained in the coal, and which is eliminated by distillation, is evolved in combination with hydrogen as ammonia. Its effect is to injure the illuminating power.	oal gas. do. do. contained in the light oil,	from the light oil.	vol. C, 2 vols. H; 100 vols. water absorb 16. Condensable by cold and great pressure. Exists in coal gas in proportions consistent	from 3 to 27 per cent, and contributes greatly to its illuminating power. It contains twice as much carbon as light carburated hydrogen. Test, brown or fuming sulphurio acid.	C H O W O
Remarks.	10) vols. water absorb 1.48 vol. The present of nitrogen in coal gas is sometimes due irregularity in the working of the exhauste by which a vacuum is created, and air draw in through the fissures of the reforts. The nitrogen contained in the coal, and which eliminated by distillation, is evolved in committee the bination with hydrogen as ammonia. I effect is to injure the illuminating power.	A constituent of coal gas. Do. do. Do. do. cont	Obtained from coal tar, from the light oil.	l vol. C, 2 vols. H; 100 vols. water absorb 16. Condensable by cold and great pressure Exists in coal cas in proportions	from 3 to 27 per cent, and contri- greatly to its illuminating power. It tains twice as much carbon as light or retted hydrogen. Test, brown or tu sulphuric acid. 2.99 vols. absorbed by 100 vols. water.	presence of oxygen in coal gas is due (like nitrogen) to the drawing in of air through the retorts and apparatus by too rapid working of the exhauster, and also to the opening of the retorts and purifiers for charging and discharging. 2 per cent, of air
Boiling Point. Degrees Fahrenheit.	:	246°	210°	:	:	
specific Gravity Water = 1.	.9718 (air = 1)	:::	:	.968 (air = 1)	1.105 (air = 1)	
Reaction.	:	Neutral Neutral Neutral	Neutral	Neutral	:	
Formula or Symbol.	z	គ្នា គឺអ ទី ទី ទី ទី	C, H14	C3 H4	0	
Name of Product.	Nitrogen	Octylene	Enanthylene	Oleflant Gas, Ethylene, or Elayl.	Oxygen .	

Name of Product.	Formula or Symbol.	Reaction.	Specific Gravity Water = 1.	Boiling Point. Degrees Fabrenheit.	Remarks.
Paraffin	C _{IT} H ₃₈ C ₂₇ H ₂₆	Neutral	028.	;	A colourless, solid, erystalline, fatty substance, chiefly obtained from the tar from Boghead cannel. It is manufactured into candles, giving a brilliant white light; and oil of high inbricating properties is made from it. Parafilu oil will only burn in the presence of a wick, and is therefore perfectly safe.
Anthracene. Parvoline, see Cumidine. Pentahiroline. Pentylene Phenio Acid, see Carbolic Acid.	C ₁₃ H ₁₅ N	1 1	1 11	: %	A constituent of coal tar, obtained from the heavy oil. A constituent of coal tar, contained in the light oil.
Phlorylio Acid, or Phlorol Picoline Pit Gas, see Light Carbu- retted Hydrogen.	C ₆ H ₁₀ O C ₆ H ₇ N	Acid Alkaline	.96.	424° 273°	Do. do. contained in the light oil.
Pittacal	11	1.1	1 1	1 1	Found in the heaviest portions of the coal tar- oil. The residue remaining of the distillation of coal tar, of which it constitutes about 66
Propyl	C ₃ H ₇	Neutral Neutral	2.97 (sir = 1) 1.455 (sir = 1)	+ +	20 70 70 10
Propy-hydride	Св. Нв	Neutral	Neutral 1.522 (air = 1)		व्यं 🛶

	NEW	BIGG	ING'S	HANDBOOK FOR
	light oil.	do,	The foul lime of the purifiers. Used as a manure or top dressing for land.	The hydrated peroxide of iron, employed in abstracting the sulphuretted hydrogen from the gas, having become charged with free sulphur to the extent of 40 to 75 per cent. by a succession of foulings and revivifications, is used by the manufacturing chemists for making sulphuric acid. The valuable salt produced by the neutralization of the animonia from anmoniated liquor with sulphuric acid. Largely used
ngnt oil.	A constituent light oil.	Do.	The foul lime manure or to	The hydrated peroxide of abstracting the sulpture the gas, having become sulpture to the extent of a succession of foulings is used by the manufacture and sulpture acid. The valuable salt production of the ammonial liquor with sulpturio.

:

:

:

Spent Lime, see also Sul-Sal Ammoniac, see Muri-

phide of Calcium. ate of Ammonia.

:

:

Spent Oxide of Iron .

:

:

:

:

Sulphate of Ammonia. . | 2 (N H4) SO4

facture of ammonia alum.

The "fonled" lime of the purifiers, and which is efficacious in absorbing from the gas the islanghide of carbon impurity, and the sulphur compounds other than sulphuretted

:

:

Salphide of Calcium, or Spent Lime.

Sulphide of Carbon, see Bisulphide of Carbon.

as a manure, and, by the addition of a solu-tion of sulphate of alumina, in the manu-

. 446°

::

Alkaline

C₁₉ H₁₄ O₃ C₁₁ H₁₇ N

Uninoline, see Leucoline

Pyrrol

Rosolic Acid Rubidine

271°

1.077

Alkaline

C, H, N

constituent of coal tar, contained in the

ight oil.

24:3

9

Alkaline

C, H, N

Pyridine, see Pyrrhidine.

Pyrene

Pyrrhidine . . .

Remarks.

Boiling Point. Degrees Fahrenheit.

Specific Gravity Water = 1.

Reaction.

Formula or Symbol.

Name of Product.

White crystalline

A constituent of coal tar.

:

:

Neutral

C16 H10

Name of Product.	Formula or Symbol.	Reaction.	Specific Gravity Water = 1.	Boiling Point. Degrees Fahrenheit.	Remarks.
Sulphocyanogen	SCN	:	:	:	A constituent of raw gas.
Sulpho-hydrocarbons	:	:	:	:	Sulphur impurities existing in coal gas.
Salphur	SO	:	:	.0220	In the best gas-producing coals the amount of sulphur present rarely exceeds 1s per cent, generally it is much less. In the process of distillation about non-half the contained sulphur remains in the residual cocks, whilst the other half is volatilized, and, combining with H and C, constitutes
Sulphuret of Carbon, see Bianphide of Carbon. Sulphuretted Hydrogen	H, S	Acid	1·1747 (air = 1)	:	Impurities requiring removal. The chief impurity in raw or crude coal gas. It is entirely removed by the use of lime or oxide of iron. It is an inflammable gas, and generates sulphurous acid in burning. I vol. of water at 60° absorbs 3.28 vols. of the gas.
Sulphurio Aoid.	H³ SO4	Aoid	1.815	3838 388	Test, acctate of lead or nitrate of silver in solution. This, which is the most important and useful of all the soids, is largely manufactured from the supplur contained in the spent oxide of iron, after having been used in the
Salphurous Acid (or Sulphur Dioxide)	80 3	Aoid	2.247 (air = 1)	:	purification of coal gas from sulphuretted hydrogen. This gas is produced when sulphur and its compounds are burnt. Hence, illuminating gas containing sulphur yields it during combustion. The quantity given out, however, even with the most impure gas (asy, with 40 grains sulphur in the 100 (set), is so inap-
			_		preciable as to be perfectly innocuous in its effects, especially where the smallest attention is paid to ventilation.

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Remarks.	duced in the destructive distillation of ocal, and from which a great variety of valuable products is obtained. It consists almost entirely of hydrocarbon compounds, with a varying proportion of soil carbon. Tar, on distillation, yields on an average— 2 4 per cent, ammoniacal liquor 1 6 crude naphtha 28 8 moreote or dead oil 66 0 mpton		benzele series of hydrocarbons. 3½ vols. C, 4 vols. H. Not soluble in water. A constituent of coal far, obtained from the	heavy oil. A constituent of coal tar. Produced as aqueous vapour, in more or less proportion, during the distillation of coal.	It is also one of the products of the combus- tion of coal gas, from the union of the hydro- gen of the gas with the oxygen of the air. the base of xylidiue, obtained from the light oil. Used in the preparation of scarlet dyes.	A constituent both of coal gas and tar. Of the bensele series of hydrocarbons. 4 vols. U, 5 vols. H. Not soluble in water.
Boiling Point. Degrees Fahrenheit.	:	335K° 2832°	:	484° 212°	c 888	259°
Specific Gravity Water = 1.	Ordinary Coal Tar. 1-120 to 1-150 Cannel Coal Tar '980 to 1-060	Liquid .670	Gas 3:179 (air = 1)	1.000	:	Liquid '867 Gas 3·662 (air == 1)
Reaction.	:	Alkaline Neutral		Alkaline Neutral	:	Neutral
Formula or Symbol.	:	C, H, N C, H,	C, H., N	$C_{13} \frac{H_{19}}{H_2} N$	C, H ₁₀	C, H ₁₀
Name of Product.		Tetrylene, see Butylene. Thiotyanogen, see Sulpho- oyanogen. Toludine	Tritylene, see Propylene.	Viridine	Xylene	Xylidine, see Collidine. Xylole.

CHEMICAL AND OTHER MEMORANDA.

The compounds of the non-metallic elements with the metals and with each other have names ending in "ide" or "uret :" as Fe S. sulphide or sulphuret of iron.

When two or more atoms or equivalents of the non-metallic elements enter into combination, the number of atoms or equivalents is expressed by prefixes.

. means 1 atom, as No O, nitrogen mon-oxide.

Di, bin, or bi means 2 atoms, as N2 O2, nitrogen di-oxide, or bin-oxide of nitrogen: CS2, bi-sulphide or di-sulphide of carbon.

. means 3 atoms, as No Os, nitrogen tri-oxide; Sbo S 3, tersulphide of antimony.

Tetr. . . means 4 atoms, as N2 O4, nitrogen tetr-oxide.

Pent or penta means 5 atoms, as No Os, nitrogen pent-oxide; PCls, penta-chloride of phosphorus.

. means $1\frac{1}{2}$ atoms (=2 to 3), as Fe₂O₃, sesqui-oxide of iron.

Proto or prot means first, as Fe O, prot-oxide of iron. Sub . . . means under, as Cu, O, sub-oxide of copper. . means the highest, as H Cl O4, per-chloric acid.

The terminations "ic" and "ous" are used for acids; the former representing a higher state of oxidation than the latter.

When a substance forms more than two acid compounds, the pre-fixes "hypo," under, and "hypher" above, are used.

The smaller number, as H2, placed to the right of, and slightly below a symbol is called the exponent, and indicates the number of times that the combining weight of the substance has to be taken. When the symbol is without a number—thus, H—the number one is understood. The small numbers modify only the symbol immediately preceding, but larger numbers prefixed to the symbol modify all that follow as far as the next comma or + sign: thus 2H, SO, signifies that four of hydrogen, two of sulphur, and eight of oxygen, or, more correctly, that two of sulphuric acid (H. SO, being the formula for sulphuric acid) are to be taken.

A base is a compound which will chemically combine with an acid.

A salt is a compound of an acid and a base.

When water is in combination with acids or bases, they are said to be hydrated.

Alkalies neutralize acids, forming salts.

Alkalies turn vegetable reds to blue, and yellows to brown. Acids turn vegetable blues to red, and browns to yellow.

A simple or elementary substance is a body that cannot be resolved or separated into any simpler substances—as oxygen, carbon, iron.

A compound substance is one consisting of two or more constituents -as water, carbonic acid gas, olefiant gas.

The equivalent number or atomic or combining weight expresses the relation that subsists between the different proportions by weight in which substances unite chemically with each other.

The equivalent or combining weight of a compound is the sum of

the combining weight of its constituents.

Specific gravity expresses the difference that subsists between the weights of equal volumes of bodies. Gases are usually compared with air as 1 000, liquids and solids with water as 1 000.

So far as chemists have been able to discover, there are about 65

elementary or simple substances.

No compound body contains all the elementary substances. Most compounds are composed of two, three, or four elements.

TABLE OF ELEMENTARY SUBSTANCES.

Names of Elements.	Symbols.	Atomic Weights.	Names of Elements.	Symbols.	Atomie Weights
Aluminium	Al	27.5	Mercury (Hydrarg.).	Hg	200
Antimony (stibium)	Sb	122	Molybdenum	Mo	96
Arsenic	As	75	Nickel	Ni	59
Barium	Ba	137	Niobium	Nb	94
Bismuth	Bi	208	Nitrogen	N	14
Boron	В	11	Osmium	Os	199
Bromine	Br	80	Oxygen	0	16
Cadmium	Cd	112	Palladium	Pd	106
Cæsinm	Cs	133	Phosphorus	P	31
Calcium	Ca	40	Platinum	Pt	197.18
Carbon	C	12	Potassium (Kalium).	K	39
Cerium	Ce	140.42	Rhodium	Rh	104
Chlorine	Cl	35.5	Rubidium	Rb	85
Chromium	Cr	52	Ruthenium	Ru	104
Cobalt	Co	59	Selenium	Se	79
Copper (Cuprum)	Cu	63.5	Silicium or Silicon .	Si	28
Didymium	D	174-57	Silver (Argentom) .	Ag	108
Erbium.	E	165 89	Sodium (Natrium) .	Na	23
Fluorine	F	19	Strontium	Sr	87.5
Glucinum or Beryl-	-	9.4	Sulphur	S	32
lium	GI	9.4	Tantalum or Colum-	Ta	100
Gold (Aurum)	Au	197	bium	Ta	182
Hydrogen	H	1	Tellurium	Te	128
Indium	In	113.4	Thallium	Tl	204
Iodine	I	127	Thorium	Th	233 41
Iridium	Ir	192	Tin (Stannum)	Sn	118
Iron (Ferrum)	Fe	56	Titanium	Ti	50
Lanthanum	La	138-52	Tungsten (Wolfram)	W	184
Lead (Plumbum) .	Pb	207	Uranium	U	238 48
Lithium	Li	7	Vanadium	V	51.3
Magnesium	Mg	24	Yttrium	Y	172.76
Manganese (Manga-)		55	Zine	Zn	65
nium)	Mn	00	Zirconium	Zr	90

LIST OF SUBSTANCES,

Simple and Compound, frequently mentioned in Connection with the Manufacture and Purification of Coal Gas and the Residual Products resulting therefrom.

Name of Substance.	Symbol.
Ammonia	NH_8
Aniline	$C_{12}H_7N$
Aqueous vapour	$H_{2}O$
Benzole	C_6H_6
Bisulphide of carbon	CS ₂
Bisulphide of iron	Fe S ₂
Butylene	C_4H_8
Carbon	C
Carbolic acid	$C_{19}H_6O_2$
Carbonate of ammonia	2 NH ₃ 3 CO ₂ + 2 HO
Carbonate of lime	Ca CO _s
Carbonic acid	CO ₂
Carbonic oxide	CO
Cyanogen	C ₂ N ₂
Hydrogen	H
Hydrochloric or muriatic acid	HCl.
Light carburetted hydrogen .	CH,
Muriate of ammonia	NHaHCl, or NHACl
Naphthaline	C ₁₀ H ₈
Nitrogen	N
Nitric acid	HNO ₂
Nitric acid	$C_{2}H_{4}$
Oxygen	0
Oxide of calcium (caustic lime)	Ca O
Oxide of potassium (caustic)	
potash)	K ₂ O
Oxide of sodium (caustic soda)	Na ₂ O
Peroxide of iron	Fe ₂ O ₅
Protoxide of iron	Fe O
Protosulphide of iron	Fe S
Protochloride of manganese.	Mn Cl.
Propylene	C ₈ H ₆
Sesquisulphide of iron	Fe ₂ S ₈
Sulphur	S
Sulphate of ammonia	2 (NH ₄) SO ₄
Sulphide of calcium	Ca S
Sulphuretted hydrogen	H ₂ S
Sulphuric acid	H ₂ SO ₄
Culphun dianida	SO ₂
Water	H ₂ O
114601 1 1 1 1 1 1 1	222

To ascertain the proportion, by weight, of the different substances in a compound, multiply the atomic weight of each substance by the exponent.

For example: Take olefiant gas, C₂ H₄, which, as its formula indicates, consists, by weight, of two atoms of carbon combined with

four atoms of hydrogen-

Atomic Weight. Exponent. Proportion. by Weight. C $12 \times 2 = 24$ or $85 \cdot 715$ per cent. H $1 \times 4 = 4$ or $14 \cdot 285$...

So that, 24 grains, or 24 ounces, or 25 pounds of carbon, combine with 4 grains, or 4 ounces, or 4 pounds of hydrogen to form 28 grains, or 28 ounces, or 28 pounds, and so on, of olefant gas.

COMMON NAMES OF CERTAIN CHEMICAL SUBSTANCES.

		440.00
Aqua fortis		Nitric acid
Aqua regia		A mixture of nitric and hydrochloric
The state of the s		acids, so called from its property of
		dissolving gold.
Bluestone, or blue vitriol	16.	Sulphate of copper.
Calomel		Chloride of mercury.
Chloroform		Chloride of formyle.
Choke-damp		Carbon dioxide.
Common salt		Chloride of sodium.
Copperas, or green vitriol	1.	Sulphate of iron.
Corrosive sublimate		Bichloride of mercury.
Dry alum		Sulphate of alumina and potash.
Epsom salts	14	Sulphate of magnesia.
Ethiops mineral		Black sulphate of mercury.
Fire-damp	5	Light carburetted hydrogen.
Galena		Sulphide of lead.
Glauber's salts	10	Sulphate of soda.
Goulard water		Basic acetate of lead.
Iron pyrites		Bisulphide of iron.
Jeweller's putty		Oxide of tin.
King's yellow		Sulphide of arsenic.
Laughing gas	-	Protoxite of nitrogen.
Lime		Oxide of calcium.
Lunar caustic	16	Nitrate of silver.
Mosaic gold	112	ACCUSATION OF THE PROPERTY OF
Muriate of lime	100	Chloride of calcium.
Nitre, or saltpetre		Nitrate of potash.
annal or omplette	88.7	

	СH	EM	IIC.	AL	SU	BSTANCES—Continued.
Oil of vitriol						Sulphuric acid.
Potash .				•		Oxide of potassium.
Realgar .						Sulphide of arsenic
Red lead .				•		Oxide of lead.
Rust of iron						Oxide of iron.
Sal ammonia	c					Muriate of ammonia.
Soda				•	•	Oxide of sodium.
Spirits of ha			ı.			Ammonia.
Spirit of salt				•		•
Stucco, or pla	aste	r o	fPε	ıris	•	
Sugar of lead	l	•	•	•		
Tincal .	•	•	•	•	•	Crude borax.
Verdigris		•		•	•	
Vermilion	•	•		•	•	
Vinegar .	•	•		•	•	
Volatile alka	li	•			•	Ammonia.
\mathbf{W} ad			•	•		Black oxide of manganese.
Water .	•				•	Oxide of hydrogen.
White vitriol	•	•	•	٠	•	Sulphate of zinc.

TABLE OF VARIOUS GASES.

Their Specific Gravity, Weight, and Solubility in Water. 60° Fahr. 80 in. Barometer.

Name.	Specific Gravity. Air equal 1:000	Cubic Foot in	of aCubic Foot in	Number of Cubic Ft. equal to 1 lb.	Solubility, 100 Vols. of Water absorb.
Hydrogen Light carburetted hydrogen Ammonia Carbonio oxide . Olefiant gas . Nitrogen . Air . Nitrio oxide .	·0691 ·559 ·590 ·967 ·968 ·9713 1·000 1·039	·00529997 ·0428753 ·045258 ·0741689 ·0742456 ·07449871 ·0767 ·0796918	87·09 800·12 816·77 519·18 519·71 521·49 536·90 557·83	188 · 68 23 · 32 22 · 09 13 · 48 13 · 46 13 · 42 13 · 03 12 · 54	1.93 Vols. 3.91 72,720 2.43 16.15 1.48 1.70 { Notsoluble in weter
Oxygen Sulphuretted hydrogen Nitrous oxide Carbonic soid Sulphurous scid Chlorine Bisulphide of carbon	1·1056 1·1747 1·527 1·529 2·247 2·470 2·640	189449	593·59 680·69 819·84 820·92 1206·41 1326·14	11·79 11·09 8·53 8·52	in water. 2'99 Vols. 323'26 ,, 77'78 ,, 100'20 ,, 4276'60 ,, 236'80 { Not

To reduce a volume of gas of any specific gravity to pounds avoirdupois, multiply the volume by the sp. gr. and by .0767.

Example.—Required the weight of 1500 cubic feet of gas whose specific gravity is .520.

$$1500 \times .520 \times .0767 = 59.826$$
 lbs.

To find the weight in pounds avoirdupois of a cubic foot of air at different temperatures, and under different pressures.

$$W = \frac{1.8253 \times B}{459 + T}$$

Example.—Required the weight of a cubic foot of air, the barometer being at 29.5 inches, and the temperature 84° Fahr.

$$\frac{1.8258 \times 29.5}{459 + 84} = .072 \text{ lb.}$$

Luting for Experiments in Chemistry.

For temporarily securing the joints of chemical vessels, glass stoppers, &c., use equal parts by weight of linseed meal and whiting made into a stiff paste with water. The two substances should be well triturated in a mortar, and the water added till of the proper consistency.

Pieces of vulcanized india-rubber tubing are very suitable for joining the ends of glass and earthenware tubes. The india-rubber is

slipped over the ends, and secured with pack-thread.

India-rubber capsules for bottle necks, having a hole through them for the insertion of glass tubes are handier, and more likely to be gastight than the ordinary corks.

AVERAGE COMPOSITION OF LONDON GAS BY VOLUME.

(Dr. Letheby, 1866.)

							Con	nmon G	las.			Ce	nnel Gas.
Hydrogen .							1	46.0					27.7
Light carburette	ed	hy	dro	gen				39.5					50.0
Olefiant gas .								3.8					13.0
Carbonic oxide		4						7.5					6.8
Carbonic acid				10				0.7					0.1
Aqueous vapour				4	5			2.0					2.0
Nitrogen	4			4	1	4		0.5		0			0.4
								100.0				-	100.0

Relative Value of Different Illuminating Agents in Regard to their Illuminating Properties. (Dr. Letheby, 1866).

Name.	Rate of Consumption per Hour.	Illum. Power. (Sperm, 120 grs.)	Quantity 14 Candles.
Cannel gas	4 feet.	18.67	8 feet.
Coal gas	. 5 ,,	14.00	5 11
Paraffin oil	. 301 grs. 265	7:11	857 grs.
Sperm oil	000	10.00	000
Colza oil	0.10	9.01	1008 "
Paraffin candles .	122 "	1.46	1171 "
Sperm	. 132 "	1.85	1440 "
Wax "	. 168 ,,	1.48	1652 ,,
Steario	. 140 ,,	1.13	1732 ,,
Composite " .	. 144 ,,	1.08	1858 ,,
Tallow " .	. 145 ,,	0.83	2542 ,,

TABLE.

Comparing Gas with the other Ordinary Light-giving Materials. (Dr. Letheby.)

5 cubic feet of common gas (at 4s. per 1000 cubic feet) give a light equal to-

2.5 Argand lamps, burning the best sperm oil at the rate of 133

grains per hour (price of sperm, 8s. per gallon); or,
23 mould tallow candles of six to the pound, each burning at the rate of 145 grains per hour (price 6d. per lb.); or, 18 common oil lamps, burning the best sperm oil at the rate of 188

grains per hour (price of sperm, 8s. per gallon); or, 18 sperm candles, six to the pound, each burning at the rate of 188 grains per hour (price 2s. per lb.); or,

15 composition candles, six to the pound, each burning at the rate

of 136 grains per hour (price 2s. per lb.); or,

16.25 wax candles, six to the pound (2s. per lb.)

Estimating the cost of the gas and other light-giving materials a the price affixed, we have the next

TABLE.

Showing the Relative Cost of the Various Illuminating Agents.

Gas					equal to	1
Sperm oil burnt in Argands			4		44	8
Mould tallow sandles six to the nound			- 71		33	10
Mould tallow candles, six to the pound					33	12
Sperm oil burnt in an open lamp .					1 20	17
			*	1.7	11	1.4
Sperm candles, six to the pound	×.	1	4			24
					31.	
Composition candles, six to the pound						29
					11.	-
Wax candles, six to the pound					33	80

In other words, 1s. worth of gas will go as far in the production of light as 8s. worth of sperm oil burnt in an Argand lamp, or 12s. worth of ordinary mould candles, or 17s. worth of sperm oil burnt in an open lamp, or 24s. worth of sperm candles, or 29s. worth of composition candles, or 30s. worth of wax candles.

TABLE.

Showing the Relative Proportions which the Ordinary Light-giving Materials bear to 1000 Cubic Feet of 18-Candle Gas, as estimated by Mr. Lewis Thompson.

1000			nmon gas were	}	44\$ lbs. of sperm candles.
	10	10	**		489 lbs. of carefully snuffed wax candles.
	15	11	**		52 0 lbs. of best mould candles.
	**	**	11	1	54 lbs. of best dip candles.
	29	15		1	6½ gallons of purified colza oil. Specific gravity, '915.
	"	"	**	1	510 gallons of sperm oil. Specific gravity, 888.

The comparative values of the different light-giving materials may be readily estimated from the foregoing tabular statement of relative proportions. Thus, for instance, if the cost of gas be 4s. 6d. per 1000 cubic feet, the cost of wax candles that yield an equal quantity of light, at 2s. 4d. per lb., would be £5 14s.

RELATIVE VALUES OF ILLUMINATING AGENTS.

In respect of their Heating and Vitiating Effects on the Atmosphere, when Burning so as to Give the Light of 12 Standard Sperm Candles. (Dr. Letheby.)

	Pounds ater He 1º Fahr	ated	1		C	Oxygen consume ubic Fe	ed		cid	Produ bic Fee	ced		(C	Air Vitiated ubic Feet).
Cannel gas .	1950			4	1	3.30				2.01				50.2
Common gas .	2786				-	5.45		16		3.21			-	80.2
Sperm oil .	2335					4.75			-	3.33				83.3
Benzole	2326					4.46				3.54				88.5
Paraffin	3619					6.81		14.0		4.50	Fair		-	112.5
Camphine	3251					6:65				4.77				119.2
Sperm candles	3517					7.57				5.27	10.1	-		131.7
Wax candles .	3831					8.41				5.90		-		149.5
Stearic candles	3747				1	8.82			-	6.25		-	-	156.2
Tallow candles	5054					12.06				8.73			1	218-3

TABLE.

Indicating the Comparative Salubrity of the Several Illuminating
Materials.

The flame of coal gas, and the flames of several combustible bodies that gave an amount of light equal to it, were burned separately in given quantities of atmospheric air, and the times were noted at which the flames were extinguished by the contamination of the air. The following were the results:—

Colza oil .						was exting	guished in	71	minutes
Olive oil						"	33	72	**
Russian tallow						"	33	75	11
Sperm oil .						25	11	76	***
Steario acid				15	10	11	"	77	11
Wax candles			10	100	3	-		79	
Spermaceti can				100	-	**	n	83	"
						"	**	98	23
Coal gas (13 car			*			33	"	-	33
Cannel gas (28	candi	les)				**	**	152	33

From which it appears that the atmosphere of a confined room lighted by cannel gas will support life twice as long as the atmosphere of the same room lighted equally by tallow candles.

Relative Cost of the Magnesium Light, Stearine Candles, and Common Coal Gas. (Dr. Frankland, 1865).

21	oz, of magnesium wire, at 21s. per oz	 	£2	12	6
20	lbs. of stearine candles, at ls		1	0	0
404	cubic feet of 12 candle gas at 4s fid ner 1000 .			1	Qs

TABLE.

Calorific Power of Various Photogenic Compounds. (F. J. Evans).

Name of Gas, &c.	-	Feet o ound,		C	ns	ds of aised : by the sumpti	on o	of		Co	ands of Water raised 1° by the ensumption of 1 lb. of Gas.
Hydrogen	. 9	0.0 2.4 6.5 6.69	 			300 650 760 1200					54,000 21,060 20,140 20,028
Sperm candles, 6 to the lb.									-	1 11	o. of candles. 17,567
Sperm oil, burnt in a lamp										1	1b of oil. 16,490

D D 2

TABLE.
Combustion, Temperature, Explosive Power, and Mechanical Power of Gases. (Lethebax).

	Per II	Per lb. Substance.	ance.	Poun	Pounds Water Heated 1° Fahr.	outed	Tem	Temperature of Combustion.	f Combus	tion.	Explosiv	Explosive Power.	Mechanical Power per lb.
1	. 6	000	Air	1	Per	Per lb.	Open Flame.	Plame.	Closed Vessel.	Vessel.	With		Tons
	Used.	Pro-	viti-	Sub- stance.	Cabio Foot Substance.	Ox. Used.	7	With Ox. With Air.	With Ox.	With Air.	Ox.	Air.	High.
	Cubic	Cubic	Cubic	Lbs.	Lbs.	Lbs.	Deg.	Deg.	Deg.	Deg.	Atmo-	Atmo-	Tons.
Tydrogen	93.4	0.0	467		329	7,754	14,510	5,744	19,035	7,852	25.6	12.6	068'12
Marsh gas	47.3	23.6	826		966	5,878	14,130	4,762	18,851	6,680	87.0	14.0	8,108
Dlefiant gas	40.2	27.0	878	-	1,585	6,225	16,535	5,217	21,844	7,200	6.56	19.1	7,360
Propylene	40.5	0.72	878	91 897	3,168	6,920	16.522	5.939	21,027	7,177	86.8	30.08	7,360
cetylene	86.3	29.1	606		1,251	5,914	17,146	6,142	22,006	600'4	87.9	17.6	6,275
Benzole	86.3	29.1	606		3,860	5,915	17,146	5,143	55,006	600'2	118.7	62.8	6,275
Carbonic oxide .	2.9	18.2	371		320	7,569	12,719	6,358	16,178	7,225	8.12	11.7	1,490
Sisulphide carbon	14.9	0.9	689		1,239	4,845	15,280	4,314	20,031	6,917	80.00	11.6	2,110
sulph. hydrogen	10.1	0.0	630		000	172,0	19,000	2,000	17,042	6,020	0.97	12.0	0,00
Cyanogen	97.5	17.6	618		650	6.816	14.890	5.928	18,101	7.001	8.66	14.6	7,262
Janual oas	81.0	25.0	698		260	6,503	14.826	5,121	19,046	7,186	88.8	18.0	6,945
Wood spirit	25.3	11.8	422		818	6,363	11,485	4,641	14,902	6,847	40.8	16.8	8,290
loohol	24.6	16.4	583		1,597	6,195	13,305	4,831	17,223	6,629	46.4	1.91	4,465
Sther	80.8	50.4	664		8,217	6,158	14,874	6,150	19,225	6,953	9.89	19.0	6,603
Camphine	38.9	8.12	880		7,184	5,942	16,271	6,026	20,953	6,922	9.4	16.0	6,760
permaceti	87.0	25.2	816			6,088	14,599	4,418				**	6,066
Vax	87.7	25.6	829		:	4,995	12,921	4,122	**	**		-	5,451
Stearic acid	34.6	24.0	783		::	6,061	15,885	4,818	***	:			0880
Stearin	84.4	14.8	527		***	6,143	15,815	5,095	**	**			6,207
Paraffin	40.2	27.0	878			6,220	16,522	6,589	**			**	7,364
Paraffin oil	40.2	0.28	878	80		6,220	16,522	6,589	0.0			**	7,864
Rape oil	88.7	24.8	801		:	6,123	15,830	6,087		**	:		6,121
perm oil	28.4	24.3	801	27		6,088	16,863	4,987		**	:	***	196,0
Carbon	0.18	9.18	5943		1	1000	WW. RI	25 (19.74)					VIOV

TABLE. Heats of Combustion with Oxygen.

Substance.	British Thermal Units of Heat.	Pounds of Water at 212° Fahr. Evaporated per Pound of Substance
Hydrogen	61,500	68 · 66
Alcohol	12,968	18.42
Bensene	18,600	19.25
Carbon bisulphide	6,152	6.37
Carbon burning to carbonic acid	12,906	13.36
Carbon burning to carbonic oxide	2,495	2.58
Carbonic oxide burning to carbonic acid	4,478	4.68
Chargonl, wood	12,455	12.90
Coal, anthracite	15,600	16.14
Coal heat hiteminons	15.504	16.06
Coke, produced from ditto	14.875	14.88
Coal, average quality	13,600	14.08
Coke, produced from ditto	12,800	13.25
Rthylene	21,500	22.25
Graphite	14,067	14.56
Light carburetted hydrogen, or marsh gas .	24,020	24.86
Lignite	11,710	12.12
Olefiant gas	21,875	22.12
Olefiant gas	17,784	18:41
Peat, dry	9,983	10.88
Petroleum	20,272	20.98
Propylene	21,200	21.94
Sulphur	4,102	4.25
Sulphurio ether	16,282	16.85
Turpentine	19,566	20.25
Wood, dry	7,824	8.10
Cubic Feet per lb.	•	
Coal gas, 17 candles 82.227	21,696	22.46
Water gas	6,649	6.88
Water gas	1,897	1.96
Producer water gas 13.478	983	1.02

The British standard unit of heat (thermal unit) is the amount of heat required to raise the temperature of 1 lb. avoirdupois of water 1° Fahrenheit.

The French standard unit of heat (calorie) is the amount of heat required to raise the temperature of 1 kilogramme of water 1° Centigrade.

The number of British units of heat required to evaporate 1 lb. of water at boiling point, 212° Fahr., is 966; and at 62° Fahr., 1116.

The number of French units of heat required to evaporate 1 kilo. of water at boiling point, 100° Cent., is 536.7; and at 16.6° Cent., 620.1.

One British unit of heat = .0251996 French units.

One French unit of heat = 8.96832 British units.

The total heating power of any fuel, expressed in British units, ÷ 966 = lbs. of water at 212° Fahr. evaporated per lb. of fuel.

Example:—1 lb. of hydrogen yields in combustion 61,500 units of heat.

Then : $-\frac{61,500}{966} = 63.66$ lbs. of water at 212° Fahr. evaporated per lb. of hydrogen.

DISTILLED WATER.

(At 62° Fahr.)

1 pint = 34.65 cubic inches, or 1.25 lbs. 1 gal. = 277.274 cubic inches, or 10 lbs. 11.2 gals., or 1.792 c. ft. = 1 cwt. 224 gals., or 35.84 c. ft. = 1 ton. 1 cubic inch = 252.45 grs. or .036075 lbs. 12 ,, inches = .434 lbs. " foot = 6.25 gals., or 1000 ozs., or 62.5 lbs. 1 1.8,, " = 1 cwt. 35.84 cubic feet = 1 ton. 1 cylindrical inch = .02842 lbs. inches = .341 lbs. 12 12 foot = 5 gals., or 49.1 lbs. 1 2.282 ,, feet = 1 cwt. 45.64 ,, ,, = 1 ton.

Centre of pressure \(\frac{2}{3} \) depth from surface.

Water is at its maximum density at 39 \cdot 2° Fahr. (4° C.), and expands

1-10th part of its bulk on freezing.

SPECIFIC HEAT OF SUBSTANCES.

The meaning implied in the term "specific heat," or more correctly "calorific capacity," is the quantity of heat required to raise the temperature of a substance 1° (independently of the unit of mass and scale of temperature); water being taken as the standard of comparison.

For example: the specific heat of mercury is '03332, by which is to be understood that thirty times as much heat is required to raise water to a given temperature as an equal weight of mercury. In other words, the quantity of heat which would raise the temperature of any given weight of mercury through 1°, would only raise the temperature of a like weight of water through '03332°.

SPECIFIC HEAT OF SOLIDS AND LIQUIDS.

(Wat	

	(water	as 1.)	
Acetic acid	6589	Lead	.0314
Alcohol (sp. gr. '793)	622	Lime, burned	.217
Aluminium	.2143	Lithium	19408
Antimony, cast	*05077	Magnesium	*2499
Arsenic	.0814	Manganese	.1217
Bees-wax	*45	Marble, white	.21585
Benzine	-3952	Mercury	.03332
Birch .	.48	Nickel	10863
Bismuth	.03084	Oil, olive	*8096
Brass	.09391	Oil, sweet	.31
Brick, common	.2	Oil of turpentine	*472
Brick, fire.	-22	Palladium	*05928
Cadmium.	.05669	Phosphorous	18949
Chalk, white.	·21485	Pine	-65
Charcoal, animal, calcined .	26085	Platinum	.03243
Charcoal, wood	.24111	Potassium	*1696
Clay, white, burned	.185	Selenium.	.07616
Conl	-2777	Silicon, crystalized	1774
Cobalt	10696	Silicon, fused	175
Copper	.09215	Silver	.05701
Diamond	.14687	Sodium	*2934
Ether	.5207	Spermaceti	*32
Glass	.19768	Steel	1175
Gold	.03244	Sulphur	.20259
Graphite	-20187	Sulphuric acid	*333
Ice	.504	Tellurium	.04737
Iodine	.05412	Thallium	.0336
Iron, cast	12983	Tin	.05695
Iron, wrought	-11379	Zinc	.09555

SPECIFIC HEAT OF GASES AND VAPOURS.

		0.54		
			Equal Weights.	Equal Volumes.
	Air		. 0.2374	0.2374
4	Oxygen		. 0.2175	0.2405
Simple	Nitrogen		. 0.2438	0.2370
gases.	Hydrogen	1 5 6	. 3.4090	0.2359
Buocos	Chlorine		. 0.1210	0.2962
Vapour.	Bromine		. 0.0555	0.3040
, mpour,	Binoxide of nitrogen .		. 0.2315	0.2406
	Carbonic oxide		0.2450	0.2370
	Carbonie acid		. 0.2163	0.3307
	Sulphuretted hydrogen		. 0.2432	0.2857
Compound	Sulphurous anhydride .		. 0.1553	0.3414
gases.	Hydrochloric acid		. 0.1845	0.2333
Baroca,	Nitrous oxide		0.2262	0.3447
	Nitric oxide		. 0.2317	0.2406
				0.2966
	Ammonia		. 0.5083	0.3277
	Marsh gas		. 0.5929	
	Olefiant gas (ethylene) .		. 0.4040	. 0.4106
	Water (steam)	A	. 0.4805	. , 0.2984
	Ether		. 0.4810	1.2296
	Chloroform		. 0.1567	0.6461
Vapours.	Alcohol		. 0.4534	0.7171
-	Turpentine		. 0.5061	2:3776
	Bisulphide of carbon .		. 0.1570	
	Benzole		. 0.3754	
	TO SECURE OF THE PARTY OF THE P		0.410#	



NEWBIGGING'S HANDBOOK FOR

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TABLE,

Showing the Expansion of Liquids in Volume from	82° to	212°	Fahr.
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1000 parts of	water	•										become	1046	
"	oil		•	•	•	•	•	•	•	•	•	11	1080	
37	mercu	ry	٠.	•		٠		•	•	•	٠.	"	1018	
,,	spirits	01	W	ne			•	•	•	•	•	11	1110	
,,													1378 to 137	5

TABLE,

Showing the Lineal Expansion of Metals produced by Raising their Temperature from 82° to 212° Fahr.

Zinc					1 part is								1 part in 682
Platinum .					,,	851	Bismuth						,, 719
Tin (pure)					**	408	Iron .						,, 819
Tin (impure)	٠	•	•	•	11	500	Antimony	•	•	•	٠	•	,, 928
Silver	•	•	•	•	**	524	Palladium						,, 1000
Copper	•	•	•	•	"	581	Platinum						,, 1100
Brass	•	•	•	•	"	584	Flint glass		٠	•	•	•	,, 1 94 8

TABLE,

Showing the Relative Power of Metals for Conducting Heat.

Gold .									1000	Iron										874.8
Bilver									978 896 · 2 881	Zino						•	•	•		868
Copper	•	•	•	•	•	٠	٠	٠	898.2	Tin	٠	٠	•	٠	•	٠	•	٠	•	808.9
PIREDE	m	•	•	٠	•	٠	•	٠	981	Teea	٠	•	٠	•	•	•	•	•	•	148.0

TABLE,

Showing the Relative Power of Metals for Reflecting Heat.

Intensity of Direct Radiation, 100.

Silver plate . Gold	•						'97 Polished plating						
Guiu	•	•	•	•	•	•	20 DAGGT ' '	 •	•	•	•		.00
Brass													•81
Speculum metal	l.						·86 Iron						.77
TQn.							-95		-	-	-	-	• •

TABLE

Melting Points.

De	grees Fahr,			1	egrees Fahr.
Antimony	810 Platinum .				. 3632
Bismuth	1044 Potassium .				. 145
Bronze	1652 Silver				. 1832
Butter	91 Sodium				. 203
Copper	2102 Spermaceti .		1		. 120
Gold	2282 Stearine	10	100		. 131
Ditto, coined	2156 Steel			2372	to 2552
Ice	32 Sulphur				. 230
Iodine	225 Tin		100	1001	. 446
Iron, cast 1922 t			10	10.113	. 154
ALCOHOL CONT.	o 2912 Ditto, yellow			200	. 144
Lead	633 Zine	15	1	10 15	. 680
Phosphorous	111				. 000

THE GAS INDUSTRY OF THE UNITED KINGDOM.

The manufacture and distribution of coal gas may be justly described as one of the important industries of the world. Like railways and the electric telegraph, it is a product of the 19th century; for, though coal gas was actually used for illuminating purposes by William Murdoch, the inventor of gas lighting, as early as 1792, at Redruth, in Cornwall, and in 1797 at his house at Old Cumnock, Ayrshire, it was not until well into the first decade of the present century that gas began to be generally applied in the lighting of streets, factories, and dwelling-houses.

The illumination of Soho Works, Birmingham, to celebrate the Peace of Amiens, took place in 1802. These works belonged to Boulton and Watt, and Murdoch was employed as manager to the firm. The first application of gas to the interior lighting of large premises was made by Murdoch in Salford, in 1805, at the cotton manufactory of Phillips and Lee; and the first street lighted with gas was Pall Mall, London, in 1807. The first gas Company incorporated by Act of Parliament was the "Chartered" (now the Gaslight and

Coke), London, in 1812.

Although in its earliest use coal gas was restricted to the purpose of affording artificial light, no long time elapsed before its value as a heating medium began to be realised. Winsor, one of the pioneers of gas lighting, claimed as an important advantage of the new invention or discovery that gas, besides its light-giving qualities, could be used both for cooking food and warming dwellings, and as early as 1825 attempts were made to apply it for these purposes. It was not, however, till later on in the century that anything like a practical application of gas was made to the cooking of food. Mr. J.

Southampton, about the year 1840, began to construct ovens heated by gas for cooking and baking, and these he used for many years, giving public lectures, in the course of which he practically demon-

strated their usefulness and value.

Gas, however, in those days was higher in price than now; and, although it was evident that it served most efficiently for culinary operations, its cost militated against its extensive adoption in this direction. The prejudice against it was strong, also, on account of the supposed liability of any food cooked by its means to be tainted with the flavour of the gas itself. This operated against its use; and though the prejudice was founded on ignorance of the facts, it is not a matter of wonder that such an idea was entertained, seeing that, even at the present day, in spite of the strongest evidence to the contrary, the same belief is still widely accepted, and still operates with many as a

bar to its adoption.

Gas has won for itself an important place as an agent for obtaining motive power. It was from the very first a matter of observation, and not unfrequently of dire and unsought experience, that when gas and atmospheric air were mixed in certain proportions, and the mixture fired, an explosion was the result. Attempts were soon made to utilise the force thus exerted by confining the explosive compound in a suitable cylinder, and exploding it to obtain prime movement as in the steam engine. After many more or less successful attempts by different inventors, and the expenditure of much ingenuity, the "Lenoir" gas engine, so named after its inventor, was produced (1860), and thus was solved the economical problem of how to utilise an explosive mixture of gas and air as a prime motor. From that time down to the present the patent records contain the description of many inventions of this character, and gas engines of great power and efficiency are now produced.

In England, Wales, and Ireland the gas actually supplied to consumers varies in illuminating power from 14 to 22 standard candles, according to the quality of the coal used; the higher figure above 17 candles being obtained by an admixture of cannel, or shale, with the ordinary bituminous coal. In Scotland the range of illuminating

value is from 22 to 30 candles.

The selling price of gas per 1000 cubic feet ranges throughout England, Wales, and Ireland from 1s. 9d. to 6s. 3d., and in Scotland from 3s. to 8s. 4d., with a few of the smallest concerns charging as much as 10s. per 1000 cubic feet. Taking into consideration, however, that in Scotland gas of a higher illuminating power is supplied than in the other portions of the kingdom, that a smaller consumption per consumer is the consequence, and calculating the price at per unit of light, the actual difference in price is not so great as appears at first sight.

The average cost of producing and distributing illuminating gas in England is about two-thirds of the selling price. Taking a selling price of, say, 2s. 6d. per 1000 cubic feet, the cost of producing and distributing the gas, including the net expenditure on coal (after deducting the income from residuals) and working expenses, will be 1s. 8d. per 1000 cubic feet. Analysing this figure, the expenditure on coal will be 1s. 3d., and deducting the value of the residuals, at present prices, which is equal to 8d., there is left 7d. as the net cost of the coal. The balance of 1s. 1d. is made up by the working expenses, which include wages, salaries, purifying materials, repairs and renewals, rates and taxes, and incidental expenses. The difference of 10d. between the prime cost of the gas, 1s. 8d., and its selling price of 2s. 6d. is absorbed in the payment of the interest and dividend on the invested capital in the case of a Company, and in the instance of the undertaking belonging to a Local Authority, in the discharge of the interest on the annuities and borrowed capital (if any), and the provision of a sinking fund.

According to the Parliamentary Returns last issued (1888) the number of gas-works in Great Britain and Ireland belonging to Companies under statutory powers and restrictions is 384; and of those in the hands of Local Authorities, the number is 168. No account is taken in the Returns of those gas-works belonging to companies which are supplying gas without statutory powers. Of these there are about 950 in the United Kingdom. Neither do the Returns include the large number of small gas-works owned by private individuals and firms throughout the country, and which have been erected for

the supply of isolated houses, workshops, and factories.

By determining, as near as may be, the number of tons of coal carbonized, the quantity of gas produced in one year, and the capital employed in gas-works, we shall be able to form a good idea of the extent of this important branch of industry as it affects the United Kingdom. Taking, therefore, the figures as they appear in the Parliamentary Returns, and supplementing these, where they are deficient, by an estimate based largely on personal knowledge, we have the results given in the following table:—

Coal	Carbonized in 1888. Tons.	Gas Produced in 1888. Cubic Feet.	Capital employed in 1888.
Gas-Works in the United Kingdom belonging to Local Authorities		30,105,457,962 61,266,055,857	
(estimated)	1,000,000	8,000,000,000	5,800,000
Total	9,962,831	99,371,513,819	62,778,015

This capital of £62,778,015, however, represents only the expenditure upon the undertakings; and if the premium amount, which ranges from 50 to 60 per cent., be added, the actual commercial value is found to be about 100 million pounds sterling.

Of the quantity of gas annually produced there is an average loss by leakage and from other causes of nearly 8000 million cubic feet, or

8 per cent, of the whole make.

The total annual rental may be set down at £14,900,000, and the profits at £4,700,000—equal to 7½ per cent. on the expended capital, and 4.85 per cent. on the capital as enhanced by the premium value.

The number of hands employed in gas-works in the United Kingdom is about 60,000, and the wages paid annually amount to £4,000,000. But, if account is taken of the different trades which have been called into existence for the production of the appliances of gas manufacture, distribution, and consumption, and of the miners who are employed in raising the coal, the figures in the two latter items may be safely quadrupled. For the distribution of the gas to the public, there is a length of about 20,000 miles of mains laid, not reckoning the service pipes. The number of consumers is 2,400,000,

and the public lamps 430,000.

It is occasionally a subject of remark by uninformed or hostile critics, that no important improvements have been effected in gas manufacture since the earlier days of its introduction. If this were so, it would either speak well for the inventors of this art, or badly for their successors in the industry. The statement, however, is altogether wide of the truth. True, the method of producing the gas, as in the earlier days, is by distillation of the coal in closed retorts, and the purification, storage, and distribution of gas are effected in apparatus and plant which, in their main features, do not greatly differ from the earlier forms. But it is obvious that a similar invidious comparison might be made in regard to all the most notable inventions. The chief characteristics of an industry are retained, whilst the processes undergo improvement and modification. As a matter of fact, great improvements have been effected in the plant and apparatus for the manufacture of illuminating gas, whilst the mechanical and chemical principles involved in its production are now carefully investigated by gas engineers, and are yearly becoming better understood.

THE CAPITAL EMPLOYED IN GAS-WORKS.

The Capital of a Gas Undertaking represents or includes (1) the amount of money that has been expended on obtaining an Act of Incorporation, if it be a Statutory Company; (2) the cost of the land

for the site of the works, and the engineering expenses incurred; (3) the cost of the general manufacturing, purifying, and storing plant; and (4) the cost of the distributing pipes and accessories; with (5) an added sum as a floating or working capital to meet current

outlay before the revenue begins to accrue.

The amount of the various items making up the aggregate, necessarily varies under different conditions. For example, take the first—the money expended on obtaining an Act of Incorporation. When a Company have had to contend with and overcome persistent and strong opposition, the cost of their Act will exceed the cost of one obtained under more favourable conditions, to the extent of 100, 200, or even 300 per cent. Again, the cost of land is a varying factor, and the expense of the erection of works is often increased by the character of the site and its subsoil. It is true that in the case of a large Company, these several items, even when greatly in excess of a normal amount, do not increase the total capital outlay by any material percentage; but on small and moderate-sized undertakings they are often peculiarly burdensome.

But there are other circumstances more distinctly marked than these, which contribute to the variations in the relative amount of capital expended by different Companies. The character of the district of supply is one of them. The district of some Companies is thickly populated with a high class of consumers throughout. Others, again, have a scanty population, and of a poorer class; and although the plant and mains of this latter may be less extensive, yet the proportion of its capital to the production and rental will usually be in excess of the other, whilst there is this paradoxical result in the instances referred to, that those who are least able to afford it have

often necessarily to pay a higher price for the gas.

In many instances, Companies have wide expanses of country to canalise with miles of mains, on some of which, except at the terminus, there is scarcely a consumer. Again, the district may be a manufacturing one, with mills and workshops consuming gas only during four or five months in the year. The proportion of capital in such case has frequently to be large to provide plant to meet the principal gas demands within a limited period of time. It is no unusual thing, under such circumstances, to find that during nearly one half of the year, seven-tenths of the whole plant is standing unproductive.

In contrast to these, there are towns whose gas consumption is comparatively steady all the year round. Take, as an example, the inland watering-places and fashionable sea-side towns. To these, there is during the summer and autumn season, a flow of visitors who consume a large quantity of gas. Such is proved by the fact that the heaviest daily make in these places is generally in the months of September or October. This tends to equalise the consumption

in the different seasons, because the resident inhabitants consume their proportion of gas during the winter and early spring months, when the visitors are absent. It is fair to conclude that, owing to this regular and steady consumption, the plant is almost continuously employed, and therefore a smaller capital in proportion to the yearly production is required than in those places where the heavy consumption is spasmodic and brief.

But although this spasmodic consumption appears, at first sight, a serious drawback, in practice it does not always necessitate a higher price for the gas, and a much larger capital outlay than is required by

those concerns whose consumption or sale of gas is steadier; for in some of the large manufacturing towns the mill consumption is so enormous that, by straining the plant for limited periods, the disadvantage is counterbalanced.

There can be no question that expensive engineering tends to an undue inflation of the capital account. A want of engineering skill in the construction of works has precisely the same effect; for here.

as in other matters, extremes meet.

Considerable thought will always be given by a capable and conscientious engineer to the proper arrangement of works. He will so perfect his designs that the works shall not be squandered or sprawling over the site, occupying unnecessary space, but compact and harmonious, so that the different processes in gas making may be

conveniently carried on, and economical in the working.

Whilst it is not necessary or desirable that the buildings of a gasworks should be as strong as a castle, it is equally objectionable to set up unstable and flimsy structures that entail an annual heavy expenditure for repairs, constituting a perpetual tax, enhancing the cost of working.

Excessive and unnecessary ornamentation is to be eschewed in all works of this kind. All ornamentation, however, is not useless. Blank thick walls, for example, are not necessarily stronger than others well proportioned—thinner and lighter in parts, but strengthened by suitable projections that add to the beauty of a building by breaking the dull uniformity. The same argument holds good as respects design in apparatus. Taste should not be neglected; and there is ample scope for the exercise of good taste in most departments of a gas-works.

On a closer examination of the question, it will be apparent that there occur times in the history of most gas undertakings when the capital expenditure is either below or in excess of the average, viz.—when the margin of its producing, storing, and distributing resources is closely worked up, and enlargement is required, then the capital compared with the production is low. But extensions have to be carried out. These must necessarily be of such extent as to provide a

margin for future increased consumption, and, being larger than the immediate requirements of the district, the capital is swelled out of proportion. This is especially true of times when trade is brisk, and labour and materials are dear. Then extensions are costly, and, singular to say, it is at such times that they are most frequently made. Under such circumstances, unless resort can be had to a reserve fund to maintain the dividends, a sacrifice of a portion of the statutory interest has to be submitted to or the price of the gas increased.

But this condition of things is by no means inevitable. One of the evidences of good administrative skill in the conduct of a gasworks is the ensuring that extensions are carried out systematically and with foresight, and in as gradual a manner as may be, not postponing them to the very last extremity; in other words, starving the concern—wearing it threadbare—which is the worst policy possible for the undertaking and all associated with it, including both share-

holders and consumers.

The capital of gas-works in the hands of Corporations and other Local Authorities is, as a rule, in excess of that of Companies; but this arises from causes well understood. Many Towns' Authorities have within comparatively recent years become possessed of gasworks by purchase from the Companies who previously owned them; and, as in most cases they have had to pay the full market price for the concern, amounting to from twenty to twenty-eight years' purchase of the annual profits, and even more in some instances, the result is that the capital outlay is large—with this compensatory advantage, however, that the percentage of interest to be paid on such capital is not more, but usually less, than that paid by the Company on the smaller capital. As time goes on, and extensions of the Corporation works are made, these are carried out with an expenditure, though not necessarily less than that of a Company, yet bearing a lower rate of interest, and consequently pressing less heavily on the resources of the undertaking.

The immediate effect of an excessively large capital outlay by a Gas Company is, as has been already remarked, either a sacrifice by the shareholders of a proportion of the statutory dividends, or an augmentation in the selling price of the gas; and not unfrequently, when the capital is greatly in excess, both these undesirable results are ex-

perienced.

One of the best, perhaps the very best method of reducing the proportion which capital expenditure bears to revenue, is to cultivate a day consumption of gas, by affording facilities for, and encouraging in every legitimate way the use of gas for cooking, heating, and motive power. This policy, if pursued to a successful issue, is virtually to reduce the percentage of capital in the proportion of such consumption,

because the plant is brought to bear in earning profit during the

daylight as well as in the lighting hours.

The "Auction Clauses," now introduced into the Bill of every Gas Company making application to Parliament for money powers, are, without doubt, an ingenious and fairly satisfactory device for securing the limitation of capital; whilst, at the same time, they tend to give stability to the undertaking, and provide a guarantee for the gradual

reduction of the price of the gas.

The "Sliding Scale" (which is not inserted compulsorily as are the "Auction Clauses") operates in the same direction, though it is open to grave objection on other grounds. The subject is one of such vital importance that it should be looked at from every point of view. No doubt the Companies who were enabled to adopt the sliding scale in the early days of its inception, are to be congratulated on the results they have achieved in the way of enhanced dividends by its application and working; but there will probably be less room for congratulation to any who may adopt it in future, with the closer limitations which will prevail in fixing the initial or standard price.

It is clear, also, that Companies seeking powers at a time when coal and materials generally are low in price, are placed at a disadvantage as compared with other Companies applying to Parliament in a time of inflated prices. Notwithstanding all experience, one of the ruling characteristics of average human nature is to conclude that that which actually exists will scarcely ever again be modified to any large extent. Injustice may, therefore, unintentionally, be meted out to one Company, and more than justice to another; and so, when the reaction comes, the circumstances of the first suffer impairment, whilst the other is glutted with a run of good fortune. This want of equal justice in the incidence of the sliding scale, whilst inevitable, is sufficient to convince any disinterested observer that its indiscriminate advocacy is a mistake. It is, moreover, a curious and interesting commentary on the action of the sliding scale that, in spite of the inducement which it offers for a low selling price, there are both Gas Companies and Local Authorities who, without it, can produce and sell gas at a price as low as, or even lower than, those who boast its possession.

It is unreasonable to expect that the capital of Gas Companies, and the selling price of gas, can ever be uniform throughout the country. It would be just as reasonable to expect that the general rates of different districts can be equalised. All the causes above pointed out,

and others not touched upon, militate against such a result.

SUNDRY USEFUL NOTES.

In choosing the site for a gas-works, consideration should be had to its position, which should be at the lowest, or nearly the lowest part of the district, to obtain the advantage of the natural increase in the pressure of the gas in travelling to the higher levels.

It should, if possible, be alongside a railway, navigable river, or canal, for convenience in the delivery of coal and other materials, and the disposal of such of the residuals as are despatched to a distance.

The buildings and plant should be so set out on the land as to admit of future extensions being made with ease and economy.

The design of a structure should be in keeping with the purpose for which the structure is intended.

Capital is best spent on substantial tanks and apparatus. Mere ornament should be a secondary consideration.

The average cost of gas-works in provincial towns is about £1 per head of the population. In very large towns it will amount to more, and in very small towns it will scarcely reach that sum.

The average cost of gas-works per million cubic feet of gas produced per annum is from £600 to £700; or at the rate of about 14s. per 1000 cubic feet.

The capital of a well-managed gas company of average size, does not usually amount to more than four times the annual gas rental. Vice versā, the gas rental should be at least one-fourth of the capital. Reckoned on the maximum production of gas in 24 hours, the capital will amount to about 2s. 3d. per cubic foot, or, say, £112 per 1000 cubic feet.

The population per mile of main is usually about 2000 people. In densely populated towns it will rise to 3000; but in fashionable residential places, where the houses stand more apart, the population per mile of main will fall below 1000.

The usual consumption of gas per mile of main in large towns is from $2\frac{1}{2}$ to 4 millions of cubic feet per annum; and in small towns from 2 to 3 millions.

The gas rental per mile of main usually ranges from £400 to £600 per annum.

The average consumption per head of the population in large towns is about 2000 cubic feet per annum; in small manufacturing towns about 1600 cubic feet, and in agricultural towns about 1000 to 1200 cubic feet per annum.

The usual annual increase in the consumption of gas is from 5 to 10 per cent. In rapidly growing districts it will range higher.

The term "Structural Value" has reference to the amount of capital expended upon works in their construction.

"Commercial Value" is the value of the net annual profits which firm or company can make by the use of their works.

TABLE.

Showing the Time in which the Yearly Consumption of Gas will be Doubled, at Different Annual Rates of Increase.

Rate per cent. of Increase per ann.	Time in which the Consumption will be Doubled.	Rate per cent. of Increase per ann.	Time in which the Consumption will be Doubled.	Rate per cent. of Increase per ann.	Time in which the Consumption will be Doubled.
2	35 years, 1 day.	51	12 years, 345 days.		8 years, 16 days.
21/2	28 years, 26 days.	6	11 years, 327 days.		7 years, 233 days.
3 31	23 years, 164 days.	61	11 years, 2 days.	10	7 years, 100 days.
81	20 years, 54 days.		10 years, 89 days.	101	6 years, 344 days.
4	17 years, 246 days.	71	9 years, 213 days.	11	6 years, 234 days.
44	15 years, 273 days.	8	9 years, 2 days.	114	6 years, 134 days.
4± 5	14 years, 75 days.	81	8 years, 181 days.	12	6 years, 42 days.

Handy Rule for Converting Capital per Million Cubic Feet into Capital per Thousand Cubic Feet.

Point off all the figures after the hundreds as decimals, and

multiply by 2.

EXAMPLE.—The capital of a gas undertaking is £725 per million cubic feet of gas sold (or produced) per annum, what is the capital per 1000 cubic feet?

Then.—7.25 × 2 = 14.50; say, 14s. 6d. per 1000 cubic feet.

TABLE.

Showing the Approximate Sum (or the Equivalent of the Annuities) paid for each £100 of Share Capital of Gas Companies on the Purchase of the Gas-Works by Municipal Corporations, Commissioners, or Local Boards, in the several under-mentioned Towns.

Name.	Year when Pur- chased.	Approximate Sum (or the Equivalent of the Annuities) paid for each £100 of Share Capital.	Remarks.
		£	
Aberdeen	1871	250	
Alloa	1877	232	
Arbroath	1871	175	
Ashton-in-Makerfield	. 1875	160	Non-statutory Company.
	1873	160	A party of the par
Bangor	1878	250	
Belfast	. 1874	193	
Birkenhead	1858	220	
Birmingham	1875	196	
Birstal	1872	187	
Blackburn	1877	235	
Bolton	1872	204	
3011011		1	A sum of £162,856 had been ex-
			pended out of profits in extending
Bradford	1871	382	the works. Capitalizing this sum
maurora	-	1	the amount paid per £100 is only
	1		£96.
Briton Ferry	. 1878	210	
1.4. Th.	. 1870	150	Non-statutory Company.
	1854	300	and a surpling of
Burslem	. 1877	222	
Bury (Lancashire)	. 1859	250)
M. M. Marian	. 1871	250	
leckheaton	. 1870	205	
Clitheroe	1878	210	
Colne	1877	237	Non-statutory Company.
Darlington	. 1854	216	and the state of t
Darwen	. 1873	188	
	1873	205	
Proitwich	. 1878	149	Non-statutory Company.
** 4.11	1877	250	The state of the s
A STATE OF THE PARTY OF THE PARTY OF THE PARTY OF THE PARTY OF THE PARTY OF THE PARTY OF THE PARTY OF THE PARTY OF THE PARTY OF THE PARTY OF THE PARTY OF THE PARTY OF THE PARTY OF THE PARTY OF THE PARTY OF THE PARTY OF T	. 1873	225	
Dumfries	. 1878	151	
	. 1868	160	
	. 1878	200	
Evesham	. 1878	129	
Forfar	. 1871	187	3
lasgow	1869	209	1-1
Ialifax	. 1856	250	A con from the second
	1 200	1	A sum of £24,000 had been ex-
	1000	001	pended out of profits in extending
Hereford	. 1872	861	the works. Capitalizing this sum
	1		the amount paid per £100 is
		, (£172.

Name.	Year when Pur- chased.	Approximate Sum (or the Equivalent of the Annuities) paid for each £100 of Share Capital.	Remarks.
A CONTRACT OF THE PARTY OF THE		£	
Heywood	1867	208	
Hindley	1872	208	In the second se
		1	Non-statutory Company. A sum of
Horneastle	1876	117	£8000 had been expended out of
	2010	2000	profits on extending the works,
Huddersfield	1070	204	which sum was capitalized.
Ilkeston	1872 1878	177	Non statutana Commen
Inverness	1875	153	Non-statutory Company.
Kilmarnock	1872	150	Company or the Company of the Company
TITIME HOOK + 1	1012	100	A sum of £1300 had been expended
			out of profits on extending the
Kirkintilloch	1878	200	works. Capitalizing this sum, the
		1	amount paid per £100 is £169.
Leeds	1870	140	
Leicester	1878	217	
Leigh	1874	200	
Llandudno	1876	175	
Longton	1877	200	100
Macclesfield	1861	250	100
Mansfield ,	1878	250	
Maryport	1876	118	
Neath	1874	125	
Nelson	1866	150	
Wamburen	1878	130	Site belonged to Corporation and
Newbury	1010	100	works and plant taken at a valua-
Newcastle-under-Lyme .	1881	250	tion.
Newry	1878	190	Non-statutory Company.
Nottingham	1874	162	Non-statutory Company.
Oldham	1853	250	
Padiham and Hapton .	1876	200	
Paisley	1845	160	
Penrith	1877	191	
Perth		156	
Boohdale	1844	167	
Rotherham	1870	205	Non statutom Commis
Saffron Walden	1878	111	Non-statutory Company.
St. Helens	1876	272 159	
Sowerby Bridge	1861	262	
est 1 m	1000	250	
Stratford-upon-Avon	1879	188	
W	1878	261	
Tyldesley	1865	167	
Ulverston	1874	212	
Warrington	1877	240	The state of the same
Wigan	. 1874	208	The Company were allowed to capitalize £12,500. Adding this to the share capital, the sum paid per £100 is £174.

TABLE, showing the Cost of Gas per Hour in Fractions of a Penny, when Burnt at the following Rates per 1000 Cubic Feet:—

10	nen	Dur	ne ac	the J	ottote	ing 1	uttes	per 1	000	Cuou	I eet		
Consump	tion	1		1-15							1		
per Hou		s.d.	s.d.	B. d.	s. d.	s. d.	8. d.	s. d.	s. d.	s.d.	s. d.	s. d.	s. d.
in Cubic F	eet.	26	27	28	29	2 10	2 11	80	31	32	3 8	8 4	8 5
2		.060	.062	.064	.066	.068	.070	.072	.074	.076	.078	.080	.082
21	7	.075	.0775	.080	.0825		.0875		.0952		.0975	.100	102
3		-090	.093	.096	099	102	105	108	111	114	117	120	102
34		105	1085		1155		1225		1295		1365		143
4		120	1000	1128	132	136	140	144	148	152	156	160	164
44		135	1395		1485		1575		1665		1755		184
5	-0	150	155	160	165	170	175	180	185	190	195	-200	205
51		165	-1705		1815		1925		2035		-2145		225
6		180	186	192	198	-204	-210	.216	-222	228	234	-240	-246
61		195	2015		2145		2275		2405		2535		-266
7		210	217	224	231	-238	245	-252	-259	266	273	280	-287
Consump	tion I	210		1	1 202	1 200	-		1	200	1 210	1	1
per Ho	ar	s. d.	s. d.	s. d.	s. d.	s. d.	s. d.	s.d.	s. d.	s.d.	s. d.	s.d.	8. d.
in Cubic i		3 6	87	38	89	3 10	3 11	40	41	4 2	4 3	44	4 5
-				000		400			.000				100
2	1111	.084	.086	-088	.090	092	094	.096	.098	.100	102	104	106
21		105	1075		1125		1175		1225		1275		132
3		126	129	132	135	.138	141	144	147	.150	153	156	159
31		147	1505		1575		1645		1715		1785		185
4	- 4	168	172	176	180	184	188	192	196	200	204	208	212
44		.189	1935		2025		2115			.225	2295		238
5		210	.215	.220	225	.230	235	240	245	.250	255	260	265
51		231	2365		2475		2585		2695		2805		291
6		252	258	264	270	*276	*282	.288	294	.300	306	*812	318
61		273	2795		2925		3055		3185		3315		344
		294	.301	.308	*315	322	329	.336	.343	*850	*857	364	371
Consump per Ho		s. d.	s. d.	s. d.	s. d.	s.d.	- 4		1.5	s. d.	s. d.	s. d.	s. d.
in Cubic I	Peet.	4 6	4 7	48	4 9	4 10	5. d. 4 11	s.d. 5 0	s.d. 51	5 2	5 3	5 4	55
			-	-	-	- Chief		-	-	_	-		-
2		•108	.110	.112	1114	.116	-118	.120	122	124	126	-128	.130
24		.135	1375		1425		.1475	-150	1525		*1575		162
3		.162	.165	.168	171	174	.177	-180	183	186	.189	192	195
31		.189	.1925		1995		*2065	210	2135		2205		227
4		216	*220	-224	.228	.232	.236	.240	244	-248	252	256	260
41		.243	.2475		*2565		2665		2745		2835		292
5	- 6	.270	-275	.280	.285	.290	*295	.300	305	.310	*315	320	825
51/2		-297	.3025		.3135		*3245		.3355		*3465		357
6		*824	*330	.336	*342	.348	.354	.360	.366	.372	378	*384	.390
61		:351	3575		3705		13835		3965		4095		422
7		'378	.385	.392	.399	.406	413	•420	427	434	1.441	448	455
Consp.	13.2		1			44	0.0	i saii	29	- 41	0		
per Hour	8. d.	s.d. 57	s.d. 58	s.d. 59	s. d. 5 10	s, d. 5 11	s. d. 6 0	s.d.	s.d.	s. d. 6 3	8. d. 6 4	s. d. 6 5	8. d. 6 6
in Co. Ft-	5 6	01	0.0	0.5	0.10	0 11	0.0	6 1	6 2	0.0	0.4	00	0.0
2	132	.134	-136	-138	+140	.142	-144	146	148	.150	.152	.154	*156
24	165			1725		1775		1825	185	1875		1925	-195
3	198	2200	-204	.207	-210	.213	216	-219	-222	225	-228	.231	234
31	231		238	2415		-2485		.2555		-2625	.266	.2695	
4	264		-272	.276	280	.284	-288	292	296	-300	-304	.308	.312
44	201	-3015		.3105		.3195		3285		.3375		.3465	
5	.330		.340	.345	.850	.355	.860	.365	.370	-375	.380	.385	.390
51	363	The same		.3795		.3905		.4015		-4125	10000	4335	-429
- 2		-402	-408	414	.420	.426	-432	•438	.444	.450	456	462	· Anc
6													
6 61	.429			.4485	455	+4615	*468	.4745	•481	.4875	*494	.5005	

GOLDEN RULES FOR GAS MANAGERS.

Keep up the heats of the retorts. Keep up the efficiency of the meters. Keep down the pressure in the mains. Keep down the arrears in the gas ledger.

These rules are as applicable to-day as they were on the first day they were penned, as they embody all the philosophy of gas management. A strict adherence to the advice which they give will ensure the success of any gas undertaking, just as a disregard of them will result in loss and disaster.

It has been attempted (with little success, and less reason) to impugn the utility of the third rule. To keep down the pressure in the daytime, say certain writers and speakers, is to discourage the use of gas for cooking and heating. But, surely, to make such a remark is to betray an amount of dulness not easy to understand. It should be obvious to the meanest comprehension that it is not advised that the pressure should be kept down to an abnormal rate. Whatever pressure is required either by day or night must, of course, be maintained; the rule indeed implies as much, but it implies something more—its object is to discountenance the maintenance of a wasteful pressure, and all pressure in excess of actual requirements is wasteful. Verbum sat sapienti.

COEFFICIENTS

OF THE

Number, Dimensions, and Cost of the various Buildings, Apparatus, Machinery, and Plant of a Gas-Works.

It is an almost impossible task to give a series of coefficients of the number, dimensions, and cost of Buildings, Apparatus, Machinery, and Plant, applicable to the individual case of every Gas-Works in the United Kingdom. That such is the fact will be clear when the variations in size, character of subsoil, design (whether substantial or otherwise), and situation of such Works, are taken into consideration.

Again, although the cost based on the prices of labour and materials ruling at the present time may be applicable, it is evident that the figures will necessarily vary with the fluctuations in the market prices, and the effect of competition.

But neither is it possible to fix with perfect accuracy a standard of prices as a basis that will apply even under existing circumstances, as such prices vary, less or more, in different parts of the country.

At the best, it is only an approximation that can be given, and an attempt in this direction is made as follows:—

Prices on which the Coefficients of Cost are based.

	the state of the s
Labour.	Average.
Skilled labour.	10d per hour
Unskilled ditto	
Bricksetting, labour only	la 9d nor sa ud 9" thick
Retort setting, labour only	. 18. od. per sq. yd. 5 thick.
Netort setting, labour only	. 228. per mouthpiece.
Materials.	Average.
Selected best pressed bricks	THE RESERVE THE PARTY OF THE PA
Common briefs boot	
	. 20s. per 1000.
Portland cement	. 50s. per ton.
Lias or hydraulic lime	. 22s. ditto. . 12s. ditto.
Ordinary lime	
Building sand	. 1s. per load.
	. 13s. 6d. der cwt.
Fire-bricks	, 60s. per 1000.
Superior refractory bricks, as silica, &c	, 85s, ditto.
Fire.clay, ground,	. 20s. per ton.
Clay retorts 21"×15"	. 4s. per lineal foot.
Cast iron nines 2" to 4" diameter	£5.5s. per ton.
Ditto 5" to 8"	£5 ditto
Ditto 0'1 to 16'1	PA 150 ditto
Ditto 9 to 10 g	(4 10- 3itte
Ditto 17" and upwards	, £4 128, ditto.
Specials, cast-iron	. £8 to £11 ditto.
The cost of laying and jointing pipes is given on	pp. 235 and 236.
Sheet lead for flashing Fire-bricks. Superior refractory bricks, as silica, &c. Fire.clay, ground. Clay retorts 21" × 15" Cast-iron pipes 2" to 4" diameter Ditto 5" to 8" Ditto 9" to 16" Ditto 17" and upwards Specials, cast-iron The cost of laying and jointing pipes is given on wards with the cost of laying and the cost of laying and the cost of laying and jointing pipes is given on wards.	
The cost of laying and jointing pipes is given on Wrought-iron tubes according to list prices, with Ditto fittings ditto.	
Ditto fittings ditto.	
Ditto fittings ditto. Labour and Materials combined.	Average.
Ditto fittings ditto. Labour and Materials combined. Stock brickwork, 9" thick	Average.
Ditto fittings ditto. Labour and Materials combined. Stock brickwork, 9" thick	Average. . 5s. 6d. per square yard. . 8s. 9d. ditto.
Ditto fittings ditto. Labour and Materials combined. Stock brickwork, 9" thick	Average. . 5s. 6d. per square yard. . 8s. 9d. ditto.
Ditto fittings ditto. Labour and Materials combined. Stock brickwork, 9" thick	Average. . 5s. 6d. per square yard. . 8s. 9d. ditto.
Ditto fittings ditto. Labour and Materials combined. Stock brickwork, 9" thick	Average. . 5s. 6d. per square yard. . 8s. 9d. ditto.
Ditto fittings ditto. Labour and Materials combined. Stock brickwork, 9" thick	Average. . 5s. 6d. per square yard. . 8s. 9d. ditto.
Ditto fittings ditto. Labour and Materials combined. Stock brickwork, 9" thick	Average. . 5s. 6d. per square yard. . 8s. 9d. ditto.
Ditto fittings ditto. Labour and Materials combined. Stock brickwork, 9" thick	Average. . 5s. 6d. per square yard 3s. 9d. ditto 3s. per cubic foot 10s. per cubic yard 3s. to 3s. 6d. per square yard 3s. 6d. to 5s. ditto 3s. 6d. to 5s. ditto 10s. per cubic yard.
Ditto fittings ditto. Labour and Materials combined. Stock brickwork, 9" thick	Average. . 5s. 6d. per square yard 3s. 9d. ditto 3s. per cubic foot 10s. per cubic yard 3s. to 3s. 6d. per square yard 3s. 6d. to 5s. ditto 3s. 6d. to 5s. ditto 10s. per cubic yard.
Ditto fittings ditto. Labour and Materials combined. Stock brickwork, 9" thick	Average. . 5s. 6d. per square yard 3s. 9d. ditto 3s. per cubic foot 10s. per cubic yard 3s. to 3s. 6d. per square yard 3s. 6d. to 5s. ditto 3s. 6d. to 5s. ditto 10s. per cubic yard.
Ditto fittings ditto. Labour and Materials combined. Stock brickwork, 9" thick	Average. . 5s. 6d. per square yard 3s. 9d. ditto 3s. per cubic foot 10s. per cubic yard 3s. to 3s. 6d. per square yard 3s. 6d. to 5s. ditto 3s. 6d. to 5s. ditto 10s. per cubic yard 12s. ditto 14s. ditto.
Ditto fittings ditto. Labour and Materials combined. Stock brickwork, 9" thick	Average. . 5s. 6d. per square yard 3s. 9d. ditto 3s. per cubic foot 10s. per cubic yard 3s. 6d. to 5s. ditto 3s. 6d. to 5s. ditto 3s. 6d. to 5s. ditto 12s. ditto 12s. ditto 14s. ditto £7 10s. per ton.
Labour and Materials combined. Stock brickwork, 9" thick. Common ditto, best, 9" thick . Superior dressed stonework . Rubble ditto Slating . Flagging, 3" flags. Paving with 5" and 6" setts Portland cement concrete 1 in 9 Ditto ditto 1 in 7 Ditto ditto 1 in 5 Cast-iron in large castings . Ditto ditto fixing only	Average. 5s. 6d. per square yard. 3s. 9d. ditto. 3s. per cubic foot. 10s. per cubic yard. 3s. 6d. to 5s. ditto. 3s. 6d. to 5s. ditto. 10s. per cubic yard. 12s. ditto. 14s. ditto. 47 10s. per ton. 15s. ditto.
Ditto fittings ditto. Labour and Materials combined. Stock brickwork, 9" thick Common ditto, best, 9" thick Superior dressed stonework Rubble ditto Flagging, 3" flags Paving with 5" and 6" setts Portland cement concrete 1 in 9 Ditto ditto 1 in 7 Ditto ditto 1 in 5 Cast-iron in large castings Ditto gmall castings Ditto gmall castings	Average. . 5s. 6d. per square yard 3s. 9d. ditto 3s. per cubic foot 10s. per cubic yard 3s. to 3s. 6d. per square yard 3s. 6d. to 5s. ditto 3s. 6d. to 5s. ditto 10s. per cubic yard 12s. ditto 14s. ditto £7 10s. per ton 15s. ditto £10 to £12 ditto.
Ditto fittings ditto. Labour and Materials combined. Stock brickwork, 9" thick Common ditto, best, 9" thick Superior dressed stonework Rubble ditto Flagging, 3" flags Paving with 5" and 6" setts Portland cement concrete 1 in 9 Ditto ditto 1 in 7 Ditto ditto 1 in 5 Cast-iron in large castings Ditto gmall castings Ditto gmall castings	Average. . 5s. 6d. per square yard 3s. 9d. ditto 3s. per cubic foot 10s. per cubic yard 3s. to 3s. 6d. per square yard 3s. 6d. to 5s. ditto 3s. 6d. to 5s. ditto 10s. per cubic yard 12s. ditto 14s. ditto £7 10s. per ton 15s. ditto £10 to £12 ditto.
Ditto fittings ditto. Labour and Materials combined. Stock brickwork, 9" thick Common ditto, best, 9" thick Superior dressed stonework Rubble ditto Flagging, 3" flags Paving with 5" and 6" setts Portland cement concrete 1 in 9 Ditto ditto 1 in 7 Ditto ditto 1 in 5 Cast-iron in large castings Ditto small castings	Average. . 5s. 6d. per square yard 3s. 9d. ditto 3s. per cubic foot 10s. per cubic yard 3s. to 3s. 6d. per square yard 3s. 6d. to 5s. ditto 3s. 6d. to 5s. ditto 10s. per cubic yard 12s. ditto 14s. ditto £7 10s. per ton 15s. ditto £10 to £12 ditto.
Ditto fittings ditto. Labour and Materials combined. Stock brickwork, 9" thick Common ditto, best, 9" thick Superior dressed stonework Rubble ditto Slating Flagging, 3" flags Paving with 5" and 6" setts Portland cement concrete 1 in 9 Ditto ditto 1 in 7 Ditto ditto 1 in 5 Cast-iron in large castings Ditto small castings Plain cast-iron columns and beams Ditto ditto fixing only Ditto small castings Plain cast-iron columns and beams Ditto ditto fixing only Ditto ditto fixing only Ditto small castings	Average. . 5s. 6d. per square yard 3s. 9d. ditto 3s. per cubic foot 10s. per cubic yard 3s. 6d. 5s. ditto 3s. 6d. to 5s. ditto 10s. per cubic yard 12s. ditto 12s. ditto 14s. ditto £7 10s. per ton 15s. ditto £10 to £12 ditto £7 5s. to £7 15s. ditto 10s. to 15s. ditto 10s. to 15s. ditto.
Ditto fittings ditto. Labour and Materials combined. Stock brickwork, 9" thick Common ditto, best, 9" thick Superior dressed stonework Rubble ditto Slating Flagging, 3" flags Paving with 5" and 6" setts Portland cement concrete 1 in 9 Ditto ditto 1 in 7 Ditto ditto 1 in 5 Cast-iron in large castings Ditto small castings Plain cast-iron columns and beams Ditto ditto fixing only Ditto small castings Plain cast-iron columns and beams Ditto ditto fixing only Ditto ditto fixing only Ditto small castings	Average. . 5s. 6d. per square yard 3s. 9d. ditto 3s. per cubic foot 10s. per cubic yard 3s. 6d. 5s. ditto 3s. 6d. to 5s. ditto 10s. per cubic yard 12s. ditto 12s. ditto 14s. ditto £7 10s. per ton 15s. ditto £10 to £12 ditto £7 5s. to £7 15s. ditto 10s. to 15s. ditto 10s. to 15s. ditto.
Ditto fittings ditto. Labour and Materials combined. Stock brickwork, 9" thick Common ditto, best, 9" thick Superior dressed stonework Rubble ditto Slating Flagging, 3" flags Paving with 5" and 6" setts Portland cement concrete 1 in 9 Ditto ditto 1 in 7 Ditto ditto 1 in 5 Cast-iron in large castings Ditto small castings Plain cast-iron columns and beams Ditto ditto fixing only Ditto small castings Plain cast-iron columns and beams Ditto ditto fixing only Ditto ditto fixing only Ditto small castings	Average. . 5s. 6d. per square yard 3s. 9d. ditto 3s. per cubic foot 10s. per cubic yard 3s. 6d. 5s. ditto 3s. 6d. to 5s. ditto 10s. per cubic yard 12s. ditto 12s. ditto 14s. ditto £7 10s. per ton 15s. ditto £10 to £12 ditto £7 5s. to £7 15s. ditto 10s. to 15s. ditto 10s. to 15s. ditto.
Ditto fittings ditto. Labour and Materials combined. Stock brickwork, 9" thick . Common ditto, best, 9" thick . Superior dressed stonework . Rubble ditto . Slating . Flagging, 3" flags . Paving with 5" and 6" setts . Portland cement concrete 1 in 9 . Ditto ditto 1 in 7 . Ditto ditto 1 in 5 . Cast-iron in large castings . Ditto ditto fixing only . Ditto small castings . Plain cast-iron columns and beams . Ditto ditto fixing only . Ditto stand castings . Plain cast-iron columns and beams . Ditto ditto fixing only . Ditto have six for roof work standard to the content of	Average. . 5s. 6d. per square yard 3s. 9d. ditto 3s. per cubic foot 10s. per cubic yard 3s. 6d. 5s. ditto 3s. 6d. to 5s. ditto 10s. per cubic yard 12s. ditto 12s. ditto 14s. ditto £7 10s. per ton 15s. ditto £10 to £12 ditto £7 5s. to £7 15s. ditto 10s. to 15s. ditto 10s. to 15s. ditto.
Ditto fittings ditto. Labour and Materials combined. Stock brickwork, 9" thick . Common ditto, best, 9" thick . Superior dressed stonework . Rubble ditto . Slating . Flagging, 3" flags . Paving with 5" and 6" setts . Portland cement concrete 1 in 9 . Ditto ditto 1 in 7 . Ditto ditto 1 in 5 . Cast-iron in large castings . Ditto ditto fixing only . Ditto small castings . Plain cast-iron columns and beams . Ditto ditto fixing only . Ditto stand castings . Plain cast-iron columns and beams . Ditto ditto fixing only . Ditto have six for roof work standard to the content of	Average. . 5s. 6d. per square yard 3s. 9d. ditto 3s. per cubic foot 10s. per cubic yard 3s. 6d. 5s. ditto 3s. 6d. to 5s. ditto 10s. per cubic yard 12s. ditto 12s. ditto 14s. ditto £7 10s. per ton 15s. ditto £10 to £12 ditto £7 5s. to £7 15s. ditto 10s. to 15s. ditto 10s. to 15s. ditto.
Labour and Materials combined. Labour and Materials combined. Stock brickwork, 9" thick. Common ditto, best, 9" thick Superior dressed stonework Rubble ditto Slating. Flagging, 3" flags. Paving with 5" and 6" setts Portland cement concrete 1 in 9 Ditto ditto 1 in 7 Ditto ditto 1 in 5 Cast-iron in large castings. Ditto small castings. Plain cast-iron columns and beams Ditto swall castings Plain cast-iron in bars with forged ends, for roof wor Ditto ditto fixing only Ditto ditto fixing only Ditto ditto fixing only Ditto ditto fixing only Ditto ditto fixing only Ditto ditto fixing only Ditto ditto fixing only Ditto ditto fixing only Ditto ditto fixing only Only Ditto ditto fixing only Ditto ditto fixing only Only Wrought-iron roofs, per square yard of floor are	Average. . 5s. 6d. per square yard 3s. 9d. ditto 3s. per cubic foot 10s. per cubic yard 3s. 6d. to 5s. ditto 3s. 6d. to 5s. ditto 10s. per cubic yard 12s. ditto 12s. ditto 14s. ditto £7 10s. per ton 15s. ditto £10 to £12 ditto £7 5s. to £7 15s. ditto 10s. to 15s. ditto £2 ditto £2 ditto £2 ditto £2 ditto £2 ditto £2 ditto £2 ditto £2 ditto £2 ditto £2 ditto £2 ditto.
Labour and Materials combined. Stock brickwork, 9" thick. Common ditto, best, 9" thick. Superior dressed stonework Rubble ditto Slating. Flagging, 3" flags. Paving with 5" and 6" setts Portland cement concrete 1 in 9 Ditto ditto 1 in 7 Ditto ditto 1 in 5 Cast-iron in large castings. Ditto ditto fixing only Ditto small castings Plain cast-iron columns and beams Ditto ditto fixing only Wrought-iron in bars with forged ends, for roof wor Ditto ditto in angle, tee, and channel Ditto ditto in angle, tee, and channel Ditto ditto fixing only Wrought-iron roofs, per square yard of floor are covered, but not including slating.	Average. 5s. 6d. per square yard. 3s. 9d. ditto. 3s. per cubic foot. 10s. per cubic yard. 3s. 6d. to 5s. ditto. 3s. 6d. to 5s. ditto. 12s. ditto. 14s. ditto. £7 10s. per ton. 15s. ditto. £10 to £12 ditto. £10 to £12 ditto. £2 ditto. £3 ditto. £4 ditto. £4 ditto. £4 ditto. £5 ditto. £6 ditto. £6 ditto. £6 ditto. £7 ditto. £15 ditto. £15 ditto. £15 ditto. £15 ditto. £15 ditto. £15 ditto. £15 ditto. £15 ditto. £15 ditto.
Labour and Materials combined. Stock brickwork, 9" thick. Common ditto, best, 9" thick. Superior dressed stonework Rubble Slating. Flagging, 3" flags. Paving with 5" and 6" setts Portland cement concrete 1 in 9 Ditto ditto 1 in 7 Ditto ditto 1 in 5 Cast-iron in large castings. Ditto ditto fixing only Ditto small castings. Plain cast-iron columns and beams Ditto ditto fixing only Wrought-iron in bars with forged ends, for roof wor Ditto ditto fixing only Ditto ditto fixing only Wrought-iron in bars with forged ends, for roof wor Ditto ditto fixing only Wrought-iron roofs, per square yard of floor are covered, but not including slating. Wrought-iron in bars, with forged ends, for holde	Average. 5s. 6d. per square yard. 3s. 9d. ditto. 3s. per cubic foot. 10s. per cubic yard. 3s. 6d. to 5s. ditto. 3s. 6d. to 5s. ditto. 12s. ditto. 12s. ditto. 14s. ditto. £7 10s. per ton. 15s. ditto. £10 to £12 ditto. £10 to £12 ditto. £2 ditto. £15 ditto. £2 ditto. £15 ditto. £2 ditto. £15 ditto. £15 ditto. £2 ditto. £15 ditto. £2 ditto. £2 ditto. £3 ditto. £15 ditto. £2 ditto. £14s. to 17s.
Labour and Materials combined. Stock brickwork, 9" thick. Common ditto, best, 9" thick. Superior dressed stonework Rubble ditto Slating. Flagging, 3" flags. Paving with 5" and 6" setts Portland cement concrete 1 in 9 Ditto ditto 1 in 7 Ditto ditto 1 in 5 Cast-iron in large castings. Ditto ditto fixing only Ditto small castings Plain cast-iron columns and beams Ditto ditto fixing only Wrought-iron in bars with forged ends, for roof wor Ditto ditto in angle, tee, and channel Ditto ditto in angle, tee, and channel Ditto ditto fixing only Wrought-iron roofs, per square yard of floor are covered, but not including slating.	Average. . 5s. 6d. per square yard 3s. 9d. ditto 3s. per cubic foot 10s. per cubic yard 3s. 6d. to 5s. ditto 3s. 6d. to 5s. ditto 3s. 6d. to 5s. ditto 10s. per cubic yard 12s. ditto 14s. ditto £7 10s. per ton 15s. ditto £10 to £12 ditto £7 5s. to £7 15s. ditto £0 to £12 ditto £2 ditto £2 ditto £2 ditto £2 ditto £2 ditto £15 ditto £2 ditto £15 ditto £2 ditto £15 ditto £2 ditto £16 to 17s £17 per ton.

	Labour and Materials combined. Average.	
Wrought-ir Ditto	on in forgings, small £18 per ton.	
Ditto	in sheets and plates cold-straightened and punched . £18 ditto.	
Ditto	rivets and fixing £2 10s. 10d. ditto.	
Ditto	fixing only	
Ditto	fixing only 10s to 15s. ditto.	
Ditto Ditto Ditto Ditto	in rolled iron girders £6 to £6 10s, ditto. fixing only	

It is on these average prices current, that the coefficients of cost to be now given are based.

Capacity of the Works.

A Gas-Works capable of producing a maximum of 630,000 cubic feet of gas per day of 24 hours is taken as a basis, and this size of Works is adopted as being, though comparatively small, about a fair average, and to give a wider applicability to the figures than they would have had a very large Works been assumed.

Using 190 as the multiplier, this is equivalent to an annual production of 120 million cubic feet. Reasonable allowance is also

made for future growth in the consumption.

The site of such a Works will comprise 2½ to 3 statute acres of land. It is assumed that the site is fairly level and such as to admit of its

being fully utilized.

This extent of land is capable of containing, without inconvenient crowding, provided the Works are laid out with judgment, the whole of the Manufacturing, Purifying, and Storage Buildings and Apparatus required for the above make of gas per day, and also the Buildings and Plant for the manufacture of Sulphate of Ammonia, the recovery of Sulphur, and the distillation of Tar.

The cost of the Apparatus in each case includes erection. The Buildings are assumed to be neat and substantial.

Estimating the production from each mouthpiece or retort (oval or D shaped 21"×15"×10 feet long) at 6000 feet of gas per day of 24 hours on the average—

The number of mouthpieces required is Add by way of surplus to meet contingencies		105 21
Total mouthpieces required ,	4	126

The retorts are assumed to be in settings of sixes or sevens, and are throughs.

		Cost re	ecko	ned d	n			
Cost.	Description.	the M	fax.	daily	Con	st per	Mot	ith-
		ductio	on p	er 100	0	piec	e.	
0		Cuh	ic E	eet.		a	2	
*			8.	a.		£	В.	d.
10,080	Stage Floor Retort House with retort stack 20 feet wide, 20 feet space on each side. Retort settings, two dwarf chim- neys, generator furnaces, all ironwork (including foul main round the inside							
	of the house), tools, and implements; also covered coal stores to contain four weeks' stock of coal calculated on the maximum days' consumption, with		0	0		80	0	0
6,255	Stage Floor Retort House and coal stores only, as above				**	49	100	0
3,825	Retort Stack and two Dwarf Chimneys		18	9	144	311	10	U
0,020	built up from basement, with generator furnaces, retort settings, and ironwork		,			90	7	
2,520	Brickwork of Retort Stack and two	6	1	3	**	30	7	U
2,020	dwarf chimneys, generator furnaces,							
	retorts, and settings, but no ironwork .	4	0	0	4.	20	0	0
1,800	Ironwork only of stack complete, includ-							
***	ing hydraulic and foul mains	2	1	3	40	10	7	0
630	Retorts, including labour in setting and							^
630	Generator Furnaces and ironwork of	1	0	0		5	0	0
000	same	1	0	0		5	0	0
7,000	Ground Floor Retort House with retort stack 20 feet wide, 20 feet space on each side, retort settings, two dwarf chimneys, all ironwork (including foul main round the inside of the house), tools, and implements; also covered coal store to contain four weeks' stock of coal calculated on the maximum			- 14.11			7	
	days' consumption, with railway com-	11	2	3		55	10	0
4,190	Ground Floor Retort House and coal	11	-	0		00	10	0
Saul	stores only, as above		13	3		33	5	0
2,810	Retort Stack, two dwarf chimneys, and							
	retort settings, with iron mountings		0			22	-	0
1,606	Brickwork of retort stack two dwarf	4	9	0	**	22	5	0
1,000	chimneys, retorts, and settings, but no							
	ironwork		11	0		12	15	0
1,194	Ironwork only of stack including hy-							
630	draulic and foul mains Retorts, including labour in setting and		18	0	9.5	9	10	0
400	fire-clay materials (no ironwork)	1	0	0	**	5	0	0
2,000	Railway Communication with an ad-							
	joining line of railway. This is an		-			10		
460	uncertain item, but say as an average.	3	2	6	(2.5)	16	0	0
100	Condenser. This may be of any form, vertical or horizontal (the respective				-			
	cost will not vary to any great extent),							
	with connections and bye-pass mains							
	and valves complete	0	14	6			-	

Cost.	Description.			Cubi	naxin	ot of	Gna
£				*****		8.	
535	Boiler and Exhauster House. Chimney a	nd setti	ing fo	or			
300	Steam Boilers of the Cornish type, two steel and of ample size to supply steam scrubbers, washer-scrubber, pumps, sulph	for exha	uster	8, 8,	0	17	0
330	and any other purpose on the works 18' 0" mountings and connections. Exhauster. Capacity 40,000 cubic feet pe direct, with its own steam engine, with nections, bye-pass mains and flap-va Duplicate exhausters are desirable in ca	r hour governo	drive r, con	n n-	0	9	6
	down				0	10	6
1,325	Tower Scrubbers, two in number, 9 feet in 44 feet high each, with pent-house in ad filling, liquor and water distributors, was	dition.	Woo	d		-	10
570	first . Washer Scrubber with steam engine, con pass mains and valves. Capacity, 700,000				2	2	0
	day				0	18	0
500	Tar and Ammoniacal Liquor Wells, two is one divided in two. These are assumed ground, built of bricks in Portland ce capacity equal to four weeks' productio	to be	unde	r-			
80	liquor; with separator	: : :			0	16 2	6
		Cost per	Square	8			
	Fo	oot of Pu		g.			
		Area					
3,780	Purifying House. Ground floor house	£ 0.	u.				
-	with cellar and six purifiers 20 ft. square × 5 ft. deep, and lifting apparatus for purifier lids, wood grids, one centre						
	valve, two 4-way change valves, and all connections 18 in. diameter, complete.	1 11	6		6	0	0
1,260 400	House only, as above	0 10	6		2	Ö	0
	pillars	0 3	4		0	12	6
4,800	Two-Storied Purifying House, including						
	six purifiers 20 feet square and 5 feet						
	deep, placed on upper floor, supported on iron beams and columns; wood						
	grids, one centre valve, and two 4-way change valves, all connections 18 in.						
	diameter; lifting apparatus for purifier						
	lids; revivifying space on ground floor,						
	steam-engine and elevating apparatus						
1 700	for oxide of iron and lime	2 0	0	44	7	12	6
1,780	House only, as above	0 16	6	20	3	3	0
1000	belting, and steam engine	0 2	6		0	9	G.
2,520	Purifiers. Six vessels, 20 ft. square x	a display	-	400	-		
	5 ft. deep in two sets. The first four						
	with centre valve, and the two last with						
	4-way valves; with wood grids, lifting tackle for covers, and all connections.	1 1	0		4	0	0
	the second and the controlling .				-		"

Cos	Description.					Cost per ibic Fee (maxin oduced	et of	Gas
£					-		8.	
500	Station Meter House, with accommodation					-	40	
100	meters, and two station governors					0	16	0
425	Station Meter. Square connections, with							
	and mountings, complete; capacity, 40				et	Ó	18	R
	per hour				*	U	10	
		Cost pe						
			8.					
5,040	Gasholder Tanks, two in number, 122 feet	- 7						
	diameter, 221 feet deep = 240,000 cubic							
	feet each, built with bricks laid in Port-		-					
7010	land cement mortar and puddled	10	10	0		8	0	O
7,040	Gasholders, two in number, two-lift,							
	telescopic, 120 feet diameter, 40 feet							
	deep, capacity 430,000 cubic feet each, to- gether 860,000 cubic feet, equal to 32							
	hours' (11) days' production; with stand							
	pipes and valves	8	0	0		11	8	6
286	Station Governors, 16-inch, two in number,	7	-	177				
	with bye-pass, connections, and valves.				+ 4	0	7	6
400	Foundations of Apparatus throughout						3	
-	the works				14	0	12	6
315	Connections, valves, and mains, through-							
	out the works 16 in. diameter. Tar					. 0	10	0
65	pipes, water-pipes, &c			,			10	
00	Weighbridge at entrance					0	-	
	The second secon							
1,700	Offices, Workshops, Stores, testing room	and I	abo	rator	v.			
14177	and furnishing						14	
700	Boundary Wall, Drains, yard paving, and	conv	enie	ences		1	2	0
21,000	Distributing Plant. Assuming that the o							
	valves, syphons, and service pipes, amo							
	cent. of the total capital expenditure,	which	18	B IS	11.	88	6	8
500	average, then the cost will be		+-	7 10		00	0	
500	liquor per 24 hours and appurtenances;							
	cast-iron purifiers, 10' 0" × 5' 0" × 5'	0"	hv	draul	ic			
	change valve and wood roof on pillars, o							
	tank to hold 10 tons, lead-lined acid store	tank	, at	d ac	id			
457	supply tank with elevator, pipes, taps, &c	,		1			16	Time.
150	Buildings and lead-lined store for ditto .	100			ON I	77.0	12	6
140	Sulphur Recovery Apparatus		. ,				10	6
810	Tar Distilling Apparatus	200			*		10	0
280	Buildings for ditto	4 4		1.41	180	0	0	0

Description.	Capital Amount,	e	Per- entage.	Cub	Cost poic Fee maxim	et of	Gas Day.
The Capital of £70,000 would be distri-	£				£	8.	d.
buted as under.							
Land, law, parliamentary, and engineering							-
expenses	6,300		9 7	19.	10	15	6
Floating capital. Buildings (including a stage floor house, the brickwork of the retort stack, the gasbolder tanks, tar wells, and founda-	4,900		*	41	1	10	0
tions of apparatus)	22,400	- + 2	32	2.4	35	11	0
the apparatus generally)	15,400	4(4)	22	22	24	9	0
Distributing plant, mains, service-pipes,	21,000	**	30	99	33	6	8
Total	£70,000	44	100		111	2	2
Dividing the £70,000 Capital under the Heads of the different Departments.							
Land, law, parliamentary, and engineering			-		46	-	
expenses	6,300	**	7	**	10	15	6
Floating capital	4,900 16,100	::	23	3			0
Purifying (including condenser, scrubbers,	10,100		20	2.2	20	**	
washer scrubber, purifiers, &c.)	9,100		13		14	9	0
Storing	12,600		18		20		0
Distributing	21,000	**	30	**	33	6	8
Total	£70,000		100		111	2	2
20001	210,000	2.7	-		-	_	

MISCELLANEOUS.

BRICKS AND BRICKWORK.

Usual Dimensions of Bricks.

9 inches long; 4½ inches broad; 2¾ inches thick.

Weight of 1000 common clay bricks, about 3½ tons.
Weight of 1000 fire-clay bricks, about 3½ tons.
305 common clay bricks weigh about 1 ton.
300 fire-clay bricks weigh about 1 ton.
32 bricks laid flat will pave one square yard.
52 bricks laid on edge will pave one square yard.
Number of bricks in a cubic yard, without mortar, 416.
Number of bricks in a cubic yard, with mortar, 384.
In England, brickwork is generally calculated by the square rod.

In England, brickwork is generally calculated by the square rod. A rod of brickwork measures $16\frac{1}{2}$ feet \times $16\frac{1}{2}$ feet \times $1\frac{1}{8}$ foot = 306 cubic feet, or $11\frac{1}{3}$ cubic yards.

A rod of brickwork = 272 superficial feet, 11 brick, or 131 inches thick, which is called the standard thickness.

Number of bricks in a rod of brickwork, allowing for waste, 4500.

To reduce brickwork from superficial feet of 9 inches thick to the standard thickness of 131 inches, deduct one-third.

To reduce brickwork from cubic feet to superficial feet of the standard thickness of 131 inches, deduct one ninth.

To reduce brickwork from cubic feet to rods, divide by 306.

To reduce brickwork of more than 1½ bricks thick to superficial feet of the standard thickness of 13½ inches, multiply the area in feet by the number of half bricks in thickness, and divide the product by 8.

To reduce brickwork footings to superficial feet of the standard thickness of 131 inches, multiply the length by the height of the courses, in feet, and the product by the number of half bricks in the mean breadth, and divide by 3. When the number of courses is odd,

the number of half bricks in the middle course is the mean. When the number of courses is even, the mean breadth is found by taking half the sum of half bricks in the upper and lower courses.

Bond in Brickwork.

English bond is the strongest, and is a course of stretchers and a course of headers alternately, or one course of headers and one course of stretchers.

Flemish bond is a header and stretcher laid alternately in the

same course.

Hoop-iron, when used as bond, should be well tarred and sanded, and bedded in Portland cement.

A rod of brickwork in ordinary buildings requires about-

1 cubic yard of lime. 23 cubic yards of sand.

A rod of brickwork in a gasholder tank requires about-

12 cubic yards of blue lias lime. 25 cubic yards of sharp river sand.

A rod of brickwork requires about-

13 cubic yards of Roman or Portland cement.

13 cubic yards of sharp river sand.

A cubic yard of quicklime . weighs about 1460 lbs.

blue lias quicklime 1470 ,, ** ** 13 2416 ,, Portland cement . ,, 11 11 ,,, Roman cement . 1700 ,, ** ** " 22 2430 .. dry sand . .

The above materials, when made into mortar, lose about onethird of their bulk.

TABLES.

Showing the Number of Bricks in Walls of different Areas, from ½ a Brick up to 4 Bricks thick. 'Reckoned at 4500 Bricks to the Rod (272 feet super.), allowing for Waste.

Table I .- From 1 to 50 Superficial Feet.

Area of Wall. Sup. Feet.	Brick on Bed.	1 Brick Thick.	1½ Bricks Thick.	2 Bricks Thick.	2½ Bricks Thick.	3 Bricks Thick.	31 Bricks Thick.	4 Bricks Thick.
1	6	11	17	22	28	33	89	44
2	11	22	33	44	55	66	77	88
8	17	33	50	66	83	99	116	132
4	22	44	66	88	110	132	154	176
5	28	55	83	110	138	165	193	221
6	33	66	99	132	165	199	232	265
7	39	77	116	154	193	232	270	309
8	44	88	132	176	221	265	309	358
9	50	99	149	199	248	298	347	897
10	55	110	165	221	276	331	386	441
11	61	121	182	243	303	364	425	485
12	66	132	199	265	331	397	463	529
13	72	143	215	287	358	430	502	574
14	77	154	232	309	386	463	540	618
15	83	165	248	331	414	496	579	662
16	88	176	265	353	441	529	618	706
17	94	187	281	875	469	563	656	750
18	99	199	298	397	496	596	695	794
19	105	210	314	419	524	629	783	838
20	110	221	331	441	551	662	772	882
21	116	232	347	463	579	695	811	926
22	121	243	364	485	607	728	849	971
23	127	254	381	507	634	761	888	1015
24	132	265	397	529	662	794	926	1059
25	138	276	414	551	689	827	965	1103
26	143	287	430	574	717	860	1004	1147
27	149	298	447	596	744	893	1042	1191
28	154	309	463	618	772	926	1081	1235
29	160	320	480	640	800	960	1119	1279
30	165	331	496	662	827	993	1158	1324
31	171	342	513	684	855	1026	1197	1368
32	176	353	529	706	882	1059	1235	1412
33	182	364	546	728	910	1092	1274	1456
34	188	375	563	750	938	1125	1313	1500
35	193	386	579	772	965	1158	1351	1544
36	199	397	596	794	993	1191	1390	1588
37	204	408	612	816	1020	1224	1428	1632
38	210	419	629	838	1048	1257	1467	1676
	215	430	645	860	1075	1290	1506	1721
39	221	441	662	882	1103	1324	1544	1765
41	226	452	678	904	1131	1357	1583	1809
	232	463	695	926	1158	1390	1621	1853
42	237	474	711	949	1186	1423	1660	1897
	243	485	728	971	1213	1456	1699	1941
44	248	496	744	993	1241	1489	1737	1941
45			761		1268	1522		
46	254	507	778	1015	1296	1555	1776	2029
47	259	518	794		1324	1588	1814 1853	2074
48	265	529		1059				2118
49 50	270 276	540 551	811 827	1081	1351 1379	1621 1654	1892 1930	2162 2206

TABLES.

Showing the Number of Bricks in Walls of different Areas, from ½ a Brick up to 4 Bricks thick. Reckoned at 4500 Bricks to the Rod (272 feet super.), allowing for Waste.

TABLE II .- 51 to 100 Superficial Feet.

Area of Wall. Sup. Feet.	Brick on Bed.	1 Brick thick.	1½ Bricks thick.	2 Bricks thick.	24 Bricks thick.	8 Bricks thick.	34 Bricks thick.	4 Bricks
51	281	563	844	1125	1406	1688	1969	2250
52	287	574	860	1147	1434	1721	2007	2294
53	292	584	877	1169	1461	1754	2046	2338
54	298	596	893	1191	1489	1787	2085	2382
55	303	607	910	1213	1517	1820	2123	2426
56	309	618	926	1235	1544	1853	2162	2471
57	314	629	943	1257	1572	1886	2200	2515
58	320	640	960	1279	1599	1919	2239	2559
59	325	651	976	1301	1627	1952	2278	2603
60	331	662	993	1323	1654	1985	2316	2647
61	336	673	1009	1346	1682	2018	2355	2691
62	342	684	1026	1368	1710	2051	2393	2735
68	347	695	1042	1890	1737	2085	2432	2779
64	353	706	1059	1412	1765	2118	2471	2824
65	358	717	1075	1434	1792	2151	2509	2868
66	364	728	1092	1456	1820	2184	2548	2912
67	369	739	1108	1478	1847	2217	2586	2956
68	375	750	1125	1500	1875	2250	2625	3000
69	381	761	1142	1522	1908	2283	2664	3044
70	386	772	1158	1544	1939	2316	2702	3088
71	392	783	1175	1566	1958	2349	2741	3132
72	397	794	1191	1588	1985	2382	2779	3177
78	403	805	1208	1610	2013	2415	2818	3221
74	408	816	1224	1632	2040	2449	2857	3265
75	414	827	1241	1654	2068	2482	2895	3309
76	419	838	1257	1676	2096	2515	2934	3853
77	425	849	1274	1699	2123	2548	2972	3397
78	430	860	1290	1721	2151	2581	3011	3441
79	436	871	1307	1748	2178	2614	3050	3485
80	441	882	1324	1765	2206	2647	3088	8529
81	447	893	1340	1787	2233	2680	3127	3574
82	452	904	1357	1809	2261	2713	3165	3618
88	458	915	1373	1831	2289	2746	3204	3662
84	468	926	1390	1853	2316	2779	3243	3706
85	469	938	1406	1875	2344	2813	3281	3750
86	474	949	1423	1897	2371	2846	3320	3794
	480	960	1439	1919	2399	2879	3358	
87		970	1456	1913	2426	2912	3397	3838 3882
88	485	982		1963	2454	2945	3436	3926
89	491	993	1472	1985	2482	2978	3474	3971
90	496	1004	1489 1506		2509	3011	3513	
91	502	1015	1522	2007 2029	2537	3044	3551	4015
92	507					3077		4059
93	513	1026 1037	1539	2051	2564	3110	3590 3629	4103
94	518		1555	2074	2592 2619	3143	3667	4147 4191
95	524	1048	1572	2096				
96	529	1059	1588	2118	2647	3176	3706	4235
97	535	1070	1605	2140	2675	3210	3744	4279
98	540	1081	1621	2162	2702	3243	3783	4324
99	546 551	1092 1103	1638 1654	2184 2206	2730 2757	3276 3309	3822 3860	4368 4412

TABLES,

Showing the Number of Bricks in Walls of different Areas, from \(\frac{1}{2}\) a Brick up to 4 Bricks thick. Reckoned at 4500 Bricks to the Rod (272 feet super.), allowing for Waste.

Table III .- From 110 to 600 Superficial Feet.

-			1	1	·	, court 1		
Area of Wall. Sup. Feet.	½ Brick on Bed.	1 Brick thick.	1½ Bricks thick.	2 Bricks thick.	21 Bricks thick.	3 Bricks thick.	3½ Bricks thick.	4 Bricks thick.
110	607	1213	1820	2426	3033	3640	4246	4853
120	662	1324	1985	2647	3309	3971	4632	5294
130	717	1434	2151	2868	3585	4301	5018	5735
140	772	1544	2316	3088	3860	4632	5404	6176
150	827	1654	2482	3309	4136	4963	5790	6618
160	882	1765	2647	3529	4412	5294	6176	7059
170	938	1875	2813	3750	4688	5625	6563	7500
180	993	1985	2978	3971	4963	5956	6949	7941
190	1048	2096	3143	4191	5239	6287	7835	8382
200	1103	2206	3309	4412	5515	6618	7721	8824
210	1158	2316	3474	4632	5790	6949	8107	9265
220	1213	2426	3640	4853	6066	7279	6493	9706
230	1268	2537	3805	5074	6342	7610	8879	
240	1324	2647	3971	5294	6618	7941	9265	10,147
250	1379	2757	4136	+5515	6893	8272		10,588
	1434	2868	4301		7169	8603	9651	11,029
260 270	1489	2978	4467	5735	7445	8934	10,037	11,471
		3088	4632	5956			10,423	11,912
280	1544			6176	7721	9265	10,809	12,353
290	1599	3199	4798	6397	7996	9596	11,195	12,794
300	1654	3309	4963	6618	8272	9926	11,581	13,235
310	1710	3419	5129	6838	8548	10,257	11,967	13,676
820	1765	3529	5294	7059	8824	10,588	12,353	14,118
330	1820	3640	5460	7279	9099	10,919	12,739	14,559
340	1875	3750	5625	7500	9375	11,250	13,125	15,000
350	1930	3860	5790	7721	9651	11,581	13,511	15,441
360	1985	3971	5956	7941	9926	11,912	13,897	15,882
370	2040	4081	6121	8162	10,202	12,243	14,283	16,324
380	2096	4191	6287	8382	10,478	12,574	14,669	16,765
390	2151	4301	6452	8603	10,754	12,904	15,055	17,206
400	2206	4412	6618	8824	11,029	13,235	15,441	17,647
410	2261	4522	6783	9044	11,305	13,566	15,827	18,088
420	2316	4632	6949	9265	11,581	13,897	16,213	18,529
430	2371	4743	7114	9485	11,857	14,228	16,599	18,971
440	2426	4853	7279	9706	12,132	14,559	16,985	19,412
450	2482	4963	7445	9926	12,408	14,890	17,371	19,858
460	2537	5074	7610	10,147	12,684	15,221	17,757	20,294
470	2592	5184	7776	10,368	12,960	15,551	18,143	20,735
480	2647	5294	7941	10,588	13,235	15,882	18,529	21,176
490	2702	5404	8107	10,809	13,511	16,213	18,915	21,618
500	2757	5515	8272	11,029	13,787	16,544	19,301	22,059
510	2813	5625	8438	11,250	14,063	16,875	19,688	22,500
520	2868	5735	8603	11,471	14,338	17,206	20,074	22,941
530	2923	5846	8768	11,691	14,064	17,537	20,460	23,382
540	2978	5956	8934	11,912	14,890	17,868	20,846	23,824
550	3033	6066	9099	12,132	15,165	18,199	21,282	24,265
560	3088	6176	9265	12,353	15,441	18,529	21,618	24,706
670	3143	6287	9430	12,574	15,717	18,860	22,004	25,147
580	3199	6397	9596	12,794	15,993	19,191	22 390	25,588
590	3254	6507	9761	13,015	16,268	19,522	22,776	26,029
600	8309	6618	9926	13,235	16,544		23,162	26,471

TABLES.

Showing the Number of Bricks in Walls of different Areas, from \(\frac{1}{2}\) a Brick up to 4 Bricks thick. Reckoned at 4500 Bricks to the Rod (272 feet super.), allowing for Waste.

Table IV .- From 610 to 2000 Superficial Feet.

rea of Wall Sup. Feet.	d Brick on Bed.	1 Brick thick.	1 Bricks thick.	2 Bricks thick.	2½ Bricks thick.	8 Bricks thick.	31 Bricks thick.	4 Brick thick.
610	3364	6728	10,092	13,456	16,820	20,184	23,548	26,912
620	3419	6838	10,257	13,676	17,096	20,515	23,934	27,358
630	3474	6949	10,423	13,897	17,371	20,846	24,320	27,794
640	3529	7059	10,588	14,118	17,647	21,176	24,706	28,235
650	3585	7169	10,754	14,338	17,923	21,507	25,092	28,676
660	3640	7279	10,919	14,559	18,199	21,888	25,478	29,118
670	3695	7390	11,085	14,779	18,474	22,169	25,864	29,559
680	3750	7500	11,250	15,000	18,750	22,500	26,250	30,000
690	3805	7610	11,415	15,221	19,026	22,831	26,636	30,44
700	3860	7721	11,581	15,441	19,301	23,162	27,022	30,889
710	3915	7831	11,746	15,662	19,577	23,493	27,408	31,32
720		7941	11,912	15,882	19,853	23,824	27,794	31,76
730	3971							
	4026	8051	12,077	16,103	20,129	24,154	28,180	32,200
740	4081	8162	12,243	16,324	20,404	24,485	28,566	32,64
750	4136	8272	12,408	16,544	20,680	24,816	28,952	33,08
760	4191	8382	12,574	16,765	20,956	25,147	29,338	83,52
770	4246	8493	12,739	16,985	21,232	25,478	29,724	33,97
780	4301	8603	12,904	17,206	21,507	25,809	30,110	34,419
790	4357	8713	13,070	17,426	21,783	26,140	30,496	34,85
800	4412	8824	13,235	17,647	22,059	26,471	30,882	35,29
810	4467	8934	13,401	17.868	22,335	26,801	31,268	35,73
820	4522	9044	13,566	18,088	22,610	27,132	31,654	36,17
830	4577	9154	13,732	18,309	22,886	27,463	32,040	36,61
840	4632	9265	13,897	18,529	23,162	27,794	32,426	37,05
850	4688	9375	14,063	18,750	23,438	28,125	32,813	87,50
860	4743	9485	14,228	18,971	23,713	28,456	33,199	37,94
870	4798	9596	14,393	19,191	23,989	28,787	33,585	38,38
880	4853	9706	14,559	19,412	24,265	29,118	33,971	38,82
890	4908	9816	14,724	19,632	24,540	29,449	34,857	39,26
900	4963	9926	14.890	19,858	24,816	29,779	84,748	39,70
910	5018	10,037	15,055	20,074	25,092	30,110	35,129	40,14
920	5074	10,147	15,221	20,294	25,368	30,441	35,515	40,58
930	5129	10,257	15,386	20,515	25,643	30,772	35,901	41,02
940	5184	10,368	15,551	20,735	25,919	31,103	36,287	41,47
950	5239	10,478	15,717	20,956	26,195	31,434	37,673	41,91
960	5294	10,588	15,882	21,176	26,471	31,765	37,059	42,35
970	5349	10,699	16,048	21,397	26,746	32,096	37,445	42,79
980	5404	10,809	16,213	21,618	27,022	32,426	37,831	43,23
990	5460	10,919	16,379	21,838	27,298	32,757	38,217	43,67
1000	5515	11,029	16,544	22,059	27,574	33,088	38,603	44,11
1100	6066	12,132	18,199	24,265	30,331	36,397	42,463	48,52
1200	6618	13,235	19,853	26,471	33,088	39,706	46,324	52,94
1300	7169	14,338	21,507	28,676	35,846	43,015	50,184	57,35
1400	7721	15,441	23,162	30,882	38,603	46,324	54,044	61,76
1500	8272	16,544	24,816	33,088	41,360	49,632	57,904	66,17
1600	8824	17,647	26,471	35,294	44,118	52,941	61,765	70,58
1700	9375	18,750	28,125	37,500	46,825	56,250	65,625	75,00
1800	9926	19,853	29,779	39,706	49,632	59,559	69,485	79,41
1900	10,478	20,956	31,434	41,912	52,390	62,868	78,346	83,89
2000	11,029	22,059	33,088	44,118		66,176	77,206	88,28

TABLES

Showing the Number of Bricks in Walls of different Areas from \(\frac{1}{2}\) a Brick up to 4 Bricks thick. Reckoned at 4500 Bricks to the Rod (272 feet super.), allowing for Waste.

Table V .- From 2100 to 250,000 Superficial Feet.

Area of Wall. Sup. Feet.	Brick on Bed.	1 Brick thick.	1 Bricks thick.	2 Bricks thick.	2½ Bricks thick.	3 Bricks thick.	8½ Bricks thick.	4 Bricks thick.
2100	11,581	23,162	34,743	46,324	57,904	69,485	81,066	92,64
2200	12,132	24,265	36,397	48,529	60,662	72,794		97,05
2300	12,684	25,368	38,051	50,735	63,419	76,103		101,47
2400	18,235	26,471	39,706	52,941	66,176	79,412		105,88
2500	13,787	27,574	41,360		68,934	82,721	96,507	
2600	14,338	28,676	43,015	57,353	71,691	86,029		110,29
2700	14,890	29,779	44,669	59,559	74,449			114,70
		30,882	46,824	61,765	77,206	89,338		119,11
2800	15,441		47,278			92,647		123,52
2900	15,998	31,985		63,971	79,963	95,956		127,94
3000	16,544	33,088	49,632	66,176	82,721	99,265		132,35
3100	17,096	34,191	51,287	68,382	85,478	102,574		136,76
3200	17,647	35,294	52,541	70,588	88,235	105,882		141,17
3300	18,199	36,397	54,596	72,794	90,993	109,191		145,58
3400	18,750	37,500	56,250	75,000	98,750	112,500	131,250	150,00
3500	19,301	38,603	57,904	77,206	96,507	115,809	135,110	154,41
3600	19,853	39,706	59,559	79,412	99,265	119,118	138,971	158,82
3700	20,404	40,809	61,213	81,618		122,426		163,28
8800	20,956	41,912		83,824	104,779	125,785		167,64
3900	21,507	43,015	64,522	86,029		129,044		172,05
4000	22,059	44,118		88,235	110,294	132,358		176,47
4100	22,610	45,221	67,831	90,441	113,051	135,662		180,88
4200	23,162	46,324	69,485		115,809			
	23,713	47,426						185,29
4300		48,529		97,059				189,7
4400	24,265							194,1
4500	24,816	49,632				148,897		198,55
4600	24,368	50,735						202,9
4700	25,919	51,838		103,676				207,3
4800	26,471	52,941	79,412					211,7
4900	27,022							216,1
5000	27,574	55,147		110,294				220,5
10,000	55,147	110,294						441,1
15,000	82,721	165,441					579,044	661,7
20,000	110,294	220,588					772,059	882,3
25,000	137,868	275,735			689,338	827,200	965,074	1,102,9
30,000	165,441	330,882	496,324	661,765	827,206	992,647	1,158,088	1,323,5
85,000	193,015	386,029	579,044	772,059	965,074	1,158,088	31,351,103	1,544,1
40,000	220,588	441,176	661,765	882,358	1,102,941	1,323,529	1,544,118	1,764,7
45,000	248,162			992,647	1,240,809	1,488,97	1,737,132	1,985,2
50,000	275,735			1,102,941	1.378,676	1.654.419	21,930,147	2,205,8
55,000	303,309						3 2,123,162	
60,000	330,882		992,647	1 323 529	1.654 419	1 985 29	4 2,316,176	2,647,0
65,000	358,456	716,919	1.075,368	1 433 824	1 792 279	2 150 78	5 2,509,191	2,867,6
70,000	386,029	779 059	1 158 088	1 544 118	1 930 147	2 916 17	6 2,702,206	3,088,2
		897 906	1 940 800	1 654 410	2 068 017	2,010,11	8 2,895,221	
75,000	413,603	880 959	1 393 590	1 764 706	2 205 89	0 0 647 05	93,088,235	
80,000	441,176							
85,000	468,750	000 645	1 400 071	1,070,000	10 401 61	0,012,00	03,281,250	
90,000	496,324						13,474,265	The second second
95,000	523,897	1,047,794	1,071,791	2,095,080	2,619,48	3,143,38	23,667,279	
100,000							4 3,860,294	The second secon
150,100							5 5,790,441	
200,000	1,102,941	2.205.882	13.303.824	4.411.76	55.514.70	66.617.64	717,720,588	8,823,
250,000		The second second		1 1 1 1 1 1 1 1 1	01077110	0 01011101	9 9,650,735	COLUM

MORTAR AND CONCRETE.

			Λ	Iorte	ır.						
	- .										Measure.
	Lime	•	•	•	•	•	•	•	•	1	part.
	Sharp river sand									8	parts.
	•			or,							•
	Lime			•						1	part.
	Sand	•	•	•	•	•	•	٠	•		*
		•	:.		•	•		•	٠		parts.
	Blacksmith's ashe	es or	clii	aker	, gr	oun	ıd	•	•	1	part.
		(oar	se M	orte	ır.					
	Lime	_	_	_			_			1	part.
	Coarse sand .	•	٠	•	•	•	·	•	•		parts.
	Course sand .	•	•	•	•	•	•	•	•	-	Pares.
		lydra			me	Mo	rtar				
	Best blue lias lim	е.								1	part.
	Clean sharp river										parts.
	Crown sharp inver	Duite	٠.			•	•	•	•	-2	Parto
	Best blue lias lim	_		or,						1	
			٠	•	•	•	•	•	•		part.
	Burnt clay	•		•	•	•	•	•	•	2	parts.
				or,							
	Best blue lias lime	е.		•						1	part.
	Puzzolana				-		-				part.
	Clean sharp sand	•	:		•	•	•	:	•		parts.
	Clean sharp sand	•	•	•	•	•	•	•	•	U	parts.
		Ce	men	t M	orte	w.					
	Cement, Portland	١.								1	part.
	Clean sharp sand							•		8	parts.
m	-										_
morta	lime should be fre for a day's work p e made as it is bei	repa	red	at o	nd r nce	ot :	mor The	e th cer	an nei	su: at r	nortar should
only b	e made as it is ben	ng u	seu.	,							
				mer							
Blu	e lias lime concret e	e (for	for	unde	tio	ns)-	_				By Measure.
	ravel, shingle, bro							ı.a.,	·nte	· wta	_,
u	11 to 0 inches on	Vell	2001	ie, i	1110	no,	OT O	ıu ı	eu)I (15	
0	$1\frac{1}{2}$ to 2 inches cul	oe .	•	•	•	•	•	•	•		. 6 parts.
C	lean sharp sand	• _ •			•	•	•		•		. 2 parts.
В	lean sharp sand lue lias or other h	ydrai	ılic	lim	е.						. 1 part.
	tland cement concr										-
G	ravel, shingle, bro	ken :	ator	ie. h	ricl	kg. 4	ח מר	ld r	etn	rte	
•	1½ inches cube					, (J. U.	1	- J.	. 40,	7 norta
_		• •	•	•	•	•	•	•	•	•	7 parts.
Õ		• •	•	•	•	•	•	•	•		. 2 parts.
P	ortland cement			•							. 1 part.
											f f Ž
											=

Mastic Cement for Buildings.

1 part red lead. 5 parts ground lime.

5 parts sharp sand. Mix with boiled linseed oil. 1 part red lead.
5 parts whiting.
10 parts sharp sand.
Mix with boiled linseed oil.

Clean sharp sand (not having its particles rounded by attrition) should always be used in the composition of mortar when it can be procured; but, otherwise, clean well-burnt ashes may be substituted.

In preparing ordinary mortar it is desirable to mix a small proportion of smithy ashes with the lime and sand. On this subject Mr. Graham Smith remarks ("Engineering Papers," p. 20): "The importance of the admixture of ashes with mortar to be atmospherically dried will be shown by the following results:—The bricklayers' mortar, with common bricks, after a lapse of 84 days, broke with 570 lbs.; when sand was substituted in place of ashes—that is, when the proportions were 1 slaked lime, 2 sand, and no ashes—it only required 257 lbs. to tear asunder the bricks. These are the averages of three experiments. This is no doubt attributable to the ashes being porous; they thus allow greater facilities for the absorption of carbonic acid from the atmosphere."

The more sand that can be incorporated with the lime, the better the mortar, provided the necessary degree of plasticity is preserved.

A load of mortar is equal to one cubic yard.

A hod of mortar measures 9 in. \times 9 in. \times 14 in.

Two hods of mortar are nearly equal to a bushel.

The mortar in a rod of brickwork (4500 bricks) is taken at 1½ cwt. of chalk lime and 2 loads of sand, or 1 cwt. of stone lime and 2½ loads of sand.

Fire-Clay.

The value of Fire-clay consists chiefly in the proportion of the alumina to the fusible matter (viz., oxide of iron, and the alkalies of magnesia, potassa and soda, &c.) and to the silica; these being the principal ingredients of which it is composed. The larger the proportion of alumina to the fusible matter, the more refractory the clay. Of two clays containing alumina and fusible matter in the same proportions, that which contains the least silica is the more refractory.

The celebrated clays of Stourbridge, Newcastle-on-Tyne, different parts of Yorkshire, Scotland, and a few other places, are valuable in the manufacture of bricks, tiles, and retorts used in furnaces for the

distillation of coal.

The table on next page will be found useful in this connection.

GAS ENGINEERS AND MANAGERS.

Locality	Silion	Almmina		Peroxide	Phos-	Limo	Mag-	Dotusen	Rode	Titanic	Water, Organic	Total
-			Iron.	ganese.	Iron.		nesia.			Acid.	Matter, &c.	
Stourbridge	65.37	86.48	2.68	:	:	.28	.83	1.26	.30	.30	:	100
Plympton, Devonshire.	74.03	21.37	1.94	:	:	OF.	98.	1.85	60.	:	:	100
Newcastle-on-Tyne	64.63	29.78	3.23			.43	.41	1.09	.24	.50	:	100
Burton-on-Trent	80.89	86.00	3.06	:		22.	71.	.30	1.88		:	100
Wortley, near Leeds .	66.25	29.71	3.07	:	ě	01-	.61	•43	1.12	.41	:	100
Derbyshire	48.08	8-98	3.56	:	:	:	:	1.88	:	:	10.89	100
Hedgerley, Bucks*	84.65	8.86	4.95		**	1.90	-38	:	:	:	:	100
Poole, Dorsetshire	28.69	34.32	2.35	:		27.	.55	3.33	:	:	:	100
Monmouthshire	75.30	16.80	1.00	:	:	06.	4	:	:	:	00.9	100
Pembrokeshire	88.43	06.9	1.90		:	3.17	٠	:	;	:	:	100
Dinas, Glamorganshire	97-62	1.40	-49	3	:	. 59	1	.10	.10	:	:	100
Kilmarnock, Scotland .	58.95	85.65	2.49	:	:	68.	98.	1.14	1.06		:	100
Perceton, Scotland	62.50	86.00	8.	.50	09.	09.	<u>ક્</u>	:	:	:	:	100
Govan, Scotland	60.20	87.70	1.10	:	:	1.00	:	:	:	:	:	100
France	66.10	19.80	:	:	:	:	:	:	:	:	14.10	8
Невве	47.50	34.37	1.24	:	:	:	1.00	:	:	:	15.89	8
Bavaria	45.79	28.10	6.55	:	:	:	:	:	:	:	19.26	8

Handy Multiplier for Wrought-Iron.

If the area in square inches of the cross section of any specimen of wrought-iron be multiplied by 3.34, the product will be the weight in pounds of a lineal foot of such specimen.

FLAT BAR IRON .- Weight in lbs. of a Lineal Foot.

Breadth			Т	hickness	in Parts	of an Inch	1.		
in Inches.	1-4th.	5-16ths.	3-8ths.	7-16ths.	1-half.	5-8ths.	8-4ths.	7-8ths.	1
1	-835	1.044	1.253	1:461	1.670	2.088	2.506	2.923	3.340
11	.939	1-174	1.409	1.644	1.878	2.348	2.818	3.287	8.756
11	1.044	1.305	1.566	1.826	2.088	2.609	3.132	3.653	4-176
18	1.148	1.435	1.722	2.009	2.296	2.870	8.444	4.018	4.592
14	1.252	1.566	1.879	2.192	2.504	3.131	3.758	4.384	5.008
18	1.358	1.696	2.035	2.874	2.716	3.392	4.070	4.749	5.439
14	1.462	1.827	2.192	2.557	2.924	8.658	4.384	5.114	5.848
17	1.566	1.957	2.348	2.740	8.132	3.914	4.696	5.479	6 - 264
2"	1.671	2.088	2.505	2.922	3.842	4-175	5.010	5.845	6.684
21	1.775	2.218	2.662	3.105	3.550	4.435	5.324	6.210	7-100
21	1.880	2.348	2.818	3.288	3.760	4.696	5.636	6.575	7 - 520
28	1.984	2.479	2.975	3.470	3.968	4.957	5.950	6.941	7.936
21	2.088	2.609	3.131	3.653	4.176	5.218	6.262	7.306	8:35
28	2.193	2.740	3 288	3.836	4.386	5.479	6.576	7.671	8.779
24	2.297	2.870	3.444	4.018	4.594	5.740	6.888	8.036	9.188
27	2.402	3.001	3.601	4.201	4.804	6.001	7.202	8.402	9.608
3	2.506	3.131	3.758	4.384	5.012	6.262	7.516	8.767	10.02
31	2.715	3.392	4.071	4.749	5.430	6.784	8.142	9.498	10.860
31	2.923	3.653	4.384	5.114	5.846	7.306	8.768	10.228	11-695
82	3.132	3-914	4.697	5.479	6.264	7:828	9.394	10.959	12-52
4	3.841	4.175	5.010	5.845	6.682	8:350	10.020	11.690	13.36
41	3.549	4.436	5.828	6.210	7.098	8.871	10.646	12.421	14.19
41	3.758	4.697	5.636	6.575	7.516	9.393	11.272	13.151	15:03
43	3.966	4.958	5.949	6:941	7:932	9.915	11.898	13.881	15.86
5	4.175	5.219	6.263	7.306	8.350	10.437	12.526	14.612	16.70
51	4.384	5.479	6.576	7.671	8.768	10.958	13'152	15.343	17.58
51	4.593	5.741	6.889	8.037	9.186	11.480	18.778	16.078	18-37
51	4.801	6.001	7.202	8.402	9.602	12.002	14.404	16.804	19.20
6	5.010	6.262	7:515	8.767	10.020	12.524	15.030	17.535	20.04

ROUND BAR IRON .- Weight in ths. of a Lineal Foot.

Diameter in Inches.	Weight in lbs.	Diameter in Inches.	Weight in lbs.	Diameter in Inches.	Weight in lbs.	Diameter in Inches.	Weight in lbs.
1	.040	18	6.870	31	25.400	48	55 640
1	.163	12	7.970	31	27.475	43	58 688
2	4363	17	9.150	38	29.625	47	61.820
Ä	*650	2	10.406	31	31.870	5	65 040
8	1:006	24	11.750	38	34.175	51	68.330
3	1.456	21	13.106	33	36.575	51	71.700
ž	1.990	28	14.670	37	39.056	58	75-150
1	2.590	21	16:256	4	41.620	51	78.700
11	3.300	28	17.925	41	44.260	58	82.300
11	4.070	24	19.600	41	46.990	53	86.006
10	4:920	21	21.500	42	49.790	57	89.800
16	5.860	8	23.406	44	52.675	6	93:650

SQUARE BAR IRON.

Weight in lbs. of a Lineal Foot.

Side in Inches.	Weight in lbs.	Side in Inches.	Weight in lbs.	Side in Inches.	Weight in lbs.	Side in Inches.	Weight in lbs.
.	.052	12	8.82	31	32.72	49	71.60
i i	·208	1 1 1	10.23	31	35.28	43	75.36
ă,	•469	1 2	11.74	3	38.16	47	79.54
i	.832	2	13.36	81	40.92	5	83 - 44
i !	1.304	21	15.08	84	44.01	51	87.90
ă '	1.876	21	16.91	32	46'96	51	52:40
i	2.557	2 1	18.84	37	50.38	51	96.67
1	8.340	24	20.86	4	53.44	54	101.0
11	4.227	2 2	23 · 10	41	56.97	58	105.8
11	5.216	23	25 · 25	41	60.32	54	110.80
14	6.814	27	27.70	43	64.08	51	115.48
1 }	7.504	3	30.02	44	67.64	6	120.0

SHEET IRON AND STEEL.

Weight of a Superficial Foot in Pounds and Fractions, with Corresponding
Number and Thickness of Birmingham Wire Gauge.

No. of Birmingham Wire Gauge.	Thickness in Parts of an Inch. Board of Trade	Bquar	t per e Foot lbs.	No. of Birmingham Wire Gauge.	Thickness in Parts of an Inch. Board of Trade	Squar	ht per e Foot lbs.
	Standard.	Iron.	Steel.		Standard.	Iron.	Steel
1	.300	12.00	12.240	19	.041	1.64	1:678
	284	11.36	11.587	20	.035	1.40	1 · 428
2 8	260	10.40	10.608	21	.032	1.28	1.306
	-238	9.52	9.710	22	.028	1.12	1.14
5	•220	8.80	8.976	23	025	1.00	1.02
6	203	8.12	8 282	24	022	0.88	0.89
4 5 6 7	·180	7.20	7.344	25	020	0.80	0.81
8	165	6.60	6.732	26	.018	0.72	0.78
9	148	5.92	6.038	27	.016	0.64	0.65
10	·135	5.40	5.508	28	.014	0.56	0.57
11	·120	4.80	4.896	29	.013	0.52	0.58
12	.109	4.36	4.447	30	·01 2	0.48	0.49
18	.095	3.80	3.876	81	.010	0.40	0.40
14	.083	3.32	3.386	82	.009	0.36	0.86
15	·072	2.88	2.938	33	.008	0.32	∵0∙32
16	.065	2.60	2.652	34	·007	0.58	0.58
17	.058	2.82	2.366	35	.005	0.50	0.54
18	.050	2.00	2.040	36	·004	0.16	0.16

STEEL.

Weight of One Foot of Round Steel.

Diameter in Inches.	1	3	1.	80	3 4	7 8	1	13	11	13	11	18	12	1;	2
Weight per Foot in lbs.	•167	•373	-669	1.04	1.05	2.05	2.67	3.38	4.18	5.06	6.02	7.07	8.2	9-41	11.71

WEIGHT IN POUNDS OF A SUPERFICIAL FOOT OF IRON, COPPER, AND BRASS.

Thickness by the Birming- ham Wire Gauge.	Iron.	Copper.	Brass.	Thickness by the Birming- ham Wire Gauge.	Iron.	Copper.	Brass.
1	12-50	14.50	13.75	16	2.50	2.90	2.75
2 3	12.00	13.90	13.20	17	2.18	2.52	2.40
3	11.00	12.75	12.10	18	1.86	2.15	2.04
4	10.00	11.60	11.00	19	1.70	1.97	1.87
5	8.74	10.10	9.61	20	1.54	1.78	1.69
6	8.12	9.40	8.93	21	1.40	1.62	1.54
7	7.50	8.70	8:25	22	1.25	1.45	1.37
8	6.86	7.90	7.54	23	1.12	1.30	1.23
9	6.24	7.20	6.86	24	1.00	1.16	1.10
10	5.62	6.50	6.18	25	-90	1.04	.99
11	5.00	5.80	5.50	26	.80	.92	*88
12	4.38	5.08	4.81	27	.72	-83	79
13	3.75	4.84	4.12	28	.64	.74	-70
14	3.15	3.60	3.43	29	.56	-64	-61
15	2.82	3.27	3.10	30	.50	.58	*55

WEIGHT OF A SUPERFICIAL FOOT OF VARIOUS METALS.

Thickness in Inches.	Wrought Iron.	Cast Iron.	Steel.	Copper.	Brass.	Lead.	Zine.	Thickness in Inches.
N. J.	Ibs.	1bs.	lbs.	lbs.	lbs.	lbs.	Ibs.	
1-16th.	2.526	2.344	2.552	2.891	2.374	3.708	2.344	1-16th.
1-8th.	5.052	4.687	5.104	5.781	5.469	7.417	4.687	1-8th.
3-16ths.	7.578	7.031	7.656	8.672	8.203	11.125	7.031	3-16ths.
1-4th.	10.104	9.875	10.208	11.563	10.938	14.883	9.375	1-4th.
5-16ths.	12.630	11.719	12.760	14.453	31.672	18.542	11.719	5-16ths.
3-8ths.	15.156	14.062	15.312	17.344	16.406	22.250	14.062	3-Sths.
7-16ths.	17.682	16.406	17.865	20.234	19.141	25.958	16.406	7-16ths.
1-half.	20.208	18:750	20.417	23.125	21.875	29.667	18.750	1-half.
9-16ths.	22.734	21.094	22-969	26.016	24.609	83.875	21.094	9-16ths.
5-8ths.	25 * 260	23.437	25.521	28 906	27.344	37.083	23 437	5-Sths.
11-16ths.	27.786	25.718	28.073	31.797	30.078	40.792	25.781	11-16ths.
3-4ths.	30.312	28 125	30.625	34.688	32.813	44.500	28.125	3-4ths.
13-16ths.	32.839	30.469	33-177	37.578	35 - 547	48.208	30.469	13-16ths.
7-8ths.	35 365	32.812	85.729	40.469	38.281	51.917	32.812	7-8ths.
15-16ths.	37.891	35.156	38-281	43.359	41.016	55-625	35.156	15-16ths.
1 inch	40.417	27.500	40.883	46.250	43.750	59.333	37.500	1 inch.

WEIGHT IN PARTS OF A POUND OF A SPHERE 1 IN. DIAM. OF VARIOUS METALS.

Brass. Cast.	Bronze.	Copper. Hammer ed.	Iron. Cast.	Iron. Wrought.	Steel.	Lead.	Tin.	Zinc.
.156	•159	167	-185	145	•147	.214	-139	.133

HOOP IRON.

Weight of 10 Lineal Feet.

Width in Inches and Parts.	9	2	7	1	11	11	12	11	13	2	21	21	24	8
No. of Gauge .	21	20	19	18	17	16	15	15	14	13	13	12	11	11
Weight in lbs. and Decimal Parts.	•685	-885	1.24	1.60	2.05	2.73	3.40	3.72	4.72	6.06	6.83	8.96	10.85	11.84

TAPER ANGLE IRON, OF EQUAL SIDES.

Length of Sides in Inches.	Thickness of Edges.	Thickness of Root.	Weight of One Lineal Foot in lbs. and Decimal Parts.
4 3	in.	ă in.	14·0 10·375
24 24 24 22	18	16	8·25 6·5
2 2 1	full full	i'a full	5·0 3·875 3·25
11	1 bare	A bare	2.625

TAPER T-IRON.

Width of Top Table in Inches.	Total Depth in Inches.	Thickness of Top Table at Root.	Thickness of Top Table at Edges.	Uniform Thickness of Rib.	Weight of One Lineal Foot in lbs.
3 3 2 2 <u>1</u> 2	84 28 3 24 14	in,	ë in.	7% in.	8·0 8·0 5·25 6·5 3·5 2·875

WEIGHT OF CORRUGATED IRON ROOFING.

							-			
B. W. Ga	uge.		Siz	e of Shee	ets,				Per Square.	Super. Feet per ton.
16		6 feet	×	2 feet	to 8 feet	×	3 feet	×	31 cwt.	800
18	••	6,,	×	2 "	8 ,,	×	8 ,,	×	24,,	1000
20		6 ,,	×	2 ,,	8 ,,	×	3 ,,	×	1 į "	1250
22		6 .,	×	2 ,,	7 ,,	×	21 ,,	×	11 ,,	1550
24		6,,	×	2 ,,	7 ,,	×	21,,	×	11 ,,	1880
26	• •	6 ,,	×	2 ,,	7,	×	24 ,,	×	1 ,,	2170

WEIGHT IN POUNDS OF NUTS AND BOLT-HEADS.

Diameter of Bolt in Inches.	‡ 	3	· 1	8	1	-	1	14	14	12	2	21	3
Weight of Hexagon Nut and Head.	.017	·U57	128	267	· 43 0	·730	1 • 10	2.14	3.77	5.62	8.75	17-2	28-8
Weight of Square Nut and Head.	.021	•070	·164	·321	•553	·882	1 · 81	2.26	4.42	7-00	10.50	21.0	36.4

WHITWORTH'S SCREWS WITH ANGULAR THREADS.

Diameter in Inches.	Number of Threads per Inch.	Diameter in Inches.	Number of Threads per Inch.	Diameter in Inches.	Number of Threads per Inch.
	40	19	6	8	31
180	24	13	6	3 <u>1</u>	3 <u>‡</u>
Ŧ	20	19	5	: 3 <u>1</u>	31
À	18	17	5	82	કે
i i	16	17	44	i 4	3
,ï,	14	! 2 ["]	41	41	21
'a"	12	21	44	43	27
í i	11	21	4	' 4¥	2≩
•	10	2	4	5	2
i	9	21	4	51	24
i	Ř	2	4	51	23 23 28 28
า้น	7	23	34	54	21
ii	7	27	34	6	24

Angle of threads 55° in every instance.

The threads do not intersect at their sides, but are rounded off one-sixth both at top and bottom, making their depth equal to twothirds of the pitch.

The number of threads to the inch in square-threaded screws is generally half the number of those in angular-threaded screws, and the depth equal to the space between the threads.

WEIGHT OF CHAINS.

Weight per Lineal Foot in lbs.	Diameter of Link in Inches.	Weight per Lineal Foot, in lbs.	Diameter of Link in Inches.	Weight per Lineal Foo in lbs.
.33	4	5.33	16	16·00 17·66
.91	1 T	7.16	170	19·25 20·83
1.50	1	9.33	18	24·17 28·33
3.00	116	11.83	178	32·50 38·33
	Lineal Foot in lbs. -38 -68 -91 1-33 1-50 2-38	Lineal Foot in Ibs.	Lineal Foot Link Lineal Foot in lbs.	Lineal Foot in Inches, Link in Ibs. Column

To Find the Safe Load on Chains.

(Diam. of link in eighths of an inch)² = safe load in tons.

 $(8 \times \text{weight to be raised}) = \text{diam. of link in eighths of inch.}$

WEIGHT AND STRENGTH OF ROUND ROPES OF HEMP AND WIRE.

	Hemp.			Iron Wire			Steel Wire	
Girth or Circum- ference in Inches.	Weight per Fathom of Six Feet in lbs.	Weight	Circum-	Fathom of Six Feet,	Weight	Circum-	Weight per Fathom of Six Feet, in 1bs.	Weight
11 1 1 2 2 2 4 2 2 3 3 4 4 4 5 5 6 6 6 6 6 7 7 8 8 8 9 9 5 10 10 11 11 11 11 12	·15 ·26 ·59 1·04 1·70 2·00 2·34 3·19 3·66 4·16 5·27 6·50 7·86 9·36 11·00 12·74 14·63 16·64 18·78 21·06 23·46 26·00 28·66 31·46 34·38 37·44	11 1 2 2 5 5 4 5 6 7 1 4 5 2 2 5 5 4 5 6 7 1 4 5 2 2 2 2 4 1 4 5 2 2 2 2 2 4 1 4 5 2 2 2 2 2 4 1 4 5 2 2 2 2 2 4 1 4 5 2 2 2 2 2 4 1 4 5 2 2 2 2 2 4 1 4 5 2 2 2 2 2 4 1 4 5 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	1 1 1 1 2 2 4 4 8 1 8 2 2 2 2 2 2 3 3 3 3 3 3 3 3 4 4 4 4 5 5 6 6	756 1 1½ 2 2½ 3 3½ 4 4½ 5 5½ 6 6 7 7½ 8 ½ 9 10 11 12 13 14 15 16 18 20 25 32 38	\$\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\	1 1 1 1 1 1 2 2 2 2 2 2 2 2 2 2 3 3 3 3	1 1 1 1 1 2 2 1 2 2 2 2 2 2 2 2 2 2 2 2	2½ 3½ 4½ 5½ 6½ 7½ 8½ 10 11½ 12½ 14 15½ 17 20½ 20½ 28½ 30½ 35 40

To find the Breaking Weight of Round Ropes of Hemp, Iron Wire, and Steel Wire.

Hemp $\frac{(\text{circum. ins.})^s}{5}$ = breaking weight in tons.

Iron wire (circum. ins.)² × 1·5 = breaking weight in tons. Steel wire (circum. ins.)² × 2·5 = breaking weight in tons. Factor of safety for hemp, iron, and steel ropes = $\frac{1}{6}$.

To find the Weight of Hemp Ropes. (Circum, ins.)² \times 26 = weight in lbs. per fathom.

ALLOYS OF METALS.

Yellow brass, 2 parts copper, 1 zinc. Rolled brass, 32 parts copper, 10 zinc, 1.5 tin. Brass casting, common, 25 parts copper, 2 zinc, 4.5 tin. Gun metal, 8 parts copper, 1 tin. Copper flanges for pipes, 9 parts copper, 1 zinc, 0.26 tin. Bell metal, 8 parts copper, 1 tin.

IRON TO RESIST THE ACTION OF FIRE.

The following mixture of iron is recommended for fire bars, furnace plates, gas retorts (iron) and any other ironwork required to resist the action of fire:—

80 per cent. Ridsdale. 20 per cent. Siemens Steel Scrap.

This is said to make a kind of pyrostatic iron, the high fusion point being due to the small percentage of carbon present in the mixture.

TABLE

Of the Velocity and Force of the Wind.

Miles per Hour.	Feet per Second.	Pressure in lbs. per Square Foot.	Description.
1	1.47	.005	Hardly perceptible.
2	2·93	·620	Just perceptible.
3	4·4	·044	
4	5·87	·079)	Gentle breeze.
5	7·38	·123)	
10 15	14·67 22·	1.107	Pleasant breeze.
20	29.34	1.968	Brisk gale.
25	36·67	3·076 }	High wind,
80	44·01	4·429 }	
85	51·34	6·027 /	Very high wind.
40	58·68	7·878 \	
45	66·01	9·996 5	Storm or tempest.
50	78·35	12·300	
60	88·02	17·718 }	Great storm.
70	102·71	24·153 }	
80	117·36	31·490	Hurricane.
100	146·7	49·200	

The pressure or force of the wind is as the square of its velocity.

The square of the velocity of the wind in feet per second $\times .002288$ = pressure in lbs. per square foot.

The wind pressure upon a cylindrical surface is one-half, and on a spherical surface one-fourth that which is exerted on a flat surface.

SPECIFIC GRAVITY AND WEIGHT OF VARIOUS SUBSTANCES.

Name of Substance.	Specific Gravity and Weight per Cub. Fo. in Ounces. Specific Gravity per cub. Foo in lbs. Avoirdupois.	Name of Substance.	Specific Gravity and Weight per Cb. Ft. in Ounces. Weight per tub. Foot in lbs. Avoirdu- pois.
Alcohol, pure	790 49.88	Brass, cast	8,240 515
Ash (timber)	. 752 47	, wire	8,480 530
Asphalt, prepared	2,496 156	Brick	2,080 180
Basalt	2,992 187	Brickwork	1,792 112
Bath stone	1,792 112	Cement, Portland	1,424 89
Beech	688 43	Roman.	960 60
Birch	704 44	Chalk	2,368 148
Bitumen	992 62	Charcoal, Oak	836 21
Boxwood	960 60	Clay	1,920 120

SPECIFIC GRAVITY AND WEIGHT OF VARIOUS SUBSTANCES—Continued.

Name of Substance.	per	Weight per Cub.Foot in Ibs. Avoirdu- pois.	Name of Substance.	Sp. Gr. and Weight per Cb. Ft. in Ounces.	Weight per Cub.Foot in lbs. Avoirdu- pois.
Clay puddle	2,560	160	Maple	784	49
Coal, anthracite, solid .	1,280	80	Marble	2,720	170
" bituminous	1,200	75	Marl	1,728	108
,, cannel, Scotch .	1,248	78	Masonry	2,240	140
" " Wigan .	1,280	80	Mercury	13,584	849
" , N'castle .	1,312	82	Mortar	1,760	110
" stored in usual)	832	52	Mud	1,600	100
way.		-	Naphtha	848	53
Coke from coking	800	50	Oak, English		50
ovens			,, American, red		54
" from gas-works	515	32.2	Oil, linseed		59
slaked	400	32.53	,, olive	912	57
" from gas-works	448	28	" whale (train)	928	58
unslaked	1 000	100	" sperm	880	55
Concrete	1,920	120	" tallow	896	56
Copper, cast	8,640	540	" colza	912	57
sheet and wire	8,800 240	550 15	Paving	2,560	160
Cork		100	Peat	1,280	80
Earth, loam	1,600	75	Pebble stone	2,704	169
Ebony	1,200 560		Petroleum	880	55
Elm		35 35	Pitch	1,152	72
Fir, red pine and spruce		29	Platinum, pure hammered .	19,520	1,220
" American larch	544	34		20,480	1,280
	2,400	150	Portland stone	20,800	1,300
Fire-Clay, natural	2,080	130	Quartz	2,096	131
Flag, Yorkshire	2,288	143	Sand, damp	2,640	165
Flint	2,624	164	3	1,888	118
Freestone	2,240	140	Candatana	2,528	90
Glass, crown	2,496	156	Shale	2,525	158
-1-1-1	2,880	180	Shingle		162 95
" flint	2,992	187	Silver, pure	1,520 10,480	655
Gold, pure	19,360	1,210	" standard	10,528	658
standard	17,728	1,108	Slate		180
Granite	2,688	168	Snow	128	8
Gravel	1,840	115	Steel	7.840	490
Grindstone	2,096	131	Sulphur	2,000	125
Gun metal	8,784	549	Sycamore	592	37
Gvpsum	2,304	144	Tar	1,040	65
Ice	- man	56.75	Tile	1,792	112
Iron, cast		448	Tin	7,360	460
Iron, wrought	7,680	480	Trap	2,720	170
Lead	11,392	712	Water, pure	1.000	62.5
" white	3,168	198	, sea	1,024.8	64.05
Limestone, lias	2,496	156	Whinstone	2,752	172
., magnesian .	2,848	178	Willow	448	28
Lime, quick	864	54	Yew	800	50
Mahogany, Honduras	640	40	Yorkshire flag	2,288	143
" Spanish	720		Zinc	7,040	440
The second secon	Moon of		e earth	5,664	354

MISCELLANEOUS ARTICLES.

Bale of	flax (Russia)	4		5 to 6 cw	t.
Barrel l	oulk			5 cubic fe	
Barrel o	of tar			261 gallon	S.
Battens				Boards 7 i	nches wide.
	of coal			80 lbs.	
Bushel	of coke			45 ,,	
Cable's	length			240 yards.	
Cask of	black lead .	-		11½ cwt.	
Chaldro		-		251 ,,	
	coke .			121 to 15 c	wt.
Cord of	wood			128 cubic fe	et.
					nches wide.
Dozen Dozen				70 117	
		*			
	of steel			. 120 lbs.	
Fodder	of lead		180	19½ cwt.	
Gross				12 doz.	
Hundre	d of deals .			. 120 in num	ber.
**	nails .			120	
Keel of	coals			21 tons 4	wt
	bricks				W U.
Load of				Tallana la marana a la	
**	inch boards.				
**	2-inch planks		*	300 square	feet.
11	lime			. 32 bushels	
**	new hay .			. 19 cwt. 32	lbs.
	old hay				
	straw			. 11 ,, 64	
	sand				
"	squared timbe			. 50 cubic fe	
**	unhewn			. 40 ,,	
**	tiles			1000 tiles.	
Mat of	flax (Dutch) .			. 126 lbs.	
Pig of l	allast		1.	. 56	
					inches wide.
or continue.				24 4	THE WILLIAM
The state of the s	f paper			The state of the s	2000
	of paper				or 480 sheets.
Roll of	parchment .			. 60 skins.	
Sack of	coals			. 224 lbs.	
		1.51	-		

Handy Multiplier for Wrought-Iron.

If the area in square inches of the cross section of any specimen of wrought-iron be multiplied by 3.34, the product will be the weight in pounds of a lineal foot of such specimen.

FLAT BAR IRON .- Weight in lbs. of a Lineal Foot.

Breadth		Thickness in Parts of an Inch.										
in Inches.	I-4th.	5-16ths.	3-8ths.	7-16ths.	1-half.	5-8ths.	3-4ths.	7-8ths.	1			
1	.835	1.044	1.253	1.461	1.670	2.088	2.506	2.923	3.340			
1#	.939	1-174	1.409	1.644	1.878	2.348	2.818	3.287	3.756			
11	1.044	1.305	1.566	1.826	2.088	2:609	3.132	3.653	4.176			
18	1.148	1.435	1:722	2.009	2.296	2.870	3:444	4.018	4.592			
14	1.252	1.566	1.879	2.192	2.504	3.131	3.758	4.384	5.008			
18	1.358	1.696	2.035	2.374	2.716	8.392	4.070	4.749	5.432			
14	1.462	1.827	2-192	2.557	2.924	3.658	4.384	5.114	5.848			
17	1.566	1.957	2.348	2.740	3.132	3.914	4.696	5.479	6.264			
2	1.671	2.088	2.505	2.922	3.842	4.175	5.010	5.845	6.684			
24	1.775	2.218	2.662	3.105	3.550	4.435	5.324	6.210	7.100			
21	1.880	2.348	2.818	3.288	3.760	4.696	5.636	6.575	7-520			
28	1.984	2.479	2-975	3.470	3.968	4.957	5.950	6.941	7.936			
21	2.088	2.609	3-131	3.653	4.176	5.218	6.262	7.306	8.352			
28	2.193	2.740	3.288	3.836	4.386	5.479	6.576	7.671	8.772			
23	2.297	2.870	3.444	4.018	4.594	5.740	6.888	8.036	9.188			
21	2.402	3.001	3.601	4.201	4.804	6.001	7.202	8.402	9.608			
3	2.506	3.131	3.758	4.384	5.012	6.262	7.516	8.767	10:024			
31	2.715	3.392	4.071	4.749	5.430	6.784	8-142	9.498	10.860			
31	2.923	3.653	4.384	5.114	5.846	7.306	8.768	10.228	11.692			
84	3.132	3.914	4.697	5.479	6.264	7.828	9.394	10.959	12.528			
4	8.341	4.175	5.010	5.845	6.682	8.350	10.020	11.690	13.364			
41	3.549	4.436	5.323	6.210	7:098	8.871	10.646	12.421	14.196			
41	3.758	4.697	5.636	6.575	7.516	9.393	11.272	13.151	15.032			
41	3.966	4.958	5.949	6.941	7.932	9.915	11.898	13.881	15.864			
5	4.175	5.219	6-263	7.306	8.350	10.437	12.526	14.612	16.700			
51	4.384	5.479	6.576	7.671	8.768	10.958	13.152	15.343	17:536			
54	4.593	5.741	6.889	8.037	9.186	11.480	13:778	16.073	18.372			
52	4.801	6.001	7.202	8.402	9.602	12.002	14.404	16.804	19.204			
6	5.010	6.262	7.515		10.020	12.524	15.030	17.585	20.042			

ROUND BAR IRON .- Weight in ths. of a Lineal Foot.

Diameter in Inches.	Weight in lbs.	Diameter in Inches.	Weight in lbs.	Diameter in Inches.	Weight in lbs.	Diameter in Inches.	Weight in lbs.
1	•040	18	6.870	31	25.400	49	55.640
1	.163	12	7.970	31	27 - 475	43	58.688
2	.363	12	9.150	38	29.625	41	61:820
À	-650	2	10.406	31	31.870	5	65.040
8	1.006	21	11.750	34	34.175	51	68:330
3	1.456	21	13.106	33	36.575	51	71 . 700
7	1.990	28	14.670	37	39.056	51	75 150
1	2.590	24	16.256	4	41.620	51	78.700
11	3.300	24	17.925	41	44.260	58	82:300
11	4.070	24	19'600	41	46.990	51	86.006
16	4.920	27	21.500	48	49.790	57	89.800
15	5.860	8	23.408	45	52.675	6	93 650

SQUARE BAR IRON.

Weight in lbs. of a Lineal Foot.

Side in Inches.	Weight in lbs.	Side in Inches.	Weight in lbs.	Side in Inches.	Weight in lbs.	Side in Inches.	Weight in 1bs.
4	.052	16	8.82	81	32.72	42	71.60
1	.208	13	10.23	31	35.28	43	75.36
2	469	17	11:74	38	38.16	47	79:54
· t	.832	2	13.36	31	40.92	5	83.44
8	1.304	24	15.08	35	44.01	51	87.90
4	1.876	21	16.91	34	46.96	51	92.40
1	2.557	28	18:84	37	50.38	52	96.67
1	3.340	24	20.86	4	53.44	54	101.04
11	4.227	28	23.10	41	56.97	58	105.87
11	5.216	23	25.25	41	60.32	54	110.80
12	6.314	27 3	27.70	48	64.08	57	115.48
14	7.504	3	30.02	41	67.64	6	120 . 08

SHEET IRON AND STEEL.

Weight of a Superficial Foot in Pounds and Fractions, with Corresponding
Number and Thickness of Birmingham Wire Gauge.

No. of Birmingham Wire Gauge.	Thickness in Parts of an Inch. Board of Trade	Squar	ht per e Foot lbs.	No. of Birmingham Wire Gauge.	Thickness in Parts of an Inch. Board of Trade	Weight per Square Foot in lbs.	
	Standard.	Iron.	Steel.	Wife Gauge.	Standard.	Iron.	Steel
1	.300	12.00	12.210	19	.041	1.64	1.678
2 3	·284	11.36	11.587	20	·035	1.40	1 · 42
8	.260	10.40	10.608	21	.032	1.28	1.30
4	·238	9.52	9.710	22	.028	1.12	1.14
5	.220	8.80	8.976	23	.025	1.00	1.02
6	•203	8.12	8 · 282	24	022	0.88	0.89
7	180	7.20	$1.7 \cdot 344$	25	.020	0.80	0.81
8 9	165	6.60	6.732	2 6	.018	0.72	0.78
9	148	5.92	6.038	27	.016	0.64	0.65
10	135	5.40	5.508	28	·01 4	0.56	0.57
11	·120	4.80	4.896	29	.013	0.52	0.28
12	.109	4.36	4 · 447	30	.012	0.48	0.49
13	.095	3.80	3.876	31	.010	0.40	0.40
14	.083	3.32	3.386	32	.009	0.36	0.86
15	.072	2.88	2.938	33	· 008	0.32	0.82
16	.065	2.60	2.652	34	·007	0.28	, 0 ⋅ 2€
17	.028	2.32	2.366	85	·005	0.30	0.24
18	.050	2.00	2.040	86	.004	0.16	0.16

17. Stores Ledger,

Into which the entries in the previous two books are posted to the credit of the several accounts (such as "Meters," "Lead Pipe," "Wrought-iron Fittings," &c.), and the items from the several invoices are posted to the debit of the several accounts. At the end of each half year the balance of each account represents the stock on hand. This latter is proved to be correct or otherwise by the result of the actual stocktaking.

18, Carbonizing Book-Daily and Weekly Statements,

Containing a record of the state of the station-meter taken twice in the 24 hours (in large works the state of the meter is recorded every hour); the quantity of coal and cannel used daily, the production of gas per ton, and the total daily production; the number of benches at work, stokers, &c. Each page serves for a week, and is then added up; an additional line is left at the foot of the page, on which is entered for comparison, the particulars of the total of the corresponding week of the previous year.

19. Public Lamp Register,

Gives particulars of the number of lamps lighted each night; the hours of lighting and extinguishing; the hours burning per lamp, the total hours burning; a column into which the number of hours, weekly, can be added, and another for remarks.

20. Test Register,

For noting the results of the different tests of the illuminating power and purity of the gas.

- 21. Shareholders' Register and Address Book.
- 22. Seal Register and Dividend List.
- 23. Register of Calls.
- 24. Register of Transfers.
- 25. Transfer Certificate Book,

Containing certificates of the registration of shares, to be torn out, leaving counterfoil behind.

26. Invoice Book,

With blank leaves, into which are gummed all invoices for goods received.

27. Minute Book.

A lettered index at the beginning of this book is handy.

A few other account-books of a less important character may be useful; but the above are indispensable in a well-regulated gas company.

Discount for Early Payment of Gas Bills.

The custom of allowing discount to consumers on gas bills paid either during the first month after the expiration of a quarter, or within a period of 21 or 30 days from the date of the delivery of the

account, is becoming very general amongst gas companies.

The most common allowance is at the rate of 10 per cent. on the amount due for gas consumed (excluding the meter-rent), but the premium varies throughout the country from 5 to 20 per cent.; some companies adopting a graduated scale of discounts according to the quarterly consumption.

The practice, wherever adopted, has been found highly beneficial. saving labour in collecting, and reducing the percentage of bad debts.

FORMS.

Renouncement of Proposed New Issue on the Transfer of Old Shares.

I, John Thompson, of Tipping Street, Newcastle, hereby renounce my right to any of the new Shares about to be issued by the Gas Company, in favour of William Jones, of Broad Street, Manchester.

(Signed) JOHN THOMPSON,

Jan. 1, 18-

To the Secretary - Gas Company. of the -

Renunciation of Shares newly Allotted.

I, John Wilson, of Birmingham, being the holder [or proprietor] of Shares in the -- Gas Company, do hereby renounce the same to and in favour of William Jackson, of Bristol. And I, the said William Jackson, hereby agree to accept and take the said Shares, subject to the conditions on which they are allotted. Dated this--, One thousand eight hundred and day of -

Signed by the said John Wilson in the presence of (Here Witness signs.) Signed by the said) William Jackson in the presence of (Here Witness signs.)

JOHN WILSON.

WILLIAM JACKSON.

Declaration for Loss of Sealed Share Certificates.

I, ----, of -----, do hereby solemnly and sincerely declare that I am possessed of and entitled to - in the - Company, _____, and that the said _____ are bona fide my property. and that they are not pledged or assigned to any person or persons whomsoever for money advanced thereon, or for any consideration whatever. And I further declare that I have made diligent search for the -, and can nowhere find the same. And I make this solemn declaration conscientiously believing the same to be true, and by virtue of the provisions of an Act made and passed in the 5th and 6th years of the reign of His late Majesty King William the Fourth, intituled "An Act to repeal an Act of the present Session of Parliament, intituled 'An Act for the more effectual abolition of Oaths and Affirmations taken and made in various departments of the State, and to substitute declarations in lieu thereof, and for the more entire suppression of voluntary and extra judicial Oaths and Affidavits, and to make other provisions for the abolition of unnecessary Oaths."

Declared at —, this — day of —, One thousand eight hundred and —, before me.

[The above Declaration is to be made before a Commissioner to administer Oaths in Chancery in England. Any person making a false Declaration is declared guilty of a misdemeanour.]

Indemnity for Loss of Share Certificates or Dividend Warrant.

Company.

Whereas -, in the Company called the -, numbered —, being the property of —, the undersigned, h— by accident been lost or destroyed, and the said Company have consented to give , on being indemnified for so doing. Now, in consideration of the said Company so granting to me, the said ----, a ----, we the undersigned - and - do hereby severally and respectively undertake and agree to save harmless and keep indemnified the Directors for the time being of the said Company of and from all losses, damages, and expenses which they, any or either of them, may sustain, incur, or be put unto, for or in consequence of their so granting such new ———; and also from and against all claim or claims to be at any time hereafter made upon the said Company for or in respect of the original - by any person or persons whomsoever.

Dated this - day of -, One thousand eight hundred and ---

Declaration of Transmission of Shares (from wife to husband) in
I, John Smith, of ———————————————————————————————————
Authority to Pay Dividends.
——— Company,
Payment of Dividends. I, the undersigned,, of, being a shareholder of and in the undertaking called the Company, do hereby request that all Dividends and Interest due to me on the Stock or Shares now registered, or that may hereafter be registered in my name may be paid to, of, until further notice, whose receipt shall be a sufficient discharge to the Company for the payment of the same. Signature
Date

^{*} Spinster or Widow, as the case may be.

Certificate Showing that Income-Tax has been Deducted.

This is to certify that on paying to John Brown the sum of £45, being the amount of one year's Dividend (or, one half year's Dividend, as the case may be) on Shares (or Stock) to December 31st, 18——, I deducted for Income-Tax the sum of 18s. 9d.

Pro the A——— B——Gas Company, WILLIAM JONES,

Secretary.

Dec. 20th.

Form of Proxy.

TERMS FOR LEASES, ETC.

Englan	Ireland.	Scotland.					
Lady Day .		March 25th	Candlemas				Feb. 2nd.
Midsummer		June 24th.	Whitsunday			6	May 15th.
Michaelmas		Sept. 29th.	Lammas.		4		August 1st.
Christmas .		Dec. 25th.	Martinmas				Nov. 11th.

When a Scottish term falls on Sunday, the Monday following is considered term day.

LAW TERMS.

		1 my cure	with Ticheren		
Hilary or Le			Jan. 11th.		n. 31st.
Easter .		11	April 15th.	 ,, Ma	ay 8th.
Trinity .			May 22nd.	,, Ju	me 12th.
Michaelmas		11	Nov. 2nd		ov. 25th.
		Sec	tland.		
Candlemas		Begins,	Jan. 15th .	 Ends, F	eb. 3rd.
Whitsunday		,,	May 12th .	,, Jı	ane 2nd.
Lammas .				,, J1	

Nov. 24th.

Martinmas

SIZES OF DRAWING PAPER.

	Ft	In.		Ft.	In.			Ft	In.		Ft.	In.
Antiquarian	4	4	×	2	7	Double Crown		3	6	×	1	8
						Imperial	1	2	6	×	1	10
Double Elephant	3	4	×	2	3	Super Royal		2	3	×	1	7
Atlas												
Columbia	2	10	×	1	11	Medium		1	10	×	1	5
Elephant	2	33	×	1	101	Demy		1	8	×	1	3

TABLE OF COLOURS

Used in Mechanical and Architectural Drawing.

Work.	Colour,
Brickwork in plan or section .	Carmine or crimson lake.
Brickwork in elevation	Venetian red or crimson lake mixed
	with burnt sienna.
Brickwork to be removed by al-	
terations	Burnt umber.
Concrete works	Sepia with darker markings.
Clay	Burnt umber.
Earth	Burnt umber.
Flintwork	Prussian blue.
Granite	Purple madder or pale Indian ink.
Stone generally	Yellow ochre or pale sepia.
Slate	Indigo and lake or Prussian blue.
English timber (oak excepted) .	Raw sienna.
Oak	Burnt sienna or Vandyke brown.
Fir and other light timber	Indian yellow or raw sienna.
Mahogany	Indian red.
Cast-iron	Payne's grey or neutral tint.
Wrought-iron	Prussian blue.
Steel, bright	Indigo with a little lake.
Brass	Gamboge or Roman ochre.
Gun metal	Dark cadmium.
Lead	Pale Indian ink, tinged with Indigo.
Meadow land	
Sky effects	Cobalt blue.
PRI 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	Annual Control of the

The presence of any slight greasiness, preventing the laying on of the colours evenly, may be counteracted in its effects by dissolving a little prepared ox-gall in the water with which the colours are mixed. The brush should always be used in mixing colours; the latter being rubbed in separate divisions of the slab.

EPITOME OF MENSURATION.

Of the Circle, Cylinder, and Sphere.

The areas of circles are to each other as the squares of their diameters.

The diameter of a circle being 1, its circumference equals 3-1416.

The diameter of a circle multiplied by 3.1416 equals its circumference.

The diameter of a circle is equal to 31831 of its circumference.

The square of the diameter of a circle being 1, its area equals .7854.

The diameter of a circle squared and multiplied by '7854 equals its

The internal circumference of a cylinder multiplied by its length or height equals its concave surface.

The area of the end of a cylinder multiplied by its length equals its

solid contents.

The area of the internal diameter of a cylinder multiplied by its

depth equals its cubical capacity.

The square of the diameter of a sphere multiplied by 3.1416 equals its convex surface.

The cube of the diameter of a sphere multiplied by 5236 equals its solid contents.

The capacity of a cylinder 1 foot in diameter and 1 foot in length equals 4.895 imperial gallons.

The capacity of a cylinder 1 inch in diameter and 1 foot in length equals 034 of an imperial gallon.

The capacity of a cylinder 1 inch in diameter and 1 inch in length

equals '002832 of an imperial gallon. Hence-

The capacity of any other cylinder in imperial gallons is obtained by multiplying the square of its diameter by its length, and by the number of imperial gallons contained in the unity of its measurement.

The capacity of a sphere 1 foot in diameter equals 3.263 imperial

The capacity of a sphere 1 inch in diameter equals .001888 of an

imperial gallon. Hence-

The capacity of any other sphere in imperial gallons is obtained by multiplying the cube of its diameter by the number of imperial gallons contained in the unity of its measurement.

Of the Square, Rectangle, and Cube.

The side of a square equals the square root of its area.

The area of a square equals the square of one of its sides.

The diagonal of a square equals the square root of twice the square of its side.

The side of a square is equal to the square root of half the square of its diagonal.

The side of a square equal to the diagonal of a given square contains

double the area of the given square.

The area of a rectangle equals its length multiplied by its breadth.

The length of a rectangle equals the area divided by the breadth;

The length of a rectangle equals the area divided by the breadth; or the breadth equals the area divided by the length.

The side or end of a rectangle equals the square root of the sum of the diagonal and opposite side to that required, multiplied by their difference.

The diagonal in a rectangle equals the square root of the sum of the squares of the base and perpendicular.

The solidity of a cube equals the area of one of its sides multiplied by the length or breadth of one of its sides.

The length or breadth of a side of a cube equals the cube root of its solidity.

The capacity of a 12-inch cube equals 6.232 imperial gallons.

Of Triangles and Polygons.

The sum of the squares of the two given sides of a right-angled triangle is equal to the square of the hypotenuse.

The difference between the squares of the hypotenuse and given side of a right-angled triangle is equal to the square of the required side.

The area of a triangle equals half the product of the base multiplied by the perpendicular height.

The side of any regular polygon multiplied by its apothegm, or perpendicular, and by the number of its sides, equals twice the area.

Of Ellipses, Cones, and Frustums.

The square root of half the sum of the squares of the two diameters of an ellipse, multiplied by 3.1416, equals its circumference.

The product of the two axes of an ellipse, multiplied by '7854, equals its area.

The solidity of a cone equals one-third of the product of its base

multiplied by its altitude, or height.

The squares of the diameters of the two ends of the frustum of a cone added to the product of the two diameters, and that sum multiplied by its height, and by 2618, equal its solidity.

Table of Common Fractional Parts and Equivalent Decimals.

Common Fractional Parts.	Decimals.	Common Fractional Parts.	Decimals.	Common Fractional Parts.	Decimals
1-100th	•01	9-14ths	6428	7-10ths	•7
1-90th	.0111	11-14ths	· 7857	9-10ths	ļ .ģ
1-80th	.0125	18-14ths	9285	1-9th	·im
1-70th	·0143	1-13th	•077	2-9ths	-2222
1-60th	.0166	2-13ths	1538	4.9ths	•4444
1-50th	.02	3-13ths	2307	5.9ths	.5555
1-40th	.025	4-13ths	•3076	7-9ths	•7777
1-30th	.0333	5-13ths	3846	8-9ths	-8888
1-20th	•05	6-13ths	.4615	1-8th	125
1-19th	·0526	7-13ths	-5384	3-8ths	.375
1-18th	.0555	8-13ths	•6153	5-8 ths	•625
1-17th	·0588	9-13ths	·6923	7-8ths	875
1-16th	.0625	10-13ths	7692	1-7th	148
8-16ths	· 1875	11-13ths	·8461	2-7ths	2857
5-16ths	3125	12-18ths	923	3-7ths	4285
7-16ths	·4375	1-12th	.0833	4-7ths	5714
9-16ths	•5625	5-12ths	•4166	5-7ths	.7142
11-16ths	9875	7-12ths	-5833	6-7ths	.8571
18 16ths	·8125	11-12ths	.9166	1-6th	1666
15.16ths	•9375	1-11th	•0909	5-6ths	.833
1-15th	.0666	2-11ths	·1818	1-5th	•2
2-15ths	•1333	3-11ths	•2727	2-5ths	•4
4-15ths	·2666	4-11ths	•3636	3-5ths	•6
7-15ths	•4666	5-11ths	4545	4-5ths	i •8
8-15ths	·5933	6-11ths	•5454	1-4th	-25
11-15ths	·7333	7-11ths	6363	3-4ths	.75
13-15ths	.8666	8-11ths	·7272	1-3rd	·333 3
14-15ths	•9333	9-11ths	•8181	2-3rds	·6666
1-14th	: '0714	10-11ths	.909	1-half	•5
3-14ths	.2142	1-10th	1 1	1	•1
4-14ths	2857	3-10ths	.8	i	-

ARITHMETICAL AND ALGEBRAICAL SIGNS.

= The sign + " × " ÷ "	of Equality, and signifies equal to, as 2 added to $3=5$. Addition , plus or more, as $4+6=10$. Subtraction , minus or less, as $6-4=2$. Multiplication , multiplied by, as $5\times 3=15$. Division , divided by, as $8\div 4=2$. or $\frac{8}{4}=2$ Proportion, : signifies is to, or to, : : signifies so is.
	Thus, 2:3::4:6 signifies that as 2 is to 3 so is 4 to 6. Evolution, or the Extraction of Roots.
√ The sig	gn of the Square Root (termed the Radical sign), as $\sqrt{16} = 4$, i.e., the square root of 16 is equal to 4. Cube Root, as $\sqrt[n]{64} = 4$, i.e., the cube root of 64 is equal to 4.
<i>*</i>	Bi-quadrate, or fourth Root, $\sqrt[4]{16} = 2$.
	Involution, or the raising of Powers.
40 ,, t	to be squared, as $4^2 = 16$. The small figure is termed the Index or Exponent. The small figure is termed the large of the squared of the small figure is termed the large of the squared of the small figure is termed the large of the small figure is termed the large of the small figure is termed the large of the small figure is termed the large of the small figure is termed the large of the small figure is termed the large of the small figure is termed the large of the small figure is termed the large of the small figure is termed the large of the small figure is termed the large of the small figure is termed the large of the small figure is termed the large of the small figure is termed the large of the small figure is termed the large of the small figure is termed the large of the small figure is termed the large of the small figure is termed the large of the small figure is termed the large of the small figure is the small figu

A vinculum placed over two or more figures, thus 3+5, signifies that they are to be taken as one quantity. Thus:

 $\frac{3+5}{\sqrt{5^2-3^2}} \times 4 = 32$, signifies that 3 plus 5 multiplied by 4 = 32, and $\frac{1}{\sqrt{5^2-3^2}} = 4$, signifies that 5 squared, minus 3 squared, and the square root of the remainder = 4, and

 $\sqrt[3]{20 \times 12}$ = 2, signifies that 20 multiplied by 12, divided by 80, and the cube root of the quotient = 2, and

 $\frac{24 \times 6 + \overline{12 \times 3} \times 4}{12} = 60, \text{ signifies that 24 multiplied by 6, and 12}$ multiplied by 3, added together, multiplied by 4 and divided by 12, the quotient = 60.

[] () Brackets; e.g. $12 - [3 + (4 \times 2)] = 1$, signify that the product of 4, multiplied by 2, added to 3, and the total subtracted from 12, leaves 1.

. . . is used to signify the word therefore.

... is used to signify the word because, or since.

? is used in the Chain Rule to signify how many.

Statute acres \times ·0015625 = square miles. Square links \times ·4356 = square feet. Square feet × 2.3 = square links. Square feet × 183.346 = circular inches. Circular inches × .00456 = square feet. Links $\times \cdot 22 = \text{yards}$. Links \times '66 = feet. Feet $\times 1.5 = links$. Cubic inches x .00058 = cubic feet. Cubic inches × .01638 = litres. Cubic feet × .037 = cubic yards. Cubic feet × 2200 = cylindrical inches. Cylindrical inches × .0004546 = cubic ya Cylindrical feet × .02909 = cubic yards. Cubic feet × 6.232 = imperial gallons. Imperial gallons × ·1604 = cubic feet. Cubic inches x .003607 = imperial gallon Imperial gallons × 277.3 = cubic inches. Imperial gallons $\times 4.541 =$ litres. Cubic feet \times '779 = bushels. Cubic inches \times '00045 = bushels. Bushels × .0476 = cubic yards. Bushels \times 1·284 = cubic feet. Bushels \times 2218·2 = cubic inches. Lineal feet \times ·00019 = statute miles. Lineal yards × .0006 statute miles. Statute miles × .869 = mean geographics

Mean geographical miles × 1·151 = statu Pounds avoirdupois × 7000 = grains. Pounds avoirdupois × ·82286 = pounds to

French tonnes $\times .984 =$ English tons. Pounds on square inch × 144 = pounds on square foot. Pounds on square foot x .007 = pounds on square inch. Miles per hour x 1.467 = feet per second. Feet per second x .682 = miles per hour. Metres × 3.281 = English feet. Litres × .2202 = imperial gallons. Hectolitres × 2.7512 = English bushels. Grammes × .002205 = pounds avoirdupois. Kilogrammes × 2.205 = pounds avoirdupois. Diameter of circle × 3.1416 = circumference. Circumference of circle × ·31831 = diameter. Diameter of circle × .8862 = side of equal square. Circumference of circle x .2821 = side of equal square. Diameter of circle × '7071 = side of inscribed square. Circumference of circle × 2251 = side of inscribed square. Area of circle × .6866 = side of inscribed square. Side of square × 1.128 = diameter of equal circle. Side of square × 3.545 = circumference of equal circle. Side of square × 1.414 = diameter of circumscribing circle. Side of square × 4.443 = circumference of circumscribing circle. Square of diameter × .7854 = area of circle. Square root of area × 1.12837 = diameter of equal circle. Square of diameter of sphere $\times 3.1416 = \text{convex surface}$. Cube of diameter of sphere × .5236 = solidity. Diameter of sphere x .806 = dimensions of equal cube. Diameter of sphere x .6667 = length of equal cylinder. One atmosphere = 14.7 pounds on square inch. = 2116 pounds on square foot. = 29.922 inches of mercury. = 33.9 feet of water.

Each 1000 cubic feet of coal gas in a holder × 37 = (approximate) weight of gas in pounds.

The atomic weight of an elementary gas × .0691 = its specific gravity.*

Half the atomic weight of a compound gas or vapour × .0691 = its specific gravity.

In round numbers, ½d. per square yard is £10 per statute acre (actually £10 1s. 8d.)

^{*} Exceptions to this rule occur in the case of the vapours of phosphorus and arsenic, whose atomic weights must be doubled, and in those of mercury, zinc, and cadmium, the atomic weights of which must be halved.

TABLE OF DIAMETERS, CIRCUMFERENCES, AND AREAS OF CIRCLES, AND SIDES OF EQUAL SQUARES.

Diam.	Circum- ference.	Area.	Side of Equal Square.	Diam.	Circum- ference.	Area.	Side of Equal Square.
1	.7854	.0490	2215	134	43.197	148 489	12.185
à	1.5708	•1963	•4431	14	43.982	153 - 938	12:406
2 2	2.3562	•4417	6646	141	44.767	159 485	12.628
1	3.1416	*7854	-8862	143	45.553	165 130	12.850
11	3.9270	1.2271	1.1077	142	46.338	170.873	13.071
11	4.7124	1.7671	1.3293	15	47.124	176:715	13.293
13	5.4978	2.4052	1.5508	151	47.909	182-654	13.514
2*	6.2832	3.1416	1.7724	151	48.694	188 692	13.736
21	7.0686	3.9760	1.9939	152	49.480	194.828	13.957
21	7.8540	4.9087	2.2155	16	50.265	201.062	14-174
23	8.6394	5.9395	2.4370	161	51.051	207 · 394	14.400
3	9.4248	7.0686	2.6586	164	51.836	213.825	14-622
31	10.210	8.2957	2.8801	162	52-621	220.353	14.843
34	10.995	9.6211	3.1017	17	53.407	226 - 980	15.065
32	11.781	11.044	3.3232	171	54.192	283 · 705	15.286
4	12.566	12.566	3.5448	174	54.978	240.528	15.508
41	13:351	14.186	3 7663	179	55.763	247 450	15.730
41	14.137	15.904	3.9880	18	56.548	254 · 469	15.951
43	14.922	17.720	4.2095	181	57:334	261.587	16-173
5	15.708	19.635	4.4310	184	58.119	268 803	16.394
51	16.493	21:647	4.6525	184	58.905	276.117	16.616
51	17.278	23.758	4.8741	19	59.690	283 - 529	16.837
54	18.064	25.967	5.0956	191	60.475	291-039	17.060
6	18.849	28:274	5.3172	194	61.261	298 648	17.280
61	19.635	30-679	5.5388	192	62.046	306:355	17:502
64	20.420	33 · 183	5.7603	20	62.832	314.160	17.724
61	21.205	35.784	5.9819	201	63.617	322.063	17.945
7	21.991	38.484	6.2034	201	64.402	330.064	18.167
71	22.776	41.282	6.4350	204	65.188	338 · 163	18.388
71	23.562	44.178	6.6465	21	65.973	346 · 361	18.610
72	24.347	47.173	6.8681	211	66.759	354.657	18.831
8	25.132	50.265	7.0897	211	67:544	363.051	19.053
81	25.918	53.456	7.3112	213	68.329	371.543	19.274
84	26.703	56.745	7.5328	22	69:115	380 · 133	19.496
84	27:489	60.132	7.7544	221	69.900	388 * 822	19.718
9	28.274	63.617	7.9760	221	70.686	397.608	19.939
91	29.059	67.200	8.1974	223	71.471	406.493	20.161
91	29.845	70.882	8.4190	23	72.256	415.476	20.382
92	30.630	74:662	8.6405	231	73.042	424.557	20.604
10	31.416	78.540	8.8620	231	73.827	433.731	20.825
101	32.201	82.516	9.0836	233	74.613	443.014	21.047
101	32.986	86.590	9.3051	24	75.398	452-390	21.268
104	33.772	90.762	9.5267	241	76.183	461 864	21.490
11	34.557	95.033	9.7482	241	76.969	471.436	21.712
111	35 . 343	99.402	9.9698	244	77.754	481.106	21.933
114	36.128	103.869	10.191	25	78.540	490.875	22.155
110	36.913	108 - 434	10.413	251	79.325	500.741	22:376
12	37.699	113.097	10.634	251	80.110	510.706	22:598
124	38.484	117.859	10.856	251	80.896	520.769	22.819
121	39.270	122.718	11.077	26	81.681	530.930	23.041
123	40.055	127.676	11.299	261	82.467	541 189	23.262
13	40.840	132.732	11:520	261	83 252	551.547	23.484
131	41.626	137.886	11.742	263	84.037	562·002 572·556	23 · 708 23 · 927
131	42.411	143 · 139	11.963	27	84.823	012 000	20 721

							20.00
Diam.	Circum-	Area.	Side of Equal	Diam.	Circum-	A	Side of
Distil.	ference.	Area.	Square,	Diam.	ference.	Area.	Equal Square.
271	85.608	583 - 208	24.149	412	131 · 161	1369.00	36.999
271	86.394	593 - 958	24.370	42	131 - 947	1385.44	37-220
274	87.179	604.807	24.592	421	132.732	1401.98	37.442
28	87.964	615 . 753	24.813	421	133.518	1418 62	37.663
281	88.750	626 - 798	25.035	424	134.303	1435 · 36	87.885
281	89.585	687 941	25.256	43	135.088	1452 20	38.106
284	90.321	649 182	25.478	431	135 874	1469 · 13	38.328
29	91-106	660.521	25.699	431	136.659	1486 17	88.549
291	91.891	671 . 958	25.921	434	137 445	1503.30	38.771
291	92.677	683 · 494	26.143	44	138 - 230	1520.53	38.993
293	93.462	695 128	26.364	441	139.015	1537.86	89.214
30	94 · 248	706.860	26.586	441	139.801	1555.28	39.436
301	95.033	718 690	26.807	443	140.586	1572.81	39.657
301	95.818	730.618	27.029	45	141.372	1590.43	39.879
303	96.604	742 644	27.250	451	142.157	1608.15	40.110
31	97.389	754.769	27.472	451	142.942	1625 - 97	40.322
311	98.175	766 992	27.693	451	143 728	1643.89	40.543
311	98.968	779 318	27.915	46	144.513	1661.90	40.765
312	99·745 100·531	791·732 804·249	28·136 28·358	461	145 · 299 146 · 084	1680·01 1698·23	40.986
32 32±	101.316	816 865	28.580	463	146 869	1716.54	41 429
324	102 102 *	829 - 578	28.801	47	147 655	1734.94	41.651
324	102 887	842 390	29.023	471	148 440	1753.45	41.873
83	103-672	855.300	29.244	473	149.226	1772.05	42.094
831	104 458	868 - 308	29 466	472	150.011	1790.76	42.316
331	105 243	881 415	29.687	48	150.796	1809.56	42.537
332	106.029	894.619	29 - 909	481	151.582	1828 · 46	42.759
34	106.814	907 - 922	30.131	484	152.367	1847 - 45	42.980
841	107.599	921 - 323	30.352	482	153.153	1866 55	43.202
841	108 - 385	934 · 822	30.574	49	153.938	1885 · 74	43.423
844	109:170	948 419	30.795	491	154.723	1905.03	43.645
35	104.956	962.115	31.017	491	155.509	1924 - 42	43.867
351	110.741	975 · 908	31.238	493	156.294	1943 91	44.088
351	111.526	989 - 800	31.460	50	157.080	1963.50	44.310
357	112.312	1003.79	31.681	501	157.865	1983 · 18	44.531
36	118.097	1017:87	31.903	501	158.650	2002.96	44.753
361	113.883	1032.06	32.124	503 51	159.436	2022.84	44.974
361	114·668 115·453	1046·39 1060·73	32·349 32·567	511	160·221 161·007	2062.90	45·196 45·417
362 37	116 239	1075.21	32.789	511	161 . 792	2083 · 07	45.639
371	117.024	1089.79	33.011	513	162.577	2103.35	45.861
371	117.810	1104.46	33.232	52	163 - 363	2123.72	46.082
374	118.595	1119-24	33.454	521	164 · 148	2144 · 19	46.304
38	119.380	1134-11	88.675	521	164.934	2164-75	46:525
381	120.166	1149.08	33.897	523	165 . 719	2185 42	46.747
381	120.951	1164.15	34.118	53	166.504	2206 · 18	46.968
881	121.737	1179.32	34.340	581	167.290	2227 05	47.190
39	122.522	1194.59	34.561	581	168.075	2248.01	47.411
391	123 · 307	1209 · 95	34.783	531	168.861	2269.06	47.633
391	124.093	1225 · 42	35.002	54	169 646	2290 · 22	47.854
394	124.878	1240.98	35 226	541	170.431	2311 48	48.076
40	125.664	1256.64	35.448	541	171.217	2332.83	48 298
401	126.449	1272.39	35.669	543	172.002	2354.28	48.519
4(1	127 - 234	1288 25	35.891	55	172.788	2375.83	48:741
403	128 020	1304.20	36.112	551	173 - 573	2397·48 2419·22	48·962 49·184
41	128·805 129·591	1320·25 1336·40	36.334	551	174·858 175·144	2419 22	49 405
411		1352.65	36.777	553	175 144	2463.01	49:627
413	130.376	1002.00	90.111	, 50	110 020	2400 01	20 021

Diam.	Circum- ference.	Area.	Side of Equal	Diam.	Circum- ference.	Area.	Side of Equal
201		0405.05	Square,	71		9050.00	Square
561	176.715	2485.05	49.848	71	223.053	3959.20	62.920
561	177.500	2507 19	50.070	711	223.839	3987-13	63 141
563	178 285	2529 - 42	50.291	711	224.624	4015.16	63 - 363
57	179.071	2551.76	50.213	712	225 · 409	4043.28	63 545
571	179.856	2574.19	50.785	72	226 • 195	4071.51	63 · 806
573	180.642	2596.72	50.956	721	226.980	4099.83	64.028
573	181 427	2619.35	51.178	721	227 . 766	4128-25	64-249
58	182.212	2642.08	51.399	723	228.551	4156.77	64-471
581	182.998	2664 91	51.621	73	229 - 336	4185.39	64 692
581	183 . 783	2687 · 83	51.842	78±	230 - 122	4214.11	64-914
584	184.569	2710.85	52.064	781	230 · 907	4242.92	65-135
59	185.354	2733 97	52.285	783	231 - 693	4271.83	65 857
591	186 139	2757 19	52.507	74	232 478	4300.85	65 578
		2780.51	52.729				
591	186 925			741	233 263	4329 • 95	65.800
591	187.710	2803 - 92	52.950	741	234 · 049	4359.16	66:022
60	188 496	2827 44	53.172	742	234 834	4388 47	66.243
601	189 281	2851.05	53.393	75	235-620	4417.87	66 465
603	190.066	2874 . 76	53.615	751	236 405	4447.37	66.686
602	190.852	2898 • 56	53.836	751	237 · 190	4476.97	66.908
61	191.637	2922.47	54.048	75%	237 - 976	4506 67	67-129
611	192.423	2946 · 47	54.279	76	238 · 761	4536 47	67:351
614	193 - 208	2970.57	54.501	761	239 547	4566.36	67:572
614	193.993	2994.77	54.723	761	240.332	4596.35	67:794
62	194 779	8019-07	54.944	763	241 117	4626 44	68.016
621	195.564	3043 • 47	55.166	77	241.903	4656-63	68 237
621	196+350	3067.96	55.387	771	242.688	4686 92	68.459
622	197.135	3092.56	55.609	771	243 474	4717.30	68 - 680
58	197.920	3117.25	55.830	771	244 259	4747.79	68 902
631	198 - 706	3142.04	56.052	78	245.044	4778:37	69.123
581	199.491	3166 - 92	56.278	781	245 830	4809.05	69.345
582	200-277	3191.91	56.495	784	246 615	4839.83	69.566
54	201.062	3216 · 99	56.716	783	247 401	4870.70	69.788
341	201 · 847	3242 17	56.938	79	248 186	4901.68	70.009
641	202.633	3267 · 46	57.159	791	248 971	4932.75	70.231
643	203 - 418	3292 · 83	57.381	794	249 757	4963 - 92	70.453
35	204 204	3318.31	57.603	793	250.542	4995 · 19	70.674
651	204 204	3343.88	57.824	80	251 328		
			58.046			5026.56	70.896
35±	205.774	3369.56		801	252.113	5058.01	71.119
551	206.560	8395 • 83	58.267	803	252-898	5089.58	71.339
66	207.345	3421.20	58.489	803	253.684	5121.24	71.562
66±	208.131	3447.16	58.710	81	254.469	5153.00	71.782
161	208.916	3473 23	58.932	811	255 255	5184.86	72.005
562	209 · 701	8499.39	59.154	813	256.040	5216.82	72.225
57	210.487	3525.66	59.375	812	256.825	5248.87	72.449
37±	211 272	3552.01	59.597	82	257:611	5281.02	72.668
371	212.058	3578 - 47	59.818	821	258 396	5313 27	72-892
372	212.843	3605.03	60.040	821	259 182	5345 62	78-111
88	213.628	3631.68	60.261	823	259 967	5370.07	73 - 335
381	214 · 414	3658 · 44	60.483	83	260.752	5410.62	78 554
	215 199	3685 • 29	60.704	831	261 538	5443.26	
881							78 778
82	215.985	8712.24	60.926	831	262.323	5476.00	78 997
19	216.770	3739 · 28	61.147	834	263 109	5508.84	74-221
391	217.555	3766 • 43	61.369	84	263.894	5541 78	74 440
394	218.341	8793 - 67	61.591	811	264.679	5574.81	74.664
192	219 · 126	3821.02	61.812	841	265 465	5607 95	74.884
70	219.912	3848 46	62.934	843	266-250	5641-18	75-107
701	220 - 697	3875 99	62.255	85	267:036	5674.51	75.327
04	221 · 482	3903.63	62 477	851	267.821	5707-94	75.550
703	222.268	3931.86	62.698	851	268 606	5741-47	75.770

Diam.	Circum- ference.	Area.	Side of Equal	Diam.	Circum- ference.	Area.	Side o Equal
851	269 392	5775 . 09	Square. 75 · 994	994	311.803	7736 - 62	87 · 958
86	270 177	5808.81	76.213	994	312.599	7775 65	88 - 179
861	270.963	5842 63	76.437	992	818.374	7814 - 79	88 40
861	271 - 748	5876 - 55	76.656	100	314.160	7854.00	88-629
862	272 533	5910.57	76.880	1001	314.945	7893 · 31	88.84
87	273 - 319	5944 · 69	77.099	100%	315.730	7932.73	89.06
87£	274-104	5978-90	77.323	1002	316.516	7972.21	89 - 287
874	274 890	6013 - 21	77:542	101	317.301	8011.86	89.508
879	275 675	6047-62	77.766	1011	318 - 087	8051 - 57	89.730
88	276 460	6082-13	77 985	101%	318 - 872	8091.38	89 - 959
881	277-246	6116.74	78.209	1012	319.657	8131 · 29	90-178
881	278 031	6151.44	78 428	102	320.443	8171.30	90.398
884	278.817	6186 - 25	78 652	1024	321 - 228	8211.40	90.616
89	279 - 602	6221 15	78.871	1024	322.014	8251.60	90+838
89±	280 - 387	6256 15	79.095	1024	322 - 799	8291.86	91.059
894	281.178	6291 25	79.315	108	823.584	8332.30	91.28
897	281 . 958	6326.44	79.538	1031	324.370	8372.80	91.509
90	282.744	6361.74	79.758	1034	325 155	8413.40	91.724
901	283 - 529	6397 - 13	79.982	1034	325.941	8454.09	91.946
903	284.314	6432-62	80.201	104	326 - 726	8494.88	92.167
909	285 100	6468 21	80.425	1041	327.511	8535 . 77	92:389
91	285.885	6503.89	80.644	1045	328 - 297	8576.76	92.610
914	286 671	6539 68	80.868	1043	329 . 082	8617.85	92.832
914	287 - 456	6573.56	81.087	105	329 868	8659.03	93.058
914	288 241	6611.54	81.311	1051	330.653	8700.31	93.275
92	289 - 027	6647 62	81.530	1051	331 · 438	8741.69	93 - 496
924	289 812	6683 - 80	81.754	105%	332 - 224	8783 17	93.718
921	290.598	6720.07	81-973	106	333.009	8824 . 75	98 940
929	291 - 383	6756 - 45	82.197	1061	333 · 794	8866 42	94 - 161
08	292 168	6792 92	82.416	1064	334 - 580	8908 20	94 · 388
031	292 - 954	6829 · 49	82.640	1062	335 - 365	8950.07	94.604
184	293 - 739	6866 · 16	82.859	107	336 · 151	8992.04	94.826
189	294 - 535	6902-92	83.083	1071	336 · 936	9034.11	95.047
14	295 - 310	6939 . 79	83 - 302	1074	337 - 722	9076 27	95 - 269
141	296.095	6976:75	83.526	1073	338 - 506	9118:54	95 · 491
143	296.881	7013.81	83.746	108	339 · 292	9160.90	95.712
44	297 666	7050 - 97	83.970	1081	340.077	9203.36	95 - 934
15	298 · 452	7088 23	84.189	1084	340.863	9245 • 92	96 155
51	299 - 237	7125 58	84.413	1082	341 . 648	9288 - 58	96.377
154	300.022	7163 04	84.632	109	342 - 434	9331 · 33	96.598
59	300 · 808	7200 - 59	84.856	1091	343 219	9374.18	96.820
06	801.593	7238 - 24	85.077	1094	344.005	9417.14	97.041
61	302-379	7275 - 99	85 . 299	1099	344.789	9460.19	97 - 263
64	303 164	7313 · 84	85.520	110	345.576	9503.34	97 - 485
62	303 949	7351 - 78	85 . 742	120	376 992	11309.76	106.348
7	304 - 735	7889 . 82	85.964	130	408 408	13278 26	115.234
71	305 - 520	7427-96	86.185	140	439 - 248	15393 84	124.079
76	306 - 306	7466 20	86 - 407	150	471 - 240	17671.50	132.935
74	307 . 091	7504 - 54	86 628	160	502 - 656	20106 24	141 . 798
8	307-876	7542-98	86.850	170	534 . 072	22698 · 06	150.659
81	308 - 662	7581.51	87.071	180	565 488	25446 96	159 521
81	309 447	7620.14	87 - 293	190	596 - 904	28352 94	168:383
87	310.233	7658-87	87.514	200	628 - 320	81416.00	177 - 247
9	311.018	7697.70	87.736	300	942-480	70686 • 00	265 869

WEIGHTS AND MEASURES.

Troy Weight.

Pennyweights. Grains. gr.

Ounces,
$$1 = 24$$
 dwt.

Pound. $1 = 20 = 480$ oz.

 $1 = 12 = 240 = 5760$ lb.

A carat = 4 grains.

 437.5 grs. troy = 1 oz. avoirdupois.

 7000 ,, = 1 lb. ,,

 100 ozs. troy = $109\frac{\pi}{2}$ ozs. avoirdupois.

 3.2 grs. troy = 4 diamond grs.

 1 oz. ,, = 150 ,,

The pound troy is the weight of 22.815 cubic inches of distilled water, at the temperature of 62° Fahr., the height of the barometer being 30 inches.

Troy weight is used in philosophical experiments, and in weighing gold, silver, and jewels. The fineness of gold and silver coins means the proportion of the precious metal which they contain. This is expressed in 1000ths of their total weight, or in carats—24ths of their total weight. British gold coins are 22 carats fine, or $0.916\frac{2}{3}$; silver coins, 0.925. Gold, if pure, is said to be 24 carats fine; if there be one of alloy, with 23 carats of pure gold, it is 23 carats fine, and so on downwards. The alloy in gold and silver coins consists of copper. The true weight of a sovereign is 123.274 grains consisting of—pure gold, 11 parts, or 113.001 grains; copper, 1 part, or 10.273 grains. Silver coin consists of—pure silver, 222 parts; copper, 18 parts. The weight of a shilling is $87\frac{1}{4}$ grains. 24 pence are made from an avoirdupois pound of copper.

Septem and Decigation.

The word septem (seven) is descriptive of the weight of the 1000th part of a decigallon of distilled water at 62° Fahr., and under a barometric pressure of 30 inches.

A decigallon of water is the tenth part of a gallon, and as a gallon of water at the above temperature and pressure weighs 70,000 grains (10 lb. avoirdupois), it follows that the tenth part, or a decigallon must weigh 7000 grains (1 lb.)

Each decigallon is divided into 1000 septems; and therefore the septem of pure water weighs 7 grains.

Apothecaries Weight.

			Drams,		Scruple	es.	Grains.	gr.
		or Drachms.			1 =		20	ser.
	Ounces.		1	=	3	=	60	dr.
Pound.	1	=	8	=	24	=	480	oz.
1 =	: 12	=	96	=	288	=	5760	lb.

The sign of the scruple is 9; the dram, 3; the ounce, 3

This weight, which is now abolished, was formerly used for compounding medicines. The grain, ounce, and pound are equal to those of troy weight. Drugs are bought and sold by avoirdupois weight.

Avoirdupois Weight.

								Ounces		Drams.	dr.
						Poun	ds.	1	=	16	oz.
			1	Stones	S.	1	=	16	=	256	lb.
	Qu	arter	s.	1	=	14	=	224	=	3584	st.
Cwts.		1	=	2	=	28	=	448	=	7168	qr.
Ton. 1	=	4	=	8	=	112	=	1792	=	28672	cwt.
1 = 20	=	80	=	160	=	2240	=	35840	=	573440	ton.
		1 11		ainda.	nin	- 7000	1	ing two			

1 lb. avoirdupois = 7000 grains troy. 1 oz. avoirdupois = 487.5 grains troy. 100 ozs. avoirdupois = 91 7 ths ozs. troy.

The imperial pound avoirdupois is the standard unit by means of which all commodities, except gold, silver, and precious stones, are weighed, and is equal to the weight of one-tenth of an imperial gallon, or of 27.7274 cubic inches of distilled water at the temperature of 62° Fahr., and when the barometer stands at 30 inches. A certain piece of platinum of this standard weight is kept in the Exchequer Office at Westminster.

Lineal or Long Measure.

	P	Rods, erches Poles	700	Yard 1	s. =	Feet	= =	Inches. 12 36
Furlongs.	Chains.	1	= 0	$\frac{5\frac{1}{2}}{22}$	=	16½ 66	=	198 792
Mile. 1 =	10 =	40	=	220	=	660	=	7920
1 = 8 = 1 link	80 = 7.92 i	320 nches.	-	1760	=	5280	=	63360

100 links = 1 chain, or 66 feet, or 22 yards.

1 league = 3 geographical or nautical miles.

1 hand = 4 inches.

1 fathom = 6 feet.

1 military pace = 21 feet.

1 geometrical pace = 5 feet.

1 geographical or nautical mile = 1.15 statute miles.

1 geographical degree = 60 geographical or nautical miles.

1 Admiralty knot = 6080 feet.

The yard is the imperial standard measure of length, and is the distance, at the temperature of 62° Fahr., between two marks on a certain bar kept in the Exchequer Office, Westminster.

Cloth Measure.

						Nails.		Inches.
			Q	uarter	S.	1	=	21
		Yards.		1	=	4	-	9
Ell.		1	=	4	=	16	=	36
1	=	114	=	5	=	20	=	45

The yard is the same as in long measure, but differs in its divisions and subdivisions.

Yarn Measure-Cotton.

				Skeins.		Yards.
		Hanks.		1	=	120
Spindle.		1	=	7	=	840
1	=	18	=	126	-	15120

Yarn Measure-Linen.

			Cuts.		Yards.
		Hears.	1	= .	300
	Hasps.	1 =	2	=	600
Spindle.	1 =	6 =	12	=	3600
1 =	4 =	24 =	48	=	14400

Square Measure.

	0-	Dalan a		Za Vand		Sq. Fe		Sq. Inches.
	1	Poles or rehes.	r	Sq. Yard		0	=	144 1296
Chatata Ca D.	111777	renes.		301	II II	2721		89204
Statute Sq. Re	oous.	40		1210		10890	=	1568160
1 = 4	=	160				43560	=	6272640
1 - 4		-		= 640 s				0272040

In round numbers, ½d. per square yard is £10 per statute acre (actually, £10 1s. 8d.).

	4,840	square	yards make	1 statute acre.
	6150.4	٠,,	,,	Scotch acre.
	7,840	,,	,,	Irish acre.
	4,000	•••	,,	Devonshire acre.
Customary	4,000	•	,,	Somersetshire acre.
Measure.	5,760	••	••	Cornwall acre.
	7,840	••	••	Inneashire acre.
•	10,240	••	,,	Cheshire acre.
	10.240		• • • • • • • • • • • • • • • • • • • •	Staffordshire acre.

To Reduce Statute Measure to Customary.

Multiply the number of perches statute measure, by the square feet in a square perch statute measure; divide the product by the square feet in a square perch customary measure, and the quotient will be the answer in square perches customary.

To Reduce Customary Measure to Statute.

Multiply the number of perches customary measure, by the square feet in a square perch customary measure; divide the product by the square feet in a square perch statute measure, and the quotient will be the answer in square perches statute.

Square Measure-Land.

The chain with which land is measured is 22 yards long.

Solid or Cubic Measure.

Cubic Yard. Cubic Feet. Cubic Inches. 1 = 1728
$$1 = 27 = 46656$$

Liquid Measure.

				Pints.		Gills.
		Quarts.		1	=	4
Gallon.		1	=	2	==	8
1	=	4	=	8	=	32

The standard measure of capacity, both for liquids and dry goods, is the imperial gallon, being equal to a volume of distilled water of 277-274 cubic inches, weighing 10 lbs. avoirdupois, at the temperature of 62° Fahr., and 80 inches atmospheric pressure.

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Liquid Measures used by Apothecaries.
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1 fluid minim = 0.0045 cubic inches. (η)
60 ,, minims = 1 dram. (ξ)
8 drams = 1 oz. (ξ)
16 ozs. = 1 pint. (⊙)
```

					Wine	M	easu:	res.			Quart	8.	Pints.
									Gallon	s.	1	=	2
						Т	'ierce	8.	1	=	4	=	8
					Hhds.		1	=	42	=	168	=	336
		Pt	ınch.		1	=	11	=	68	=	257	=	504
	Pipes.		1	=	11	=	2	=	84	=	336	=	672
Tun.	1	=	11	=	2	=	8	=	126	=	504	=	1008
1 =	: 2	=	8	=	4	=	6	=	252	=	1008	=	2016

Ale and Beer Measure.

Quarts. Pints.

Gallons. 1 = 2 Firkins. 1 = 8 Kildkns. 1 = 9 = **36** = 72 2 = Barrels. 1 = 18 =72 = 144Hhds. = 2 =4 = 86 = 144 = 2881 Punch. $1\frac{1}{4} = 3 =$ 6 =54 = 216 = 43211 Butt. 2 = 4 = 8 = 72 = 288 = 57611 8 = 6 = 12 = 108 = 432 = 864

Dry Measure.

									Gallons	•	Pints.
							Pecks.		1	=	8
				В	ushe	ls.	1	=	2	=	16
		Qı	ıarte	rs.	1	=	4	==	8	=	64
Loads o	or	Weys.	1	=	8	=	32	=	64	=	512
Last.	1	=	5	=	40	=	160	=	820	=	60
1 =	2	=	10	=	80	==	320	=	640	=	120
		3 bus	hels	= 1	sack	: = 1	B∙85 cubi	c fe	et.		
12 sacks = 1 chaldron = 46.2 cubic feet.											

The imperial bushel contains 80 lbs. avoirdupois of distilled water, and its content is 2218·192 cubic inches, or 1·283 cubic feet.

Table of Time.

				1	Iinutes.		Seconds.
			Hours		1	=	60
	Days.		1	=	60	=	3600
Week.	ĺ	=	24	=	1440	=	86400
1 =	- 7	=	168	=	10080	=	604800

28 days = 1 lunar month.
28, 29, 80, or 81 days = 1 calendar month.
1 common year = 365 days, or 52 weeks 1 day.
1 leap year = 366 days, or 52 weeks 2 days.
1 Julian year = 365 days 6 hours.
1 solar year = 365 days 5 hours 48 minutes 49 seconds.
30 degrees = 1 sign.
12 signs = 1 circle of the zodiac.

CIRCULAR AND ANGULAR SPACE.

60'' (seconds)		i	60°		l sextant.
60' ` 30°	1º (degree).		90°	=	{1 quadrant. 1 right angle.
45°	1 sign. 1 octant.		860°	=	A circle.

The earth moves through 860° in 24 hours, therefore $15^\circ=1$ hour, and $1^\circ=4$ minutes

TIME IN WHICH ANY SUM DOUBLES ITSELF, AT RATES OF INTEREST BOTH SIMPLE AND COMPOUND.

Rate of		ich the sum is led, at	Rate of		Years in which the sum i doubled, at			
Interest per cent.	Simple Interest.	Compound Interest.	Interest per cent.	Simple Interest.	Compound Interest.			
1	100	69 · 6603	5	20	14 · 2067			
2	50	35 0028	<u>6</u>	163	11 8957			
24	40	28.0701	7	149	10.2448			
8	331	23 · 4498	8	121	9.00646			
83	28#	20.1488	9	111	8.04323			
4	25	17 · 67303	10	10	7 · 27254			
44	223	15.7478	11	91	6 · 64 189			
-	1		12	8	6.11626			

FRENCH WEIGHTS AND MEASURES—DECIMAL SYSTEM. Weights.

Milligramme =		·001 gramme	<u>-</u> =	English. 0.01548	grains.
Centigramme =	$=\frac{1}{100}$ or		:	0.1548	,,
Décigramme =	$=\frac{1}{10}$ or	·1 .,		1.5432	,,
•	• •		1	15.432349	,,
			1	0.648	dwt.
GRAMME	= 1		!	0.03215	oz. troy.
GRAMME		••	•	0.03527	oz. avoir.
			- 1	0.0022	lb.
			,	0.0000197	cwt.
			- (154.32	grains.
Décagramme =	= 10	gramme	S -==	0.3527	oz. avoir.
Ü		J	(0.022	lb. "
			i	1,549.28	grains.
Hectogramme	= 100	,,	·	3.527	ozs. avr.
Ŭ			(0.22046	lb. "
			_i 1	15,432.349	grains.
			- (32·15	ozs. troy.
			1	35· 278 9	,, avoir.
Kilogramme	= 1,000	••	- !	$2 \cdot 2046$	lbs.
Ū			Ì	2.679	"troy.
			- 1	0.01968	cwt.
			1	0.00098	ton.
			1	22.046	lbs. avr.
Myriagramme	= 10,000	••	'	0.1968	cwt.
• 0	•		(0.00984	ton.
Quintal =	100,000	grammes =	220	0.46 lbs. or 1	ewt. 8 ars.
•	·	Ü		24 1 lbs.	•
Millier or bar =	= 1,000,000	=	2,204	1.62 lbs. or 19	ewt. 2 ars.
	, , , , , ,	,,		20 3 lbs.	1
The Gramm	e is the uni	t of measures		eight, and is t	he weight
of a cubic cer	atimètre of	distilled wa	ter a	t its maximu	m density
(89° Fahr.) in					
29:922 inches					Ozzac W I

29.922 inches.

		En	glisl	h.				F	rench.
Grain			•				=	0.064799	grammes.
Dwt							=	1.555	•••
Dram							=	1.771846	••
Ounce,	troy	, .					=	31.1085	••
Ounce,			ıpoi	S			==	28.3496	,,
Pound			-				1	158.59	,,
rouna		,,	,		•	•	== ,	0.454	kilogramme.

• • • • • • • • • • • • • • • • • • • •		=	
Pound, troy	= { 87	8·226 0·373226	grammes. kilogrammes.
Cwt	= 5	0.8	J
Own.	$= \begin{cases} 5\\1,01 \end{cases}$	6·05	**
Ton	_] 1,01	1·01605	tonnes
	1	1 tonne \times .984.	omilos.
	•	- tollac × 001.	
Liva	il or Long	Magazes	
French.	u or rong	English	_
r renon.		0.0398	
$Millimètre = \frac{1}{1000} \text{ or } \cdot 001$	mètre =		•
1000 01 002		0.0010	
		0.8987	
Centimètre = $\frac{1}{100}$ or $\cdot 01$:	0.0328	
100 22		0.010	
		3.9371	
Décimètre = $\frac{1}{10}$ or ·1	,, . <u>-</u>	0.3281	
10 32	**	0.1098	
		89.8707	
1/		3.2808	
Metre = 1	.,		33056 yards.
		0.0006	
		393.7079	
Diame News 10		99.900	feet.
Décamètre = 10	mètres.	10.986	yards.
		0.0062	mile.
		i 3,987·079	inches.
Hectomètre – 100		828.09	feet.
Hectomètre – 100	•• •	109.36	yards.
		0.0621	4 mile.
		(39,870.79	inches.
Kilomètre - 1,000		3,280.9	feet.
Anometre - 1,000	•,	1,098.68	y a rds.
		0.6218	
		(898, 7 07·9	inches.
Myriamètre == 10,000	_	82,809.0	feet.
Mynametre 10,000	,, .	10,986.8	yards.
		6.2188	
Ligne or line		= 0.0888	
		= 1.0658	
Pied or foot = 12 pouces		= 12.789 9	96 ,.
Toise $= 6$ French feet .		= 76.74	**
The Mètre is the unit of	lineal mea	sure, and is the	e 10 millionth

part of 90° of the meridian.

	English.	French. 25:39954 millimètres.										
		2.54 centimètres.										
Inch	= -	0.254 décimètre.										
		0·0254 mètre.										
Foot	_ '	0.0040										
Yard	=	0.9144										
Fathom .	=											
	=	1·8287 mètres.										
Pole	=	5·0291 ,,										
Chain		20.116 ,,										
Furlong .	= {	201.16										
		0.20116 kilomètre.										
Mile	= {	1,609·815 mètres.										
		1·609815 kilomètres.										
Square Measure.												
	French.	English.										
	(lor :001 are)	155.00 sq. ins.										
Milliare	$= \left\{ \begin{array}{c} \frac{1}{1000} \text{ or } \cdot 001 \text{ are } \\ \text{or sq. décamètre.} \end{array} \right\} = \left\{ \begin{array}{c} \frac{1}{1000} &$	1.0764 ,, feet.										
	(or sq. decametre.)	0·1196 ,, yard.										
	4	(1,550·0 ,, ins.										
Centiare 1		10·764 ,, feet.										
or sq.	$= \left\{ \frac{1}{100} \text{ or } \cdot 01 \text{ sq.} \right\} = \left\{ \frac{1}{100} \text{ or } \cdot 01 \text{ sq.} \right\} = \left\{ \frac{1}{100} \text{ or } \cdot 01 \text{ sq.} \right\}$	1·196033292 ,. yard.										
mètre.	décamètre	0.03954 ,, perch.										
metre.	-	0.00099 ,, rood.										
		0.00025 ,, acre.										
	ı	(15,501·0 ,, ins.										
		107·64 ,, feet.										
Distant	$= \left\{ \begin{array}{c} \frac{1}{10} \text{ or } \cdot 1 \text{ sq. déca-} \\ \text{mètre} \end{array} \right\} = \frac{1}{10} \left\{ \begin{array}{c} \frac{1}{10} \text{ or } \cdot 1 \text{ sq. déca-} \\ \frac{1}{10} \text{ or } \cdot 1 \text{ sq. déca-} \end{array} \right\} = \frac{1}{10} \left\{ \begin{array}{c} \frac{1}{10} \text{ or } \cdot 1 \text{ sq. déca-} \\ \frac{1}{10} \text{ or } \cdot 1 \text{ sq. déca-} \end{array} \right\} = \frac{1}{10} \left\{ \begin{array}{c} \frac{1}{10} \text{ or } \cdot 1 \text{ sq. déca-} \\ \frac{1}{10} \text{ or } \cdot 1 \text{ sq. déca-} \end{array} \right\} = \frac{1}{10} \left\{ \begin{array}{c} \frac{1}{10} \text{ or } \cdot 1 \text{ sq. déca-} \\ \frac{1}{10} \text{ or } \cdot 1 \text{ sq. déca-} \end{array} \right\} = \frac{1}{10} \left\{ \begin{array}{c} \frac{1}{10} \text{ or } \cdot 1 \text{ sq. déca-} \\ \frac{1}{10} \text{ or } \cdot 1 \text{ sq. déca-} \end{array} \right\} = \frac{1}{10} \left\{ \begin{array}{c} \frac{1}{10} \text{ or } \cdot 1 \text{ sq. déca-} \\ \frac{1}{10} \text{ or } \cdot 1 \text{ sq. déca-} \end{array} \right\} = \frac{1}{10} \left\{ \begin{array}{c} \frac{1}{10} \text{ or } \cdot 1 \text{ sq. déca-} \\ \frac{1}{10} \text{ or } \cdot 1 \text{ sq. déca-} \end{array} \right\} = \frac{1}{10} \left\{ \begin{array}{c} \frac{1}{10} \text{ or } \cdot 1 \text{ sq. déca-} \\ \frac{1}{10} \text{ or } \cdot 1 \text{ sq. déca-} \end{array} \right\} = \frac{1}{10} \left\{ \begin{array}{c} \frac{1}{10} \text{ or } \cdot 1 \text{ sq. déca-} \\ \frac{1}{10} \text{ or } \cdot 1 \text{ sq. déca-} \end{array} \right\}$	11.96038 ,, yards.										
Déciare	= metre } = -	0·8954 ,, perch.										
	•	0.0099 ,, rood.										
		0.0025 ,, acre										
		1,076·4 ,, feet.										
À		119·6099 ,, yards.										
ARE or sq.	= 1 sq. décamètre. =	8.954 ,, prchs.										
décamètre.	- I by. accumose.	0.099 rood.										
		0.0247 ,, acre.										
		(1,196.088 , yards.										
	(10 area or so)	1 00 74										
Décare	$=\begin{cases} 10 & \text{ares or sq.} \\ \text{décamètres} \end{cases} =$	1 000 E										
	(doomettes)	0.0471										
		, 44 000 0										
	(100 amon on en)	11,960·8 ,, yards. 395·4 ,, prchs.										
Hectare	$=\left\{\begin{array}{cccccccccccccccccccccccccccccccccccc$	395·4 ,, prehs.										
	= { décamètres } =	9'09 ,, roous,										
		2·4712 ,, acres.										

The are, which is a square décamètre, is the unit of square measure.

			Eng	lish			French.				
Square inc	h					•		$=\frac{1}{1}$	645·187 0·000645	sq.	millimètres. mètre.
Square foo		•						= '	0.0929	,,	,,
Square yas			:	:	•		:	=	0·8861 25·29 2	"	mètres.
Square roo		•	•	•		•	•	=	1,011.7	,,	,,
Square acr Square mil		•		•	•	•	:	=	4,046·7 2·59	,,	kilomètres.

Solid Measure.

```
French.
                                                                            English.
                         \left\{ \begin{array}{c} \frac{1}{1000} \, \text{or } \cdot 001 \, \text{stere} \\ \text{or cubic metre} \, . \end{array} \right\} =
                                                                     61.028
                                                                                      cubic inches.
Millistère
                                                                      0.085817
                                                                                        ,, foot.
                     = \left\{ \begin{array}{ccc} \frac{1}{100} & \text{or } \cdot 01 & \text{stère} \\ \text{or cubic mètre} \end{array} \right\}
                                                                   610.28
                                                                                              inches.
Centistère
                                                                      0.85817
                                                                                              foot.
                                                                 6,102.8
                                                                                              inches.
                  Décistère
                                                                       8.5317
                                                                                              feet.
                                                                       0.1808
                                                                                              yard.
                                                               61.028.0
STERE OF
                                                                                              inches.
                     = \left\{ \begin{array}{ccc} 1 & \text{st\`ere} & \text{or} & \text{cubic} \\ \text{m\`etre} & . & . & . \end{array} \right\}
   cubic
                                                                     85.817
                                                                                              feet.
                                                                       1.808
                                                                                              vards.
                                                                                              feet.
                                                                    858.17
Décastère = 10 stères or cubic mètres =
                                                                        18.0802
                                                                                              yards.
                                                                 8,531.7
                                                                                              feet.
Hectostère =
                         100
                                                                   130.802
                                                                                              yards.
                                                               85,317.0
                                                                                              feet.
Kilostère = 1,000
                                                                1,308.02
                                                                                              yards.
                                                               18,080.224
Myriastère = 10,000
   The Stère, which is a cubic mètre, is the unit of solid measure.
```

English.	French.
Cubic inch . $=$	0.000016886 stère or cubic mètre. 16,896.0 cubic millimètres.
Cubic foot =	0·028315 stère or cubic mètre.
1,000 cubic feet. =	
Cubic yard =	0·7645181 stère or cubic mètre.

	Dry and Fluid Measur	e. (Capacity.))
	French.	Englis	ь.
Millilitre	$= \left\{ \frac{1000}{1000} \text{ or } 001 \text{ litre } \right\} = \left\{ $	0.0610	cubic inch.
Millimore	or cubic décimètre	0.00022	imperial bushel.
Centilitre	$= \left\{ \begin{array}{c} \frac{1}{100} \text{ or } \cdot 01 \text{ litre or } \right\} = \left\{ \begin{array}{c} 0 \\ 0 \\ 0 \end{array} \right\}$	0.61028	cubic inch.
CCHMING	(cubic décimètre . , - i	0.0022	imperial bushel.
Décilitre	$= \left\{ \begin{array}{ccc} \frac{1}{10} & \text{or } \cdot 1 & \text{litre or } \\ \text{cubic décimètre} & \cdot \end{array} \right\} = \left\{ \begin{array}{ccc} \frac{1}{10} & \text{or } \cdot 1 & \text{litre or } \\ \frac{1}{10} & \text{or } \cdot 1 & \text{litre or } \end{array} \right\}$	6.1028	cubic inches.
200111110	(cubic décimètre .)	0.022	imperial bushel.
_	1	61.028	cubic inches.
LITRE Or	(1 litre or cubic)	0.0858	,, foot.
cubic dé-	- (1 litre or cubic)	1.76172	imperial pints.
cimètre)	(40011110110		,, gallon.
	'	0.0275	" bushel.
	(610.28	cubic inches.
Décalitre	10 litres or cubic =	0.858	,, foot.
	(décimètres	2.2	imperial gallons.
	,	0.276	,, bushel.
	1001:	6,102.8	cubic inches.
Hectolitre	= 100 litres or cubic = 1	8.58171	,, feet.
	(décimètres)	22.0	imperial gallons.
	(2.751	,, bushels.
77'1 1'4	= (1,000 litres or) = (cubic décimètres.	85.8171	cubic feet.
Kilolitre	cubic décimètres.	220.02	imperial gallons.
			" bushels.
35 . 114	(10,000 litres or)	858.171	,, cubic feet.
Mynalitre	= (10,000 litres or) = {	2,202.15	imperial gallons.
mi T **	lih ihi . /	2/5.121	,, bushels.
The Litr capacity.	e, which is a cubic décimèt	re, is the uni	t of measures of
- •			

			Eng	lish.	•				French.	
Cubic inch .								=	0.016386	litre.
Cubic foot .	,							===		litres.
1,000 cubic fe										,,,
Imperial pint										litre.
Imperial gallo	n	•	٠	•	•	•	•		4.541	litres.
Imperial bush	ıel	•	•	•	•	•	•	777	36.328	**

MONEY TABLES.

France.

Name.								English Value.
Centime								ુધા or ∙095d.
Franc	=	100	ce	ntim	29		17	9 1 d.
Sou	=	5		,,				18 or ·175d.
Napoléon	=	20	fir	ancs			:=	15s. 10d.

Accounts are kept in francs and centimes. For convenience in reckoning, a sou may be taken as equal to ½d., a franc as 10d., and 25 francs as 20s.

Belgium.

The Belgian currency is in centimes and francs, having the same English money value as those of France.

To convert centimes per cubic mètre into pence per 1,000 cubic feet, and vice versa.

Centimes per cubic metre $\times 2.7 = \text{pence per } 1,000 \text{ cubic feet.}$ Pence per 1,000 cubic feet $\times .37 = \text{centimes per cubic metre.}$

To convert centimes per litre into pence per 1,000 cubic feet, and vice versa.

Centimes per litre \times 2700 = pence per 1,000 cubic feet. Pence per 1,000 cubic feet \times 00037 = centimes per litre.

UNITED STATES OF AMERICA.

		Name							English Value.
Cent.								===	ૈ કુતે.
Dollar	=	100	cei	nts				_=	4s. 2d.
44, or									£1
Dollars	3 ×	•20	84					-=-	£1

To convert dollars and cents per 1,000 cubic feet into pence per 1,000 cubic feet, and vice versa.

Dollars and cents per 1.000 cubic feet \times 50 = pence per 1,000 cubic feet.

Pence per 1,000 cubic feet × .02 = dollars and cents per 1,000 cubic feet.

TABLE.

Foreign and Colonial Equivalents of English Money. (Actual or Approximate).

COUNTRY.	Pound Sterling.	SHILLING.	PENNY.
Argentine Republic .	10 Patacon or Dollars	50 Centimos	4 Centimos.
Austria	101 Florins	Florin, or 50 Kreutzers	4 Kreutzers.
Belgium Bolivia	25 Francs	1½ Francs	10 Centimes. 3 Centenas.
Brazil	10 Milreis	Milreis or 500	40 Reis.
Canada	4 Dollars	25 Cents	2 Cents.
Chili	5 Pesos 5 Dollars, or 31)	25 Centavos 25 Cents, or 17	2 0
China	Taels, or 35	Mace	Candareen.
Columbia	5 Pesos	25 Centavos	2 Centavos.
Ecuador	5 Pesos	25 Centavos	8½ Ore. 2 Centavos.
Egypt	100 Piastres	5 Piastres	Paras.
Finland	25 Marks	1 Marks	10 Penni. 10 Centimes.
German Empire	20 Marks	1 Mark or 100)	81 Pfennig.
Greece	25 Drachmæ	Pfennig	10 Lepts.
Holland	12 Florins	60 Cents	5 Ceuts.
Hungary	101 Florins	Florin, or 50 Kreutzers	4 Kreutzers,
India	10 Rupees and 4	9 Annas	8 Pies.
Italy	25 Lira	11 Lira	10 Centesimi.
Japan	5 Yen	25 Sen	2 Sen.
Java	12 Florins	60 Cents	5 Cents. 12 Grani.
Malta	5 Pesos or 5 Dols.	7 Tari, 4 Grani . 25 Centavos	2 Centavos.
Mexico	20 Krona	1 Krona	8ª Ore.
Norway	64 Dollars	36 Centena	3 Centena.
Persia.	21 Toman	12 Shahis	1 Shahi.
Peru	5 Sol	24 Dineros	2 Centos.
Portugal	5 Milreis	24 Testoes	20 Reis.
Russia	61 Silver Roubles	48 Copecks	4 Copecks
Spain	26 Pesetas	11 Pesetas	10 Centimos.
Sweden	20 Krona	1 Krons	8½ Ore.
Switzerland	25 Francs	11 Francs	10 Centimes.
Tunis	40 Piastres	2 Piastres	The same of the sa
Turkey	120 Pisstres	6 Piastres	Paras.
United States	4ª Dollars	25 Cents	2 Cents.
Uruguay	5 Peses	25 Centavos	2 Centavos.
Venezuela	5 Pesos	25 Centavos	2 Centavos.

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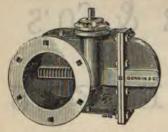
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Fig. 26.

Internal Worm and Rack Gas-Valve.



Rack and Pinion

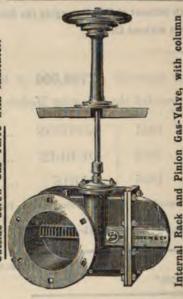
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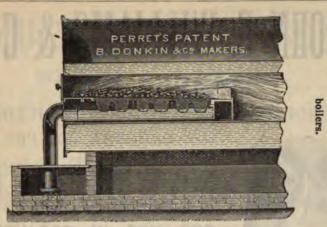
Fig. 6. Outside Rack and Pinion Gas-Valve.

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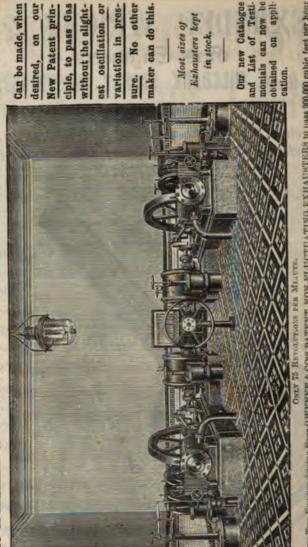
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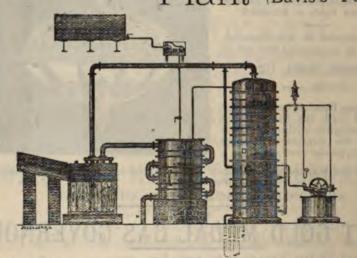


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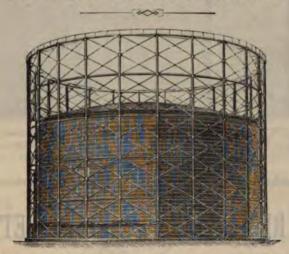
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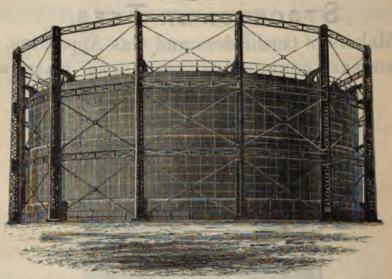
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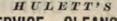
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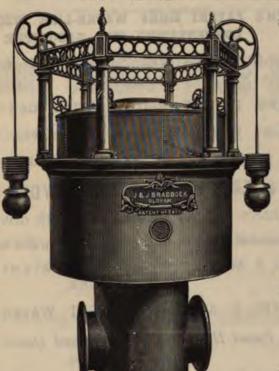
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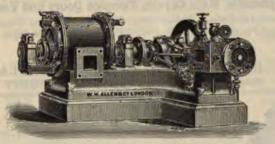
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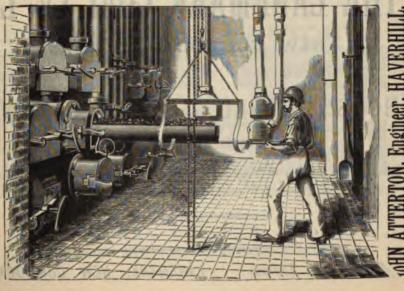
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